

MODELLING THE MICROCLIMATE IN A CONICAL BOTTOMED CIRCULAR GRAIN SILO

by

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DECLARATION

I hereby declare that this thesis is the result of my own research and has not been submitted for a degree to any other university.

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ABSTRACT

A three-dimensional mathematical model for predicting the behaviour of microclimate in the stored grain silo is presented. This analysis is implemented by calculating the air pressure field within an aerated conical bottomed circular silo, to continuing prediction the velocity field. The obtaining results are used to compute the simultaneous heat and mass transfer processes that occur in non-aerated and aerated grain silos. The conservation equations of momentum, mass and energy are employed in this study. The numerical scheme is based on applying a mapping technique with an algebraic grid generation method, to discretise the governing equations in the arbitrary geometries that describe the grain stores.

The finite different solution of the governing equations are obtained by using Alternating Direction Implicit method, Thomas algorithm and explicit method. The numerical experiments have been performed to investigate the effects of the non-uniform grid size, time step, duct shape and placement. Results in graphical form are presented for the pressure, velocity, temperature, moisture content, absolute humidity, wet bulb temperature, dry matter loss, seed viability and pesticide decay.

Significantly, a novel configuration of an annular aeration duct and a traditional linear aeration duct in farm silos have been investigated. It was found that the annular aeration system provides uniform airflow results in better protection of the stored grains

than in the linear aeration system, in that the beneficial grain quality indices remain high, and the rate of growth of insect population is retarded.

An outcome of the research has been improved the designs of commercially available grain silos.

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NOMENCLATURE

a_1, a_2, a_3, a_4	- isosteric specific empirical constants ($1/m$)
aeration	- ventilation
b_1, b_2, b_3, b_4	- respiration specific empirical constants
b_5, b_6, b_7, b_8	- respiration specific empirical constants
B	- pesticide specific empirical constants ($1/s$)
$c_{1v},$	- empirical constants in latent heat equation (J/kg)
c_{2v}	- empirical constants in latent heat equation ($J/kg K$)
c_{c1}, c_{c2}	- species specific constants
c_a	- specific of dry air (J/kgK)
$(c_1)_\sigma$	- specific heat of liquid water (J/kgK)
$(c_2)_\sigma$	- specific heat of grain kernel (J/kgK)
$(c_1)_\gamma$	- specific heat of vapour water ($J/kg \text{ water } K$)
C_i	- initial concentration of the pesticide (kg/m^3)
C_{pes}	- pesticide concentration (kg / m^3)
dtg	- time step during aeration cycle (s)
D_{eff}	- effective diffusivity (m^2 / s)
Fo	- Fourier number
gn	- ratio of molecular weights of water and air
G_{sc}	- solar constant (W/m^2)
h_w	- differential heat of wetting (J / kg)
h_s	- heat of sorption (J / kg)

h_{vap}	- latent heat of evaporation of free water (J / kg)
$\frac{\partial h_{vap}}{\partial T}$	- differential of heat of vaporisation respect to the temperature (J/kgK)
H	- absolute humidity of the air (kg/kg)
H^*	- function of the saturation humidity of air
H_{duct}	- humidity of air entering aeration duct (kg/kg)
H_{life}	- half life of seeds (s)
H_w	- integral heat of wetting (J / kg)
H_{wall}	- height of the vertical wall of the silo (m)
\bar{H}_d	- average of daily diffuse radiation (J/m^2)
\bar{H}_b	- total average of daily beam radiation (J/m^2)
\bar{H}_t	- average of daily total radiation (J/m^2)
$ifreq$	- number of heat and mass transfer iterations
I_b	- total intensity of beam radiation (W/m^2)
I_t	- total intensity of radiation (W/m^2)
I_d	- total intensity of diffuse radiation (W/m^2)
Δl	- space distance (m)
k	- intrinsic permeability (m^2)
K_{eff}	- effective thermal dispersivity tensor ($J / kg / K$)
m	- mass of the substrate lost (kg)
$\frac{dm}{dt}$	- rate of dry matter loss (kg/s)
M_w	- grain moisture content wet basis ($\%$)
n	- day of the year
n_s	- average of sunshine hours per day
$n\xi, n\eta, n\phi$	- maximum nodes points in the three components directions
N	- length of the day ($hours$)
P	- pressure gradient (Pa / m)

ΔP	- pressure difference (Pa / m)
P_{atm}	- atmospheric pressure (Pa)
P_{sat}	- saturation vapour pressure (Pa)
P_{vap}	- vapour pressure (Pa)
$P\text{-centre}$	- pressure at centre of silo (Pa)
$P_{con-min}$	- pressure at centre of silo with minimum value of iteration step (Pa)
$P_{si\ max}$	- the largest value of ψ_{\max} ,
Q_r	- cumulative consumption of oxygen, (kg)
rh	- relative humidity of air in equilibrium with the grain
r, ϕ, z	- cylindrical coordinates
r_s	- intrinsic rate of insect population growth ($1/s$)
$r_{duct\ min}, r_{duct\ max}$	- length bounds of the duct (m)
R	- radius of the grain silo (m)
R_b	- ratio of the total intensity of beam radiation
R_i	- ratio of the total intensity of radiation
R_d	- ratio of the total intensity of the diffuse radiation
R_p	- coefficient resistance to the airflow ($Pa\ s/m$)
R^P	- previous population of insect pests
S	- second Ergun (1952) coefficients ($Pa\ s^2/m^3$)
ΔS	- element of length (m)
Δt	- iteration time step (s)
t^*	- pesticide specific empirical constants (s)
t_{ime}	- total elapsed time of storage (s)
$time^*$	- total elapsed time of heat and mass transfer iteration (s)
T	- temperature ($^{\circ}C$)
T_a	- ambient air temperature ($^{\circ}C$)
T_g	- ground temperature ($^{\circ}C$)

T_s	- surface temperature of the silo (K)
T_{sky}	- sky temperature (K)
T_{wetb}	- wet bulb temperature of the intergranular air ($^{\circ}C$)
V	- velocity (m/s)
V_{wind}	- wind velocity across the surface of the silo (m/s)
V_{iab}	- fractional viability of seeds
V_r, V_{ϕ}, V_z	- three components of velocity in the cylindrical coordinates (m/s)
$V_{\xi}, V_{\theta}, V_{\eta}$	- three components of velocity in the dimensionless coordinates ($1/s$)
$V_{T\xi}, V_{T\eta}, V_{T\theta}$	- effective velocities with respect to the temperature (m/s)
$V_{W\xi}, V_{W\theta}, V_{W\eta}$	- effective velocities with respect to the moisture content (m/s)
W	- moisture content of the grains
Z_{total}	- total height of the silo (m)

GREEK SYMBOLS

α_p	- false transient factor
β	- sloping angle (<i>radians</i>)
Γ	- second partial derivatives of the scalar
γ_1	- angle of silo floor to the horizontal plane (<i>radians</i>)
γ_2	- angle between upper surface of silo to horizontal plane (<i>radians</i>)
δ	- weighting factor of Crank-Nicholson method
δ_d	- angle of the declination (<i>radians</i>)
ε	- seed bulk porosity
ε_r	- initial void fraction of the bulk of grain

$\xi_{duct\ min}, \xi_{duct\ max}$	- length bounds of the duct in transformed coordinates
ξ, ϕ, η	- non-dimensional transformed coordinates
θ	- angle of beam radiation (<i>radians</i>)
θ_z	- zenith angle (<i>radians</i>)
Θ	- arbitrary variable
μ	- dynamic viscosity (<i>Pa</i>)
$\nu_1, \nu_2, \nu_3, \nu_4$	- seed specific constants
ρ_a	- density rate of the dry air (<i>kg/m³</i>)
ρ_b	- bulk density (<i>kg/m³</i>)
ρ	- the density of air (<i>kg/m³</i>)
σ	- Stefan-Boltzman constant (<i>W/m²T⁴</i>)
ω_a	- solar hour angle (<i>radians</i>)
ω_s	- sunset hour angle (<i>radians</i>)
ϕ_l	- latitude of the geographical location (<i>radians</i>)
$\phi_{duct\ min}, \phi_{duct\ max}$	- width bounds of the duct (<i>radians</i>)

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CHAPTER 1

INTRODUCTION

1.1 BACKGROUND

Humans have been storing grains and their products for a long time. At about 8000 BC, when humans began to cultivate plants and raise domesticated animals, they were concerned to build up reserve food supplies to alleviate hunger that might arise in the future. Over the last 10,000 years, the existence of hunger and malnutrition have become unacceptable morally and socially. Humans have recognised that the unavailability of a sufficient quantity and quality of food has been one of the major constraints in the socioeconomic progress throughout the world.

Grains contribute more than any other staple foods with regard to calorie, carbohydrate, protein, lipid, mineral and vitamin requirements of the world population (Godon, 1994). The particular regional ecologies and climates provide the world population with its basic food: rice in Asia, wheat in North American, Europe, the Middle East, and North Africa, maize in Latin American. According to F. A. O. analysis, that 90% of the world's food supplies come from the land, among which grains have occupied an incredible 68% of the total world harvested crops. The other 22% is accounted for fruits and vegetables. The remaining 10% of man's food comes from the world's oceans, seas and lakes (Bushuk and Rasper, 1994). This can be shown in a pie chart in figure 1.1.

Moreover, the grain supply in national and international trade is of great concern and influence in world markets.

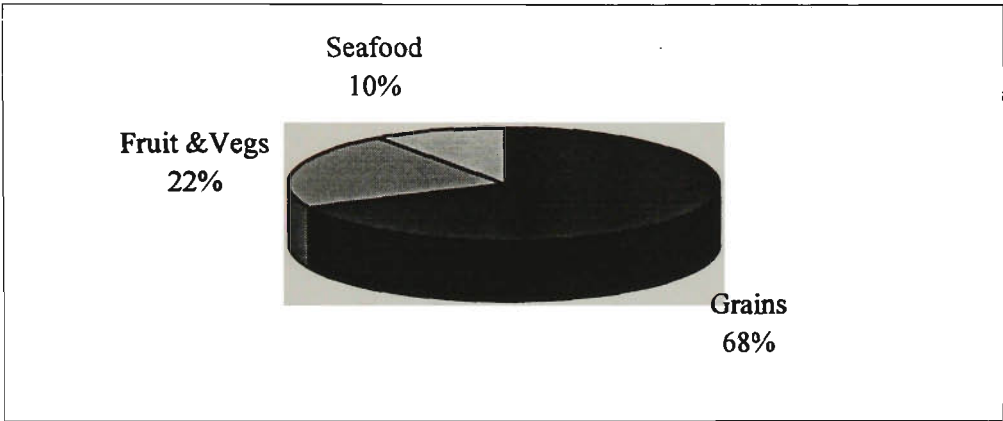


Figure 1.1 Food structure of world population

From 1982 to 1987, the world grain production exceeded 1500 million metric tonnes annually (table 1.1), about 360 kg per world inhabitant , that is therefore an important source of food in the world.

Table 1.1 The world production of grains

Million tonnes		
Grain type	1982	1987
Wheat	453.2	515.4
Rye	24.3	34.8
Barley	160.4	182.0
Oats	46.0	48.0
Maize	438.0	451.6
Rice	410.9	457.5
Total	1630.8	1788.6

Source: Chelkowski (1991)

It is estimated that 10~30% of total world grain production is lost after harvest (Chelkowski, 1991), and it will vary from country to country and from year to year.

The reasons for this huge amount of losses are highly complex and governed by various natural factors: Harvesting, drying, transportation, storage, processing and marketing. Especially, the major cause of this losses in the quantity and quality of grains is during storage.

During storage, grains are liable to suffer changes in texture, colour, flavour, and nutritive value (Holdsworth, 1983). That is to say, stored grains form an ecological system in which deterioration arises from interactions among physical, chemical and biological variables. These can be described as: Moisture movement, temperature increasing, oxygen consumption, insects, mites, moulds and rodents causing damage.

Moisture is one of the basic physico-chemical variables. The moisture content of stored grain is defined as the amount of water that can be removed without alterations to its chemical structure. The variation of moisture content is dependent on the type of grain, the variety of grain, chemical composition, moisture at harvest, relative humidity of the atmosphere, and seasonal fluctuations (Salunkhe *et al.*, 1985).

Moreover, the maximum moisture content for safe storage of grains are normally based on the equilibrium moisture content at 25° C and 75% relative humidity. These have summarized in table 1.2.

Temperature is a physical variable in grain storage, its value is strongly affected by the storage environment conditions, thus: the initial grain temperature, the intergranular air temperature, solar radiation which affects the surface temperature of the storage wall, metabolic heating due to the formation of hot spots and weather conditions.

The oxygen of atmospheric air is the most important single chemical variable influencing the growth and development of all harmful organisms in storage, because insects, mites, mould and rodents all require free oxygen for their development.

Table 1.2 Advised maximum moisture content for safe storage of grain
at 25°C and 75% RH.

Grain type	Moisture (%)
Wheat	
durum	14.1 (25-28 Celsius)
red	14.7 "
white	15.0 "
Rye	14.9 "
Barley	14.3 "
Oats	13.4 "
Maize	14.3
Rice	14.0

Source: Kent and Evers (1994)

Besides, grain pests such as insects, mites, rodents and mould are the commonest biological variables which are associated with stored grains. Insects harbour microbes in grain stores, and they can act as vectors of organisms causing human and animal diseases. Moulds can serve as food for insects (Sinha, 1971). The degree of grain pests activity in grain store is dependent on grain moisture and temperature, grain history and grain genotype, source of pests, available food, cleaning, drying, chemical residues in the grain mass, pesticide resistance of the grain pests (Brooker *et al.*, 1992).

Mould damage to stored grain includes: Decrease in viability and discolouration of seeds, production of toxins, biochemical changes and loss in dry matter (Brooker *et al.*, 1992). Similarly, the insect pests damage stored grain also includes: Consumption of whole grains or germ, generation of heat which results in quantitative, qualitative and viability loss (Salunkhe *et al.*, 1985).

In addition, viability and respiration are the two important biological properties responsible for the death of seed and the spoilage of grain in storage. Seed as an index

of grain soundness. The loss of seed viability is associated with respiration, which is a function of grain moisture content, temperature and light (Pomeranz, 1987). Respiration may contribute to a loss of dry matter, raise the level of carbon dioxide in the intergranular air, and also increase the temperature of the grain. The process of respiration is regulated by moisture and temperature, size and shape of grain, harvesting and postharvest ripening (Sinha and Mair, 1973).

A major proportion of the stored grain is damaged by insects, mites and rodents, thus infestation, growth and survival of insect pests in the stored grains are highly interrelated and need a careful appraisal to plan the strategy for their effective control.

A number of control methods have been developed, such as: Hygiene, pesticides, fumigants, controlled atmosphere, high temperature heating, ambient and refrigerated aeration. Amongst them, aeration control is one of the most powerful physical methods. Ambient aeration is the process of moving air at ambient temperature through stored grain, it lead to an improvement of the grain temperature and storage conditions, and can be accomplished in any regions of the world. Refrigerated aeration relies on mechanically cooling the air behaviour to continue the process of aeration.

Grain must be protected during all stages of handling, from the time of harvest through storage, transportation, and processing up to the time it is ready to be consumed. As the population increases and resources become more limited, the continuing challenge to feed the world's population is becoming more increasingly urgent. If that 10~30% of losses of grains are eliminated through improved postharvest biotechnology, the world's food supply can be increased by 10~30% without any additional cultivating, labouring and energy consuming.

In order to protect resources, to reduce hunger, ensure humanity's health and to have sufficient food supply, the study of preservation of stored grain for improvement the

technology in the postharvest handling and processing is the important responsibility for scientists and engineers.

1.2 CONTRIBUTIONS

The main contributions of this thesis are addressed as follows:

- A numerical method of finite different mathematical model has been presented for an aerated conical bottomed circular silo .
- A mesh transformation technique that may be used to model grain stores of arbitrary shape has been applied.
- Energy of solar radiation which has a significant effect on the surface temperature of the silo has been accounted.
- The SILO3DFTN computer program for accommodating the specific characteristics of the silo has been modified.
- The numerical experimental results of simulating the different mesh sizes and time steps have been obtained for evaluating the accuracy of the solution .
- The two types of aeration duct layouts fitted with conical bottomed circular silos have been investigated, for determining the best controlling results of aeration system to improve the design and the manufacture of the farm silos.
- A prototype grain silo fitted with an annular duct has been designed and built.

1.3 ORGANIZATION

The contents of the remaining chapters are reviewed below:

Chapter 2 describes the background information necessary to understand the significant postharvest knowledge on controlling the quality and preservation of grain. These are considered in the two major parts of review: The relationship between air velocity to the pressure gradient for the physics of air flow through the silo are mentioned. The crucial importance of grain temperature and moisture content on grain quality are highlighted.

Chapter 3 provides the numerical method of finite difference for analysing the conservation of momentum, mass and energy in an arbitrary geometry, and formulation the governing differential equations and the appropriate boundary conditions, by introducing the first step of mapping technique - the coordinate transformation scheme, which transforms the non-orthogonal mesh in the physical domain into a orthogonal mesh in the computational domain.

Chapter 4 provides the solution of finite difference method by means of creating the second step of mapping technique - non-uniform grid mesh scheme, to discretise the governing differential equations and boundary conditions in the computational domain by using a central difference approximation for the space derivatives, and a forward difference approximation for the time derivative. The results are obtained by employing the Samarskii-Andreyev (1963) alternating direction implicit method, the Thomas algorithm and an explicit method for heat and mass conservation equations.

Chapter 5 covers the physical and biological properties of grain bulk ecosystems, which affect on the stored grain, such as: thermal capacity, conduction, absorption, diffusion, germination, respiration and insect infestation. The major environmental variables affecting the microclimate in the grain bulk, namely radiation and ambient conditions.

These properties are associated with heat and mass transfer processes and physiological changes in the grain silo.

Chapter 6 presents the experiments of numerical investigation by using the computer program SILO3DFTN to simulate the performance of a conical bottomed circular silo, in which the effects on the time step and mesh size different have been investigated. Fourier number (Fo) is applied to examine the prospects of convergence and accuracy of the pressure and temperature distribution solutions. In addition, two types of aeration system layouts are also simulated.

Chapter 7 discusses the heat and mass transfer processes occurring in the three dimensional ecological systems by simulating with three different causes, namely the silo with non-aerated system, the silos fitted with linear aeration and annular aeration systems. The predictions are carried out to estimate the variation of pressure, velocity, temperature, moisture content, absolute humidity, wet bulb temperature, dry matter loss, seed viability and pesticide distributions in the grain silo.

Chapter 8 summarizes the contributions presented in this thesis, and gives some further suggestion for continuing this research.

CHAPTER 2

REVIEW OF RELATED WORK

This chapter reviews literature related to grain storage technology, which was used to develop novel silo design and insights into the ecology of grain storage.

2.1 AERATION

Aeration is a commonly used storage technique for cooling and drying grain reducing thermal gradients, avoiding the incidence of moisture migration, decreasing insect and mould activity, lowering the rate of pesticide decay and preserving the grain quality (Thorpe, 1986).

Aeration cooling is achieved by blowing cold night air through the stored grain by means of a fan, perforated air distribution and ducting on the silo floor (Elder, 1978). When grain is cooled by aeration, moisture content may be very slightly reduced. When grain is warmed by aeration through the movement of air at ambient temperature, moisture is added. Aeration systems can also be used for distributing fumigants, temporarily holding wet grains and clearing dust during grain movement operations.

The practice of aerating stored grain was established during the 1950s and is now an accepted quality maintenance measure (Foster, 1967). Aeration development was

coincident with the build up of reserve stocks of grain following World War II, the larger flat storages were used to hold the reserve grains, aeration was for the first time applied for the control of grain quality. The experience with aeration in storage was favourable. Today, aeration has become a powerful tool for protecting the grain during storage.

There are two somewhat different types of aeration systems: Ambient aeration and refrigerated aeration. In temperate and subtropical climates, grain can be effectively cooled by means of ambient aeration. In tropical climates, the high relative humidity and temperature of ambient air make aeration less feasible, the cooling of grain must by refrigerated aeration.

Aeration systems consist of a fan, a supply duct leading from the fan to the perforated duct placed in the grain bulk. Some provision must be made for airflow into or out of the air space over the grain surface.

The operation of aeration systems depends on a number of factors: the rate of airflow, the moisture content of the product, the shape and size of the grain kernels, the density of the grain bulk, the type, number and location of the duct (Yang and Williams, 1990).

2.2 AIRFLOW RATE

Agricultural products are commonly stored in aerated stores for both short and long term storage. In order to maintain the temperature throughout the grain to prevent moisture migration, aeration generally uses an above floor duct system which creates non-uniformity and non-linearity in the airflow pattern. Therefore, the determination of

pressure and airflow distributions is important to simulate the aeration system and storability, while ensuring that all areas of stored grain can receive sufficient airflow.

Early studies of airflow rate and pressure difference relationships have been presented by Ergun (1952) and Shedd (1953). Ergun (1952) predicted a formulation for incompressible airflow through a packed bed, and it can be expressed as:

$$\frac{\Delta P}{L} = RV + SV^2 \quad (2.1)$$

where ΔP is pressure difference along the length L , V is the velocity in the direction of airflow, R and S are empirical coefficients depending on the type of products.

Shedd (1953) measured the static pressure drop across common grains and seeds, and proposed the possibility of expressing this relationship by the mathematical equation, thus:

$$= A\left(\frac{\Delta P}{L}\right)^B \quad (2.2)$$

where A and B are seed - specific constants, which are determined from Shedd's (1953) experimental data.

Hukill and Ives (1955) suggested that Shedd's (1953) equation can only apply approximately for narrow ranges of velocity fields, if the constant coefficients in equation can be modified, the accuracy throughout of the velocity ranges will be increase. The logarithmic formula which they proposed is:

$$\frac{\Delta P}{L} = \frac{aV^2}{\ln(1+bV)} \quad (2.3)$$

where a and b are also the seed - specific constants.

Two major numerical methods have been developed to solve the pressure and velocity fields in storage, namely finite difference and finite element methods. (In this study, we shall exploit the finite difference method).

Brooker (1961, 1969) used the information given by Shedd (1953) to develop a finite difference computer simulation model, for establishing pressure patterns in a grain mass subjected to non-linear airflow resistance. Jindal and Thompson (1972) modified Brooker's model, and adapted it for predicting the pressure distribution and airflow paths through the long triangular shaped piles of grains. Pierce and Thompson (1975) modified Jindal and Thompson's (1972) simulation model for prediction airflow characteristics in conical shaped piles of grain. However, the mathematical models which describes the flow of air through stored grain assume that the steady state has been established and the flow of air is taken as incompressible.

By stating of the Ergun's (1952) equation in a vectorial form, Stanek and Szekely (1972, 1973, 1974) presented a formulation and measured the effect of non-uniform porosity on airflow maldistribution in isothermal and non-isothermal packed bed chemical reactors. They observed that the airflow maldistribution through packed bed results from a spatially non-uniform resistance to the airflow. This resistance is caused by variable porosity, particle size distribution and hot spot generation within the bed. Lai (1980) developed Ergun's (1952) equation into three vector components, and introduced the stream function for solving the non-linear partial differential equations that describe the airflow through porous media of grain bed. Hunter (1983) has given resistance coefficients for airflow through 28 different seeds, which are obtained from Ergun's (1952), by fitting them to Shedd's (1953) data. He analysed experimental data and compared them with Hukill and Ives' (1955) logarithmic expression for pressure gradient. Hunter's(1983) formula can be applied to most common duct store situations.

The application of the finite element method to solve the airflow problem was first used by Marchant (1976b) for calculating the airflow distribution and pressure patterns in several different storage structures. Since then, several finite element models have been

developed by Segerlind (1982), Smith (1982), Rumsey and Fortis (1984) and Chapman *et al.* (1989) to analyse air velocity and pressure in grain store.

Thorpe and Hunter (1977) have presented a finite difference solution of Laplace equation to airflow distribution in a non-uniformed aeration circular silo. The linear algebraic technique is used to solve the banded form of the coefficient matrix. The explicit analytic expressions allow pressure and velocity distributions to be easily calculated. Jayas and Muir (1991) have developed a method of incorporating the effect of airflow direction on pressure drops across granular beds in the mathematical models, for predicting the static airflow pressure patterns. Goudie *et al.* (1995) presented a computer model for simulation the linear analysis in low velocities and the non-linear approach in larger velocities. They have shown that velocity in the non-linear analysis was lower than the velocity in the linear analysis; the effect of the non-linearity is to move airflow away from the higher velocity regions towards the lower velocity regions.

2.3 CHANGES IN GRAIN MOISTURE CONTENT DUE TO TEMPERATURE GRADIENTS

Grain temperature and moisture content are the two major factors affecting grain quality during storage. Seasonal and diurnal variations in ambient temperature and solar radiation can create temperature gradients in the grain store, and cause moisture to migrate from warmer to cooler regions of the grain mass. This migration occurs slowly but steadily in grain storage. In order to attain the local equilibrium with the surrounding air, the warmer region of grain loses moisture and the colder region of grain gains moisture. That is because the transport processes tend to reduce the water vapour gradient and at same time the sorption relationship tends to maintain gradients, and the problem of moisture migration becomes dynamic in nature.

Therefore, the moisture migration process can be primarily considered as the diffusive and convective transport of the water vapour through the intergranular spaces of the grain storage where grain moisture acts as a source for the water vapour. The flow diagram of moisture migration phenomena is shown in figure 2.1 (Khankari *et al.*, 1994).

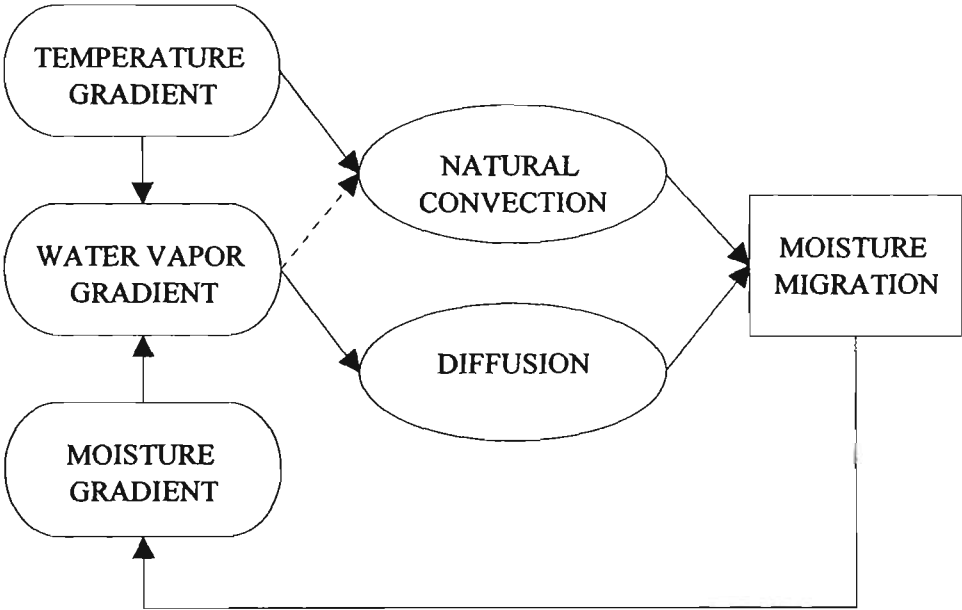


Figure 2.1 Moisture migration phenomena (after Khankari *et al.*, 1994)

However, the behaviour of migration of moisture is dependent on the amount of water present, structure of the storage, history of the grain temperature and atmospheric of relative humidity. Noyes *et al.* (1989) reported that moisture migration in stored grain is considered second to insect damage as a source of storage loss. The accumulation of moisture in a localised area of the grain mass stimulates the growth and development of fungi and insects (Hunt and Pixton, 1974), makes this region more susceptible, and leads to spoilage and microbial activity.

Several investigators have studied that moisture movement through the grain storage caused by water vapour diffusion or convection. Pixton and Griffiths (1971) described

the diffusion of moisture through stored wheat by means of a diffusion coefficient which is an empirically determined function of grain moisture content and temperature. The relationship between the moisture content of grain and its equilibrium relative humidity is assumed to be essentially linear in the moisture content range considered. Stewart (1975) showed that the gradient of vapour pressure, which is responsible for the diffusion transport of moisture, can be developed from the gradients of moisture and temperature. His theoretical analysis stated that temperature gradient provided the driving force for moisture migration during storage. Thorpe (1981) has carried out an analysis of Pixton and Griffiths's (1971) work, and presented the mechanism of moisture migration is the equalisation of vapour pressure by molecular diffusion in the gas phase.

Grain and surrounding air are always in thermodynamic equilibrium, therefore grain moisture, relative humidity and temperature of the air can be determined from the sorption isotherm. Thorpe (1982) developed Smith's (1947) formula for sorption isotherm, and predicted the thermodynamic and physical properties of wheat, which may be used to calculate the rate of diffusion of moisture through wheat bulks subjected to a temperature gradient.

The relationship between equilibrium moisture content and equilibrium relative humidity of grain is used to predict the moisture content of the stored grain in equilibrium with intergranular air, to optimise storage conditions and quality of grain. Many theories have been forwarded to explain the phenomenon of hysteresis in the desorption and adsorption isotherms of porous grain, they are developed by: Henderson (1952), Chung and Pfoest (1967a, 1967c), Foster (1967), Whitney and Porterfield (1968), Pixton and Warburton (1971), Versavel and Muir (1988), Mazza *et al.* (1990) and Sun and Woods (1993).

Most of work on predicting moisture movement in grain has been related to drying problems (Parry, 1985). Drying is the removal of moisture through grain and it is carried out by artificial means. It is likely to be a continuous process with changes in grain moisture content, temperature and absolute humidity all occurring simultaneously (Thompson *et al.*, 1968). In fact, these changes are related to different drying methods and different locations in the drying bed. Many tests have been made to describe the drying process, to determine drying time and safe drying conditions. Mathematical modelling and computer simulation are also widely used in research, in designing and in developing more efficient and safe grain drying. Normally, developing these models consists of two steps: Thin layer drying model and an in-bin drying model.

The application of thin layer drying models in deep beds has been given by Thompson *et al.* (1986), Henderson and Henderson (1968), Barre *et al.* (1971), Tang and Sokhansanj (1993), Parti (1993), Arinze *et al.* (1994) and Sun and Woods (1994). In-bin drying models have been developed by Spencer (1969), Bloome and Shove (1972), Ingram (1979), Smith *et al.* (1992) and Abawi (1993).

Drying has been the most common method for preserving grain in both cool and moist regions of the world and tropical regions. The proper drying is a precondition for safe storage and delivery. The climate, weather, airflow rate and depth of grain bed, the management of filling, fan and supplemental heat are all important factors affecting the performance of deep bed driers (Sharp, 1982).

2.4 INVESTIGATIONS IN CYLINDRICAL AND OTHER STORES

Numerical methods have served as useful tools for predicting the temperature and moisture content in grain storage. During the last 20 years, a number of models have

been developed for modelling heat transfer in stored grain in cylindrical bins, neglecting the interaction with moisture transfer (Jayas *et al.*, 1992). In recent years, a few numerical models in cylindrical storage have been developed:

Obaldo *et al.* (1991) has presented a two dimensional finite difference model which is based on Fick's Law of diffusion, to predict moisture content in an unventilated steel bin. They concluded: (1). The change in moisture content of unventilated storage was more pronounced at the top grain surface than any region of the storage. (2). The moisture gradient tended to be higher in the vertical axis than along the radius of the storage.

Abbouda *et al.* (1992) applied finite difference methods to modify a two dimensional model by free convection and heat generation from respiration of grain to predict grain temperature in cylindrical bin. Experimental data showed: (1). The bin size and initial moisture content affected the grain temperature difference between the top surface and the bottom of the bin. (2). The average grain temperature followed the trend of the ambient air temperature with a time delay.

Jayas *et al.* (1992) used a three dimensional finite element model to simulate the influence on the grain temperature of bin diameter, grain bulk height, bin wall material, bin ship and time. They found that: (1). Large diameter bins maintained warmer centre temperatures than small diameter bins. (2). The influence of heat loss from the grain surface on the grain centre temperatures was negligible for tall grain bulks. (3). A small diameter tall grain bulk maintained lower grain temperature than a larger diameter short grain bulk. (4). A white painted steel bin maintained coolest temperature and a galvanised steel bin gave the highest temperature among the bin wall. (5). The shape of the bins had little influence on the grain temperature.

Khankari *et al.* (1993a, 1993b) has presented the two dimensional numerical simulation models to predict the patterns of temperature, moisture and natural convection flows in stored grain. The predictions showed: (1). Moisture migration during winter caused an increase near the top of the bin and decrease near the bottom of the bin. (2). During spring or summer grain moisture decreased at the outer boundaries of the bin. (3). The moisture migration occurs in all size of bins, and the moisture starts accumulating earlier in small bins. (4). The effect of natural convection is more evident in the moisture transfer process than in the heat transfer.

Casada and Young (1994) developed two dimensional finite difference model to predict heat and moisture transfer due to short term and long term natural convection and diffusion in arbitrarily shaped porous media. They reported: (1). The energy and moisture transport equation were best solved using a modified Crank-Nicolson method that was developed to control the tendency for instability caused by the source terms in the equations. (2). The differences between the solid and fluid temperatures in porous media were largest near the side boundaries. (3). The natural convection currents contribute the temperature solution at the upper corners of the porous media.

Chang *et al.* (1994) have presented a two dimensional model in cylindrical silo using finite difference method, for periodic aeration and daily variations in soil temperature, ambient air conditions, and solar radiation. They concluded: (1). Moisture content difference between grain near the silo wall and away from silo wall were small for grain 1.0 m or more below the top surface. (2). During summer months, moisture content of the grain near the top of surface decrease, and were small for grain in the middle and bottom layers.

Fohr and Moussa (1994) carried out a experimental investigations of heat and mass transfer in a cylindrical grain silo submitted to a uniform and periodic wall heat flux, for understanding the mechanisms of the particular convection and to predict the amount of

water displaced. They observed: (1). The atmospheric factors, thus: solar radiation, air temperature, and wind velocity do not create a uniform heat flux. (2). The moist airflow out of the bulk grain can condense on the colder walls and be transformed into water drops.

Moreover, the heat and mass transfer processes occurring in any enclosure storage have been developed by numerical method. They are Andales *et al.* (1979), Fortes and Okos (1981), Khanhari *et al.* (1990), Freer *et al.* (1990), Singh and Thorpe (1992), Singh *et al.* (1993) and Khankair *et al.* (1994).

2.5 RELATED TOPICS

The simulation and measurement of cooling performance of aeration systems have been carried out by many workers. Thompson (1972) developed a simulation model to evaluate the effects of harvest date, initial moisture content, initial grain temperature and weather conditions on the temporary storage of high moisture shelled corn, through continuous ambient aeration. Hunter and Taylor (1980) have designed and applied a refrigerated aeration system to produce conditions hostile to insects throughout the grain bulk and to determine the design factors of airflow rate and distribution, heat loads and sources. Sutherland *et al.* (1983) applied an equilibrium model to predict the formation of temperature and moisture fronts, due to variation of front velocity successive cooling and heating or drying and wetting interact during aeration.

Thorpe and Elder (1982) have presented a finite difference mathematical model of the processes of heat and moisture transfer and pesticide decay in aerated grain, to obtain the effects on the rate of pesticide decay of initial grain moisture content, initial grain temperature, fan operation, airflow rates and geographic location. Thorpe (1986) has outlined and quantified the advantages and benefits of aeration, he also described

the fundamental processes of heat and mass transfer that govern the rate and amount of cooling during the aeration process, such as the dry matter loss due to respiration, insect population dynamics, seed viability, and the rate of pesticide decay. Hunter (1986) has presented the formula which are based on thermodynamic considerations to calculate the variation of aeration time fraction and airflow rate. Bridges *et al.* (1988) developed a computer model that determine duct sizes and duct location for aeration of grains in flat rectangular structures based on system design. Ismail *et al.* (1991) have carried out a experiment to predicate the performance of solar-regenerated aeration system. This solar cooling system is particularly effective in tropical climates.

Several researchers have proposed empirical models for the effect of physical damage, hybrid and weather conditions on estimated dry matter loss: Thompson (1972), Krishnamurthy *et al.* (1975), Freer *et al.* (1990), Stroshine and Yang (1990) and Singh *et al.* (1993).

In addition, moisture and temperature are dependent on transport properties which make the moisture migration and heat transfer problems coupled and nonlinear. Dutta *et al.* (1988) and Deshpande *et al.* (1993) have determined physical properties of grain. Kazarian and Hall (1965) and Dutta *et al.* (1988) have estimated the thermal properties of grain. An isostere equation for calculate the ratio of differential heat of sorption to latent heat is presented by Hunter (1987). Thorpe *et al.* (1990) have modified Hunter's isostere equation to derive an equation for the integral heat of wetting.

In this thesis, some of the above approaches and characterizations of grain and system properties will be drawn together to formulate a mathematical model of ventilated grain bulks stored in conical bottomed farm silos.

CHAPTER 3

ANALYSIS

This chapter marks the first major step in the development of the numerical method with the form and the meaning of the momentum, mass and thermal conservation equations, that apply in the physical domain, to be transformed into a computational domain. The boundaries conditions which apply to the silo walls, the conical base of silo, the upper surface of grains and the aeration duct are also implemented in each equation. The physical configuration of the system studied in this thesis is shown in figure 3.1.

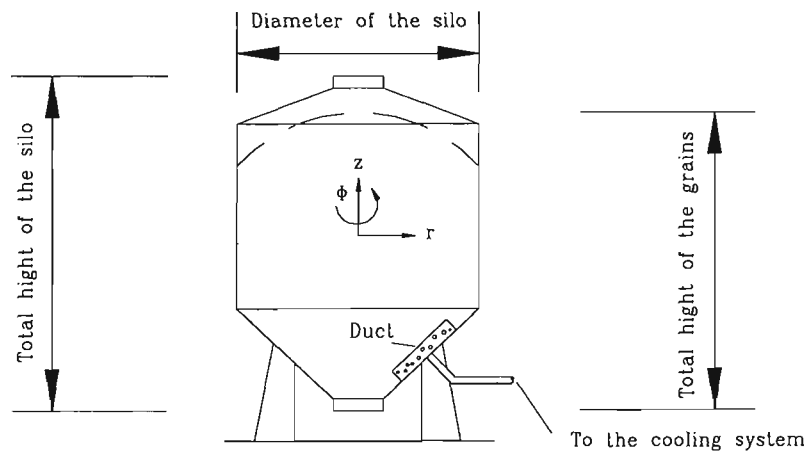


Figure 3.1 The physical configuration of the system

3.1 MOMENTUM EQUATION

The theory to predict air pressure and air velocity distributions through in aerated grain silo is based on Darcy's Law (1856). It is recognised that variables such as velocity,

pressure, temperature and grain moisture content vary on the length scales of the grain kernels and intergranular pores. In this thesis the relative length scales of these microscopic phenomena are very small (typically 10^{-3} times the height of the silo) and volume averaged quantities, *sensu* Thorpe *et al* (1991a, b), are used. In vectorial form of this momentum transfer is given by:

$$-\text{grad } P = \left(\frac{\mu}{k}\right) V \quad (3.1)$$

where μ is the dynamic viscosity, k is the intrinsic permeability, V is the air velocity vector, P is the air pressure pattern.

3.1.1 Pressures at interior nodes

A good approximation for calculation the air pressure distribution in aerated grain silo is to assume the pressure field satisfies the Laplace equation, which requires that the pressure can be take as constant with respect to time. In cylindrical coordinates (r, ϕ, z) , the governing equation may be written as:

$$\frac{\partial^2 P}{\partial r^2} + \frac{1}{r} \frac{\partial P}{\partial r} + \frac{1}{r^2} \frac{\partial^2 P}{\partial \phi^2} + \frac{\partial^2 P}{\partial z^2} = 0 \quad (3.2)$$

When the notional time tends to infinity (∞), and the pressure distribution become stable, a false transient term of the pressure flow can be effectively integrated to the steady state. This is expressed as:

$$\frac{1}{\alpha_p} \frac{\partial P}{\partial t} = 0 \quad (3.3)$$

where α_p is a false transient factor and assigned that ensures a converged solution.

Combination equations (3.2) and (3.3) together, the pressure distribution in grain silo can be determined by solving the following equation:

$$\frac{1}{\alpha_p} \frac{\partial P}{\partial t} = \frac{\partial^2 P}{\partial r^2} + \frac{1}{r} \frac{\partial P}{\partial r} + \frac{1}{r^2} \frac{\partial^2 P}{\partial \phi^2} + \frac{\partial^2 P}{\partial z^2} \quad (3.4)$$

3.1.2 Pressures at boundary nodes

In finite difference approximation, the boundary conditions of the domain require special treatment. At the upper surface of the grain, the pressure field is zero relative to atmosphere, so we have:

$$P = 0 \quad (3.5)$$

$$\text{when} \quad \begin{cases} 0 \leq r \leq R \\ 0 \leq \phi \leq 2\pi \\ z = H_{wall} + R \tan \gamma_1 + (R - r) \tan \gamma_2 \end{cases}$$

where H_{wall} is the height of the vertical wall of the silo, γ_1 is the angle of the silo floor to horizontal plane, and γ_2 is the angle between upper surface silo to horizontal plane, R is the radius of the silo.

At the internal vertical wall of the silo the normal velocity component is zero from which it follows that the pressure gradient is given by:

$$\frac{\partial P}{\partial r} = 0 \quad (3.6)$$

$$\text{when} \quad \begin{cases} r = R \\ 0 \leq \phi \leq 2\pi \\ R \tan \gamma_1 \leq z \leq R \tan \gamma_1 + H_{wall} \end{cases}$$

At the bottomed cone base of the silo, the pressure field is determined by:

$$\frac{\partial P}{\partial z} = 0 \quad (3.7)$$

$$\text{when} \quad \begin{cases} r = 1 \\ 0 \leq \phi \leq 2\pi \\ z = 1 \end{cases}$$

Along the sloping floor of the silo, the pressure gradient is obtained by:

$$\frac{\partial P}{\partial r} \frac{\partial r}{\partial n} + \frac{\partial P}{\partial \phi} \frac{\partial \phi}{\partial n} + \frac{\partial P}{\partial z} \frac{\partial z}{\partial n} = 0 \quad (3.8)$$

when
$$\begin{cases} 0 \leq r \leq R \\ 0 \leq \phi \leq 2\pi \\ z = 1 \end{cases}$$

At the aeration duct, the pressure distribution is deemed to consist of a line source of pressure pattern along the floor of the silo. We can write as:

$$P = P_{duct} \quad (3.9)$$

when
$$\begin{cases} r_{duct \min} \leq r \leq r_{duct \max} \\ \phi_{duct \min} \leq \phi \leq \phi_{duct \max} \\ z = r \tan \gamma_1 \end{cases}$$

where $r_{duct \min}$ and $r_{duct \max}$ are the length bounds of the duct, in the cylindrical coordinates (r, ϕ, z) , they are along the r direction of the silo. $\phi_{duct \min}$ and $\phi_{duct \max}$ are the width bounds of the duct, they are along the ϕ direction of the silo.

3.1.3 Velocity components

Equation (3.1) describes the relationship between air velocity with air pressure difference, when the pressure field is substituted into the momentum equation, the resulting of velocity field will satisfy the continuity equation, namely the velocity field is equal to the negative gradient of the pressure. By means of equation (3.1), we obtain:

$$V = -\frac{k}{\mu} \cdot \frac{\Delta P}{\Delta S} \quad (3.10)$$

where ΔP is the pressure difference and ΔS is an element of length. So the three components of the velocity field can be expressed in cylindrical coordinates as:

The radial components velocity (V_r) is:

$$V_r = -\frac{1}{R_p} \frac{\partial P}{\partial r} \quad (3.11)$$

The angular components velocity (V_ϕ) is:

$$V_\phi = -\frac{1}{R_p} \frac{1}{r} \frac{\partial P}{\partial \phi} \quad (3.12)$$

The vertical components velocity (V_z) is:

$$V_z = -\frac{1}{R_p} \frac{\partial P}{\partial z} \quad (3.13)$$

where R_p is the coefficient resistance to the airflow given by Hunter (1983) for applying airflow distribution through 28 different seeds. For spherical particles, we can estimate values of R_p from:

$$R_p = \frac{49\mu\epsilon^2}{\rho^2} S^2 \quad (3.14)$$

where S is the second Ergun (1952) coefficients, ρ and μ are the density and viscosity of air, and ϵ is the seed bulk porosity.

3.2 THERMAL ENERGY CONSERVATION EQUATION

3.2.1 Temperatures at interior nodes

Thorpe (1994, 1995) has presented a mathematical description of the heat and mass transfer phenomena that occur in ventilated beds of respiring grains. By following this work, the thermal energy conservation equation in cylindrical coordinates is written as:

$$\begin{aligned} & \left[\rho_b \left\{ (c_2)_\sigma + (c_1)_\sigma W + \frac{\partial H_w}{\partial T} \right\} + \epsilon_r \rho_a \left\{ c_a + H((c_1)_r + (c_{2v})) \right\} \right] \frac{\partial T}{\partial t} \\ & - \rho_b h_s \frac{\partial W}{\partial t} - \rho_b \frac{dm}{dt} \int_0^w h_s dW + \rho_a (c_a + H((c_1)_r + c_{2v})) \times \\ & \left\{ V_r \frac{\partial T}{\partial r} + \frac{V_\phi}{r} \frac{\partial T}{\partial \phi} + V_z \frac{\partial T}{\partial z} \right\} = K_{eff} \left\{ \frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} + \frac{\partial^2 T}{\partial z^2} \right\} \\ & + \rho_b \frac{dm}{dt} (Q_r - 0.6h_{vap}) \end{aligned} \quad (3.15)$$

In order to solve equation (3.15) numerically, it is convenient to express the temperature transient ($\frac{\partial T}{\partial t}$) as the formula as below:

$$\begin{aligned} \frac{\partial T}{\partial t} = \frac{1}{denom} \{ & K_{eff} \left\{ \frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} + \frac{\partial^2 T}{\partial z^2} \right\} \\ & + \rho_b \frac{dm}{dt} (Q_r - 0.6h_{vap}) + \rho_b h_s \frac{\partial W}{\partial t} + \rho_b \frac{dm}{dt} \int_0^w h_s dW \\ & - \rho_a \{ c_a + H((c_1)_r + c_{2v}) \} \times \left\{ V_r \frac{\partial T}{\partial r} + \frac{V_\phi}{r} \frac{\partial T}{\partial \phi} + V_z \frac{\partial T}{\partial z} \right\} \} \end{aligned} \quad (3.16)$$

$$\text{where} \quad denom = \rho_b \left\{ (c_2)_\sigma + (c_1)_\sigma W + \frac{\partial H_w}{\partial T} \right\} + \epsilon_r \rho_a \{ c_a + H((c_1)_r + (c_{2v})) \} \quad (3.17)$$

in which T is the temperature distribution of the stored grains, W is the grain moisture content field, H is the absolute humidity of the air flow, K_{eff} is the effective thermal dispersivity tensor, H_w is the integral heat of wetting of grains, and other physical properties have been given in the list of nomenclature. The further discussion of these physical properties will be given in Chapter 5.

3.2.2 Temperatures at boundary nodes

On the internal circular wall and floor of the grain silo, the temperature distribution is the function of solar radiation and ambient temperature. The best way for solving these boundary conditions of temperatures is to treat the wall and floor separately, because the intensity of solar radiation is clearly different on each of these components of the silo.

At the circular wall of the silo the equation can be written as:

$$T = f_{wall}(R, \phi, z) \quad (3.18)$$

$$\text{when} \quad \begin{cases} 0 \leq \phi \leq 2\pi \\ R \tan \gamma_1 \leq z \leq R \tan \gamma_1 + H_{wall} \end{cases}$$

On the bottom of the silo floor, the function is:

$$T = f_{\text{floor}}(r, \phi, z) \quad (3.19)$$

when

$$\begin{cases} 0 \leq r \leq R \\ 0 \leq \phi < \phi_{\text{duct min}} \\ \phi_{\text{duct max}} < \phi \leq 2\pi \\ z = r \tan \gamma_1 \end{cases}$$

At the aeration duct, the temperature field of the grain is set equal to the inlet air, thus:

$$T = T_{\text{duct}}(r, \phi, z) \quad (3.20)$$

when

$$\begin{cases} r_{\text{duct min}} \leq r \leq r_{\text{duct max}} \\ \phi_{\text{duct min}} \leq \phi \leq \phi_{\text{duct max}} \\ z = r \tan \gamma_1 \end{cases}$$

At the upper surface of the grain, the temperature gradient is considered to have a zero gradient normal to the surface of grain, thus:

$$\frac{\partial T}{\partial r} \frac{\partial r}{\partial n} + \frac{\partial T}{\partial \phi} \frac{\partial \phi}{\partial n} + \frac{\partial T}{\partial z} \frac{\partial z}{\partial n} = 0 \quad (3.21)$$

when

$$\begin{cases} 0 \leq r \leq R \\ 0 \leq \phi \leq 2\pi \\ z = H_{\text{wall}} + R \tan \gamma_1 + (R - r) \tan \gamma_2 \end{cases}$$

At the upper surface of the centre silo, the temperature field is expressed in equation as:

$$\frac{\partial T}{\partial z} = 0 \quad (3.22)$$

when

$$\begin{cases} r = 0 \\ 0 \leq \phi \leq 2\pi \\ z = H_{\text{wall}} + R \tan \gamma_1 + (R - r) \tan \gamma_2 \end{cases}$$

At the bottom of the cone of the centre silo, the temperature distribution is given in the following equation:

$$\frac{\partial T}{\partial z} = 0 \quad (3.23)$$

when

$$\begin{cases} r = 0 \\ 0 \leq \phi \leq 2\pi \\ z = 0 \end{cases}$$

3.3 MOISTURE CONSERVATION EQUATION

3.3.1 Moisture contents at interior nodes

Grain moisture is transported within the bulk from regions of high intergranular vapour pressure to regions of low vapour pressure by means of diffusion and convection, and lead the air entering regions of low temperature increase its relative humidity. This movement causes grain to adsorb moisture, and render grainself more susceptible to spoilage and microbial activity. According to Thorpe's (1994, 1995) analyses, the air and grain kernels are considered to be in thermodynamic equilibrium, and it does not need to consider a finite resistance to mass transfer. In this cause, the moisture conservation equation is expressed in cylindrical coordinates as:

$$\begin{aligned}
 & \frac{\partial W}{\partial t} + \frac{\rho_a}{\rho_b} \left\{ V_r \frac{\partial H}{\partial r} + \frac{V_\phi}{r} \frac{\partial H}{\partial \phi} + V_z \frac{\partial H}{\partial z} \right\} \\
 &= D_{eff} \frac{\rho_a}{\rho_b} \left\{ \frac{\partial^2 H}{\partial r^2} + \frac{1}{r} \frac{\partial H}{\partial r} + \frac{1}{r^2} \frac{\partial^2 H}{\partial \phi^2} + \frac{\partial^2 H}{\partial z^2} \right\} \\
 &+ \frac{dm}{dt} (0.6 + W)
 \end{aligned} \tag{3.24}$$

A small re-arrangement of equation (3.24) yields the equation governing the behaviour of moisture content of grains in the intergranular air, and it is conveniently expressed explicitly in term of $(\frac{\partial W}{\partial t})$, thus:

$$\begin{aligned}
 \frac{\partial W}{\partial t} &= D_{eff} \frac{\rho_a}{\rho_b} \left\{ \frac{\partial^2 H}{\partial r^2} + \frac{1}{r} \frac{\partial H}{\partial r} + \frac{1}{r^2} \frac{\partial^2 H}{\partial \phi^2} + \frac{\partial^2 H}{\partial z^2} \right\} \\
 &- \frac{\rho_a}{\rho_b} \left\{ V_r \frac{\partial H}{\partial r} + \frac{V_\phi}{r} \frac{\partial H}{\partial \phi} + V_z \frac{\partial H}{\partial z} \right\} \\
 &+ \frac{dm}{dt} (0.6 + W)
 \end{aligned} \tag{3.25}$$

where $\frac{dm}{dt}$ is the rate of dry matter loss, and this will be detailed in Chapter 5. D_{eff} is the effective diffusion coefficient of the moisture, this may be obtained from experimental relationships with the particle Reynolds number, and it has been calculated from first principle by Thorpe *et al.*, (1991a, b).

In order solving the moisture conservation equation, firstly the distribution of absolute humidities flow is must be calculated. At the interior nodes of the silo, it is obtained by solving equation (5.6) (see chapter 5). At the boundary conditions of the silo, the absolute humidities of the air can be solved by the equation as following.

3.3.2 Absolute humidities at boundary nodes

The floor of the silo is impermeable to moisture vapour, hence the distribution of absolute humidities of the air is expressed as the following equation:

$$\frac{\partial H}{\partial r} \frac{\partial r}{\partial n} + \frac{\partial H}{\partial \phi} \frac{\partial \phi}{\partial n} + \frac{\partial H}{\partial z} \frac{\partial z}{\partial n} = 0 \quad (3.26)$$

when

$$\begin{cases} 0 \leq r \leq R \\ 0 \leq \phi < \phi_{duct \min} \\ \phi_{duct \max} < \phi \leq 2\pi \\ z = r \tan \gamma_1 \end{cases}$$

Along the vertical wall of the silo, the absolute humidities of the air field is:

$$\frac{\partial H}{\partial r} = 0 \quad (3.27)$$

when

$$\begin{cases} r = R \\ 0 \leq \phi \leq 2\pi \\ R \tan \gamma_1 \leq z \leq R \tan \gamma_1 + H_{wall} \end{cases}$$

Along the upper surface of the grain, the flow of absolute humidities of the air is:

$$\frac{\partial H}{\partial z} = 0 \quad (3.28)$$

when
$$\begin{cases} 0 \leq r \leq R \\ 0 \leq \phi \leq 2\pi \\ z = R \tan \gamma_1 + H_{wall} + (R - r) \tan \gamma_2 \end{cases}$$

At the aeration duct, the distribution of absolute humidities of the air is the entering air through aeration duct to the grain silo, so we have:

$$H = H_{duct} \quad (3.29)$$

when
$$\begin{cases} r_{duct \min} \leq r \leq r_{duct \max} \\ \phi_{duct \min} \leq \phi \leq \phi_{duct \max} \\ z = r \tan \gamma_1 \end{cases}$$

At the bottomed cone base of the silo, the absolute humidities of the air is given by:

$$\frac{\partial H}{\partial z} = 0 \quad (3.30)$$

when
$$\begin{cases} r = 1 \\ 0 \leq \phi \leq 2\pi \\ z = 1 \end{cases}$$

At the peak of the grain, the absolute humidities of the air flow can be written as:

$$\frac{\partial H}{\partial z} = 0 \quad (3.31)$$

when
$$\begin{cases} r = 1 \\ 0 \leq \phi \leq 2\pi \\ z = nz \end{cases}$$

3.4. COORDINATE TRANSFORMATION

In this study, the three dimensional physical domain of conical bottomed circular silo has a complicated geometry and boundary conditions. In the numerical solution procedure, it required that enables zero flux boundary conditions to be treated in a straight forward manner.

A useful technique for solving this problem is to employ the finite difference approximations to control the mapping, and using the non-orthogonal grid in the physical three-dimensional domain to transform into a simplistic three-dimensional computational domain which can be used to discretise the governing partial differential equations and the appropriate boundary conditions on an orthogonal grid. The easy way for implementing this technique is to apply the original circular cone in terms of the spatial variables (r, ϕ, z) in cylindrical space to map into a right circular cylinder in terms of the variables (ξ, ϕ, η) in cylindrical coordinates, this is illustrated in figure 3.2 as below.

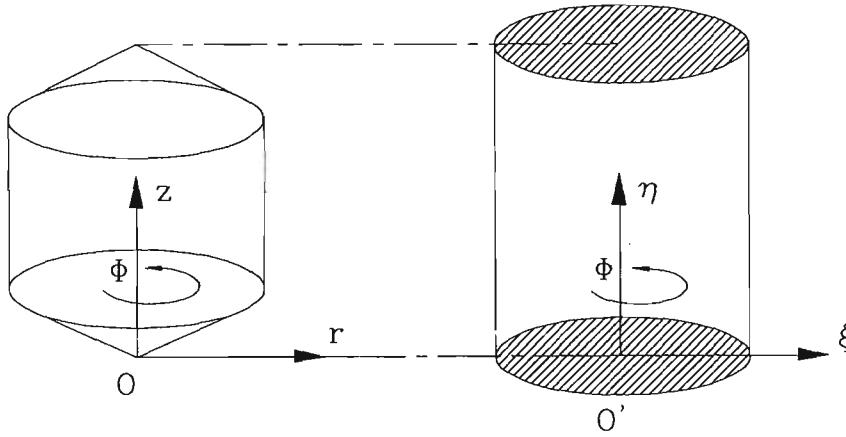


Figure 3.2 The original circular cone transformed to the right circular cylinder

Evidently, as figure 3.2 shows, the origins in both coordinates are $O(0,0,0)$ and $O'(0,0,0)$, the length of radius r in transformed coordinates is dimensionless radius ξ , the height of silo z in transformed coordinates is dimensionless height η , and the angles $\phi(0 \leq \phi \leq 2\pi)$ of both domains are equal.

In order to transform the original partial differential equations and boundary conditions from the circular conic domain (r, ϕ, z) to the right circular cylinder domain (ξ, ϕ, η) , the relations of an arbitrary scalar Γ is found by the chain rule of partial differentiation in the first partial derivative, thus:

$$\frac{\partial \Gamma}{\partial r} = \frac{\partial \Gamma}{\partial \xi} \frac{\partial \xi}{\partial r} + \frac{\partial \Gamma}{\partial \eta} \frac{\partial \eta}{\partial r} + \frac{\partial \Gamma}{\partial \phi} \frac{\partial \phi}{\partial r} \quad (3.32)$$

$$\frac{\partial \Gamma}{\partial \phi} = \frac{\partial \Gamma}{\partial \xi} \frac{\partial \xi}{\partial \phi} + \frac{\partial \Gamma}{\partial \eta} \frac{\partial \eta}{\partial \phi} + \frac{\partial \Gamma}{\partial \phi} \frac{\partial \phi}{\partial \phi} \quad (3.33)$$

$$\frac{\partial \Gamma}{\partial z} = \frac{\partial \Gamma}{\partial \xi} \frac{\partial \xi}{\partial z} + \frac{\partial \Gamma}{\partial \eta} \frac{\partial \eta}{\partial z} + \frac{\partial \Gamma}{\partial \phi} \frac{\partial \phi}{\partial z} \quad (3.34)$$

where

$$\frac{\partial \phi}{\partial r} = \frac{\partial \phi}{\partial z} = \frac{\partial \xi}{\partial \phi} = \frac{\partial \eta}{\partial \phi} = \frac{\partial \phi}{\partial \xi} = 0 \quad (3.35)$$

and

$$\frac{\partial \phi}{\partial \phi} = 1 \quad (3.36)$$

where Γ can represent any function of ξ , ϕ and η .

Rearranging equations (3.32), (3.33) and (3.34), the formula can be written as:

$$\frac{\partial \Gamma}{\partial r} = \frac{\partial \Gamma}{\partial \xi} \frac{\partial \xi}{\partial r} + \frac{\partial \Gamma}{\partial \eta} \frac{\partial \eta}{\partial r} \quad (3.37)$$

$$\frac{\partial \Gamma}{\partial z} = \frac{\partial \Gamma}{\partial \xi} \frac{\partial \xi}{\partial z} + \frac{\partial \Gamma}{\partial \eta} \frac{\partial \eta}{\partial z} \quad (3.38)$$

From the cross-section of the cone, the half of the original circular conic silo is defined by four functions. These geometries are shown in the cylindrical coordinates at figure 3.3.

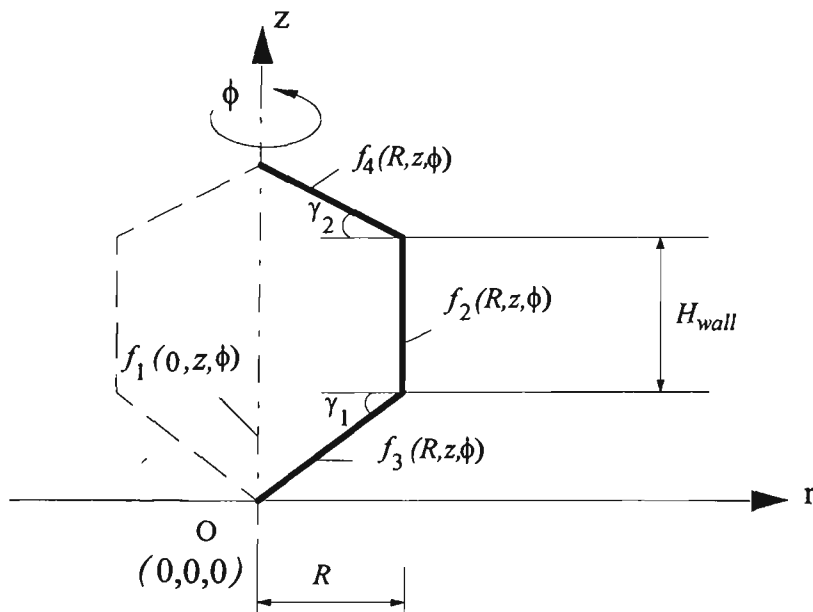


Figure 3.3 The four functions of original circular conic silo

In the above figure, R is the radius of the conical bottomed circular silo, H_{wall} is the wall height of the silo, O is the origin of the coordinate system, ϕ is the angular direction, and in the region of $0 \leq \phi \leq 2\pi$.

The four functions are expressed as:

$$f_1(0, z, \phi) = 0 \quad (3.39)$$

$$f_2(R, z, \phi) = R \quad (3.40)$$

$$f_3(r, z, \phi) = r \tan \gamma_1 \quad (3.41)$$

$$f_4(r, z, \phi) = H_{wall} + R \tan \gamma_1 + (R - r) \tan \gamma_2 \quad (3.42)$$

We define the relationship between the functions in cylindrical coordinates (r, ϕ, z) and the variables of ξ and η in transformed coordinates (ξ, ϕ, η) , after the manner of Moretti and Abbett (1966), thus:

$$\xi = \frac{r - f_1(r, z, \phi)}{f_2(r, z, \phi) - f_1(r, z, \phi)} \quad (3.43)$$

$$\eta = \frac{z - f_3(r, z, \phi)}{f_4(r, z, \phi) - f_3(r, z, \phi)} \quad (3.44)$$

where the value of both ξ and η are assumed to be between 0 and 1. Substituting equations (3.39), (3.40), (3.41) and (3.42) into equations (3.43) and (3.44), results in the variables ξ and η being determined as:

$$\xi = \frac{r}{R} \quad (0 \leq r \leq R) \quad (3.45)$$

$$\begin{aligned} \eta &= \frac{z - r \tan \gamma_1}{H_{wall} + R \tan \gamma_1 + (R - r) \tan \gamma_2 - r \tan \gamma_1} \\ &= \frac{z - r \tan \gamma_1}{Z_{total} - r(\tan \gamma_1 + \tan \gamma_2)} \end{aligned} \quad (3.46)$$

where Z_{total} is the total height of the silo.

Therefore the first partial derivatives of the $\frac{\partial \xi}{\partial r}$, $\frac{\partial \eta}{\partial r}$, $\frac{\partial \xi}{\partial z}$ and $\frac{\partial \eta}{\partial z}$ are obtained:

$$\frac{\partial \xi}{\partial r} = \frac{1}{R} \quad (3.47)$$

$$\begin{aligned} \frac{\partial \eta}{\partial r} &= \frac{-\tan \gamma_1 (H_{wall} - r(\tan \gamma_1 + \tan \gamma_2)) - (z - r \tan \gamma_1)(-(\tan \gamma_1 + \tan \gamma_2))}{(H_{wall} - r(\tan \gamma_1 - \tan \gamma_2))^2} \\ &= \frac{A^* - C^* \cdot D^*}{(B^*)^2} \end{aligned} \quad (3.48)$$

we set

$$A^* = -\tan \gamma_1 \quad (3.49)$$

$$B^* = Z_{total} - r(\tan \gamma_1 + \tan \gamma_2) \quad (3.50)$$

$$C^* = z - r \tan \gamma_1 \quad (3.51)$$

$$D^* = -(\tan \gamma_1 + \tan \gamma_2) \quad (3.52)$$

and

$$\frac{\partial \xi}{\partial z} = 0 \quad (3.53)$$

$$\begin{aligned} \frac{\partial \eta}{\partial z} &= \left(\frac{z - r \tan \gamma_1}{Z_{total} - r(\tan \gamma_1 + \tan \gamma_2)} \right)' \\ &= \frac{1}{Z_{total} - r(\tan \gamma_1 + \tan \gamma_2)} \end{aligned} \quad (3.54)$$

A notation has been presented by Singh and Thorpe (1993a, b) for the first partial derivative by which we express:

$$\frac{\partial \Gamma}{\partial r} = \alpha_1 \frac{\partial \Gamma}{\partial \xi} + \alpha_2 \frac{\partial \Gamma}{\partial \eta} \quad (3.55)$$

$$\frac{\partial \Gamma}{\partial z} = \alpha_3 \frac{\partial \Gamma}{\partial \xi} + \alpha_4 \frac{\partial \Gamma}{\partial \eta} \quad (3.56)$$

we define

$$\alpha_1 = \frac{\partial \xi}{\partial r} \quad (3.57)$$

$$\alpha_2 = \frac{\partial \eta}{\partial r} \quad (3.58)$$

$$\alpha_3 = \frac{\partial \xi}{\partial z} \quad (3.59)$$

$$\alpha_4 = \frac{\partial \eta}{\partial z} \quad (3.60)$$

Singh and Thorpe (1993a) have presented an expression for the second partial derivatives of the scalar Γ , which we are able to write as:

$$\frac{\partial^2 \Gamma}{\partial r^2} + \frac{\partial^2 \Gamma}{\partial z^2} = \beta_1 \frac{\partial^2 \Gamma}{\partial \xi^2} + \beta_2 \frac{\partial^2 \Gamma}{\partial \eta^2} + \beta_3 \frac{\partial^2 \Gamma}{\partial \xi \partial \eta} + \beta_4 \frac{\partial \Gamma}{\partial \xi} + \beta_5 \frac{\partial \Gamma}{\partial \eta} \quad (3.61)$$

in which

$$\beta_1 = \alpha_1^2 + \alpha_3^2 \quad (3.62)$$

$$\beta_2 = \alpha_2^2 + \alpha_4^2 \quad (3.63)$$

$$\beta_3 = 2(\alpha_1 \alpha_2 + \alpha_3 \alpha_4) \quad (3.64)$$

$$\beta_4 = 2\left(\frac{\partial^2 \xi}{\partial r^2} + \frac{\partial^2 \xi}{\partial z^2}\right) \quad (3.65)$$

$$\beta_5 = 2\left(\frac{\partial^2 \eta}{\partial r^2} + \frac{\partial^2 \eta}{\partial z^2}\right) \quad (3.66)$$

From equations (3.47), (3.48), (3.53) and (3.54), we can determine the second partial derivatives $\frac{\partial^2 \xi}{\partial r^2}$, $\frac{\partial^2 \eta}{\partial r^2}$, $\frac{\partial^2 \xi}{\partial z^2}$ and $\frac{\partial^2 \eta}{\partial z^2}$, thus:

$$\frac{\partial^2 \xi}{\partial r^2} = \left(\frac{1}{R}\right)' = 0 \quad (3.67)$$

$$\begin{aligned} \frac{\partial^2 \eta}{\partial r^2} &= \left(\frac{B^* \cdot A^* - C^* \cdot D^*}{(B^*)^2}\right)' \\ &= 2 \frac{(-B^* \cdot A^* + C^* \cdot D^*)D^*}{(B^*)^3} \end{aligned} \quad (3.68)$$

$$\frac{\partial^2 \xi}{\partial z^2} = 0 \quad (3.69)$$

$$\frac{\partial^2 \eta}{\partial z^2} = \left(\frac{1}{Z_{total} - r(\tan \gamma_1 + \tan \gamma_2)}\right)' = 0 \quad (3.70)$$

3.5 MOMENTUM EQUATION IN TRANSFORMED COORDINATES

3.5.1 Pressures at interior nodes in transformed coordinates

In transformed coordinates, equation (3.4) that governs the pressure field in the grain silo, it may be expressed as:

$$\frac{1}{\alpha_p} \frac{\partial P}{\partial t} = \beta_1 \frac{\partial^2 P}{\partial \xi^2} + \beta_2 \frac{\partial^2 P}{\partial \eta^2} + \beta_3 \frac{\partial^2 P}{\partial \xi \partial \eta} + \beta_6 \frac{\partial P}{\partial \xi} + \beta_7 \frac{\partial P}{\partial \eta} + \frac{1}{R^2 \xi^2} \frac{\partial^2 P}{\partial \phi^2} \quad (3.71)$$

where we define

$$\beta_6 = \beta_4 + \frac{\alpha_1}{R\xi} \quad (3.72)$$

$$\beta_7 = \beta_5 + \frac{\alpha_2}{R\xi} \quad (3.73)$$

$$\text{and} \quad r = R\xi \quad (3.74)$$

3.5.2 Pressures at boundary nodes in transformed coordinates

Equation (3.6) that governs pressure boundary conditions at the vertical wall of the grain silo, it can be expressed in transformed coordinates as:

$$\alpha_1 \frac{\partial P}{\partial \xi} + \alpha_2 \frac{\partial P}{\partial \eta} = 0 \quad (3.75)$$

$$\text{when} \quad \begin{cases} \xi = 1 \\ 0 \leq \phi \leq 2\pi \\ 0 \leq \eta \leq 1 \end{cases}$$

In transformed coordinates, the conical floor is transformed into horizontal floor, and the normal distance is independent of ϕ . So equation (3.8) can be written in cylindrical coordinates as:

$$\frac{\partial P}{\partial r} \frac{\partial r}{\partial n} + \frac{\partial P}{\partial z} \frac{\partial z}{\partial n} = 0 \quad (3.76)$$

we observe that

$$\frac{\partial r}{\partial n} = -\sin \gamma_1 \quad (3.77)$$

$$\frac{\partial z}{\partial n} = \cos \gamma_1 \quad (3.78)$$

Rearranging equation (3.76), enables it to be written in the transformed coordinates as following:

$$(\alpha_1 \frac{\partial P}{\partial \xi} + \alpha_2 \frac{\partial P}{\partial \eta})(-\sin \gamma_1) + (\alpha_3 \frac{\partial P}{\partial \xi} + \alpha_4 \frac{\partial P}{\partial \eta}) \cos \gamma_1 = 0 \quad (3.79)$$

when
$$\begin{cases} 0 \leq \xi \leq 1 \\ 0 \leq \phi \leq 2\pi \\ \eta = 0 \end{cases}$$

Equation (3.5) governs the pressure field at the upper surface of the grain. In transformed coordinates it is:

$$P = 0 \quad (3.80)$$

when
$$\begin{cases} 0 \leq \xi \leq 1 \\ 0 \leq \phi \leq 2\pi \\ \eta = 1 \end{cases}$$

Equation (3.7) is expressed the pressure pattern at the bottomed conical base of the silo, in transformed coordinates is:

$$\frac{\partial P}{\partial \eta} = 0 \quad (3.81)$$

when
$$\begin{cases} \xi = 0 \\ 0 \leq \phi \leq 2\pi \\ \eta = 0 \end{cases}$$

Equation (3.9) shows the pressure flow at aeration duct, in transformed coordinates is:

$$P = P_{duct} \quad (3.82)$$

when

$$\begin{cases} \xi_{duct\ min} \leq \xi \leq \xi_{duct\ max} \\ \phi_{duct\ min} \leq \phi \leq \phi_{duct\ max} \\ \eta = 0 \end{cases}$$

Where $\xi_{duct\ min}$, $\xi_{duct\ max}$ are the length bounds of the duct in the transformed coordinates of ξ direction of the silo.

3.5.3 Velocity components in transformed coordinates

The three components of the velocity field in transformed coordinates is obtained by modifying equations (3.11), (3.12) and (3.13), which govern the velocity field in cylindrical coordinates. The expressions are given as following:

The components of the radial velocity is presented in transformed coordinates as:

$$V_r = -\frac{1}{R_p}(\alpha_1 \frac{\partial P}{\partial \xi} + \alpha_2 \frac{\partial P}{\partial \eta}) \quad (3.83)$$

The components of the angular velocity is obtained in transformed coordinates as:

$$V_\phi = -\frac{1}{R_p} \frac{1}{R\xi} \frac{\partial P}{\partial \phi} \quad (3.84)$$

The components of the vertical velocity is written in transformed coordinates as:

$$V_z = -\frac{1}{R_p}(\alpha_3 \frac{\partial P}{\partial \xi} + \alpha_4 \frac{\partial P}{\partial \eta}) \quad (3.85)$$

3.6 THERMAL ENERGY CONSERVATION EQUATION IN TRANSFORMED COORDINATES

3.6.1 Temperatures at interior nodes in transformed coordinates

Equation (3.16) is governing the temperature field which can be written in the transformed coordinates system as:

$$\begin{aligned}
\frac{\partial T}{\partial t} = \frac{1}{denom} \{ & K_{eff} \left\{ \beta_1 \frac{\partial^2 T}{\partial \xi^2} + \beta_2 \frac{\partial^2 T}{\partial \eta^2} + \beta_3 \frac{\partial^2 T}{\partial \xi \partial \eta} + \beta_6 \frac{\partial T}{\partial \xi} + \beta_7 \frac{\partial T}{\partial \eta} + \beta_8 \frac{\partial^2 T}{\partial \phi^2} \right\} \\
& + \rho_b \frac{dm}{dt} (Q_r - 0.6 h_{vap}) + \rho_b h_s \frac{\partial W}{\partial t} + \rho_b \frac{dm}{dt} \int_0^w h_s dH - \rho_a \{ c_a + H((c_1)_\gamma + c_{2v}) \} \\
& \times \left\{ V_r (\alpha_1 \frac{\partial T}{\partial \xi} + \alpha_2 \frac{\partial T}{\partial \eta}) + \frac{V_\phi}{R\xi} \frac{\partial T}{\partial \phi} + V_z (\alpha_3 \frac{\partial T}{\partial \xi} + \alpha_4 \frac{\partial T}{\partial \eta}) \right\} \} \quad (3.86)
\end{aligned}$$

where $denom = \rho_b \left\{ (c_2)_\sigma + (c_1)_\sigma W + \frac{\partial H_w}{\partial T} \right\} + \epsilon_\gamma \rho_a \{ c_a + H((c_1)_\gamma + (c_{2v})) \}$

3.6.2 Temperatures at boundary nodes in transformed coordinates

Equation (3.18) governs the temperature field in the circular wall of the silo. In the transformed coordinates, it may expressed as:

$$T = f_{wall}(1, \phi, \eta) \quad (3.87)$$

when
$$\begin{cases} 0 \leq \phi \leq 2\pi \\ 0 \leq \eta \leq 1 \end{cases}$$

At the floor of the silo, equation (3.19) can be given by transformed coordinates as:

$$T = f_{floor}(\xi, \phi, 0) \quad (3.88)$$

when
$$\begin{cases} 0 \leq \xi \leq 1 \\ 0 < \phi \leq \phi_{duct \min} \\ \phi_{duct \min} < \phi \leq 2\pi \end{cases}$$

At the aeration duct, equation (3.20) becomes:

$$T = T_{duct} \quad (3.89)$$

when
$$\begin{cases} \xi_{duct \min} \leq \xi \leq \xi_{duct \max} \\ \phi_{duct \min} \leq \phi \leq \phi_{duct \max} \\ \eta = 0 \end{cases}$$

Equation (3.21) is zero flux boundary condition. It is written in transformed coordinates as (the value of ϕ is constant):

$$(\alpha_1 \frac{\partial T}{\partial \xi} + \alpha_2 \frac{\partial T}{\partial \eta}) \frac{\partial r}{\partial n} + (\alpha_3 \frac{\partial T}{\partial \xi} + \alpha_4 \frac{\partial T}{\partial \eta}) \frac{\partial z}{\partial n} = 0 \quad (3.90)$$

when
$$\begin{cases} 0 \leq \xi \leq 1 \\ 0 \leq \phi \leq 2\pi \\ \eta = 1 \end{cases}$$

Substitution of equations (3.77) and (3.78) into equation (3.90), yields:

$$(\alpha_1 \frac{\partial T}{\partial \xi} + \alpha_2 \frac{\partial T}{\partial \eta})(-\sin \gamma_2) + (\alpha_3 \frac{\partial T}{\partial \xi} + \alpha_4 \frac{\partial T}{\partial \eta}) \cos \gamma_2 = 0 \quad (3.91)$$

Equation (3.22) presents the temperatures at the upper surface of the centre silo, it is written in transformed coordinates as:

$$\frac{\partial T}{\partial \eta} = 0 \quad (3.92)$$

when
$$\begin{cases} \xi = 0 \\ 0 \leq \phi \leq 2\pi \\ \eta = 1 \end{cases}$$

Equation (3.23) is expressed the temperature field at the bottom of the cone base of the silo, it can be written in transformed coordinates as:

$$\frac{\partial T}{\partial \eta} = 0 \quad (3.93)$$

when
$$\begin{cases} \xi = 0 \\ 0 \leq \phi \leq 2\pi \\ \eta = 0 \end{cases}$$

3.7 MOISTURE CONSERVATION EQUATION IN TRANSFORMED COORDINATES

3.7.1 Moisture contents at interior nodes in transformed coordinates

Equation (3.24) governs the moisture content field in the silo. In transformed coordinates it can be expressed as:

$$\begin{aligned} \frac{\partial W}{\partial t} = D_{eff} \frac{\rho_a}{\rho_b} & \left\{ \beta_1 \frac{\partial^2 H}{\partial \xi^2} + \beta_2 \frac{\partial^2 H}{\partial \eta^2} + \beta_3 \frac{\partial^2 H}{\partial \xi \partial \eta} + \beta_6 \frac{\partial H}{\partial \xi} + \beta_7 \frac{\partial H}{\partial \eta} + \beta_8 \frac{\partial^2 H}{\partial \phi^2} \right\} \\ & - \frac{\rho_a}{\rho_b} \left\{ V_r \left(\alpha_1 \frac{\partial H}{\partial \xi} + \alpha_2 \frac{\partial H}{\partial \eta} \right) + \frac{V_\phi}{R\xi} \frac{\partial H}{\partial \phi} + V_z \left(\alpha_3 \frac{\partial H}{\partial \xi} + \alpha_4 \frac{\partial H}{\partial \eta} \right) \right\} \\ & + \frac{dm}{dt} (0.6 + W) \end{aligned} \quad (3.94)$$

3.7.2 Absolute humidities at boundary nodes in transformed coordinates

Along the floor of the silo, equation (3.26) expresses the absolute humidities of the air in the grain silo. Because in the transformed horizontal floor along ϕ direction is constant, so in transformed coordinates we will have:

$$\frac{\partial H}{\partial \xi} \frac{\partial \xi}{\partial n} + \frac{\partial H}{\partial \eta} \frac{\partial \eta}{\partial n} = 0 \quad (3.95)$$

when

$$\begin{cases} 0 \leq \xi \leq 1 \\ 0 \leq \phi < \phi_{duct \min} \\ \phi_{duct \max} < \phi < 2\pi \\ \eta = 0 \end{cases}$$

Substituting the transformed coordinates equations (3.55), (3.56), (3.77) and (3.78) into equation (3.95), results in:

$$\left(\alpha_1 \frac{\partial H}{\partial \xi} + \alpha_2 \frac{\partial H}{\partial \eta} \right) (-\sin \gamma_1) + \left(\alpha_3 \frac{\partial H}{\partial \xi} + \alpha_4 \frac{\partial H}{\partial \eta} \right) \cos \gamma_1 = 0 \quad (3.96)$$

Equation (3.27) governs the absolute humidities of the air in the silo along the wall. Substituting the transformed coordinates equation (3.55) into equation (3.27), we get:

$$\frac{\partial H}{\partial r} = \alpha_1 \frac{\partial H}{\partial \xi} + \alpha_2 \frac{\partial H}{\partial \eta} = 0 \quad (3.97)$$

when

$$\begin{cases} \xi = 1 \\ 0 \leq \phi \leq 2\pi \\ R \tan \gamma_1 \leq \eta \leq H_{wall} + R \tan \gamma_1 \end{cases}$$

Equation (3.28) governs the absolute humidities of the air along the upper surface of the grain. In the transformed coordinates it is:

$$\frac{\partial H}{\partial \eta} = 0 \quad (3.98)$$

when

$$\begin{cases} 0 \leq \xi \leq 1 \\ 0 \leq \phi \leq 2\pi \\ \eta = 1 \end{cases}$$

Equation (3.29) expresses the absolute humidities of the air at the aeration duct, it can be written in transformed coordinates as:

$$H = H_{duct} \quad (3.99)$$

when

$$\begin{cases} \xi_{duct \min} \leq \xi \leq \xi_{duct \max} \\ \phi_{duct \min} \leq \phi \leq \phi_{duct \max} \\ \eta = 0 \end{cases}$$

Equation (3.30) shows the formula of the absolute humidities of the air at the bottomed cone base of the silo, it has been given in the transformed coordinates as:

$$\frac{\partial H}{\partial \eta} = 0 \quad (3.100)$$

when

$$\begin{cases} \xi = 0 \\ 0 \leq \phi \leq 2\pi \\ \eta = 0 \end{cases}$$

Equation (3.31) governs the absolute humidities of the air at the peak of the grain, in the transformed coordinates it can be written as:

$$\frac{\partial H}{\partial \eta} = 0$$

(3.101)

when

$$\begin{cases} \xi = 0 \\ 0 \leq \phi \leq 2\pi \\ \eta = 1 \end{cases}$$

CHAPTER 4

NUMERICAL METHOD

The goals of this chapter are to complete the description of the numerical solution of finite difference method for solving the partial differential equations in transformed coordinates, which will include: Alternating Direction Implicit method, explicit method for heat and mass transfer equations and Thomas algorithm.

4.1 FINITE DIFFERENCE SCHEME

Numerical approximation methods that employ the finite difference methods have more advantageous than the others for solving partial differential equations. This is because, the finite difference equations are obtained by using the local expansions for the variables, the derivatives at a point are approximated by difference quotients over a small grid mesh. The solution produce is relatively simple, straightforward and flexible. When the results of solutions can be satisfactorily calculated from the analytical formulas, the accuracy of the approximate solution can usually also be improved by increasing the number of mesh points and iteration time step in the approximations.

In this thesis, the finite difference method will be used for deriving the approximate computational solutions in an aerated conical bottomed circular silo.

4.2 APPROXIMATION GRID MESH

The basic objective of the finite difference method is to represent the time-space continuum by a set of discretely spaced points. A separate algebraic approximation of the partial differential equation is derived for every one of these points. The solution of the partial differential equation is found by solving these algebraic equations. Therefore, the network of grid mesh throughout the region of interest is first required to be established. A meshed section of the three dimensional cylindrical domain is shown in figure 4.1. In the ξ direction, the row spacings are non-uniform, and the mesh spacing $h\xi(i)$ is the distance between $(i-1)th$ point to ith point along the ξ axis. In the η direction, the columns are uniform, the mesh spacing $h\eta(k)$ is the distance between $(k-1)th$ point to kth point and respectively in η axis. In the ϕ direction, the mesh spacing $h\phi(j)$ is equal divided.

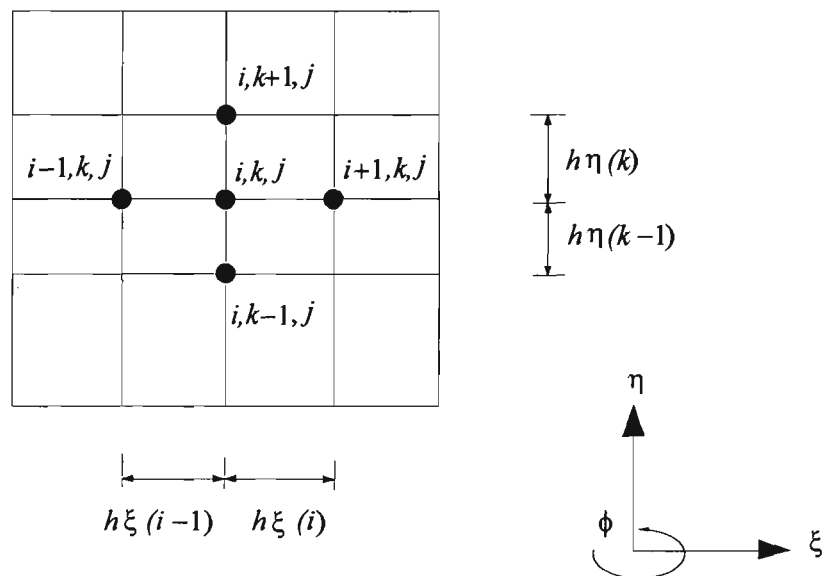


Figure 4.1 Three points grid mesh in three dimensional space.

In order to get the exact solution of the finite difference equation which is near to the true solution of the governing partial differential equation, it is important to set up the

grid mesh spacing for increasing the accuracy of the solution. The respective mesh spacings $h_{\xi}(i)$, $h_{\eta}(k)$ and $h_{\phi}(j)$ are defined by the following equations:

When $1 \leq i \leq 0.7n_{\xi}$

$$h_{\xi}(i) = \frac{1 - 0.15/R}{n_{\xi} - 7} \quad (4.1)$$

When $i = 0.75n_{\xi}$

$$h_{\xi}(i) = \frac{0.05}{R} \quad (4.2)$$

When $0.8n_{\xi} \leq i \leq n_{\xi}$

$$h_{\xi}(i) = \frac{0.02}{R} \quad (4.3)$$

and

$$h_{\eta}(k) = \frac{1}{n_{\eta} - 1} \quad (4.4)$$

$$h_{\phi}(j) = \frac{2\pi}{n_{\phi}} \quad (4.5)$$

where n_{ξ} , n_{η} and n_{ϕ} are the maximum node points in the three components directions (ξ, ϕ, η) . R is the radius of the grain silo as indicated in Chapter 3.

In the above, we obtain the fine mesh close to the wall of the silo where there are significant diurnal variations, and the wide mesh in the centre.

4.3 FINITE DIFFERENCE OPERATORS: INTERIOR NODES

The three point finite difference operators $c_{\xi 1}(i)$, $c_{\xi 2}(i)$, $c_{\xi 3}(i)$, $c_{\xi 4}(i)$, $c_{\xi 5}(i)$, $c_{\xi 6}(i)$, $c_{\eta 1}(k)$, $c_{\eta 2}(k)$, $c_{\eta 3}(k)$, $c_{\eta 4}(k)$, $c_{\eta 5}(k)$, $c_{\eta 6}(k)$, $c_{\phi 4}(j)$, $c_{\phi 5}(j)$ and $c_{\phi 6}(j)$ can be achieved by applying Taylor's series expansion for the arbitrary scalar forward to $\Gamma_{i+1,j,k}$ and backward to $\Gamma_{i-1,j,k}$ about the central value $\Gamma_{i,j,k}$, to describe the first and second partial derivatives. These are presented a couple information at the neighbouring points of a grid as following:

Taylor's expansion about the (i, j, k) th node in the direction of ξ is:

$$\Gamma_{i+1,j,k} = \Gamma_{i,j,k} + h\xi(i) \frac{\partial \Gamma}{\partial \xi} + \frac{h\xi(i)^2}{2!} \frac{\partial^2 \Gamma}{\partial \xi^2} + O(h\xi(i)^2) \quad (4.6)$$

$$\Gamma_{i-1,j,k} = \Gamma_{i,j,k} - h\xi(i-1) \frac{\partial \Gamma}{\partial \xi} + \frac{h\xi(i-1)^2}{2!} \frac{\partial^2 \Gamma}{\partial \xi^2} + O(h\xi(i-1)^2) \quad (4.7)$$

Omitting terms of order $O(h\xi(i)^2)$, $O(h\xi(i-1)^2)$ and higher, eliminating the second-order derivative $\frac{h\xi(i)^2}{2!} \frac{\partial^2 \Gamma}{\partial \xi^2}$ and $\frac{h\xi(i-1)^2}{2!} \frac{\partial^2 \Gamma}{\partial \xi^2}$ by means of equation (4.7) multiplies term $h\xi(i)^2$, and equation (4.6) multiplies term $h\xi(i-1)^2$, then subtracting equation (4.6) from equation (4.7). Therefore the first partial derivative is obtained as:

$$\begin{aligned} \frac{\partial \Gamma}{\partial \xi} = & \frac{-h\xi(i)}{h\xi(i-1)(h\xi(i-1) + h\xi(i))} \Gamma_{i-1,j,k} + \frac{h\xi(i) - h\xi(i-1)}{h\xi(i-1)h\xi(i)} \Gamma_{i,j,k} + \\ & \frac{h\xi(i-1)}{h\xi(i)(h\xi(i-1) + h\xi(i))} \Gamma_{i+1,j,k} \end{aligned} \quad (4.8)$$

we define

$$c_{\xi 1}(i) = \frac{-h\xi(i)}{h\xi(i-1)(h\xi(i-1) + h\xi(i))} \quad (4.9)$$

$$c_{\xi 2}(i) = \frac{h\xi(i) - h\xi(i-1)}{h\xi(i-1)h\xi(i)} \quad (4.10)$$

$$c_{\xi 3}(i) = \frac{h\xi(i-1)}{h\xi(i)(h\xi(i-1) + h\xi(i))} \quad (4.11)$$

So the simplified equation (4.8) becomes:

$$\frac{\partial \Gamma}{\partial \xi} = c_{\xi 1}(i) \Gamma_{i-1,j,k} + c_{\xi 2}(i) \Gamma_{i,j,k} + c_{\xi 3}(i) \Gamma_{i+1,j,k} \quad (4.12)$$

In an analogous manner, the second partial derivative is:

$$\frac{\partial^2 \Gamma}{\partial \xi^2} = c_{\xi 4}(i) \Gamma_{i-1,j,k} + c_{\xi 5}(i) \Gamma_{i,j,k} + c_{\xi 6}(i) \Gamma_{i+1,j,k} \quad (4.13)$$

where

$$c_{\xi 4}(i) = \frac{2}{h\xi(i-1)(h\xi(i) + h\xi(i-1))} \quad (4.14)$$

$$c\xi 5(i) = \frac{-2}{h\xi(i-1)h\xi(i)} \quad (4.15)$$

$$c\xi 6(i) = \frac{2}{h\xi(i)(h\xi(i) + h\xi(i-1))} \quad (4.16)$$

Similarly, in the η direction we have:

$$\frac{\partial \Gamma}{\partial \eta} = c\eta 1(k)\Gamma_{i,j,k-1} + c\eta 2(k)\Gamma_{i,j,k} + c\eta 3(k)\Gamma_{i,j,k+1} \quad (4.17)$$

where

$$c\eta 1(k) = \frac{-h\eta(k)}{h\eta(k-1)(h\eta(k-1) + h\eta(k))} \quad (4.18)$$

$$c\eta 2(k) = \frac{h\eta(k) - h\eta(k-1)}{h\eta(k-1)h\eta(k)} \quad (4.19)$$

$$c\eta 3(k) = \frac{h\eta(k-1)}{h\eta(k)(h\eta(k-1) + h\eta(k))} \quad (4.20)$$

and

$$\frac{\partial^2 \Gamma}{\partial \eta^2} = c\eta 4(k)\Gamma_{i,j,k-1} + c\eta 5(k)\Gamma_{i,j,k} + c\eta 6(k)\Gamma_{i,j,k+1} \quad (4.21)$$

where

$$c\eta 4(k) = \frac{2}{h\eta(k-1)(h\eta(k) + h\eta(k-1))} \quad (4.22)$$

$$c\eta 5(k) = \frac{-2}{h\eta(k-1)h\eta(k)} \quad (4.23)$$

$$c\eta 6(k) = \frac{2}{h\eta(k)(h\eta(k) + h\eta(i-1))} \quad (4.24)$$

Again in the ϕ direction, we define the first partial derivative :

$$\frac{\partial \Gamma}{\partial \phi} = c\phi 1(j)\Gamma_{i,j,k-1} + c\phi 2(j)\Gamma_{i,j,k} + c\phi 3(j)\Gamma_{i,j,k+1} \quad (4.25)$$

where

$$c\phi 1(j) = -\frac{1}{2\phi} \quad (4.26)$$

$$c\phi 2(j) = 0 \quad (4.27)$$

$$c\phi 3(j) = \frac{1}{2\phi} \quad (4.28)$$

and the second partial derivative is:

$$\frac{\partial^2 \Gamma}{\partial \phi^2} = c\phi 4(j)\Gamma_{i,j-1,k} + c\phi 5(j)\Gamma_{i,j,k} + c\phi 6(j)\Gamma_{i,j+1,k} \quad (4.29)$$

where

$$c\phi 4(j) = \frac{1}{\Delta \phi^2} \quad (4.30)$$

$$c\phi 5(j) = \frac{-2}{\Delta \phi^2} \quad (4.31)$$

$$c\phi 6(j) = \frac{1}{\Delta \phi^2} \quad (4.32)$$

Moreover, the finite difference approximation of the mixed derivative $\frac{\partial^2 \Gamma}{\partial \xi \partial \eta}$ is also derived by applying Taylor's expansion. We have obtained the differential expression as following:

$$\begin{aligned} \frac{\partial^2 \Gamma}{\partial \xi \partial \eta} = & c\eta 1(k)(c\xi 1(i)\Gamma_{i-1,j,k-1} + c\xi 2(i)\Gamma_{i,j,k-1} + c\xi 3(i)\Gamma_{i+1,j,k-1}) + \\ & c\eta 2(k)(c\xi 1(i)\Gamma_{i-1,j,k} + c\xi 2(i)\Gamma_{i,j,k} + c\xi 3(i)\Gamma_{i+1,j,k}) + c\eta 3(k) \\ & (c\xi 1(i)\Gamma_{i-1,j,k+1} + c\xi 2(i)\Gamma_{i,j,k+1} + c\xi 3(i)\Gamma_{i+1,j,k+1}) \end{aligned} \quad (4.33)$$

4.4 FINITE DIFFERENCE OPERATORS: BOUNDARY NODES

In the boundary conditions, the three point finite difference operators are also derived by applying Taylor's expansion. Figure 4.2 shows the boundary nodes at the ξ direction of the silo boundaries, such as:

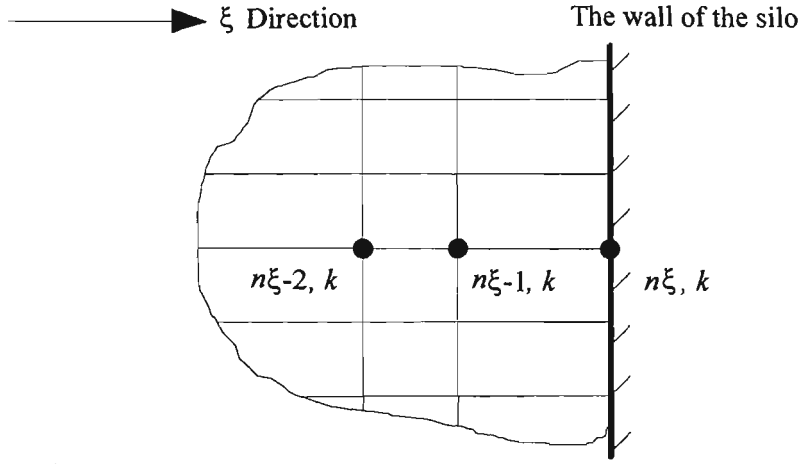


Figure 4.2 The boundary nodes in the ξ direction of the silo.

we have:

$$\frac{\partial \Gamma}{\partial \xi} = c_{\xi} b_4 \Gamma_{n_{\xi}, j, k} + c_{\xi} b_5 \Gamma_{n_{\xi}-1, j, k} + c_{\xi} b_6 \Gamma_{n_{\xi}-2, j, k} \quad (4.34)$$

where

$$c_{\xi} b_4 = \frac{2h_{\xi}(n_{\xi}-1) + h_{\xi}(n_{\xi}-2)}{h_{\xi}(n_{\xi}-1)(h_{\xi}(n_{\xi}-1) + h_{\xi}(n_{\xi}-2))} \quad (4.35)$$

$$c_{\xi} b_5 = \frac{-(h_{\xi}(n_{\xi}-1) + h_{\xi}(n_{\xi}-2))}{h_{\xi}(n_{\xi}-1)h_{\xi}(n_{\xi}-2)} \quad (4.36)$$

$$c_{\xi} b_6 = \frac{h_{\xi}(n_{\xi}-1)}{h_{\xi}(n_{\xi}-2)(h_{\xi}(n_{\xi}-1) + h_{\xi}(n_{\xi}-2))} \quad (4.37)$$

In the η direction at the bottom of the cylinder, the boundary condition is depicted in figure 4.3 as:

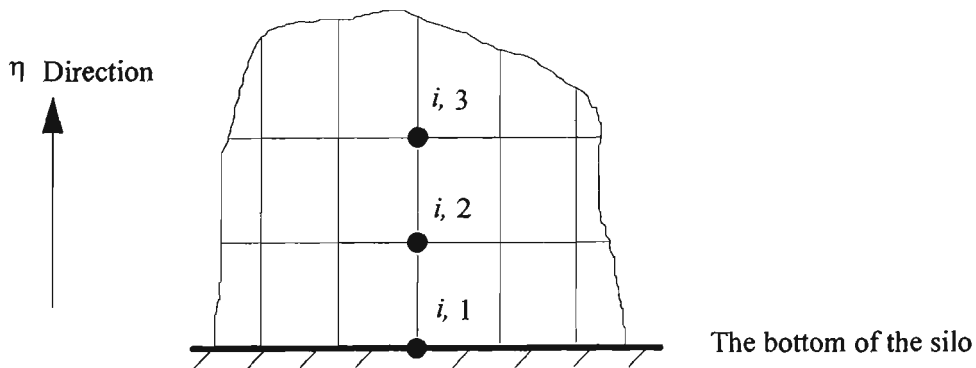


Figure 4.3 The boundary nodes in the η direction of the bottom of the silo

we obtain:

$$\frac{\partial \Gamma}{\partial \eta} = c\eta b1\Gamma_{i,j,1} + c\eta b2\Gamma_{i,j,2} + c\eta b3\Gamma_{i,j,3} \quad (4.38)$$

where

$$c\eta b1 = \frac{-2h\eta(1) + h\eta(2)}{h\eta(1)(h\eta(1) + h\eta(2))} \quad (4.39)$$

$$c\eta b2 = \frac{h\eta(1) + h\eta(2)}{h\eta(1)h\eta(2)} \quad (4.40)$$

$$c\eta b3 = \frac{-h\eta(1)}{h\eta(2)(h\eta(1) + h\eta(2))} \quad (4.41)$$

In the η direction at the upper surface of the grains, the boundary condition as shown in figure 4.4:

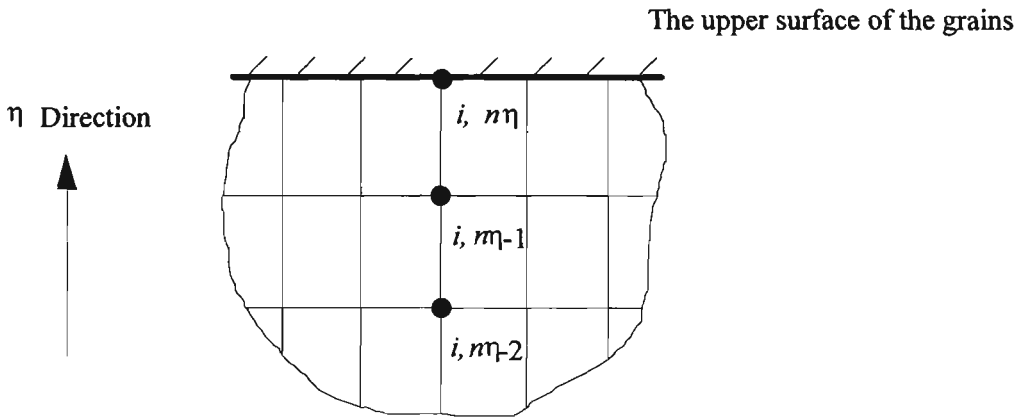


Figure 4.4 The boundary nodes in the η direction of the upper surface of the grains

we get:

$$\frac{\partial \Gamma}{\partial \eta} = c\eta b4\Gamma_{i,j,n\eta} + c\eta b5\Gamma_{i,j,n\eta-1} + c\eta b6\Gamma_{i,j,n\eta-2} \quad (4.42)$$

where

$$c\eta b4 = \frac{2h\eta(n\eta-1) + h\eta(n\eta-2)}{h\eta(n\eta-1)(h\eta(n\eta-1) + h\eta(n\eta-2))} \quad (4.43)$$

$$c\eta b5 = \frac{-(h\eta(n\eta-1) + h\eta(n\eta-2))}{h\eta(n\eta-1)h\eta(n\eta-2)} \quad (4.44)$$

$$c\eta b6 = \frac{h\eta(n\eta - 1)}{h\eta(n\eta - 2)(h\eta(n\eta - 1) + h\eta(n\eta - 2))} \quad (4.45)$$

4.5 ANDREYEV - SAMARSKII ALGORITHM

In the numerical solution procedure, the finite difference equation governing the pressure distribution is discretised by replacing spatial derivatives and applying the three point finite difference scheme in a non-uniform grid mesh. In order to better derive the appropriate difference equation, to eliminate some of the difficulties and to associate with solving the equation directly, a simplified method - the Alternating Direction Implicit method is developed as proposed by Peaceman and Rachford (1955) and modified by Samarskii and Andreyev (1963). In this study, the governing equation of pressure distribution in transformed coordinates will be solved by this method. In the Andreyev-Samarskii algorithm, a new variable ω is defined, thus:

$$\omega = \frac{1}{\alpha_p} \frac{\partial P}{\partial t} = \frac{P^{n+1} - P^n}{\alpha_p \Delta t} \quad (4.46)$$

where P^{n+1} is the pressure value at the $(i, j, k)th$ node after $(n+1)th$ iteration. During the iteration time step Δt is within the integration interval, and the intermediate value of the pressure P is given by:

$$P = \alpha_p \cdot \delta \cdot \omega \cdot \Delta t + P^n \quad (4.47)$$

where δ is a weighting factor which value is between 0 and 1. If $\delta = 0$, the scheme is fully explicit. If $\delta = 1$, the scheme is fully implicit. If $\delta = 0.5$, the scheme yields Crank-Nicholson method (1947), it is splitting the solution of equation (4.47) into a series of locally one dimensional problems.

4.5.1 Solution of the pressures at interior nodes

In order to solve Laplace equation, as equation (3.71) in transformed coordinates by using Andreyev-Samarskii (1963) method, the solution process is obtained by substitution equation (4.47) into the right hand side of equation (3.71), and equation (4.46) is replaced at the left hand side of equation (3.71). The new rearrangement of the expression is written as follows:

$$\begin{aligned} \omega - \alpha_p \delta \Delta t (\beta_1 \frac{\partial^2 \omega}{\partial \xi^2} + \beta_2 \frac{\partial^2 \omega}{\partial \eta^2} + \beta_3 \frac{\partial^2 \omega}{\partial \xi \partial \eta} + \beta_6 \frac{\partial \omega}{\partial \xi} + \beta_7 \frac{\partial \omega}{\partial \eta} + \frac{1}{R^2 \xi^2} \frac{\partial^2 \omega}{\partial \phi^2}) \\ = \beta_1 \frac{\partial^2 P}{\partial \xi^2} + \beta_2 \frac{\partial^2 P}{\partial \eta^2} + \beta_3 \frac{\partial^2 P}{\partial \xi \partial \eta} + \beta_6 \frac{\partial P}{\partial \xi} + \beta_7 \frac{\partial P}{\partial \eta} + \frac{1}{R^2 \xi^2} \frac{\partial^2 P}{\partial \phi^2} \end{aligned} \quad (4.48)$$

In equation (4.48), the right hand side of the pressures have been omitted, and the mixed derivative is treated explicitly.

Firstly, the ω^* is solved by applying implicit equation (4.48) in the ξ direction, thus:

$$\omega^* - \alpha_p \cdot \delta \cdot \Delta t (\beta_1 \frac{\partial^2 \omega^*}{\partial \xi^2} + \beta_6 \frac{\partial \omega^*}{\partial \xi}) = RHS1 \quad (4.49)$$

where

$$RHS1 = \beta_1 \frac{\partial^2 P}{\partial \xi^2} + \beta_2 \frac{\partial^2 P}{\partial \eta^2} + \beta_3 \frac{\partial^2 P}{\partial \xi \partial \eta} + \beta_6 \frac{\partial P}{\partial \xi} + \beta_7 \frac{\partial P}{\partial \eta} + \beta_8 \frac{\partial^2 P}{\partial \phi^2} \quad (4.50)$$

and

$$\beta_8 = \frac{1}{R^2 \xi^2} \quad (4.51)$$

The first and second order partial derivatives are represented by the three point backward and forward difference scheme with the finite difference operators, so substituting equations (4.12), (4.13), (4.17), (4.21) and (4.29) into equation (4.49). The discretization of the linear algebraic equation is became as ($1 < i < n\xi$):

$$\begin{aligned} \omega_{i,j,k}^* - \alpha_p \cdot \delta \cdot \Delta t (\beta_1 (c\xi 4(i) \omega_{i-1,j,k}^* + c\xi 5(i) \omega_{i,j,k}^* + c\xi 6(i) \omega_{i+1,j,k}^*) + \\ (\beta_6 (c\xi 1(i) \omega_{i-1,j,k}^* + c\xi 2(i) \omega_{i,j,k}^* + c\xi 3(i) \omega_{i+1,j,k}^*)) = RHS2 \end{aligned} \quad (4.52)$$

in which

$$RHS2 = \beta_1 (c\xi 4(i) P_{i-1,j,k} + c\xi 5(i) P_{i,j,k} + c\xi 6(i) P_{i+1,j,k}) + \beta_2 (c\eta 4(k) P_{i,j,k-1} +$$

$$\begin{aligned}
& c\eta 5(k)P_{i,j,k} + c\eta 6(k)P_{i,j,k+1} + \beta_3(c\eta 1(k)(c\xi 1(i)P_{i-1,j,k-1} + \\
& c\xi 2(i)P_{i,j,k-1} + c\xi 3(i)P_{i+1,j,k-1}) + c\eta 2(k)(c\xi 1(i)P_{i-1,j,k} + c\xi 2(i)P_{i,j,k} + \\
& c\xi 3(i)P_{i+1,j,k}) + c\eta 3(k)(c\xi 1(i)P_{i-1,j,k+1} + c\xi 2(i)P_{i,j,k+1} + \\
& c\xi 3(i)P_{i+1,j,k+1}) + \beta_6(c\xi 1(i)P_{i-1,j,k} + c\xi 2(i)P_{i,j,k} + c\xi 3(i)P_{i+1,j,k}) + \\
& \beta_7(c\eta 1(k)P_{i,j,k-1} + c\eta 2(k)P_{i,j,k} + c\eta 3(k)P_{i,j,k+1}) + \\
& \beta_8(c\phi 4(j)P_{i,j-1,k} + c\phi 5(j)P_{i,j,k} + c\phi 6(j)P_{i,j+1,k})
\end{aligned} \tag{4.53}$$

we define again

$$\begin{aligned}
a_{ii} &= -\Delta t \cdot \alpha_p \cdot \delta(c\xi 1(i)\beta_6 + c\xi 4(i)\beta_1) \\
&= -atd(c\xi 1(i)\beta_6 + c\xi 4(i)\beta_1)
\end{aligned} \tag{4.54}$$

where

$$atd = \alpha_p \cdot \delta \cdot \Delta t \tag{4.55}$$

$$b_{ii} = 1 - atd(c\xi 2(i)\beta_6 + c\xi 5(i)\beta_1) \tag{4.56}$$

$$c_{ii} = -atd(c\xi 3(i)\beta_6 + c\xi 6(i)\beta_1) \tag{4.57}$$

$$d_{ii} = RHS2 \tag{4.58}$$

in which

$$ii = i - 1, ii = 1, 2, \dots, n\xi - 2, i = 2, 3, \dots, n\xi - 1.$$

The simplified expression of equation (4.52) is written as:

$$a_{ii}\omega_{i-1,j,k}^* + b_{ii}\omega_{i,j,k}^* + c_{ii}\omega_{i+1,j,k}^* = d_{ii} \tag{4.59}$$

From equation (4.59), a set of simultaneous linear equations may be represented algebraically by:

$$b_1\omega_{2,j,k}^* + c_1\omega_{3,j,k}^* = d_1 - a_1\omega_{1,j,k}^*$$

$$a_2\omega_{2,j,k}^* + b_2\omega_{3,j,k}^* + c_2\omega_{4,j,k}^* = d_2$$

$$a_3\omega_{3,j,k}^* + b_3\omega_{4,j,k}^* + c_3\omega_{5,j,k}^* = d_3$$

.....

$$a_{n\xi-3}\omega_{n\xi-3,j,k}^* + b_{n\xi-3}\omega_{n\xi-2,j,k}^* + c_{n\xi-3}\omega_{n\xi-1,j,k}^* = d_{n\xi-3}$$

$$a_{n\xi-2}\omega_{n\xi-2,j,k}^* + b_{n\xi-2}\omega_{n\xi-1,j,k}^* = d_{n\xi-2} - c_{n\xi-2}\omega_{n\xi,j,k}^* \tag{4.60}$$

where

$$\text{if } ii = 1 \quad d_1 = d_1 - a_1\omega_{1,j,k}^* ; \tag{4.61}$$

$$\text{if } ii = n\xi - 2 \quad d_{n\xi-2} = d_{n\xi-2} - c_{n\xi-2}\omega_{n\xi,j,k}^* \tag{4.62}$$

The coefficients a, b, c, d of the linear system can be expressed as a tri-diagonal matrix and solved by means of the Thomas (1949) algorithm which is a special case of the Gaussian Elimination method (see Appendix I).

The second step for solving ω^{**} is implicit equation (4.48) in the ϕ direction, thus:

$$\omega^{**} - atd \cdot \beta_8 \frac{\partial^2 \omega}{\partial \phi^2} = \omega^* \quad (4.63)$$

Replacing the second partial derivative in equation (4.63), with the finite difference operators and three point difference scheme, we obtain ($1 < j < n\phi$):

$$\omega^{**} - atd \cdot \beta_8 (c\phi 4(j)\omega_{i,j-1,k}^{**} + c\phi 5(j)\omega_{i,j,k}^{**} + c\phi 6(j)\omega_{i,j+1,k}^{**}) = \omega^* \quad (4.64)$$

we define again

$$a_{jj} = -atd \cdot \beta_8 \cdot c\phi 4(j) \quad (4.65)$$

$$b_{jj} = 1 - atd \cdot \beta_8 \cdot c\phi 5(j) \quad (4.66)$$

$$c_{jj} = -atd \cdot \beta_8 \cdot c\phi 6(j) \quad (4.67)$$

$$d_{jj} = \omega^* \quad (4.68)$$

where

$$jj = j - 1,$$

$$jj = 1, 2 \dots n\phi - 2, \text{ and } j = 2, 3 \dots n\phi - 1.$$

we get:

$$a_{jj}\omega_{i,j-1,k}^{**} + b_{jj}\omega_{i,j,k}^{**} + c_{jj}\omega_{i,j+1,k}^{**} = d_{jj} \quad (4.69)$$

This tri-diagonal matrix can be again solved by the Thomas (1949) algorithm.

The third step for solving ω^{***} is implicit equation (4.48) in the η direction, we will obtain:

$$\omega^{***} - atd(\beta_2 \frac{\partial^2 \omega}{\partial \eta^2} + \beta_7 \frac{\partial \omega}{\partial \eta}) = \omega^{**} \quad (4.70)$$

Replacing the first and second order partial derivatives in equation (4.70), with the finite difference operators and three point difference scheme, we get ($1 < k < m\eta$):

$$\omega^{***} - atd(\beta_2(c\eta 4(k)\omega_{i,j,k-1}^{***} + c\eta 5(k)\omega_{i,j,k}^{***} + c\eta 6(k)\omega_{i,j,k+1}^{***}) + \beta_7(c\eta 1(k)\omega_{i,j,k-1}^{***} + c\eta 2(k)\omega_{i,j,k}^{***} + c\eta 3(k)\omega_{i,j,k+1}^{***})) \quad (4.71)$$

let

$$a_{kk} = -atd(\beta_2 \cdot c\eta 4(k) + \beta_7 \cdot c\eta 1(k)) \quad (4.72)$$

$$b_{kk} = 1 - atd(\beta_2 \cdot c\eta 5(k) + \beta_7 \cdot c\eta 2(k)) \quad (4.73)$$

$$c_{kk} = -atd(\beta_2 \cdot c\eta 6(k) + \beta_7 \cdot c\eta 3(k)) \quad (4.74)$$

$$d_{kk} = \omega^{**} \quad (4.75)$$

where $kk = k - 1$, $kk = 1, 2, \dots, n\eta - 2$, and $k = 2, 3, \dots, n\eta - 1$. Therefore we have the tri-diagonal matrix:

$$a_{kk}\omega_{i,j,k-1}^{***} + b_{kk}\omega_{i,j,k}^{***} + c_{kk}\omega_{i,j,k+1}^{***} = d_{kk} \quad (4.76)$$

By applying the Thomas (1949) algorithm, the final intermediate values of ω^{***} are obtained, then the updated final values of the pressures P_{new} are determined from the following expression:

$$P_{new} = P + atd \cdot \omega^{***} \quad (4.77)$$

4.5.2 Solution of the pressures at boundaries

Equation (3.75) governs the pressure field at the vertical wall of the silo and it is expressed in the transformed coordinates. Substituting equations (4.34) and (4.17) into equation (3.75) for $\frac{\partial P}{\partial \xi}$ and $\frac{\partial P}{\partial \eta}$, the discretised form of equation (3.75) can be written as

below:

$$\alpha_1(c\xi b4 P_{n\xi,j,k} + c\xi b5 P_{n\xi-1,j,k} + c\xi b6 P_{n\xi-2,j,k}) + \alpha_2(c\eta 1(k) P_{n\xi,j,k-1} + c\eta 2(k) P_{n\xi,j,k} + c\eta 3(k) P_{n\xi,j,k+1}) = 0 \quad (4.78)$$

we define

$$a_{kk} = \alpha_2 c\eta 1(k) \quad (4.79)$$

$$b_{kk} = \alpha_2 c\eta 2(k) + \alpha_1 c\xi b4 \quad (4.80)$$

$$c_{kk} = \alpha_2 c \eta 3(k) \quad (4.81)$$

$$d_{kk} = -\alpha_1 c \xi b 5 P_{n\xi-1,j,k} - \alpha_1 c \xi b 6 P_{n\xi-2,j,k} \quad (4.82)$$

where

$$\text{If } kk = 1, \quad d_{kk} = d_{kk} - c_{kk} P_{n\xi,j,1} \quad (4.83)$$

$$\text{If } kk = n\xi - 2, \quad d_{kk} = d_{kk} - c_{kk} P_{n\xi,j,n\xi} \quad (4.84)$$

So equation (4.78) becomes:

$$a_{kk} P_{n\xi,j,k-1} + b_{kk} P_{n\xi,j,k} + c_{kk} P_{n\xi,j,k+1} = d_{kk} \quad (4.85)$$

Equation (3.76) governs the pressure field along the sloping floor of the grain silo and it is expressed in transformed coordinates. The discretised equation is formed by employing the three point finite difference scheme, the first partial derivatives $\frac{\partial P}{\partial \xi}$ and $\frac{\partial P}{\partial \eta}$ are given by equations (4.12) and (4.38), so we will obtain ($\alpha_3 = 0$ and $0 < i < n\xi - 1$):

$$\begin{aligned} & -\sin \gamma_1 (\alpha_1 (c \xi 1(i) P_{i-1,j,1} + c \xi 2(i) P_{i,j,1} + c \xi 3(i) P_{i+1,j,1})) \\ & + \alpha_2 (c \eta b 1 P_{i,j,1} + c \eta b 2 P_{i,j,2} + c \eta b 3 P_{i,j,3})) + \cos \gamma_1 (\alpha_4 (\\ & c \eta b 1 P_{i,j,1} + c \eta b 2 P_{i,j,2} + c \eta b 3 P_{i,j,3})) \end{aligned} \quad (4.86)$$

we define

$$a_{ii} = -\alpha_1 \sin \gamma_1 c \xi 1(i) \quad (4.87)$$

$$b_{ii} = -\sin \gamma_1 \alpha_1 c \xi 2(i) - \sin \gamma_1 \alpha_2 c \eta b 1 + \cos \gamma_1 \alpha_4 c \eta b 1 \quad (4.88)$$

$$c_{ii} = -\sin \gamma_1 \alpha_1 c \xi 3(i) \quad (4.89)$$

$$\begin{aligned} d_{ii} = & (\sin \gamma_1 \alpha_2 - \cos \gamma_1 \alpha_4) c \eta b 2 P_{i,j,2} + \\ & (\sin \gamma_1 \alpha_2 - \cos \gamma_1 \alpha_4) c \eta b 3 P_{i,j,3} \end{aligned} \quad (4.90)$$

where

$$\text{if } ii = 1, \quad d_{ii} = d_{ii} - c_{ii} P_{1,1,1} \quad (4.91)$$

$$\text{if } ii = n\xi - 2, \quad d_{ii} = d_{ii} - c_{ii} P_{n\xi,j,1} \quad (4.92)$$

Equation (4.86) may be written as:

$$a_{ii}P_{i-1,j,1} + b_{ii}P_{i,j,1} + c_{ii}P_{i+1,j,1} = d_{ii} \quad (4.93)$$

Equation (3.81) expresses the pressure field at the bottomed conical base of the silo in transformed coordinates. Using the three point finite difference scheme to replace equation (4.38) into equation (3.81), we get:

$$\frac{\partial P}{\partial \eta} = c\eta b1 P_{1,j,1} + c\eta b2 P_{1,j,2} + c\eta b3 P_{1,j,3} = 0 \quad (4.94)$$

so we will have:

$$P_{1,j,1} = \frac{c\eta b2 \cdot P_{1,j,2} + c\eta b3 \cdot P_{1,j,3}}{c\eta b1} \quad (4.95)$$

At the intersection of the vertical wall and the conical bottom of the silo, the pressure field is calculated by means of linear interpolation, and the expressed form takes as:

$$P_{coner} = P_{n\xi,j,1} = P_{n\xi-1,j,1} + \frac{h\xi(n\xi-1)}{h\xi(n\xi-1) + h\eta(1)} (P_{n\xi,j,2} - P_{n\xi-1,j,1}) \quad (4.96)$$

we define

$$a_{ii} = \frac{h\xi(n\xi-1)}{h\xi(n\xi-1) + h\eta(1)} - 1 \quad (4.97)$$

$$b_{ii} = 1 \quad (4.98)$$

$$c_{ii} = -\frac{h\xi(n\xi-1)}{h\xi(n\xi-1) + h\eta(1)} \quad (4.99)$$

$$d_{ii} = 0 \quad (4.100)$$

Equation (4.96) becomes:

$$a_{ii}P_{n\xi-1,j,1} + b_{ii}P_{n\xi,j,1} + c_{ii}P_{n\xi,j,2} = 0 \quad (4.101)$$

So the set of equations which comprise equations (4.85), (4.93) and (4.101) are solved simultaneously to yield the pressure distribution along the floor and wall of the silo.

At the centre of the silo, the pressure field is obtained by averaging the sum of the values which occur at the second centre nodes, and the equation may be written as:

$$P_{1,j,k} = \frac{\text{sigma}P(k)}{n\phi} \quad (4.102)$$

where

$$\text{sigma}P(k) = \sum_{j=1}^{n\phi} P_{2,j,k} \quad (4.103)$$

4.5.3 Solution of the velocity components

According to Darcy's law, when the pressure field is given, the solution of the momentum equation can be obtained by employing equations (3.83), (3.84) and (3.85), which are governing the components of the velocity field in transformed coordinates. In these equations, the first partial derivatives can be replaced by using finite difference operators as equations (4.12), (4.17) and (4.29), so we have:

The components of the radial velocity is discretised in the transformed coordinate as:

$$\begin{aligned} V_{\xi} = & -\frac{1}{R_p} \{ \alpha_1 (c\xi 1(i) P_{i-1,j,k} + c\xi 2(i) P_{i,j,k} + c\xi 3(i) P_{i+1,j,k}) \\ & + \alpha_2 (c\eta 1(k) \Gamma_{i,j,k-1} + c\eta 2(k) \Gamma_{i,j,k} + c\eta 3(k) \Gamma_{i,j,k+1}) \} \end{aligned} \quad (4.104)$$

The components of the angular velocity is discretised in the transformed coordinate as:

$$V_{\theta} = -\frac{1}{R_p} \frac{1}{R_{\xi}} (c\phi 1(j) P_{i,j-1,k} + c\phi 2(j) P_{i,j,k} + c\phi 3(j) P_{i,j+1,k}) \quad (4.105)$$

The components of the vertical velocity is discretised in the transformed coordinate as:

$$\begin{aligned} V_{\eta} = & -\frac{1}{R_p} \{ \alpha_3 (c\xi 1(i) P_{i-1,j,k} + c\xi 2(i) P_{i,j,k} + c\xi 3(i) P_{i+1,j,k}) \\ & + \alpha_4 (c\eta 1(k) \Gamma_{i,j,k-1} + c\eta 2(k) \Gamma_{i,j,k} + c\eta 3(k) \Gamma_{i,j,k+1}) \} \end{aligned} \quad (4.106)$$

4.6 SOLUTION OF THE THERMAL ENERGY EQUATION

The transient thermal energy conservation equation is discretised by applying upwind finite difference scheme and solved by an explicit method. Equation (3.86) governing the temperature field in transformed coordinates is rearranged as following:

$$\begin{aligned} \frac{\partial T}{\partial t} = \frac{1}{denom} \{ & K_{eff} \left\{ \beta_1 \frac{\partial^2 T}{\partial \xi^2} + \beta_2 \frac{\partial^2 T}{\partial \eta^2} + \beta_3 \frac{\partial^2 T}{\partial \xi \partial \eta} + \beta_8 \frac{\partial^2 T}{\partial \phi^2} \right\} \\ & + \rho_b \frac{dm}{dt} (Q_r - 0.6h_{vap}) + \rho_b h_s \frac{\partial W}{\partial t} + \rho_b \frac{dm}{dt} \int_0^w h_s dw - \rho_a \{ c_a + w((c_1)_\gamma + c_{2v}) \} \\ & \times \left\{ V_{T\xi} \frac{\partial T}{\partial \xi} + V_{T\eta} \frac{\partial T}{\partial \eta} + V_{T\phi} \frac{\partial T}{\partial \phi} \right\} \} \end{aligned} \quad (4.107)$$

where

$$denom = \rho_b \left\{ (c_2)_\sigma + (c_1)_\sigma W + \frac{\partial H_w}{\partial T} \right\} + \epsilon_r \rho_a \{ c_a + w((c_1)_\gamma + (c_{2v})) \}$$

$$V_{T\xi} = V_r \alpha_1 + V_z \alpha_3 - \beta_6 \cdot K_{eff} \quad (4.108)$$

$$V_{T\eta} = V_r \alpha_2 + V_z \alpha_4 - \beta_7 \cdot K_{eff} \quad (4.109)$$

$$V_{T\phi} = \frac{V_\phi}{R\xi} \quad (4.110)$$

in which $V_{T\xi}$, $V_{T\eta}$ and $V_{T\phi}$ are effective velocities in the thermal energy balance.

Simplifying equation (4.107) again, we obtain:

$$\frac{\partial T}{\partial t} = \Pi_i + S_i - C_c (V_{T\xi} \frac{\partial T}{\partial \xi} + V_{T\eta} \frac{\partial T}{\partial \eta} + V_{T\phi} \frac{\partial T}{\partial \phi}) \quad (4.111)$$

where

$$\Pi_i = K_{eff} \left\{ \beta_1 \frac{\partial^2 T}{\partial \xi^2} + \beta_2 \frac{\partial^2 T}{\partial \eta^2} + \beta_3 \frac{\partial^2 T}{\partial \xi \partial \eta} + \beta_8 \frac{\partial^2 T}{\partial \phi^2} \right\} \cdot denom \quad (4.112)$$

$$S_i = (\rho_b \frac{dm}{dt} (Q_r - 0.6h_{vap}) + \rho_b h_s \frac{\partial W}{\partial t} + \rho_b \frac{dm}{dt} \int_0^w h_s dw) \cdot denom \quad (4.113)$$

$$C_c = \rho_a \{ c_a + w((c_1)_\gamma + c_{2v}) \} \cdot denom \quad (4.114)$$

4.6.1 Upwind finite difference operators

The upwind finite difference operators $a_{\xi 1u}$, $a_{\xi 2u}$, $a_{\xi 3u}$, $a_{\eta 1u}$, $a_{\eta 2u}$, $a_{\eta 3u}$, $a_{\phi 1u}$, $a_{\phi 2u}$ and $a_{\phi 3u}$ are obtained by employing the centre difference scheme, it is shown in figure 4.5 for the ξ direction:

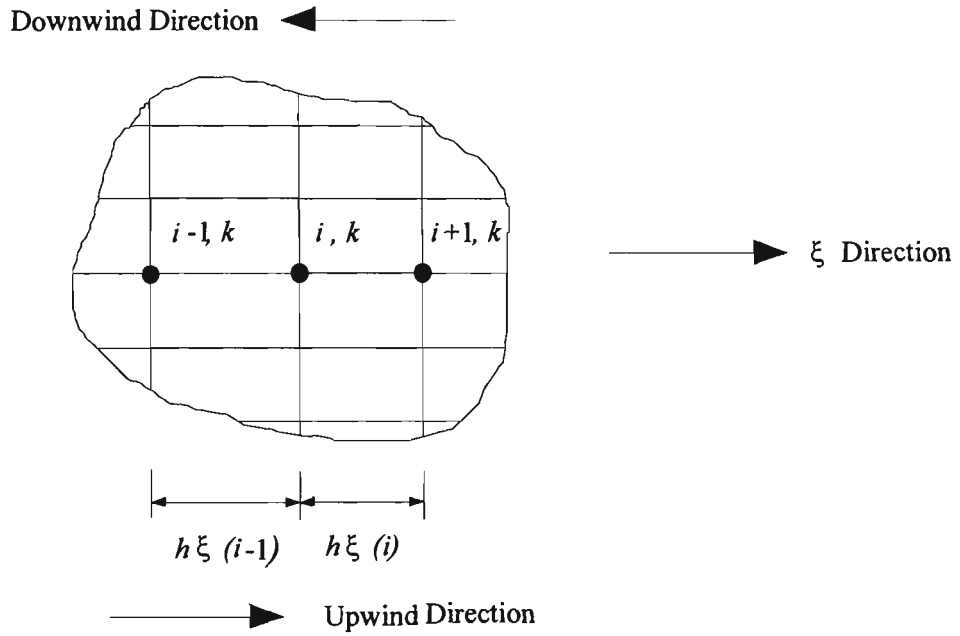


Figure 4.5 The three points used in determining the upwind operators

In the ξ direction, the first order derivative $\frac{\partial \Theta}{\partial \xi}$ is solved by the centre point (i)

upwind to the point ($i-1$), such as:

$$\frac{\partial \Theta}{\partial \xi} = \frac{\Theta_{i,j,k} - \Theta_{i-1,j,k}}{h_{\xi}(i-1)} \quad (4.115)$$

where Θ is an arbitrary variable.

we define

$$a_{\xi 1u} = -\frac{1}{h_{\xi}(i-1)} \quad (4.116)$$

$$a_{\xi 2u} = \frac{1}{h_{\xi}(i-1)} \quad (4.117)$$

$$\alpha_{\xi}^3 u = 0 \quad (4.118)$$

So equation (4.115) becomes:

$$\frac{\partial \Theta}{\partial \xi} = \alpha_{\xi}^1 u \Theta_{i-1,j,k} + \alpha_{\xi}^2 u \Theta_{i,j,k} + \alpha_{\xi}^3 u \Theta_{i+1,j,k} \quad (4.119)$$

When the flow is in the opposite direction of ξ , we have:

$$\frac{\overleftarrow{\partial \Theta}}{\partial \xi} = \frac{\Theta_{i+1,j,k} - \Theta_{i,j,k}}{h_{\xi}(i)} \quad (4.120)$$

In this case, the upwind finite difference operators in equation (4.119) assume the value as:

$$\alpha_{\xi}^1 u = 0 \quad (4.121)$$

$$\alpha_{\xi}^2 u = -\frac{1}{h_{\xi}(i)} \quad (4.122)$$

$$\alpha_{\xi}^3 u = \frac{1}{h_{\xi}(i)} \quad (4.123)$$

Similarly, in the η direction, the first order derivative $\frac{\partial \Theta}{\partial \eta}$ is also solved by the centre point (k) upwind to the point ($k-1$), we have:

$$\frac{\overrightarrow{\partial \Theta}}{\partial \eta} = \frac{\Theta_{i,j,k} - \Theta_{i,j,k-1}}{h_{\eta}(k-1)} \quad (4.124)$$

we define again

$$\alpha_{\eta}^1 u = -\frac{1}{h_{\eta}(k-1)} \quad (4.125)$$

$$\alpha_{\eta}^2 u = \frac{1}{h_{\eta}(k-1)} \quad (4.126)$$

$$\alpha_{\eta}^3 u = 0 \quad (4.127)$$

So equation (4.124) becomes:

$$\frac{\partial \Theta}{\partial \eta} = \alpha_{\eta}^1 u \Theta_{i,j,k-1} + \alpha_{\eta}^2 u \Theta_{i,j,k} + \alpha_{\eta}^3 u \Theta_{i,j,k+1} \quad (4.128)$$

When the flow is in the opposite direction of η , we have:

$$\frac{\partial \Theta}{\partial \eta} = \frac{\Theta_{i,j,k+1} - \Theta_{i,j,k}}{h\eta(k)} \quad (4.129)$$

The upwind finite difference operators in equation (4.128) assume the value as:

$$\alpha\eta 1u = 0 \quad (4.130)$$

$$\alpha\eta 2u = -\frac{1}{h\eta(k)} \quad (4.131)$$

$$\alpha\eta 3u = \frac{1}{h\eta(k)} \quad (4.132)$$

In the ϕ direction, the first order derivative $\frac{\partial \Theta}{\partial \phi}$ is determined by the centre point (j)

to the upwind point ($j-1$), we get:

$$\frac{\partial \Theta}{\partial \phi} = \frac{\Theta_{i,j,k} - \Theta_{i,j-1,k}}{h\phi(j-1)} \quad (4.133)$$

we define

$$\alpha\phi 1u = -\frac{1}{h\phi(j-1)} \quad (4.134)$$

$$\alpha\phi 2u = \frac{1}{h\phi(j-1)} \quad (4.135)$$

$$\alpha\phi 3u = 0 \quad (4.136)$$

So equation (4.133) becomes:

$$\frac{\partial \Theta}{\partial \phi} = \alpha\phi 1u \Theta_{i,j-1,k} + \alpha\phi 2u \Theta_{i,j,k} + \alpha\phi 3u \Theta_{i,j+1,k} \quad (4.137)$$

When the flow is in the opposite direction of ϕ , we also have:

$$\frac{\partial \Theta}{\partial \phi} = \frac{\Theta_{i,j+1,k} - \Theta_{i,j,k}}{h\phi(j)} \quad (4.138)$$

The upwind finite difference operators in equation (4.128) assume the value as:

$$\alpha\phi 1u = 0 \quad (4.139)$$

$$\alpha\phi 2u = -\frac{1}{h\phi(j)} \quad (4.140)$$

$$\alpha\phi 3u = \frac{1}{h\phi(j)} \quad (4.141)$$

4.6.2 Explicit method for the thermal energy equation

The solution procedure of explicit method for solving thermal energy equation is presented by the following. In equation (4.111), the first derivative with respect to temperatures $\frac{\partial T}{\partial \xi}$ is calculated by the upwind finite difference scheme as equation (4.119). The upwind finite difference operators are given by equations (4.116), (4.117) and (4.118). So we will have:

$$\frac{\partial T}{\partial \xi} = c\xi 1uT_{i-1,j,k} + c\xi 2uT_{i,j,k} + c\xi 3uT_{i+1,j,k} \quad (4.142)$$

Similarly, the first derivatives with respect to temperatures $\frac{\partial T}{\partial \eta}$ and $\frac{\partial T}{\partial \phi}$ are also given by the upwind finite difference scheme as equations (4.128) and (4.137). The upwind finite difference operators are determined by equations (4.125), (4.126), (4.127), (4.134), (4.135) and (4.136), we will obtain:

$$\frac{\partial T}{\partial \eta} = \alpha\eta 1uT_{i,j,k-1} + \alpha\eta 2uT_{i,j,k} + \alpha\eta 3uT_{i,j,k+1} \quad (4.143)$$

and
$$\frac{\partial T}{\partial \phi} = \alpha\phi 1uT_{i,j-1,k} + \alpha\phi 2uT_{i,j,k} + \alpha\phi 3uT_{i,j+1,k} \quad (4.144)$$

In equation (4.111), the second order derivatives $\frac{\partial^2 T}{\partial \xi^2}$, $\frac{\partial^2 T}{\partial \phi^2}$, $\frac{\partial^2 T}{\partial \xi^2}$ and the mixed derivative $\frac{\partial^2 T}{\partial \xi \partial \eta}$ are determined by the three point finite difference scheme, which are defined in equations (4.13), (4.21) (4.29) and (4.33). So we are able to write:

$$\begin{aligned}
\beta_1 \frac{\partial^2 T}{\partial \xi^2} + \beta_2 \frac{\partial^2 T}{\partial \eta^2} + \beta_3 \frac{\partial^2 T}{\partial \xi \partial \eta} + \beta_8 \frac{\partial^2 T}{\partial \phi^2} = & \beta_1 (c\xi 4(i)T_{i-1,j,k} + c\xi 5(i)T_{i,j,k} + c\xi 6(i)T_{i+1,j,k}) + \\
& \beta_2 (c\eta 4(k)T_{i,j,k-1} + c\eta 5(k)T_{i,j,k} + c\eta 6(k)T_{i,j,k+1}) + \\
& \beta_3 (c\eta 1(k)(c\xi 1(i)T_{i-1,j,k-1} + c\xi 2(i)T_{i,j,k-1} + \\
& c\xi 3(i)T_{i+1,j,k-1}) + c\eta 2(k)(c\xi 1(i)T_{i-1,j,k} + c\xi 2(i)T_{i,j,k} \\
& + c\xi 3(i)T_{i+1,j,k}) + c\eta 3(k)(c\xi 1(i)T_{i-1,j,k+1} + \\
& c\xi 2(i)T_{i,j,k+1} + c\xi 3(i)T_{i+1,j,k+1})) + \\
& \beta_8 (c\phi 4(j)T_{i,j-1,k} + c\phi 5(j)T_{i,j,k} + \\
& c\phi 6(j)T_{i,j+1,k})
\end{aligned} \tag{4.145}$$

In the left hand side of equation (4.111), the partial derivative with respect to time $\frac{\partial T}{\partial t}$ is discretised as a forward finite difference, thus:

$$\frac{\partial T}{\partial t} = \frac{T_{i,j,k}^{P+1} - T_{i,j,k}^P}{\Delta t} \tag{4.146}$$

where $T_{i,j,k}^{P+1}$ is expressed in terms of temperatures pertaining to the previous iteration time step P . Substituting equations (4.145) and (4.146) into equation (4.111), the updated values of the temperatures $T_{i,j,k}^{P+1}$ in grain silo can be obtained by:

$$T_{i,j,k}^{P+1} = T_{i,j,k}^P + \Delta t \{ \Pi_i + S_i - C_c (V_{T\xi} \frac{\partial T}{\partial \xi} + V_{T\eta} \frac{\partial T}{\partial \eta} + V_{T\phi} \frac{\partial T}{\partial \phi}) \} \tag{4.147}$$

4.6.3 Solution of the temperatures at boundaries

Equation (3.90) governs the temperature field at the upper surface of the grain silo in transformed coordinates. This equation is found by applying the three point differencing scheme, and discretization the first partial derivatives $\frac{\partial T}{\partial \xi}$ and $\frac{\partial T}{\partial \eta}$, which occur pertained in equation (4.12) and equation (4.38). So we will obtain ($\alpha_3 = 0$ and $0 < i < n\xi - 1$):

$$\sin \gamma_2 (\alpha_1 (c\xi 1(i)T_{i-1,j,n\eta} + c\xi 2(i)T_{i,j,n\eta} + c\xi 3(i)T_{i+1,j,n\eta})$$

$$+\alpha_2(c\eta b4T_{i,j,n\eta} + c\eta b5T_{i,j,n\eta-1} + c\eta b6T_{i,j,n\eta-2})) + \cos\gamma_2(\alpha_4(c\eta b4T_{i,j,n\eta} + c\eta b5T_{i,j,n\eta-1} + c\eta b6T_{i,j,n\eta-2})) = 0 \quad (4.148)$$

we define

$$a_{ii} = \alpha_1 \sin\gamma_2 c\xi 1(i) \quad (4.149)$$

$$b_{ii} = \sin\gamma_2 \alpha_1 c\xi 2(i) + \sin\gamma_2 \alpha_2 c\eta b4 + \cos\gamma_2 \alpha_4 c\eta b4 \quad (4.150)$$

$$c_{ii} = \sin\gamma_2 \alpha_1 c\xi 3(i) \quad (4.151)$$

$$d_{ii} = -(\sin\gamma_2 \alpha_2 + \cos\gamma_2 \alpha_4) c\eta b5T_{i,j,n\eta-1} - (\sin\gamma_2 \alpha_2 + \cos\gamma_2 \alpha_4) c\eta b6T_{i,j,n\eta-2} \quad (4.152)$$

where

$$\text{if } ii = 1, \quad d_{ii} = d_{ii} - c_{ii}T_{1,j,n\eta} \quad (4.153)$$

$$\text{if } ii = n\xi - 2, \quad d_{ii} = d_{ii} - c_{ii}T_{n\xi,j,n\eta} \quad (4.154)$$

Equation (4.148) can be written as:

$$a_{ii}T_{i-1,j,n\eta} + b_{ii}T_{i,j,n\eta} + c_{ii}T_{i+1,j,n\eta} = d_{ii} \quad (4.155)$$

The tri-diagonal matrix form of equation (4.155) is readily solved by applying the Thomas (1949) algorithm (see Appendix I).

Along the vertical line of the centre silo, the temperature field is calculated by averaging of second nodes at radial direction, that is:

$$T_{1,j,k} = \frac{\sigma T(k)}{n\phi} \quad (4.156)$$

where

$$\sigma T(k) = \sum_{j=1}^{n\phi} T_{2,j,k} \quad (4.157)$$

Equation (3.87) expresses the temperature field at the vertical wall of the silo in the transformed coordinates, this temperature field ($T_{n\xi,j,k}$) is related with solar radiation and ambient temperature flopping on the vertical wall of the silo ($ts1$, see figure 5.1), thus:

$$T_{n\xi,j,k} = ts1 \quad (4.158)$$

Similarly, in transformed coordinates equation (3.88) governs the temperature field ($T_{i,j,1}$) along the sloping floor of the silo, which is depending on solar radiation and ambient air temperature flopping on the silo surface ($ts2$, see figure 5.1), such as:

$$T_{i,j,1} = ts2 \quad (4.159)$$

Equation (3.92) and equation (3.93) are determined the temperature field at the upper surface and the bottom cone base of the silo in transformed coordinates. Employing the three point finite difference scheme at the boundaries, which is expressed by equation (4.42), we get:

$$c\eta b4T_{1,j,\eta\eta} + c\eta b5T_{1,j,\eta\eta-1} + c\eta b6T_{1,j,\eta\eta-2} = 0 \quad (4.160)$$

let

$$T_{1,j,\eta\eta} = \frac{c\eta b5T_{1,j,\eta\eta-1} + c\eta b6T_{1,j,\eta\eta-2}}{c\eta b4} \quad (4.161)$$

Again the temperatures at the bottomed cone base of the silo ($T_{1,j,1}$) is also dependent on solar radiation and ambient air temperature ($ts2^*$, see figure 5.1) which is striking on the same point of the silo surface, namely,

$$T_{1,j,1} = ts2^* \quad (4.162)$$

4.7 SOLUTION OF THE MOISTURE CONSERVATION EQUATION

The moisture conservation equation is discretised by using the upwind finite difference scheme and solved by a explicit method. Equation (3.94) that governs moisture contents in transformed coordinates may be written in a compact form as:

$$\frac{\partial W}{\partial t} = D_{eff} \frac{\rho_a}{\rho_b} \left\{ \beta_1 \frac{\partial^2 H}{\partial \xi^2} + \beta_2 \frac{\partial^2 H}{\partial \eta^2} + \beta_3 \frac{\partial^2 H}{\partial \xi \partial \eta} + \beta_8 \frac{\partial^2 H}{\partial \phi^2} \right\}$$

$$-\left\{V_{w\xi} \frac{\partial H}{\partial \xi} + V_{w\theta} \frac{\partial H}{\partial \phi} + V_{w\eta} \frac{\partial H}{\partial \eta}\right\} + \frac{dm}{dt}(0.6 + W) \quad (4.163)$$

where

$$V_{w\xi} = \frac{\rho_a}{\rho_b} (V_r \alpha_1 + V_z \alpha_3 - \beta_6 \cdot D_{eff}) \quad (4.164)$$

$$V_{w\eta} = \frac{\rho_a}{\rho_b} (V_r \alpha_2 + V_z \alpha_4 - \beta_7 \cdot D_{eff}) \quad (4.165)$$

$$V_{w\theta} = \frac{\rho_a}{\rho_b} \frac{V_\phi}{R\xi} \quad (4.166)$$

where $V_{w\xi}$, $V_{w\theta}$ and $V_{w\eta}$ are the effective velocities with respect to the moisture contents.

If we define again

$$\Pi_w = D_{eff} \left\{ \beta_1 \frac{\partial^2 H}{\partial \xi^2} + \beta_2 \frac{\partial^2 H}{\partial \eta^2} + \beta_3 \frac{\partial^2 H}{\partial \xi \partial \eta} + \beta_8 \frac{\partial^2 H}{\partial \phi^2} \right\} \quad (4.167)$$

$$S_w = (0.6 + W) \frac{dm}{dt} \quad (4.168)$$

Equation (4.163) becomes:

$$\frac{\partial W}{\partial t} = \Pi_w - \left\{ V_{w\xi} \frac{\partial H}{\partial \xi} + V_{w\theta} \frac{\partial H}{\partial \phi} + V_{w\eta} \frac{\partial H}{\partial \eta} \right\} + S_w \quad (4.169)$$

4.7.1 Explicit method for the moisture conservation equation

The solution procedure of explicit method for solving the moisture content equation is given as follows. In equation (4.169), the first derivative with respect to the absolute humidities of the air $\frac{\partial H}{\partial \xi}$ is obtained by the upwind finite difference scheme given by equation (4.119) with the upwind finite difference operators which are determined by equations (4.116), (4.117) and (4.118), so we will find that:

$$\frac{\partial H}{\partial \xi} = c\xi 1uH_{i-1,j,k} + c\xi 2uH_{i,j,k} + c\xi 3uH_{i+1,j,k} \quad (4.170)$$

In the same way, the first derivatives with respect to the absolute humidities of the air $\frac{\partial H}{\partial \eta}$ and $\frac{\partial H}{\partial \phi}$ are given by upwind finite difference scheme in equations (4.128) and

(4.137), and the upwind finite difference operators which are calculated by equations (4.125), (4.126), (4.127), (4.134), (4.135) and (4.136), so the expressions are:

$$\frac{\partial H}{\partial \eta} = a\eta 1uH_{i,j,k-1} + a\eta 2uH_{i,j,k} + a\eta 3uH_{i,j,k+1} \quad (4.171)$$

and

$$\frac{\partial H}{\partial \phi} = a\phi 1uH_{i,j-1,k} + a\phi 2uH_{i,j,k} + a\phi 3uH_{i,j+1,k} \quad (4.172)$$

In equation (4.169), the second derivatives $\frac{\partial^2 H}{\partial \xi^2}$, $\frac{\partial^2 H}{\partial \eta^2}$ and $\frac{\partial^2 H}{\partial \phi^2}$ and the mixed derivative $\frac{\partial^2 H}{\partial \xi \partial \eta}$ are determined by the three point finite difference scheme, it is reflected in equations (4.13), (4.21) (4.29) and (4.33). We have:

$$\begin{aligned} \beta_1 \frac{\partial^2 H}{\partial \xi^2} + \beta_2 \frac{\partial^2 H}{\partial \eta^2} + \beta_3 \frac{\partial^2 H}{\partial \xi \partial \eta} + \beta_8 \frac{\partial^2 H}{\partial \phi^2} = & \beta_1 (c\xi 4(i)H_{i-1,j,k} + c\xi 5(i)H_{i,j,k} + c\xi 6(i)H_{i+1,j,k}) + \\ & \beta_2 (c\eta 4(k)H_{i,j,k-1} + c\eta 5(k)H_{i,j,k} + c\eta 6(k)H_{i,j,k+1}) + \\ & \beta_3 (c\eta 1(k)(c\xi 1(i)H_{i-1,j,k-1} + c\xi 2(i)H_{i,j,k-1} + \\ & c\xi 3(i)H_{i+1,j,k-1}) + c\eta 2(k)(c\xi 1(i)H_{i-1,j,k} + \\ & c\xi 2(i)H_{i,j,k} + c\xi 3(i)H_{i+1,j,k}) + c\eta 3(k) \\ & (c\xi 1(i)H_{i-1,j,k+1} + c\xi 2(i)H_{i,j,k+1} + c\xi 3(i)H_{i+1,j,k+1})) + \\ & \beta_8 (c\phi 4(j)H_{i,j-1,k} + c\phi 5(j)H_{i,j,k} + \\ & c\phi 6(j)H_{i,j+1,k}) \end{aligned} \quad (4.173)$$

The partial derivative with respect to time $\frac{\partial W}{\partial t}$ which is in the left hand side of equation (4.169) is discretised by forward finite difference scheme, such as:

$$\frac{\partial W}{\partial t} = \frac{W_{i,j,k}^{P+1} - W_{i,j,k}^P}{\Delta t} \quad (4.174)$$

where $W_{i,j,k}^{P+1}$ is the term of moisture contents pertaining to the previous iteration time step P of the moisture contents. So updated value of the grain moisture content distribution $W_{i,j,k}^{P+1}$ is found from:

$$W_{i,j,k}^{P+1} = W_{i,j,k}^P + \Delta t \{ \Pi_i + S_i - C_c (V_{\tau\xi} \frac{\partial H}{\partial \xi} + V_{\tau\eta} \frac{\partial H}{\partial \eta} + V_{\tau\phi} \frac{\partial H}{\partial \phi}) \} \quad (4.175)$$

4.7.2 Solution of the absolute humidities at boundaries

The boundary conditions along the floor of the silo in equation (3.95) is expressed the absolute humidities of the air at the transformed coordinates. In order to discretise the partial derivatives $\frac{\partial H}{\partial \xi}$ and $\frac{\partial H}{\partial \eta}$, the three point finite difference scheme will be employed by equations (4.12) and (4.38), we will get ($\alpha_3 = 0$ and $0 < i < n\xi - 1$):

$$\begin{aligned} & -\sin \gamma_1 (\alpha_1 (c\xi 1(i) H_{i-1,j,1} + c\xi 2(i) H_{i,j,1} + c\xi 3(i) H_{i+1,j,1}) \\ & + \alpha_2 (c\eta b1 H_{i,j,1} + c\eta b2 H_{i,j,2} + c\eta b3 H_{i,j,3})) + \cos \gamma_1 (\alpha_4 (\\ & c\eta b1 H_{i,j,1} + c\eta b2 H_{i,j,2} + c\eta b3 H_{i,j,3})) \end{aligned} \quad (4.176)$$

we define

$$a_{ii} = -\alpha_1 \sin \gamma_1 c\xi 1(i) \quad (4.177)$$

$$b_{ii} = -\sin \gamma_1 \alpha_1 c\xi 2(i) - \sin \gamma_1 \alpha_2 c\eta b1 + \cos \gamma_1 \alpha_4 c\eta b1 \quad (4.178)$$

$$c_{ii} = -\sin \gamma_1 \alpha_1 c\xi 3(i) \quad (4.179)$$

$$\begin{aligned} d_{ii} = & (\sin \gamma_1 \alpha_2 - \cos \gamma_1 \alpha_4) c\eta b2 H_{i,j,2} + \\ & (\sin \gamma_1 \alpha_2 - \cos \gamma_1 \alpha_4) c\eta b3 H_{i,j,3} \end{aligned} \quad (4.180)$$

where

$$\text{if } ii = 1, \quad d_{ii} = d_{ii} - c_{ii} H_{1,1,1} \quad (4.181)$$

$$\text{if } ii = n\xi - 2, \quad d_{ii} = d_{ii} - c_{ii} H_{n\xi,j,1} \quad (4.182)$$

Equation (4.176) can be rewritten as:

$$a_{ii} H_{i-1,j,1} + b_{ii} H_{i,j,1} + c_{ii} H_{i+1,j,1} = d_{ii} \quad (4.183)$$

Equation (3.97) is expressed the absolute humidities of the air along the vertical wall of the silo and written in transformed coordinates, the first partial derivatives $\frac{\partial H}{\partial \xi}$ and

$\frac{\partial H}{\partial \eta}$ are discretised from the finite difference scheme as equations (4.17) and (4.34), it can be presented as following:

$$\begin{aligned} & \alpha_1 (c_{\xi}^{\xi} b_4 H_{n_{\xi},j,k} + c_{\xi}^{\xi} b_5 H_{n_{\xi}-1,j,k} + c_{\xi}^{\xi} b_6 H_{n_{\xi}-2,j,k}) \\ & + \alpha_2 (c_{\eta}^1(k) H_{n_{\xi},j,k-1} + c_{\eta}^2(k) H_{n_{\xi},j,k} + c_{\eta}^3(k) H_{n_{\xi},j,k+1}) = 0 \end{aligned} \quad (4.184)$$

we define

$$a_{kk} = \alpha_2 c_{\eta}^1(k) \quad (4.185)$$

$$b_{kk} = \alpha_2 c_{\eta}^2(k) + \alpha_1 c_{\xi}^{\xi} b_4 \quad (4.186)$$

$$c_{kk} = \alpha_2 c_{\eta}^3(k) \quad (4.187)$$

$$d_{kk} = -\alpha_1 c_{\xi}^{\xi} b_5 H_{n_{\xi}-1,j,k} - \alpha_1 c_{\xi}^{\xi} b_6 H_{n_{\xi}-2,j,k} \quad (4.188)$$

where

$$\text{If } kk = 1, \quad d_{kk} = d_{kk} - c_{kk} H_{n_{\xi},j,1} \quad (4.189)$$

$$\text{If } kk = m_{\eta} - 2, \quad d_{kk} = d_{kk} - c_{kk} H_{n_{\xi},j,m_{\eta}} \quad (4.190)$$

So equation (4.184) becomes:

$$a_{kk} H_{n_{\xi},j,k-1} + b_{kk} H_{n_{\xi},j,k} + c_{kk} H_{n_{\xi},j,k+1} = d_{kk} \quad (4.191)$$

The absolute humidities of the air at the intersection of the floor and wall of the silo is determined by linear interpolation, it can be written as:

$$H_{coner} = H_{n_{\xi},j,1} = H_{n_{\xi}-1,j,1} + \frac{h_{\xi}(n_{\xi}-1)}{h_{\xi}(n_{\xi}-1) + h_{\eta}(1)} (H_{n_{\xi},j,2} - H_{n_{\xi}-1,j,1}) \quad (4.192)$$

we define

$$a_{ii} = \frac{h_{\xi}(n_{\xi}-1)}{h_{\xi}(n_{\xi}-1) + h_{\eta}(1)} - 1 \quad (4.193)$$

$$b_{ii} = 1 \quad (4.194)$$

$$c_{ii} = -\frac{h_{\xi}(n_{\xi}-1)}{h_{\xi}(n_{\xi}-1) + h_{\eta}(1)} \quad (4.195)$$

$$d_{ii} = 0 \quad (4.196)$$

Equation (4.192) becomes:

$$a_{ii}H_{n\xi-1,j,1} + b_{ii}H_{n\xi,j,1} + c_{ii}H_{n\xi,j,2} = 0 \quad (4.197)$$

Similar, the set of equations (4.183), (4.191) and (4.197) can be solved simultaneously by means of Thomas (1949) algorithm (see Appendix I) for obtaining the absolute humidity field along the floor and the wall of the silo.

At the middle of the silo, the absolute humidities of the air is obtained by averaging of second nodes in the radial direction, thus:

$$H_{1,j,k} = \frac{\sigma H(k)}{n\phi} \quad (4.198)$$

where

$$\sigma H(k) = \sum_{j=1}^{n\phi} H_{2,j,k} \quad (4.199)$$

At the upper surface of the grains, equation (3.98) govern the absolute humidities of the air in transformed coordinates, the first partial derivative $\frac{\partial H}{\partial \eta}$ can be solved by the three point finite difference scheme from equations (4.42) and (3.98), we will obtain:

$$c\eta b4 H_{n\xi,j,n\eta} + c\eta b5 H_{n\xi,j,n\eta-1} + c\eta b6 H_{n\xi,j,n\eta-2} = 0 \quad (4.200)$$

so we have

$$H_{n\xi,j,n\eta} = -\frac{c\eta b5 H_{n\xi,j,n\eta-1} + c\eta b6 H_{n\xi,j,n\eta-2}}{c\eta b4} \quad (4.201)$$

Equation (3.100) yields the absolute humidities of the air at the bottomed cone base of the silo in transformed coordinates, the first partial derivative $\frac{\partial H}{\partial \eta}$ is discretised by using the three point finite difference scheme which is given by equation (4.38), we get:

$$\frac{\partial H}{\partial \eta} = c\eta b1 H_{1,j,1} + c\eta b2 H_{1,j,2} + c\eta b3 H_{1,j,3} = 0 \quad (4.202)$$

so we have

$$H_{1,j,1} = \frac{c\eta b2 \cdot H_{1,j,2} + c\eta b3 \cdot H_{1,j,3}}{c\eta b1} \quad (4.203)$$

Equation (3.101) is used to calculate the absolute humidities of the air at the peak of the grain in transformed coordinates, discretising it with the three point finite difference scheme given by equation (4.42), we will obtain:

$$c\eta b4 H_{1,j,\eta} + c\eta b5 H_{1,j,\eta-1} + c\eta b6 H_{1,j,\eta-2} = 0 \quad (4.204)$$

let

$$H_{1,j,\eta} = \frac{c\eta b5 H_{1,j,\eta-1} + c\eta b6 H_{1,j,\eta-2}}{c\eta b4} \quad (4.205)$$

4.7.3 Solution of the moisture contents at boundaries

According to the numerical solution of the grain moisture content field at the interior nodes, the grain moisture contents at boundary conditions can easily solve:

At the centre of the silo, the grain moisture content distribution is obtained by averaging the sum of the grain moisture contents which were given from the second centre nodes, the formula is written as:

$$W_{1,j,k} = \frac{\text{sigma}W(k)}{n\phi} \quad (4.206)$$

where

$$\text{sigma}W(k) = \sum_{j=1}^{n\phi} W_{2,j,k} \quad (4.207)$$

Along the floor of the silo, the grain moisture contents are determined by employing the Taylor expansion, thus:

$$W_{1,j,1} = W_{1,j,2} - h\eta(1) \frac{\partial W}{\partial \eta} \quad (4.208)$$

and

$$W_{i,j,1} = W_{i,j,3} - (h\eta(1) + h\eta(2)) \frac{\partial W}{\partial \eta} \quad (4.209)$$

Re-arranging both of equations (4.208) and (4.209), we get

$$W_{i,j,1} = \frac{(h\eta(1) + h\eta(2))W_{i,j,2} - h\eta(1)W_{i,j,3}}{h\eta(2)} \quad (4.210)$$

At the upper surface of the grain, the moisture contents of grain are also obtained by applying the Taylor expansion, the results are from the formula as following:

$$W_{i,j,n\eta} = \frac{(h\eta(n\eta - 1) + h\eta(n\eta - 2))W_{i,j,n\eta-1} - h\eta(n\eta - 1)W_{i,j,n\eta-2}}{h\eta(n\eta - 2)} \quad (4.211)$$

Along the wall of the silo, Taylor expansion is employed, the update rule of the moisture contents are:

$$W_{n\xi,j,k} = \frac{(h\xi(n\xi - 1) + h\xi(n\xi - 2))W_{n\xi-1,j,k} - h\xi(n\xi - 1)W_{n\xi-2,j,k}}{h\xi(n\xi - 2)} \quad (4.212)$$

CHAPTER 5

SYSTEM PROPERTIES

The heat and mass transfer conservation equations that govern the behaviour of forced convective processes occurrence in ventilated grain silos have been discussed in chapter 3 and 4. In this chapter we shall consider some of the thermodynamic properties of grain that are the essential constitution for requiring to model heat and mass transfer phenomenon, and other relevant biological properties required for modelling the stored grain ecosystem. In this work typical values of the physical and biological parameters that govern the rate processes have been used. It should be borne in mind, however, that stored grains and their spoilage agents are biological in nature, and therefore extremely variable. The results presented in this thesis therefore must, by necessity, indicate trends rather than absolute values.

5.1 INTERRELATIONS

Stored grains have several physical and biological properties, these are interrelated with one another and are affected by other variables. The interrelationship among physical and biological properties will be divided into two categories:

(1). Physical - Thermal properties which are related to the air / grain / water system are responsible for transfer and exchange of heat and moisture through stored grain.

They include heat conductivities, thermal capacitance, moisture diffusivity, absorption and desorption characteristics of the grain, and boundary conditions. The latter include the impermeable nature of the silo wall, and the absorptivity and emissivity of the silo surfaces which are the system properties.

(2). Biological properties are the external sources which invade the quality of grain. They are included: the response of insect population to their local environments, the rates at which moulds respire and cause damage to the grain by loss in the dry weight, and the viability of seed to germinate and develop into strong and healthy seedlings. The degree of deterioration is affected by the interaction of temperature, moisture content and stored grains.

5.2 SORPTION ISOTHERMS

Grains are hygroscopic materials, because they adsorb and desorb water. When water is absorbed by grain, it can be take up to about half of the dry weight in water. When the water content is about 30-40% of the air-dry basis of the grain, germination occurs. In general, grain can contents moisture and be considered in three forms: (a) Water of composition or bound water, it is an integral part of organic molecules, such as carbohydrate, protein, vitamin, mineral, fat and fibre. (b) Absorbed water which is more closely linked to the sorbing surface. (c) Free water or absorbed water, it is held in the intergranular spaces and within the pores of the material. These hygroscopic properties of the grain and the water exchange relationships do not cut clearly for demarcation the three forms. The water content of grain alone is insufficient to assess its keeping qualities. When the relative humidity of the air surrounding the grain is in the range of 65-75%, the critical moisture of stored grains will be arise, and heat is liberated as fungi becomes active. When the vapour pressure of the water is decreased, the heat of sorption exceeds the latent heat of vaporisation of free water.

In this section, the behaviour of hygroscopic porous media will be considered as the relationship between grain temperature, grain moisture content, and the humidity of the intergranular air. The mathematical descriptions that related to these variables are called sorption isotherms and are formulated as following.

In order to use Smith's (1947) equation that relates the relative humidity of the intergranular air with grain temperature and moisture content, it is necessary to determine the value of the wet basis grain moisture content (M_w) corresponding to a given the fractional dry basis grain moisture content ($W_{i,j,k}$). The expression is:

$$M_w = \frac{100 \cdot W_{i,j,k}}{1 + W_{i,j,k}} \tag{5.1}$$

According to Smith's (1947) isosteric relationship, the wet basis grain moisture content is function of grain temperature and the relative humidity of the intergranular air (rh) in equilibrium with the grain, and it can be written as:

$$M_w = a_1 + a_2 T_{i,j,k} - (a_3 + a_4 T_{i,j,k}) \ln(1 - rh) \tag{5.2}$$

so we obtain

$$rh = 1 - e^{\frac{(a_1 + a_2 T_{i,j,k}) - M_w}{a_3 + a_4 T_{i,j,k}}} \tag{5.3}$$

where a_1 , a_2 , a_3 and a_4 are the isosteric specific empirical constants for wheat given by Sutherland (1983) and presented in table 5.1.

Table 5.1 Isosteric specific empirical constants

a_1	a_2	a_3	a_4
9.304	-0.052076	4.1483	0.0215

The equation that relates the saturation vapour pressure of free water (P_{sat}) and temperature ($T_{i,j,k}$) is proposed by Hunter (1987) to be:

$$P_{sat} = \frac{6 \times 10^{25}}{(T_{i,j,k} + 273)^5} \cdot e^{\frac{-6800}{T_{i,j,k} + 273}} \quad (5.4)$$

Therefore the vapour pressure of moisture (P_{vap}) in the intergranular air is defined as:

$$P_{vap} = rh \cdot P_{sat} \quad (5.5)$$

and since the absolute humidity of air ($H_{i,j,k}$) at the interior nodes is found from:

$$H_{i,j,k} = \frac{gn \cdot P_{vap}}{P_{atm} - P_{vap}} \quad (5.6)$$

where P_{atm} is atmospheric pressure, and gn is ratio of molecular weights of water and air.

The heat of sorption is obtained by Gallaher's (1951) expression, that is reasonably thermodynamically consistent with the above sorption isotherm. The formula can be written as:

$$h_s = h_{vap} (1 + 23 \cdot e^{(-40 \cdot W_{i,j,k})}) \quad (5.7)$$

where h_{vap} is the latent heat of evaporation of free water, it is accurately approximated by a linear function of temperature, hence we have:

$$h_{vap} = c_{1v} + c_{2v} \cdot T_{i,j,k} \quad (5.8)$$

where c_{1v} and c_{2v} are the empirical constants, and in which:

$$c_{2v} = \frac{\partial h_{vap}}{\partial T} \quad (5.9)$$

where $\frac{\partial h_{vap}}{\partial T}$ is the differential of latent heat of vaporisation of water with respect to the temperature, and it is obtainable from steam tables.

So that the integral of the heat of sorption may be found by the following equation, thus:

$$\int_0^W h_s dW = h_s \{0.575(1 - e^{(-40 \cdot W)}) + W\} \quad (5.10)$$

By definition, the integral heat of wetting that arises from the hygroscopic nature of the grain is written in formula as:

$$H_w = \int_0^W h_w dW \quad (5.11)$$

where W is the moisture content of the grain on a dry basis, h_w is the isothermal differential heat of wetting of grain, and it is given by:

$$h_w = -23h_{vap} \cdot e^{(-40 \cdot W)} \quad (5.12)$$

Substituting equation (5.12) into equation (5.11), we get:

$$\begin{aligned} H_w &= \int_0^W -23h_{vap} \cdot e^{(-40 \cdot W)} dW \\ &= -23h_{vap} \left(-\frac{1}{40} \right) e^{(-40 \cdot W)} \Big|_0^W \\ &= 0.575h_{vap} (e^{(-40 \cdot W)} - 1) \end{aligned} \quad (5.13)$$

By the following, the differential heat of wetting which is obtained from equation (5.13) may be written as:

$$\frac{\partial H_w}{\partial T} = 0.575 \frac{\partial h_{vap}}{\partial T} (e^{(-40 \cdot W)} - 1) \quad (5.14)$$

5.3 RATE OF RESPIRATION

When grains respire, the solid substrate is oxidised, carbon dioxide and water are produced along with the heat of chemical reaction. This signifies that the oxidation of carbohydrate liberates thermal energy and together with water vapour, the results may be translated into dry matter loss. The loss of dry matter of the grain is associated with a deterioration in quality.

The formula that enables to calculate the cumulative consumption of oxygen (Q_r) by respiring wheat has been presented by Lacey *et al.* (1994), thus:

$$Q_r = \frac{b_1 + b_2 t_{ime}}{Y(1 + e^{\{(b_5 + b_6 t + b_7 T_{i,j,k})(b_8 + M_w)\}})} \quad (5.15)$$

where t_{ime} is the total elapsed time of storage.

$$Y = 1 + e^{b_3(b_4 - T_{i,j,k})} \quad (5.16)$$

where $b_1, b_2, b_3, b_4, b_5, b_6, b_7$ and b_8 are the grain specific empirical constants. They are reported by Lacey *et al.* (1994), and have the values given in table 5.2.

Table 5.2 Respiration specific empirical constants

b_1	b_2	b_3	b_4
3.4583E-04	3.478E-08	0.1737	20.33
b_5	b_6	b_7	b_8
0.9143	-2.878E-07	-0.013634	24.38

Therefore the differential equation of the rate of oxygen production is the function of grain moisture content, temperature and time, and is obtained by:

$$\begin{aligned} \frac{\partial Q_r}{\partial t_{ime}} &= \left(\frac{b_1 + b_2 t_{ime}}{Y(1 + e^{\{(b_5 + b_6 t_{ime} + b_7 T_{i,j,k})(b_8 - M_w)\}})} \right)', \\ &= \frac{(1 + e^{\{(b_5 + b_6 t_{ime} + b_7 T_{i,j,k})(b_8 - M_w)\}}) b_2 - (b_1 + b_2 t_{ime}) e^{\{(b_5 + b_6 t_{ime} + b_7 T_{i,j,k})(b_8 - M_w)\}} (b_6 (b_8 - M_w))}{Y(1 + e^{\{(b_5 + b_6 t_{ime} + b_7 T_{i,j,k})(b_8 - M_w)\}})^2} \end{aligned} \quad (5.17)$$

we define

$$\arg = e^{\{(b_5 + b_6 t_{ime} + b_7 T_{i,j,k})(b_8 - M_w)\}} \quad (5.18)$$

$$z_1 = 1 + \arg \quad (5.19)$$

$$z_2 = b_2 \quad (5.20)$$

$$z_3 = b_1 + b_2 t_{ime} \quad (5.21)$$

$$z_4 = b_6 (b_8 - M_w) \quad (5.22)$$

So equation (5.17) becomes:

$$\frac{\partial Q_r}{\partial t_{ime}} = \frac{(z_1 z_2 - z_3 z_4)}{Y z_1^2} \quad (5.23)$$

According to Lacey *et al.*'s (1994) paper, the respiration quotient of the respiring wheat is taken to the unity. From the stoichiometric equation that is governing the oxidation of hexose, it follows that the rate of dry matter loss ($\frac{dm}{dt}$) is determined by:

$$\frac{dm}{dt} = \frac{20}{21} \frac{\partial Q_r}{\partial t_{ime}} \quad (5.24)$$

where $\frac{20}{21}$ is the specific constant for equation (5.24).

5.4 SURFACE TEMPERATURE OF SILO RESULTING FROM SOLAR RADIATION

5.4.1 Introduction

Radiation is emitted from the sun with an energy distribution as if it were a 'black body', at the temperature of 6000K. Radiation travels with a velocity of 3×10^8 m/s, taking approximately 8 minutes to reach the earth's atmosphere. Some of the radiation entering the atmosphere of earth is scattered by dust, molecules of air and water vapour, and some of them is absorbed by atmosphere ozone, water vapour and carbon dioxide. As the value of solar constant is 1353 W/m^2 , the energy of solar radiation striking the top of the earth's atmosphere, only about 85% can reach the earth's surface.

Solar radiation can be regarded as the only original energy source for living creatures on the earth. From the viewpoint of the aerated grain silo, solar radiation

makes an important contribution to reduce the high humid air during the four seasons, and gives rise to a considerable amount of cooling load in the hot weather, especially in tropical regions. The variation of interior temperatures in the aerated grain silos not only very much depend on the amount of incident solar radiation and ambient temperatures on the exterior surface of the silo during the day, but also depends on the heat loss during the night as well.

The estimation of the boundary conditions as the temperatures along the vertical wall (ts_1) and the sloping floor (ts_2), and at the bottom cone (ts_2^*) of the silo (see figure 5.1) will be carried out as following:

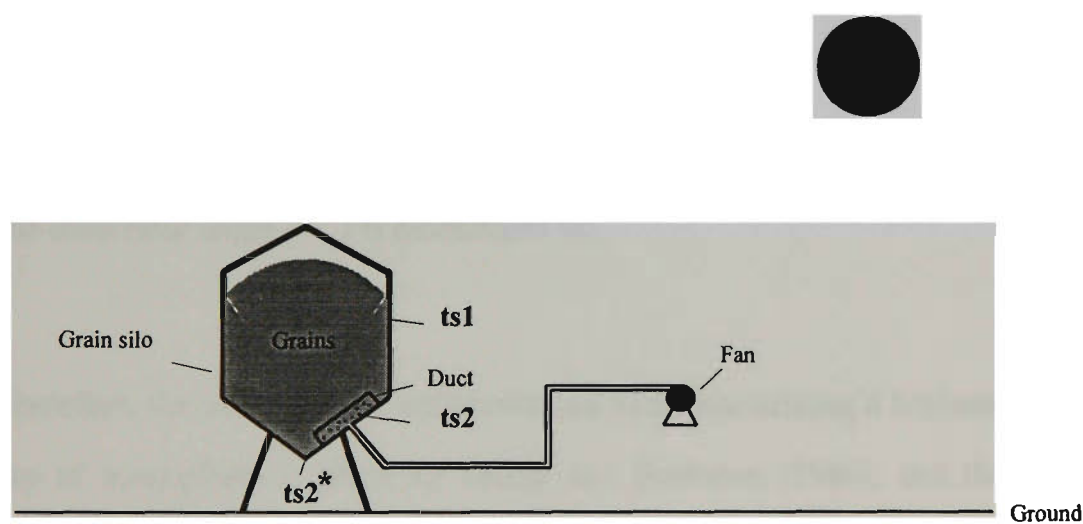


Figure 5.1 Solar radiation and ambient air around the surface of a grain silo

5.4.2 Extraterrestrial solar radiation

Solar radiation is received outside the earth's atmosphere. The earth follows an elliptical path round the sun, and takes one year for each cycle. The earth's axis is tilted at a constant angle of $23^{\circ}27'$ relative to the plane of rotation at all times. The daily motion of the sun across the sky viewed from any particular location on earth varies cyclically throughout the year, it is defined by the angle of declination. Cooper (1969) has derived a approximate equation for determining the angle of declination (δ_d) as:

$$\delta_d = 23.45 \sin\left(\frac{360(284 + n)}{n}\right) \quad (5.25)$$

where n is the day of the year.

The variation of the angle of declination will affect the angle of incidence of the solar radiation on the earth's surface, and cause seasonal variations in the length of the day. Duffie and Beckman (1980) have presented the equation for calculation the length of the day (N), it can be written as:

$$N = \frac{2}{15} \cos^{-1}(-\tan \phi_l \tan \delta_d) \quad (5.26)$$

where ϕ_l is the latitude of the geographical location under consideration.

The sunset hour angle (ω_s) is also given by:

$$\omega_s = \cos^{-1}(-\tan \phi_l \tan \delta_d) \quad (5.27)$$

and the solar hour angle (ω_a) is determined as:

$$\omega_a = 15t_h \quad (5.28)$$

Therefore, the average daily extraterrestrial radiation striking a horizontal surface at the top of atmosphere is given by Duffie and Beckman (1980), and the equation is written as:

$$\begin{aligned} \bar{H}_0 = \frac{0.0864 G_{sc}}{\pi} \left\{ 1 + 0.033 \cos\left(\frac{360n}{365}\right) \right\} \{ \cos \phi_l \cos \delta \sin \omega_s \\ + \frac{\pi \omega_s}{180} \sin \phi_l \sin \delta_a \} \end{aligned} \quad (5.29)$$

where G_{sc} is the solar constant.

5.4.3 Mean intensities of solar radiation

The total solar radiation reaching the ground consists of both beam and diffuse radiation components. A high accuracy method for calculating the average of daily diffuse

radiation (\bar{H}_d) is reported by Page (1961) and recommended by Ma and Iqbal (1984). It may be written as:

$$\bar{H}_d = \bar{H}_t \left\{ (1 - 1.13) \frac{\bar{H}_t}{\bar{H}_0} \right\} \quad (5.30)$$

where \bar{H}_t is the average of daily total radiation falling on a horizontal surface given by Rietveld (1978), thus:

$$\bar{H}_t = H_0 \left\{ 0.18 + 0.62 \left(\frac{n_s}{N} \right) \right\} \quad (5.31)$$

where n_s is the average of sunshine hours per day.

So the total average of daily beam radiation (\bar{H}_b) is readily obtained by the equation as following:

$$\bar{H}_b = \bar{H}_t - \bar{H}_d \quad (5.32)$$

5.4.4 Intensities of solar radiation

According to Collares-Pereira and Rabl's (1979) presentation, the total intensity of radiation (I_t) on a horizontal surface is given as:

$$I_t = \frac{\pi}{24} \{a + b \cos \omega_a\} \left\{ \frac{\cos \omega_a - \cos \omega_s}{\sin \omega_s - \omega_s \cos \omega_s} \right\} \frac{\bar{H}_t}{3600} \quad (5.33)$$

where

$$a = 0.409 + 0.5016 \sin(\omega_s - 60t_s) \quad (5.34)$$

$$b = 0.6609 - 0.4767 \sin(\omega_s - 60t_s) \quad (5.35)$$

and

$$t_s = \frac{\pi}{180} \quad (5.36)$$

Liu and Jordan (1960) have presented the expression of the total intensity of diffuse radiation (I_d) falling on a horizontal surface, thus:

$$I_d = \frac{\pi}{24} \left\{ \frac{\cos \omega_a - \cos \omega_s}{24(\sin \omega_s - \omega_s \cos \omega_s)} \right\} \frac{\bar{H}_d}{3600} \quad (5.37)$$

By following, the total intensity of beam radiation (I_b) is obtained by:

$$I_b = I_t - I_d \quad (5.38)$$

5.4.5 Ratios of solar radiation

In practice, on the top, bottom and wall of the silo surfaces are usually at angle other than horizontal. The method for definition the ratio (R_t) of the total intensity of radiation falling on a tilted surface (I_{tT}) to the total intensity of radiation falling on a horizontal surface (I_t) is written as:

$$R_t = \frac{I_{tT}}{I_t} \quad (5.39)$$

Similarly, the ratio (R_d) of the total intensity of the diffuse radiation (I_{dT}) falling on a sloping surface to the total intensity of diffuse radiation falling on a horizontal surface (I_d) is given by:

$$R_d = \frac{I_{dT}}{I_d} \quad (5.40)$$

The ratio (R_b) of the total intensity of beam radiation falling on a inclined surface to the total intensity of beam radiation falling on a horizontal surface is obtained as:

$$R_b = \frac{I_{bT}}{I_b} \quad (5.41)$$

Because the total intensity of radiation is sum of the total intensity of diffuse radiation and the total intensity of beam radiation, so we have:

$$I_{tT} = I_{bT} + I_{dT} \quad (5.42)$$

Replacing equations (5.39), (5.40) and (5.41) into equation(5.42), we get:

$$R_t I_t = R_b I_b + R_d I_d = I_{tT} \quad (5.43)$$

we obtain

$$R_t = \frac{R_b I_b + R_d I_d}{I_t} \quad (5.44)$$

Duffie and Beckman (1980) have recommend a procedure for calculating ratio R_t , as following:

When the surface is inclined at an angle to the horizontal, some of the diffuse radiation comes from sky and some of it reaches the surface by reflection from the ground. The value of ratio R_d is:

$$R_d = \frac{1 + \cos\beta}{2} \quad (5.45)$$

where β is the angle between a flat surface and the horizontal plane. The value of β is obtained by:

$$\beta = \begin{cases} \frac{\pi}{2} & \text{on the vertical wall} \\ \pi - \gamma_1 & \text{on the sloping floor} \end{cases} \quad (5.46)$$

A view factor of the ground of the tilted surface is:

$$V_e = \frac{1 - \cos\beta}{2} \quad (5.47)$$

The fraction of the total radiation hitting the ground then the total solar radiation hitting the sloping surface is:

$$g_s = (I_b + I_d)\rho \cdot V_e \quad (5.48)$$

where ρ is the reflected fraction and equation (5.44) becomes:

$$\begin{aligned} R_t &= \frac{I_b R_b + I_d \left(\frac{1 + \cos\beta}{2} \right) + g_s}{I_t} \\ &= \frac{I_b R_b + I_d \left(\frac{1 + \cos\beta}{2} \right)}{I_t} + \rho \left(\frac{1 - \cos\beta}{2} \right) \end{aligned} \quad (5.49)$$

The total intensity of radiation on the tilted surface is expressed as:

$$I_{IT} = I_b R_b + I_d \left(\frac{1 + \cos \beta}{2} \right) + (I_b + I_d) \rho \left(\frac{1 - \cos \beta}{2} \right) \quad (5.50)$$

The ratio of beam radiation (R_b) on a tilted surface to a horizontal surface is:

$$R_b = \frac{\cos \theta}{\cos \theta_z} \quad (5.51)$$

where θ_z is the zenith angle, it is between the sun and a vertical wall of the silo through the point of interest, θ is the angle of incidence of the beam radiation, and between the beam and the normal to the plane. It is given by the expression as:

$$\begin{aligned} \cos \theta = & \sin \delta \sin \phi_i \cos \beta - \sin \delta \cos \phi_i \sin \beta \cos \gamma + \cos \delta \cos \phi_i \cos \beta \cos \omega_a \\ & + \cos \delta \sin \phi_i \sin \beta \cos \gamma \cos \omega_a + \cos \delta \sin \beta \sin \gamma \sin \omega_a \end{aligned} \quad (5.52)$$

where γ is the surface azimuth angle, it is the angler deviation from a line running north and south through the location of the silo, and the value of γ is calculated by:

$$\gamma = -\frac{\pi}{2} + 2\pi \frac{j-1}{nphi} \quad (5.53)$$

The zenith angle (θ_z) is also determined by :

$$\cos \theta_z = \cos \delta \cos \phi_i \cos \omega_a + \sin \delta \sin \phi_i \quad (5.54)$$

5.4.6 Surface temperatures of the silo

The temperatures of the surface of the silo are obtained by carrying out a numerical heat balance scheme and assuming the total heat fluxes into the surface of the silo is zero.

This can be written in words as:

$$\begin{aligned} & \text{Beam Radiation Flux} + \text{Diffuse Radiation Flux} + \text{Solar Radiation Flux} \\ & \text{Reflected from the Ground} + \text{Radiation Flux to the Sky} + \text{Radiation} \\ & \text{Flux to the Ground} + \text{Convective Heat Loss through Convection} = 0 \end{aligned} \quad (5.55)$$

Swinbank (1963) has presented the following relationship between the ambient temperature (T_a) to the sky temperature (T_{sky}), thus:

$$T_{sky} = 0.05522 T_a^{1.5} \quad (5.56)$$

The heat exchange between the surface of the silo to the sky is given by:

$$q_s = \sigma \cdot \epsilon (T_{sky}^4 - T_s^4) \left(\frac{1 + \cos \beta}{2} \right) \quad (5.57)$$

where σ is the Stefan-Boltzman constant. ϵ is the emissivity of the external surface of the grain silo.

The exchange of radiation between the ground temperature (T_g) to the surface temperature of the silo (T_s) is written as:

$$q_g = \sigma \cdot \epsilon (T_g^4 - T_s^4) \left(\frac{1 - \cos \beta}{2} \right) \quad (5.58)$$

The convective heat transfer coefficient is given by:

$$h_0 = 2.8 + 3V_{wind} \quad (5.59)$$

where V_{wind} is the wind velocity across the surface of the silo.

So equation (5.55) in algebraic form is written as:

$$\begin{aligned} \alpha I_b R_b + \alpha I_d \left(\frac{1 + \cos \beta}{2} \right) + \alpha (I_b + I_d) \rho \left(\frac{1 - \cos \beta}{2} \right) \\ + q_g + q_s + h_0 (T_a - T_s) = 0 \end{aligned} \quad (5.60)$$

Re-arranging equation (5.60), we get:

$$\begin{aligned} \alpha I_b R_b + \alpha I_d \left(\frac{1 + \cos \beta}{2} \right) + \alpha (I_b + I_d) \rho \left(\frac{1 - \cos \beta}{2} \right) + \sigma \cdot \epsilon (T_{sky}^4 - T_s^4) \\ \left(\frac{1 + \cos \beta}{2} \right) + \sigma \cdot \epsilon (T_g^4 - T_s^4) \left(\frac{1 - \cos \beta}{2} \right) + (2.8 + 3V_{wind}) (T_a - T_s) = 0 \end{aligned} \quad (5.61)$$

Equation (5.61) is solved by applying Newton-Raphson method (see Appendix II), we define:

$$\begin{aligned}
f(T_s) = & \alpha I_b R_b + \alpha I_d \left(\frac{1 + \cos \beta}{2} \right) + \alpha (I_b + I_d) \rho \left(\frac{1 - \cos \beta}{2} \right) \\
& + \sigma \cdot \varepsilon (T_{sky}^4 - T_s^4) \left(\frac{1 + \cos \beta}{2} \right) + \sigma \cdot \varepsilon (T_g^4 - T_s^4) \left(\frac{1 - \cos \beta}{2} \right) \\
& + (2.8 + 3V_{wind}) (T_a - T_s)
\end{aligned} \tag{5.62}$$

and

$$T_s^{P+1} = T_s^P - \frac{f(T_s^P)}{f'(T_s^P)} \tag{5.63}$$

where T_s^P is the previous surface temperature at the commencement of the iteration step P , hence we have:

$$f'(T_s^P) = -4\sigma\varepsilon T_s^3 \left(\frac{1 + \cos \beta}{2} \right) - 4\sigma\varepsilon T_s^3 \left(\frac{1 - \cos \beta}{2} \right) - h_0 \tag{5.64}$$

So equation (5.63) sets the stage for using the Newton-Raphson method to solved the updated value of the surface temperatures of the silo (T_s), such as:

$$T_s = T_s^{P+1} \tag{5.65}$$

We note that the temperatures varies with radial position, may cause the temperatures on the vertical wall and sloping floor of the silo different, so the surface temperature (T_s) can be defined as following:

At the vertical wall of the silo, T_s is in the three components space $(n\xi, j, k)$, we obtain:

$$T_{s-(n\xi, j, k)} = ts1 \tag{5.66}$$

Along the sloping floor of the silo, T_s is in the space $(i, j, 1)$, we have:

$$T_{s-(i, j, 1)} = ts2 \tag{5.67}$$

At the bottom of the cone of the silo, T_s is in the space $(1, j, 1)$, we get:

$$T_{s-(1, j, 1)} = ts2^* \tag{5.68}$$

5.5 VIABILITY OF STORED GRAINS

Seeds of different plant species vary widely in their life spans under identical storage conditions. If seed is alive or dead it dose not influence its food value, but it is inevitable that grains spoilage will always be accompanied by loss of germination. A fundamental difference exists between seeds stored as seeds, and seeds stored as food, but the essential requirement for successful storage is to maintain a high viability of stored grains.

The loss of viability of grain seeds is related to the temperature and wet basis moisture content within the grain store, and both of them vary with time and space. Roberts (1960) has presented an expression for determining the half-life of the seeds, and it may be written as:

$$H_{life} = 10^{(v_1 + v_2 M_w + v_3 T_{ijk})} \quad (5.69)$$

where v_1 , v_2 and v_3 are seed-specific constants, M_w is wet basis of moisture content, it is defined by equation (5.1).

The standard deviation of the mortality of grain seeds is given by:

$$\sigma = v_4 H_{life} \quad (5.70)$$

where v_4 is also a seed specific constant.

Moreover, the fraction of the seeds dead is determined by:

$$d_{ead} = 1 - V_{iab} \quad (5.71)$$

where V_{iab} is the fractional viability of seeds.

In general, we consider that the initial viability of grain seeds is 99%, that is:

$$d_{ead} = 1 - 0.99 = 0.01 \quad (5.72)$$

So the time required the half of the seeds to be dead (when viability of the grain is 99%) is determined as following:

If $d_{ead} \geq 0.5$, then

$$d_{ead1} = 0.5 + 0.5 \cdot erf(x) \quad (5.73)$$

where the $erf(x)$ is the error function, it is given by:

$$erf(x) = \frac{2}{\sqrt{\pi}} \int_0^x e^{(-x^2)} d(x) \quad (5.74)$$

in which, if $x \leq 1$, the error function is solved by series expansion, thus:

$$erf(x) = x + \frac{2}{\sqrt{\pi}} \left(\sum_{n=2}^{\infty} \frac{(-1)^{n-1} (x)^{2n-1}}{(2n-1)n!} \right) \quad (5.75)$$

and if $x > 1$, the error function is evaluated by Simpson's rule, namely:

$$\begin{aligned} erf(x) &= \int_0^x e^{(-x^2)} d(x) \\ &= \int_0^1 e^{(-x^2)} d(x) + \int_1^x e^{(-x^2)} d(x) \\ &= 0.8427008 + \int_1^x e^{(-x^2)} d(x) \end{aligned} \quad (5.76)$$

and the first term $\int_0^1 e^{(-x^2)} d(x) = 0.8427008$ is found from a table of the error function, and the second term $\int_1^x e^{(-x^2)} d(x)$ is solved by Simpson's rule.

So we have (when $d_{ead} \geq 0.5$):

$$func_1 = d_{ead1} - \{0.5 + 0.5 \cdot erf(x)\} \quad (5.77)$$

and the Newton-Raphson method (see Appendix II) is used for determining x , thus:

$$x^{P+1} = x^P + \frac{func_1}{0.5 \cdot derf(x)} \quad (5.78)$$

where x^P is the previous error function at the commencement of the iteration step P , and $derf(x)$ is the first derivative of $erf(x)$ from equation (5.74), we get:

$$derf(x) = \frac{2}{\sqrt{\pi}} e^{(-x^2)} d(x) \quad (5.79)$$

Update the value x from equation (5.78), we have:

$$x_1 = x^{P+1} \quad (5.80)$$

and we know

$$x = \frac{|t_v - H_{life}|}{\sigma\sqrt{2}} \quad (5.81)$$

So when viability of seed is 99% and $d_{ead} \geq 0.5$, the value of t_v can be obtained from equation (5.81) that is:

$$t_{v1} = x_1 \cdot \sigma\sqrt{2} + H_{life} \quad (5.82)$$

If $d_{ead} \leq 0.5$, then

$$d_{ead2} = 0.5 - 0.5 \cdot erf(x) \quad (5.83)$$

$$func_2 = d_{ead2} - \{0.5 - 0.5 \cdot erf(x)\} \quad (5.84)$$

The Newton-Raphson method (see Appendix II) for determining x is:

$$x^{P+1} = x^P - \frac{func_2}{0.5 \cdot derf(x)} \quad (5.85)$$

Update the value x from equation (5.85), it is:

$$x_2 = x^{P+1} \quad (5.86)$$

Re-arrange equation (5.81) again, we have:

$$t_{v2} = H_{life} - x_2 \cdot \sigma\sqrt{2} \quad (5.87)$$

where t_{v2} is the value of when $d_{ead} \leq 0.5$ and the viability of grain seeds is 99%.

Then the total elapsed time ($time^*$) of heat and mass transfer iteration required the time of half seeds to be dead is calculated as:

$$t_{v1-new} = t_{v1} + time^* \quad (5.88)$$

$$t_{v2-new} = t_{v2} + time^* \quad (5.89)$$

where

$$time^* = \frac{dtg \cdot ifreq}{3600 \times 24} \quad (5.90)$$

in which *ifreq* is the number of heat and mass transfer iterations, because the viability of seed changes very slowly compared with other changes, and since the computation of seed viability is numerically intensive, so it is calculated infrequently. The number of the seeds dead are obtained by:

When $t_{v1-new} > H_{life}$, that:

$$d_{ead1-new} = 0.5 + 0.5 \cdot erf(x_{new1}) \quad (5.91)$$

where

$$x_{new1} = \frac{|t_{v1-new} - H_{life}|}{\sigma\sqrt{2}} \quad (5.92)$$

so the viability of grain seeds is:

$$V_{iab1} = 1 - d_{ead1-new} \quad (5.93)$$

When $t_{v2-new} < H_{life}$, that:

$$d_{ead2-new} = 0.5 - 0.5 \cdot erf(x_{new2}) \quad (5.94)$$

which

$$x_{new2} = \frac{|t_{v2-new} - H_{life}|}{\sigma\sqrt{2}} \quad (5.95)$$

Again the viability of grain seeds is:

$$V_{iab2} = 1 - d_{ead2-new} \quad (5.96)$$

5.6 PESTICIDE DECAY

Pesticides may be effective against the insect pests for many months, and they are often admixed with grains to resist the attack by insect pests. When pesticides are applied to

warm and damp grains, they can decompose to ineffectively low levels only in few weeks. The pesticides studied in this thesis are not labile, hence we need not study their movement within the grain store. The kinetics of pesticide decay has been presented by Desmarchelier and Bengston (1979) and Thorpe (1989), and it can be shown that the concentration of pesticide on the grain as a function of the relative humidity of the intergranular air (rh), grain temperature ($T_{i,j,k}$) and total elapsed time (t_{ime}) of storage. It can be written in algebraic form as:

$$C_{pes} = C_i e^{(-1.3863(rh)t_{ime} \times 10^{B(T_{i,j,k}-30)/t^*})}$$

(5.97)

where C_i is the initial concentration of the pesticide, B and t^* are the pesticide specific empirical constants.

The relative humidity of the intergranular air is obtained by:

$$rh = \frac{P_{vap}}{P_{sat}}$$

(5.98)

where

$$P_{vap} = \frac{P_{atm}H_{i,j,k}}{gn + H_{i,j,k}}$$

(5.99)

and P_{sat} is calculated by Hunter's (1987) equation as same as equation (5.4), namely:

$$P_{sat} = \frac{6 \times 10^{25}}{(T_{i,j,k} + 273)^5} \cdot e^{\frac{-6800}{T_{i,j,k} + 273}}$$

(5.100)

Desmarchelier and Bengston (1979) have determined that the values of B and t^* for fenitrothion are those given in table 5.3, thus:

Table 5.3 Pesticide specific empirical constants

B	t *
0.036	8.467E06

5.7 INSECT POPULATION GROWTH

Stored products insect pests are ubiquitous and they are detected in storage or during transport. They are spread throughout the world. They easily adapt themselves to a new environment, and readily become established. Stored grain damage by insect pests attack will cause enormous quantitative and qualitative losses.

The growth of insect pests are dependent on the moisture content and temperature of the grains. Desmarchelier (1988) reported the intrinsic weekly multiplication rate of the insect population growth is calculated by equation as:

$$r_s = c_{c1}(T_{wetb} - c_{c2}) \quad (5.101)$$

where c_{c1} and c_{c2} are species specific constants, T_{wetb} is the wet bulb temperature of the intergranular air, which is a function of the saturation humidity of air (H^*), absolute humidity ($H_{i,j,k}$) and dry bulb temperature (T_{dryb}), and it expressed as:

$$\begin{aligned} (T_{dryb} - T_{wetb}) + H_{i,j,k} (2502 + 1.809T_{dryb} - 4.186T_{wetb}) \\ - H^* (2502 - 2.377T_{wetb}) = 0 \end{aligned} \quad (5.102)$$

in which the dry bulb temperature (T_{dryb}) is determined by Smith's (1947) isosteric, it is expressed as:

$$T_{dryb} = \frac{M_w - a_1 + a_3 \cdot \ln(1 - rh)}{a_2 - a_4 \cdot \ln(1 - rh)} \quad (5.103)$$

and the saturation humidity of air is function of wet bulb temperature. it is obtained as:

$$H^* = \frac{gn \cdot p_s}{P_{atm} - p_s} \quad (5.104)$$

where

$$p_s = \frac{6 \times 10^{25}}{(T_{wetb} + 273)^5} \cdot e^{\frac{-6800}{T_{wetb} + 273}} \quad (5.105)$$

The wet bulb temperature T_{wetb} is obtained by solving equation (5.102), by employing the Newton-Raphson method (see Appendix II), we define:

$$f(T_{wetb}) = (T_{dryb} - T_{wetb}) + H_{i,j,k} (2502 + 1.809T_{dryb} - 4.186T_{wetb}) - H^* (2502 - 2.377T_{wetb}) \quad (5.106)$$

and

$$T_{wetb}^{P+1} = T_{wetb}^P - \frac{f(T_{wetb}^P)}{f'(T_{wetb}^P)} \quad (5.107)$$

where T_{wetb}^P is the previous wet bulb temperature at the commencement of the iteration step P , and the first derivative of T_{wetb} is:

$$f'(T_{wetb}) = -1 - 4.186H_{i,j,k} + 2.377H^* - 2502 \frac{dH^*}{dT_{wetb}} + 2.377T_{wetb} \cdot \frac{dH^*}{dT_{wetb}} \quad (5.108)$$

By the chain rule of the differentiation, we get:

$$\frac{dH^*}{dT_{wetb}} = \frac{dH^*}{dp_s} \frac{dp_s}{dT_{wetb}} \quad (5.109)$$

So from equation (5.104), we have:

$$\begin{aligned} \frac{dH^*}{dp_s} &= \left(\frac{gn \cdot p_s}{P_{atm} - p_s} \right)' \\ &= \frac{gn \cdot P_{atm}}{(P_{atm} - p_s)^2} \end{aligned} \quad (5.110)$$

and from equation (5.105), we get:

$$\begin{aligned} \frac{dp_s}{dT_{wetb}} &= \left(\frac{6 \times 10^{25}}{(T_{wetb} + 273)^5} \cdot e^{\frac{-6800}{T_{wetb} + 273}} \right)' \\ &= \frac{6 \times 10^{25}}{(T_{wetb} + 273)^5} \cdot e^{\frac{-6800}{T_{wetb} + 273}} \cdot \left(\frac{6800}{T_{wetb} + 273} - 5 \right) \end{aligned} \quad (5.111)$$

Substituting equations (5.110) and (5.111) into equation (5.109), we will obtain:

$$\frac{dH^*}{dT_{wetb}} = \frac{gn \cdot P_{atm}}{(P_{atm} - p_s)^2} \cdot \frac{6 \times 10^{25}}{(T_{wetb} + 273)^5} \cdot e^{\frac{-6800}{T_{wetb} + 273}} \cdot \left(\frac{6800}{T_{wetb} + 273} - 5 \right) \quad (5.112)$$

So equation (5.107) sets the stage for the Newton-Raphson method (see Appendix II) is to easily find the updated value of the wet bulb temperature (T_{wetb}), thus:

$$T_{wetb} = T_{wetb}^{P+1} \quad (5.113)$$

Then the population of insect pests after dtg weeks may be obtained by :

$$R^{P+1} = R^P \cdot e^{r_s \cdot dt_{week}} \quad (5.114)$$

where R^P is the previous population of insect pests at the commencement of the time step P . dt_{week} is the end of time step that is calculated by weeks, it is written as:

$$dt_{week} = \frac{dtg}{3600 \times 7 \times 24} \quad (5.115)$$

where dtg is the time step used during the aeration cycle.

CHAPTER 6

NUMERICAL EXPERIMENTS

Since computational methods have become an important tool for scientific investigations, the solution of finite difference scheme has been realized to numerically solve the problems in an efficient manner. In this chapter, the numerical experiments implicate a study of factors that have significant influence on the effect of convergence and accuracy of the numerical results, they include grid mesh size, iteration time step and aeration duct layouts (The discussion is included in chapter 7).

6.1 PROGRAM EXPLANATION

The program SILO3DFTN is largely based on the software CBHMT developed, to calculate the response of bulk respiring grains contained in a conical bottomed circular silo to aeration with ambient or conditioned air, written by Thorpe (1994). The main modifications were in aspects of program control and in the inclusion of variation of duct positioning. The program was also modified to accommodate specific characteristics of the conical bottomed circular silo, such as located at the Academy of Grain Technology at Werribee.

Program SILO3DFTN has provided three major categories of outputs, namely: (a). pressure and velocity fields, (b). temperature and moisture content fields, and (c)

fields of biological activity and the rate of pesticide decay. The procedures of this FORTRAN program is illustrated in flow charts as shown in figures 6.1 and 6.2, and the program instruction is explained as following.

To start, subroutines INPUT, SETCON, PROPS and INITIAL are all input for setting up the initial conditions, system properties and parameters. Subroutine SURTEMP calculates the surface temperature of grain silo subjected to heating and cooling by radiation and convection. Subroutines PRESSURE and VELOCITY predict the pressure and velocity distributions by replacing the spatial derivative for the governing equations. Subroutine ITERP estimates the approach to responsible the convergence of the pressure distribution. Subroutine FLOWRATE calculates the air flow rate through the upper surface of the grain silo.

The inner loop of HMTR is a system control of aeration and the second major loop for heat and mass transfer calculations. Subroutine HUMSM obtains the absolute humidity of air from the temperature and moisture content of the grain. Subroutine RESPL determines the rate of respiration of wheat as the dry matter loss of grain. Subroutine MOISTU and TEMPERA solve moisture conservation and thermal energy equations. Subroutine TBC, HUMBC and MCBC calculate the boundary conditions of temperature, humidity and moisture content in stored grain. Subroutine WETBULB uses the dry bulb temperature of air to calculate the wet bulb temperature of air. Subroutine INSECTS obtains the insect population growth in the silo, and subroutine VIABLE calculates the updated viability of the seeds after a time, and the subroutine PESTI calculates the concentrations of pesticide on the stored grain.

When the inner loop HMTR is equal to the maximum iteration time, the inner loop will be returned to the main program, and the final results will be obtained by calling subroutine RESULTS, then program stop.

In addition, program SILO3DFTN is shown in Appendix III.

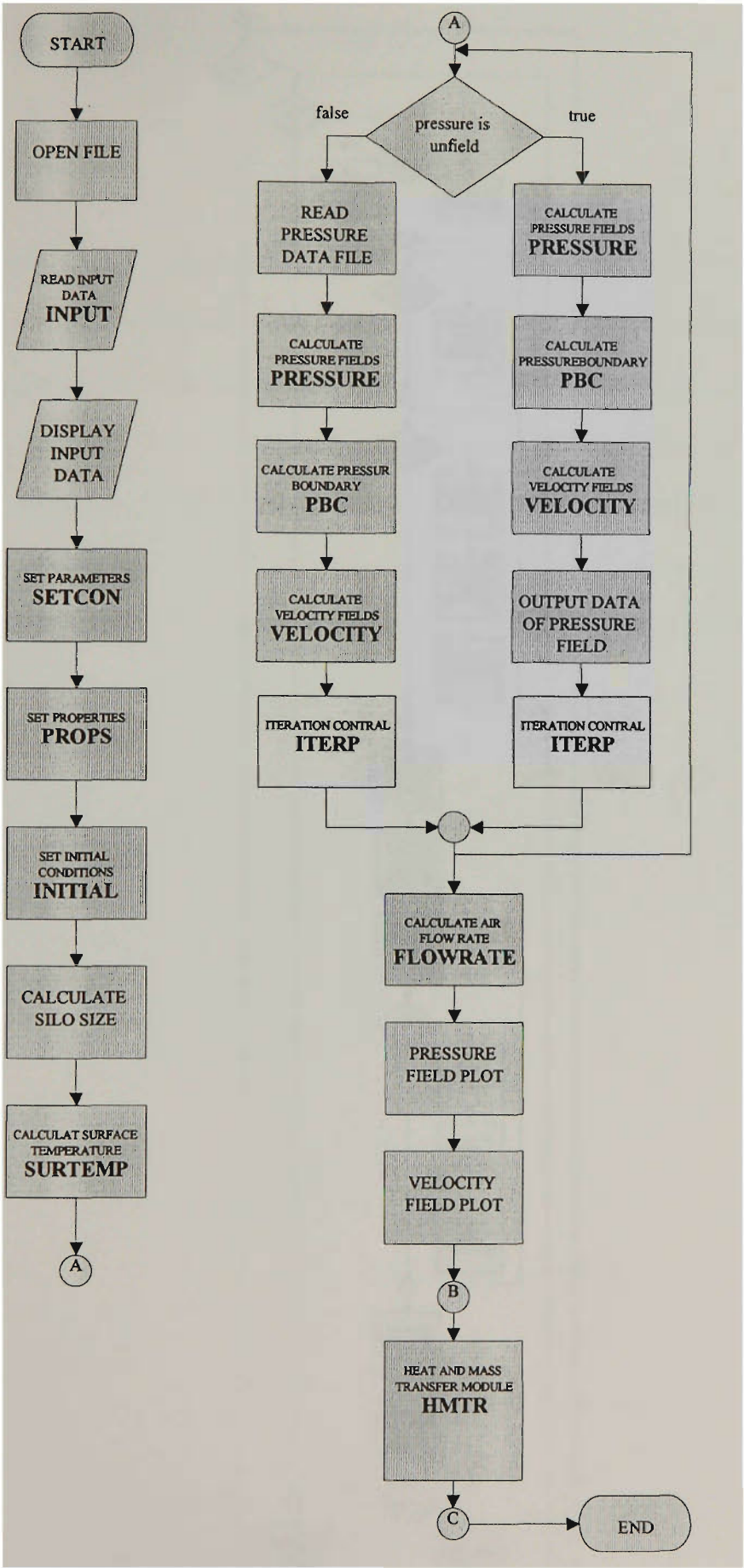


Figure 6.1 The main loop of program SILO3DFTN

6.2 SYSTEM INVESTIGATIONS

6.2.1 The silo

Traditionally most grains are stored in circular type of silos which provide a convenient mean for handling and management. In this study, the design parameters of the silo are measured on a prototype conical bottomed circular steel silo, which is located at the Academy of Grain Technology at Werribee. The aeration cooling system is consist of a fan and a duct operation. The stored grains are wheat (about 10 tonnes). The total height of the silo is $4220mm$, and the diameter is $1230mm$. The volume of the silo is $11.9675m^3$. The length of the linear duct is $1000mm$. Further information of this grain silo can be found in the drawing below (figure 7.1).

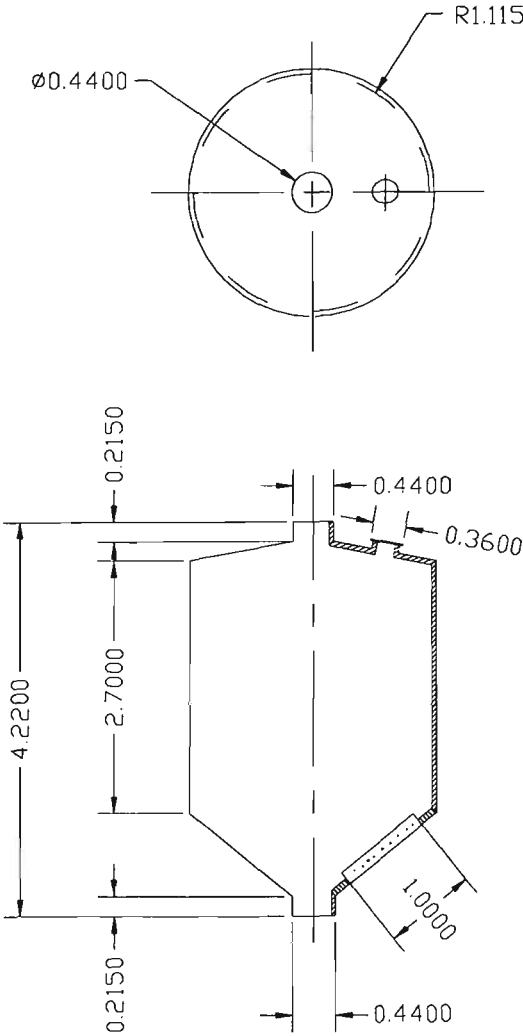


Figure 6.3 The detailed drawing of the silo

6.2.2 The ducts

In the numerical experiments, two type of aeration systems were simulated. In one case, a conventional linear aeration duct was used, and in the other case, the effect on cooling processes of an annular duct was investigated (see figure 6.4). The details of this information are included in table 6.1.

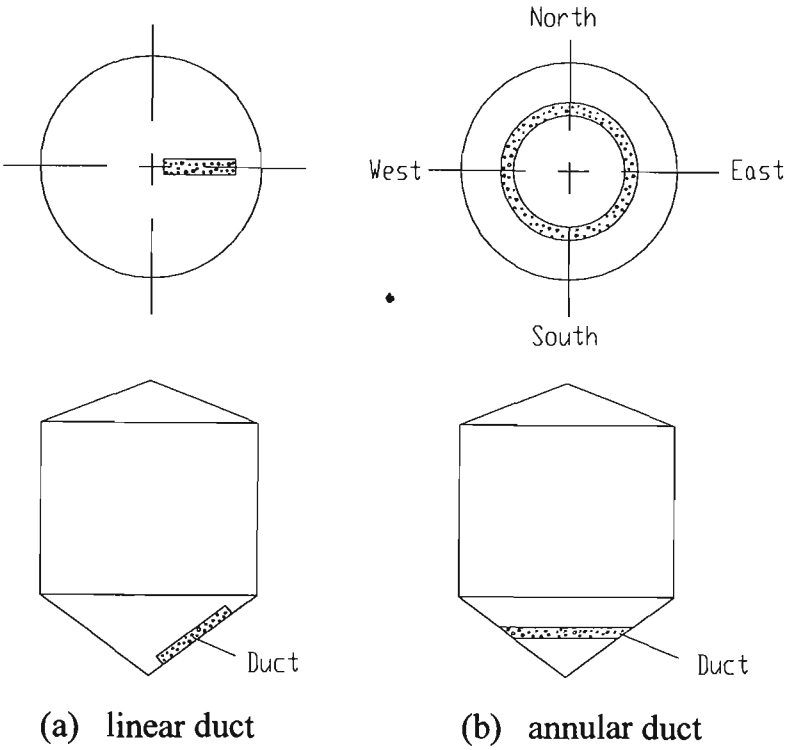


Figure 6.4 The two types of ducts: linear and annular ducts

Table 6.1 The character of linear and annular ducts

Type	Length of duct	Configuration
Linear duct	1000 mm	Laid on the sloping base of the silo
Annular duct	2170 mm (Perimeter)	Placing on the conical base of the silo

The simulation results of linear and annular aeration systems are implemented by applying program SILO3DFTN, as shown in chapter 7.

6.2.3 Further investigations

Aeration system must be carefully controlled to achieve minimum grain temperature with a minimum of moisture increase. Excessive fan operation with humid air will cause moisture uptake by the grain near the perforated duct, and may result in bulging on the silo walls. The following variables were used in simulating aeration systems of linear and annular ducts. Consideration low capital costs of the electric power, the aeration fan is operated between midnight to 6am each day, and the airflow rate through the silo of grain is 1.47 l/s/tonne . The duration of aeration cooling are 60 days. Further details are listed in table 6.2.

Table 6.2 Physical data of aeration system

Initial grain temperature	30 °C
Initial grain moisture content (wet basis)	12%
Initial grain moisture content (dry basis)	13.64%
Airflow rate through aeration	1.47 l/s/tonne
Aeration fan turned on	0 hours
Aeration fan turned off	6 hours
Duration of aeration	60 days
Mean minimum daily temperature	14.2 °C
Mean maximum daily temperature	24.3 °C
Mean daily sunshine hours	8.1 hours / per day
Mean absolute ambient humidity	0.008 kg / kg
Latitude	-37.67
Absorptivity of silo material	0.8
Emissivity of silo material	0.9
Silo of volum	11.9675 cubic meter
Angle of conical corn to horizontal	38.67 °
Angle of silo roof to horizontal	10.17 °
Mean ambient temperature	15.973 °C
Mean ambient wet-bulb temperature	12.997 °C
Humidity of air entering grain	0.005 kg/kg
Months	January-February

6.3 CONVERGENCE OF ITERATION SCHEME

Convergence criterion is the expression used to indicate that the approximate computed solution of partial differential equation approaches to the exact solution of the finite difference problem as the grid spacing in time and distance tend to zero (Carnahan *et al.*, 1969). In this study, equation (4.48) of Laplace equation in transformed coordinates is solved by adding a false transient term ($\frac{1}{\alpha_p}$) as proposed by Mallinson and Vahl

Davis (1973), the solution procedure corresponding to equation (4.48) was iterated to a steady state, until the following convergence criterion which is called *Psimax* was satisfied as:

$$\frac{\sum_i \sum_j \sum_k |\psi^{n+1} - \psi^n|}{\sum_i \sum_j \sum_k |\psi^n|} \leq Psimax \quad (6.1)$$

Here the superscripts $(n+1)$ and n represent the $(n+1)^{th}$ and $(n)^{th}$ iterations respectively. The indices i, j , and k represent grid location in the space (ξ, ϕ, η) .

Table 6.3 shows the first inner loop of program SILO3DFTN calculating the pressure distribution at the centre of the silo (as the values of *Pcon-min*), to represent the finite difference scheme consistent with the given partial differential equation. The *Pcon-min* computational results are obtained by employing Implicit method with the three different types of grid mesh. Moreover, the best advice for decision the right size of grid mesh in the computer simulation will be provide.

Observing has been made, as iter-number increase, the values of *Pcon-min* can be tended to similarity, that means the convergence of the solution is appeared. The worthy of note is: when a non-uniform mesh of 11x10x11 grid is used, and the values of *Pcon-min* are changed from $Psimax=0.00001$ to $Psimax=0.000001$, the accuracy of the pressure distribution can be improved by 1%. So $Psimax=0.00001$ is small enough to obtain the reasonable accurate results for the pressure distribution.

When non-uniform grid mesh 21x20x21 is used, from $Psimax=0.000001$ to $Psimax=0.0000001$, the difference between values $Pcon-min$ is 0.3% increase, but the iteration time step is 1.5 times greater, so it can be seen when $Psimax$ is less than 0.000001, the solution of pressure will converge. It is also clear when the mesh size is 31x30x31, from iter-number=90159, to iter-number=160000, $Psimax$ is still in the region of $<10^{-7}$ and $>10^{-8}$, the solution for the pressure field improves very slowly.

Table 6.3 Convergence effect of grid mesh

Mesh size	Time step	$Psimax$	Iter number	$Pcon-min$
11x10x11	0.5	0.01	47	37.6242
11x10x11	0.5	0.001	552	181.0662
11x10x11	0.5	0.0001	2315	343.1566
11x10x11	0.5	0.00001	4726	377.9526
11x10x11	0.5	0.000001	7206	381.7996
11x10x11	0.5	0.0000001	9633	382.1920
11x10x11	0.5	0.00000001	10724	382.2184
21x20x21	0.5	0.01	56	15.7051
21x20x21	0.5	0.001	612	87.9188
21x20x21	0.5	0.0001	3918	260.3447
21x20x21	0.5	0.00001	9947	331.7149
21x20x21	0.5	0.000001	17081	339.9291
21x20x21	0.5	0.0000001	25369	340.9936
21x20x21	0.5	0.00000001	33346	341.1255
31x30x31	0.5	0.01	72	2.7542
31x30x31	0.5	0.001	559	24.7522
31x30x31	0.5	0.0001	5160	103.8654
31x30x31	0.5	0.00001	22373	184.1912
31x30x31	0.5	0.000001	48908	204.1521
31x30x31	0.5	0.0000001	90159	206.6867
31x30x31	0.5	0.0000001	160000	207.1201
				It hasn't converged yet

Theoretically, the small mesh size, such as 31x30x31 can increase the accuracy of the results, but it will cause the program to take very long time to run. (In Apollo

workstation, I use 12 days to run the results, but still can not get the solution of convergence). From the view of economy, this is unsuitable choice. Oppositely, the mesh size 11x10x11 can rapidly reach convergence, (in Apollo workstation, I can get the results of convergence in 10 hours), but the accuracy of the results is lower.

Clearly, mesh size 21x20x21 can achieve the good balance on the accuracy and economic time of the computational results to reach the convergence of the numerical solution. (I can get the results of convergence in 3 days at Apollo workstation).

At the following chapter 7, the simulation results are employed at the mesh size of 21x20x21 in the cause of non-aerated silo, and the silos fitted with linear and annular ducts.

Figure 6.5 shows the convergence of pressure distribution at the centre of the silo by grid mesh 21x20x21, on the accurate of numerical solution to reach the steady state with different iteration time step. It is clear when iteration number is over 15000, the pressure distribution is convergent.

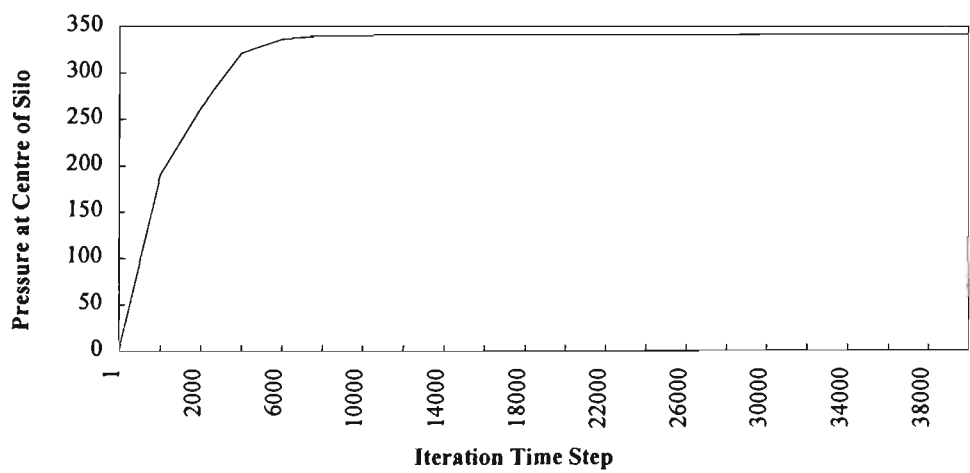


Figure 6.5 Convergence of pressure distribution

As Patankar (1980) noted, an iterative process is said to have converged when further iterations will not produce any change in the values of the dependent variables.

In practice, the iterative process is terminated when some arbitrary convergence criterion is satisfied. An appropriate convergence criterion depends on the nature of the problem and on the objectives of the computation.

6.3 EFFECT OF TIME STEP AND GRID MESH

Accuracy of a numerical solution depends on two major classes of error: Roundoff and truncation errors. Roundoff error is a property of the computer and the program. Truncation error is a property of the method. Often the real danger as far as roundoff error are concerned results from the fact that solution obtained in one cycle of calculations. Therefore, the danger of error propagation and error growth can be generated as solution proceeds over a larger number of steps.

As Croft and Lilley (1977) discussed, roundoff error is caused by finite significant figure restriction and associated with the Fourier number (Fo) to given space - time grid. Such instability phenomenon is inherent in finite difference representation, and obviously yields an unsatisfactory computed solution. However, roundoff error can have tendency to grow with time in unstable scheme. Croft and Lilley (1977) also recommend that the Fourier number (Fo) is the well-known stability criterion to analyse the oscillation of the solution, and to limit the maximum value of Δt for a given mesh size subdivision. This can be expressed by the formula as :

$$Fo = \alpha_p \frac{\Delta t}{(\Delta l)^2} \quad (6.2)$$

where Δt is the iteration time step, Δl is the space distance, and α_p is the false transient factor.

Sometimes, refining the time step Δt and distance step Δl can improve the accuracy of the solution. Table 6.4 presents the second inner loop of program as the numerical

solution of temperature distribution at the centre of the silo by simulated with 6 groups of different time step. In this explicit scheme, the large value of time step is employed for handling the multiple iterations.

Table 6.4 Solution effect by different time step at centre of silo

Time step	Temperatures at centre of the silo						Mesh size
	Day 10	Day20	Day30	Day40	Day50	Day60	
dt=45	23.0992	19.5796	19.7011	19.8235	19.7937	19.8158	21x20x21
dt=90	23.1325	19.6750	19.8481	19.9260	19.8827	19.9108	21x20x21
dt=180	23.1783	19.8284	20.0178	20.0380	19.9937	20.0452	21x20x21
dt=270	23.2124	19.9017	20.0745	20.0805	20.0376	20.0963	21x20x21
dt=315	23.6912	20.1885	20.2524	20.2321	20.2187	20.2808	21x20x21
dt=360	Floating point appearing						21x20x21

Evidently, with time step increments and grid mesh size stable, the numerical results show (see table 6.4), from time step dt=45 to dt=270, the temperatures difference between each neighbouring step is about 0.2% increase. According to equation 6.2, as Fourier number (Fo) is limited, the time step increase is real dangerous for the very large time step, such as dt=270 and dt=315, it is 2% increase between both of them, but when dt=360, the solution of temperature field can rapidly diverge, tend to infinity and cause floating point error appearing, this is indicated in table 6.4.

Conversely, the relatively small time step leads to a better accuracy in predicting the solution to be converge, such as dt=45, but the program running time (in Apollo station I use 7 days to get this results) is two times large than that dt=90. Even through dt=180 and dt=270 can diminish the CPU time, but the accuracy of the results are still not good enough, so the best choice for simulation program SILO3DFTN is dt=90.

However as equation (6.2) of Fourier number (Fo) shown, the gain in accuracy of numerical solution is associated with an necessary small time step in stability reason,

the infinite small time step only can increase in labour without specially increasing the desired accuracy.

In this study, the principle arrangement of non-uniform grid mesh has been mentioned in Chapter 4 of section 4.2, and it is calculated by equations (4.1), (4.2), (4.3), (4.4) and (4.5). In order to select a suitable mesh size that yields the accurate results, the effect of grid points on the numerical solution is tested by a series running of the program. A $21 \times 20 \times 21$ non-uniform grid mesh was constructed in table 6.5.

Table 6.5 Non-uniform grid mesh: $21 \times 20 \times 21$

	Space from the centre of silo to the silo wall
ξ direction	6.1819x6.1819x6.1819x6.1819x6.1819x6.1819x6.1819x6.1819 x6.1819x6.1819x6.1819x6.1819x6.1819x6.1819x4.4843x 1.7937x1.7937x1.7937x1.7937x1.7937

A $31 \times 30 \times 31$ non-uniform grid mesh was designed in table 6.6 as follows:

Table 6.6 Non-uniform grid mesh: $31 \times 30 \times 31$

	Space from the centre of silo to the silo wall
ξ direction	0.036x0.036x0.036x0.036x0.036x0.036x0.036x0.036x0.036x 0.036x0.036x0.036x0.036x0.036x0.036x0.036x0.036x0.036x 0.036x0.036x0.036x0.036x00036x0.036x0.045x0.018x0.018x 0.018x0.018x0.018

Table 6.7 shows the numerical solution effect by trial different grid mesh. In the pressure distribution calculation, the governing equation of Laplace formula is solved by a false transient method. The time step is set quite small for the suitable number of iterations. Obviously, the decrease grid mesh size can achieve the solution of the desired accuracy, but can lead the CPU time limit increase as same percentage as grid mesh decrease. Table 6.7 indicates, at the same iter-number, the *P-centre* can given the different results by the different grid mesh. As we discussed before, grid mesh 21x20x21 is the best choice for improve the accuracy of the results.

Table 6.7 Effect of grid mesh on the solution

Non-uniformed mesh	Time step	Iter number	<i>P-centre</i>
11x10x11	1	4500	349.0681
	1	6000	366.2688
	1	7040	372.6066
	1	8040	376.3117
21x20x21	1	4500	200.3025
	1	6000	232.2351
	1	7040	249.0050
	1	8040	261.8310
31x30x31	1	4500	192.4070
	1	6000	200.8912
	1	7040	203.7110
	1	8040	205.1922

* *P-centre* is the pressure fields at the centre of the silo

Practice has been proved, as observed from Fourier number (Fo), reducing time step and space distance can increase in accuracy of the solution, but it is also important in adjusting a reasonable balance between accuracy and efficiency.

CHAPTER 7

COMPARISONS AND DISCUSSION

The main objective of this chapter is to compare the ecosystems in a non-aerated silo, and silos fitted with linear and annular aeration ducts. These simulations are carried out using climatic data obtained for Melbourne, Australia. Each of the simulations assumes the same initial conditions, the same physical properties, the same silo dimensions and the same period of storage.

7.1 DEFINITIONS

A non-aerated silo is by definition not ventilated, and cooling occurs in practice by conduction and free convection processes. In this thesis, only thermal conduction is considered. Work conducted by Jayas *et al* (1992) has shown that cooling in silos is dominated by thermal conduction, but free convection processes become important when studying moisture migration and the distribution of fumigant gases.

The linear aeration system is defined as a silo fitted with a linear aeration duct which is single straight and placed on the conical base of the silo, as illustrated in figure 6.3 (a).

The annular aeration system is also defined as a silo fitted with an annular aeration duct which is seat on the conical base of the silo, as shown in figure 6.3 (b).

The orientation of the silo is defined by means of the points of the compass, that is to say the top is north, the bottom is south, the left is west, and the right is east, as indicated in figure 6.4 (b).

7.2 PRESSURE AND VELOCITY DISTRIBUTIONS

Airflow is the major factor affecting the performance of the aeration system. Airflow resistance is overcome by providing the pressure in the aeration duct. When air is forced through grain mass, air pressure and air velocity fields develop. The simulations of the silos fitted with linear and annular ducts have been implemented. The predictions have shown that the different type of ducts can significantly effect the air pressure and air velocity distributions.

Figures 7.3 and 7.4 show, the contour maps of pressures and velocities in the silos fitted with the two type of ducts investigated. It is observed, that the pressure gradients in the silo with the annular duct are more uniform than that the silo fitted with the linear duct. However, it can be observed that in both of the aeration systems considered the pressure patterns become very similar, particularly near the grain surface. One reason for their similarity in this region is that the air flow rate are the same in each system.

The component of vertical velocity in the silo fitted with the annular duct is generally more uniform in the conical base than in the silo fitted with a linear duct, as can be seen from figure 7.3 (c) and figure 7.4 (c). As would be expected, the radial velocity in the silo fitted with the annular duct is symmetrical about the centre line of the silo. However, in the case of the silo fitted with the linear duct, air flow from one side of the silo to the other. These phenomena can be observed in figures 7.3 (b) and 7.4 (b).

The vertical component of velocity along the walls in both cases of aeration systems are reflected by the pressure distributions, they are indicated in figures 7.1 and

7.2. It can be inferred that the vertical velocity is generally higher on the eastern side of the silo where a linear duct is placed, and lowest on the opposite side. Interestingly, the vertical pressure gradients on the north and south, and the west facing portions of the wall are very similar.

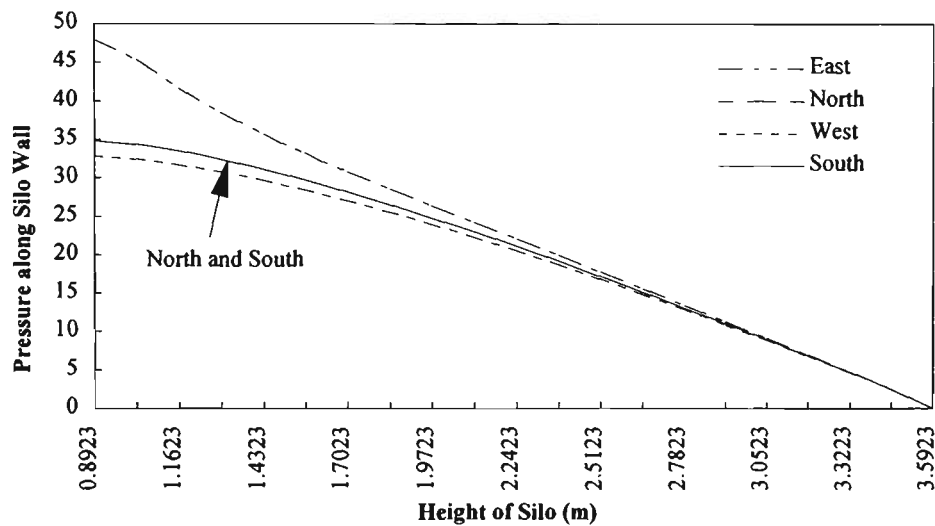


Figure 7.1 Pressure distributions along the wall of silo in the linear duct case

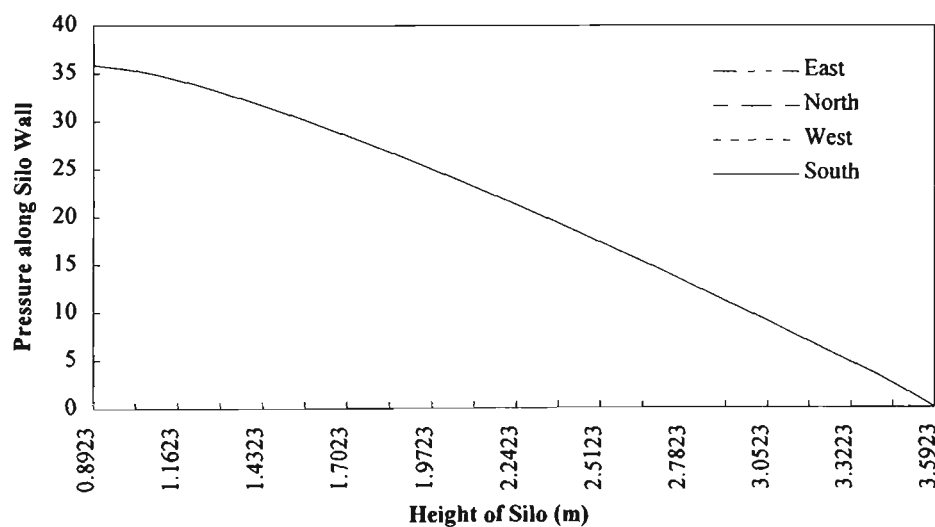
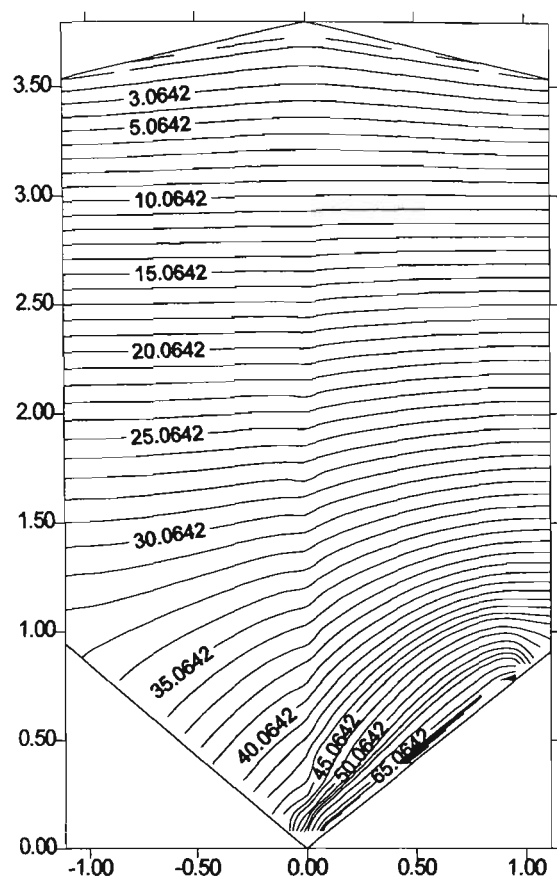
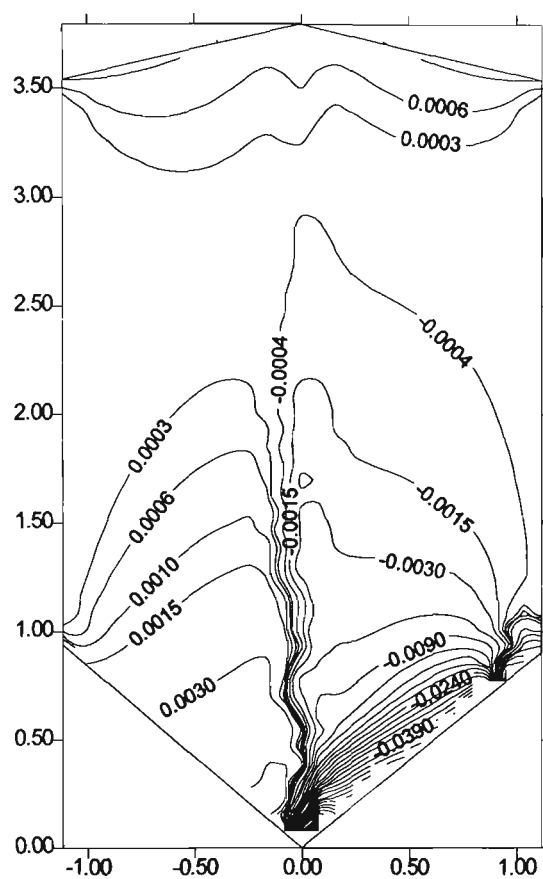


Figure 7.2 Pressure distributions along the wall of silo in the annular duct case

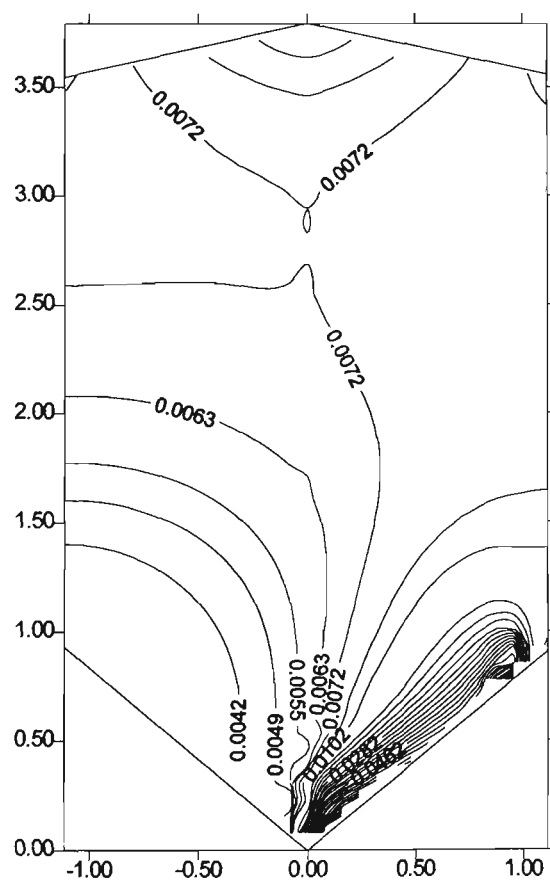
The pressure distributions on the wall of the silo fitted with an annular duct (as shown in figure 7.2) are symmetrical, as would be expected. Hence, the components of velocity distributions are also symmetrical in this case.



(a) Pressure distributions (linear duct)



(b) Component of radial velocity (linear duct)



(c) Component of vertical velocity (linear duct)

Figure 7.3 Pressure and velocity distributions in a silo fitted with linear aeration duct

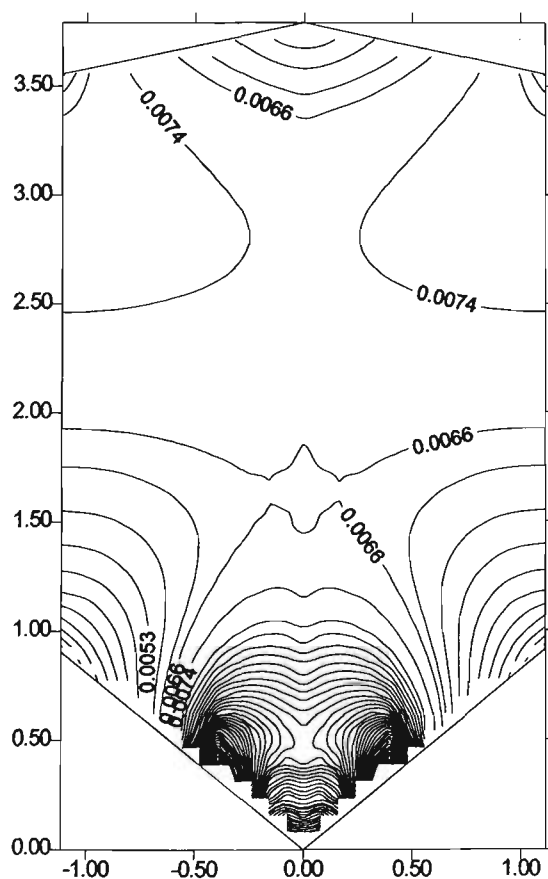
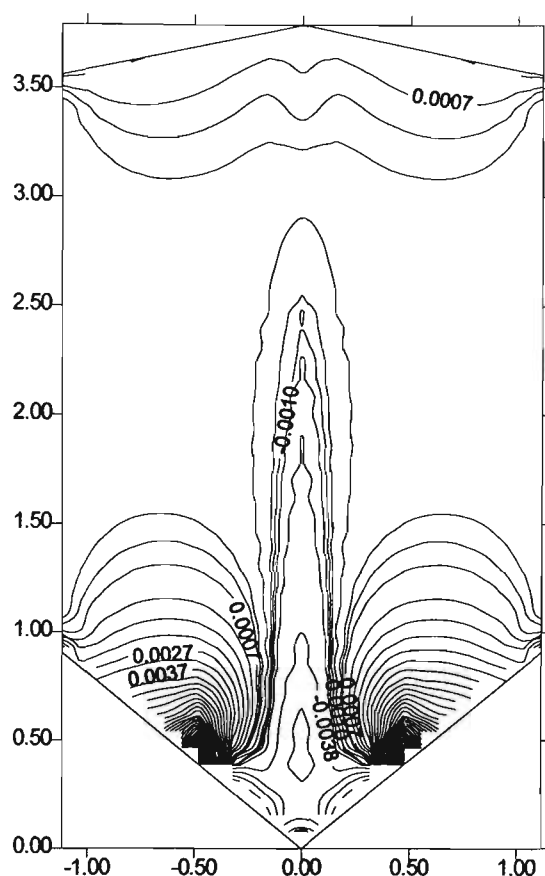
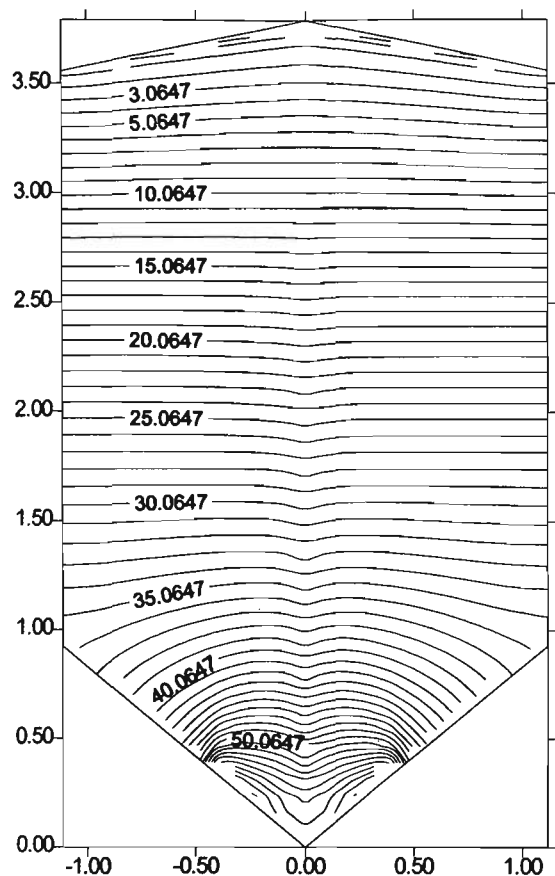


Figure 7.4 Pressure and velocity distributions in a silo fitted with annular aeration duct

7.3 TEMPERATURE DISTRIBUTIONS

Temperature changes in stored grain may come from two heat sources: Internal and external sources. Internal sources are the heat, generated by the respiration of grains, moulds and insects. External sources largely come from the atmospheric environment around the silo, especially solar energy which is transferred from the wall and the roof of the silo to create uncomfortably hot conditions.

The temperatures in the unaerated silo have been developed as shown in figure 7.8. The temperature distributions in the silo fitted with linear and annular aeration ducts are shown in figures 7.9 and 7.10 respectively. Comparison of three figures shows that for a same initial temperature of 30°C, and after 60 days storage, the centre temperature of the non-aerated silo remain at 26°C, in the silo fitted with the linear duct, the temperatures after 60 days has fallen to about 20°C, and in the silo fitted with the annular duct, the corresponding temperature is 16°C.

In figure 7.8, it can be seen that the centre temperature reduces typically average 1~2°C by every 20 days. This is because ambient temperatures are generally lower in Melbourne than that the initial grain temperatures in the centre of the silo.

In figure 7.9, it is clear that the grain temperature in a silo fitted with a linear duct falls quickly, and after 20 days storage, much of the grain on the side of the silo with the linear aeration duct is about 20°C. After 40 days aeration, the grain temperature is 20°C in the most of the centre region of the silo. After 60 days aeration, the temperature in the central region has not changed much. However, the volume of 20°C grain is slightly reduced, because the climate of Melbourne in February is warmer than that of January.

As figure 7.10 presented, after 20 days aeration, most of the grain in the silo fitted with an annular duct has a temperature about 19°C, as can be seen in figure 7.10. This

is because the annular aeration system has a symmetric layout, and the air flow distribution is uniform in the silo. After 40 days aeration, the grain in the centre region of the silo has fallen to around 16°C, After two months aeration, the temperature in the central region within the silo has increased somewhat to 18°C. This change is effected by the climatic conditions.

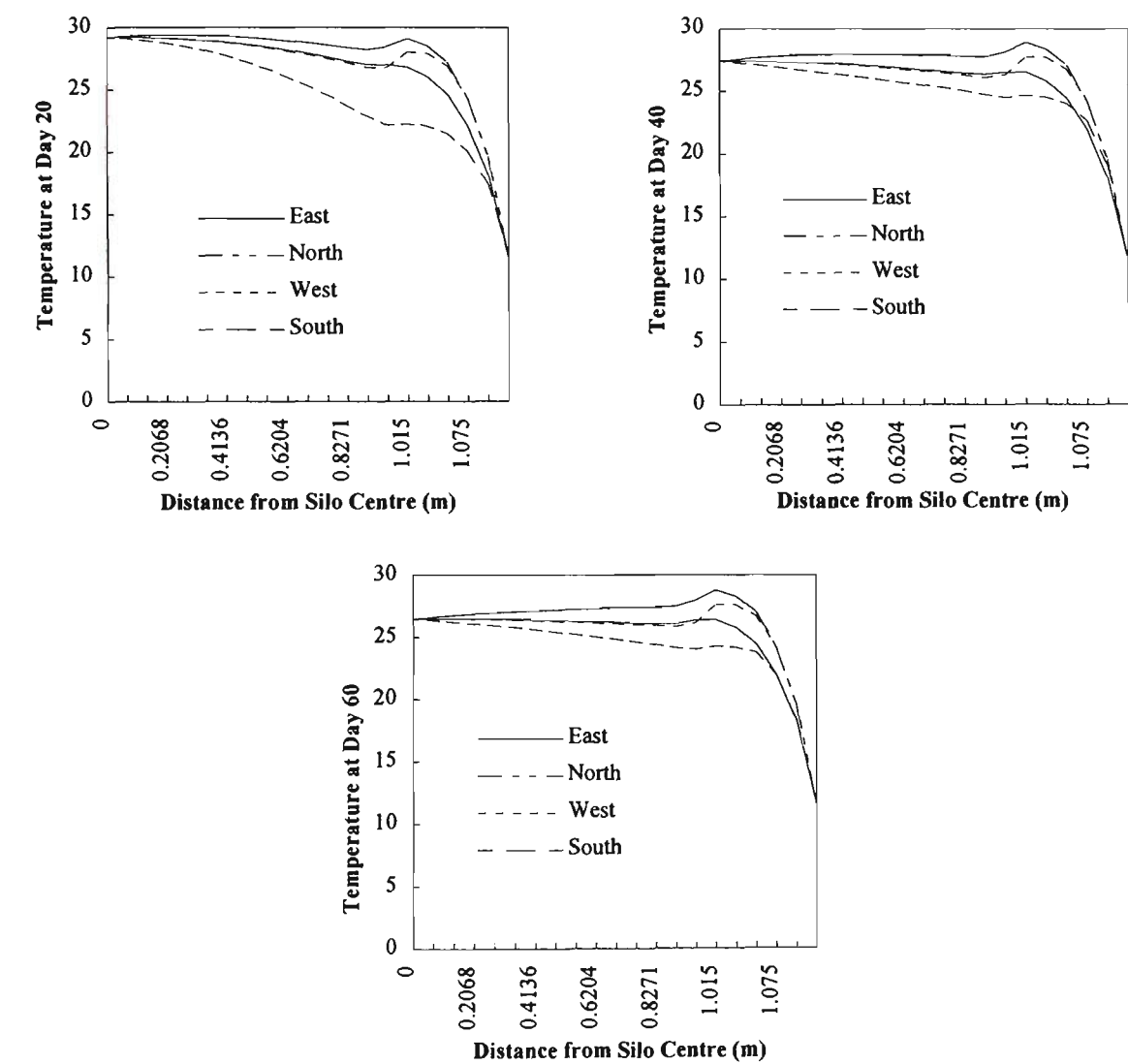


Figure 7.5 Radial profiles of the temperature in the non-aerated case

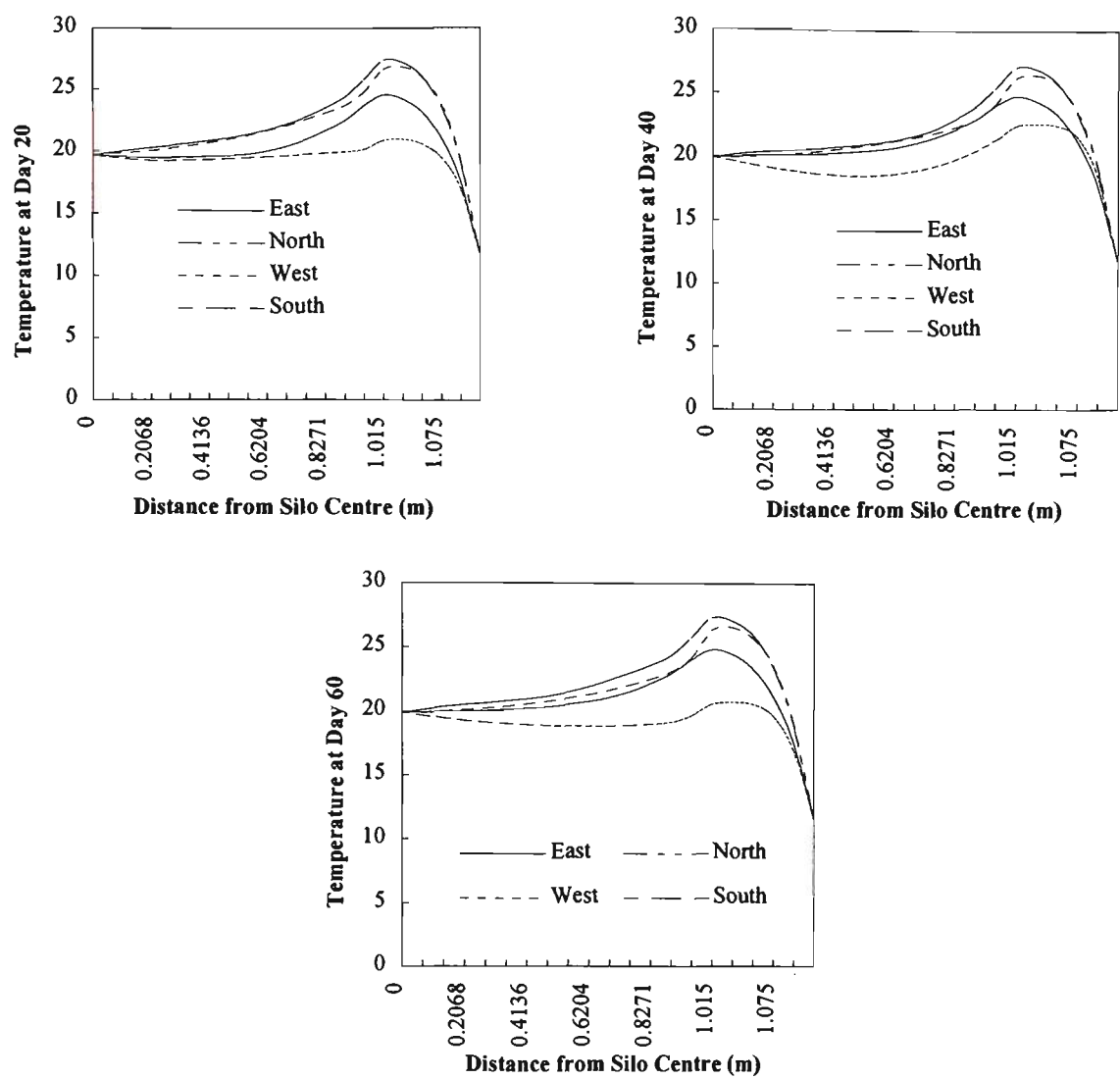
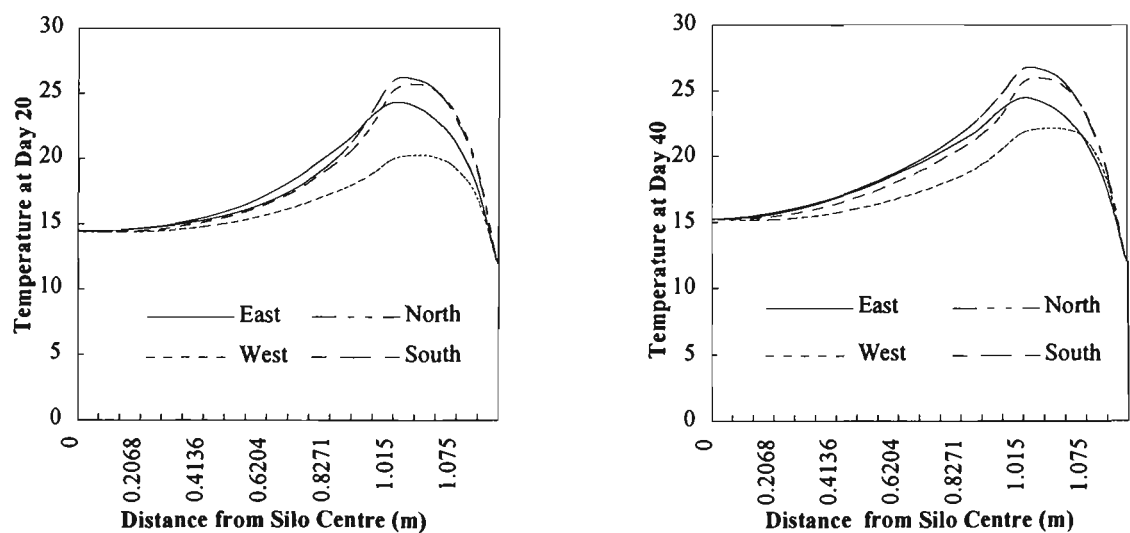


Figure 7.6 Radial profiles of the temperature in the linear duct case



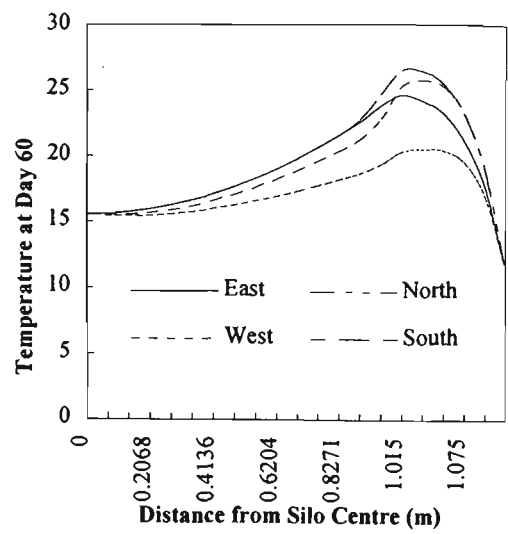


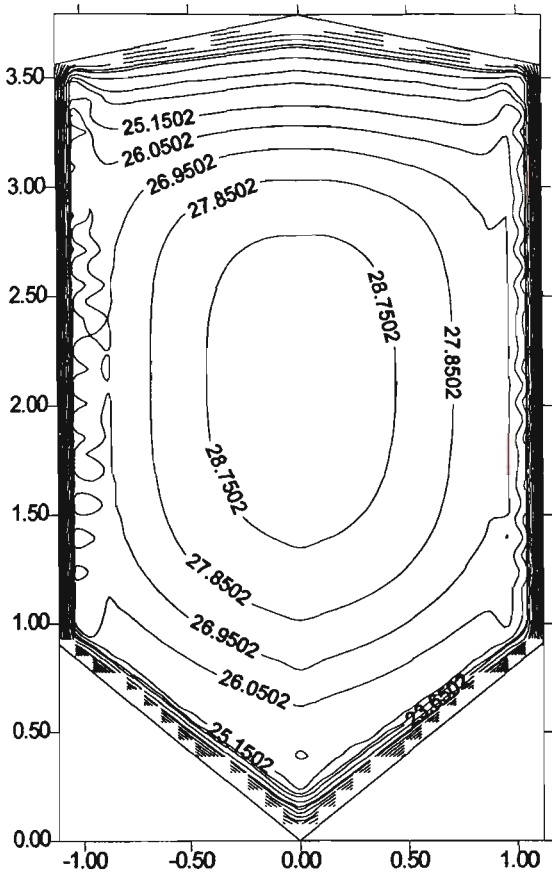
Figure 7.7 Radial profiles of the temperature in the annular duct case

Generally, the temperature of the stored grain does not change rapidly unless it is aerated. Figures 7.5, 7.6 and 7.7 reflect the temperature distributions show in figures 7.8, 7.9 and 7.10, that results from the imposition of varying temperatures in the east, north, west and south facing portions of the wall. It can be seen that the temperature of the grain in the centre of the non-aerated silo is much slower to cool than that in either of the two aerated silos, and it rises towards to the centre of silo (around 26-28 °C).

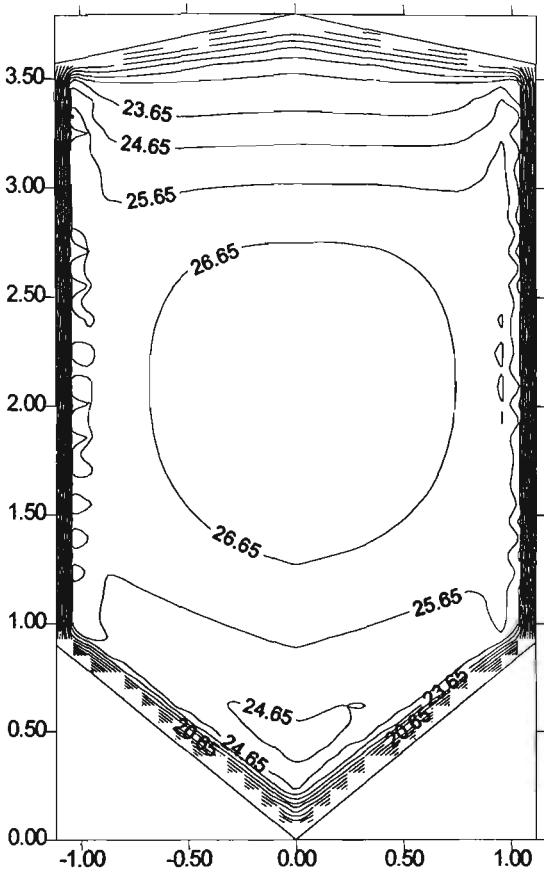
Figures 7.6 and 7.7 show that the aerated silo fitted with an annular duct performs much more effectually than the one fitted with a linear duct. The silo with the linear duct is cooler towards to the centre of the silo, around 19-20 °C, and the performance of annular aeration system is better towards to the centre of the silo, when grain temperatures in the region of 14-17 °C are observed.

Importantly, it can be seen that the temperature near the walls of all three cases considered are quite similar. Figures 7.5, 7.6 and 7.7 capture the situation during the night, when the walls of the silo are cold. At this time, the maximum temperature occurs about 10cm distant from those portions of the wall that are exposed to solar radiation.

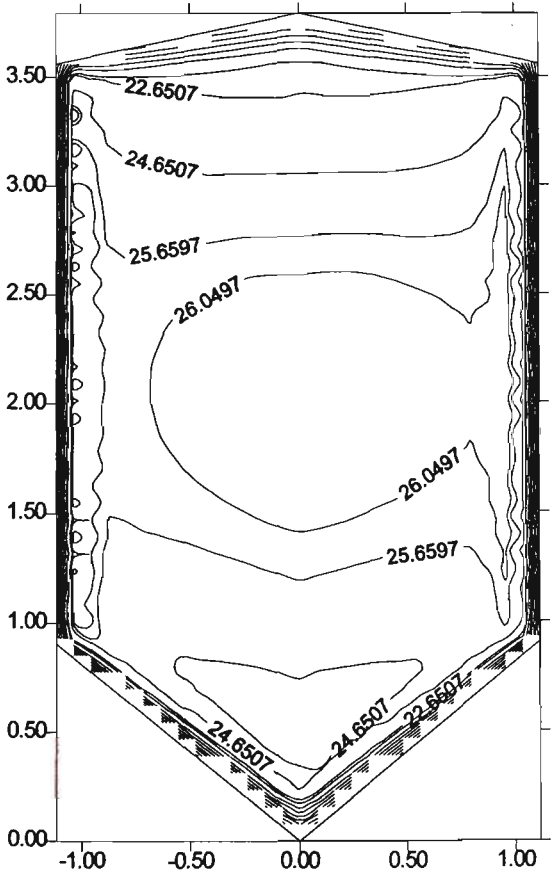
However, the grain near the southern wall, which receives no sunlight, has a minimum temperature similar to the mean ambient temperature. It is noteworthy that the maximum temperature occur on the north and west facing portions of the wall, where there is a combination of high ambient temperature, and a high intensity of solar radiation which is insolated particularly around noon.



Temperature at day 20 (non-aerated)

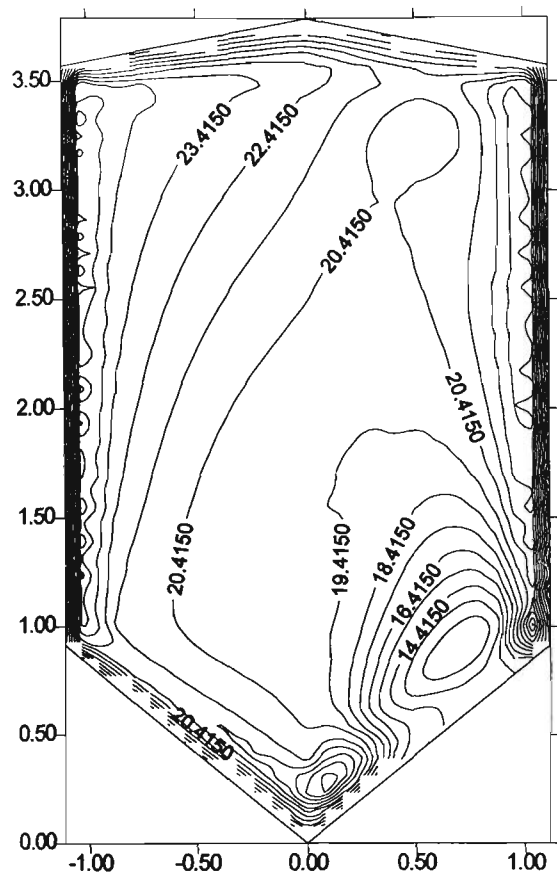


Temperature at day 40 (non-aerated)

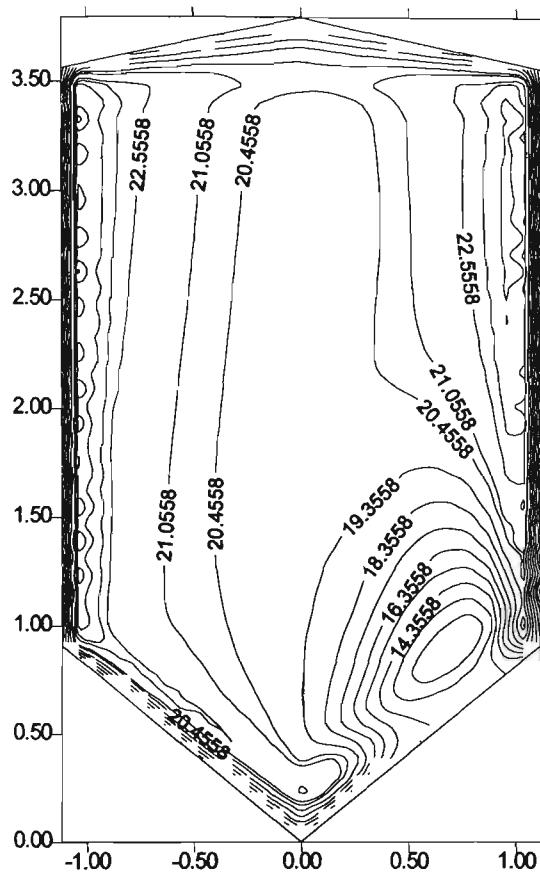


Temperature at day 60 (non-aerated)

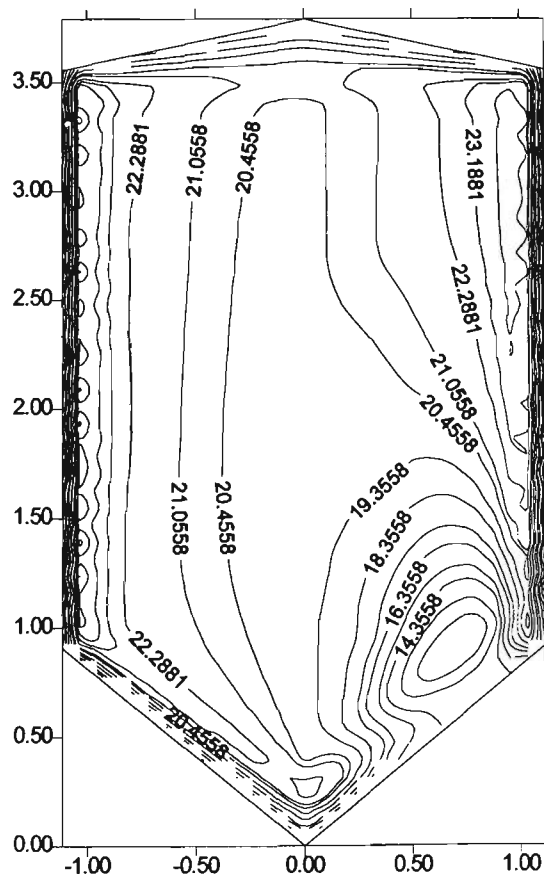
Figure 7.8 Temperature distributions in the non-aerated silo



Temperature at day 20 (linear duct)

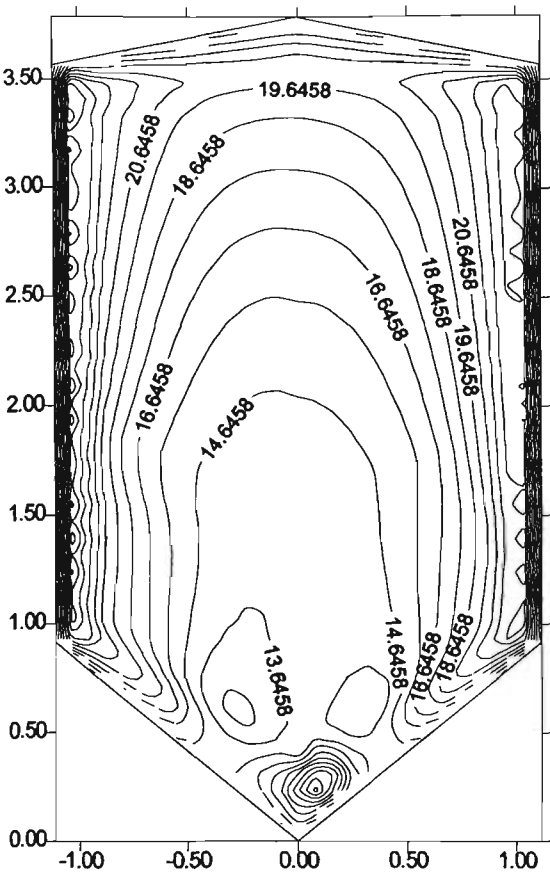


Temperature at day 40 (linear duct)

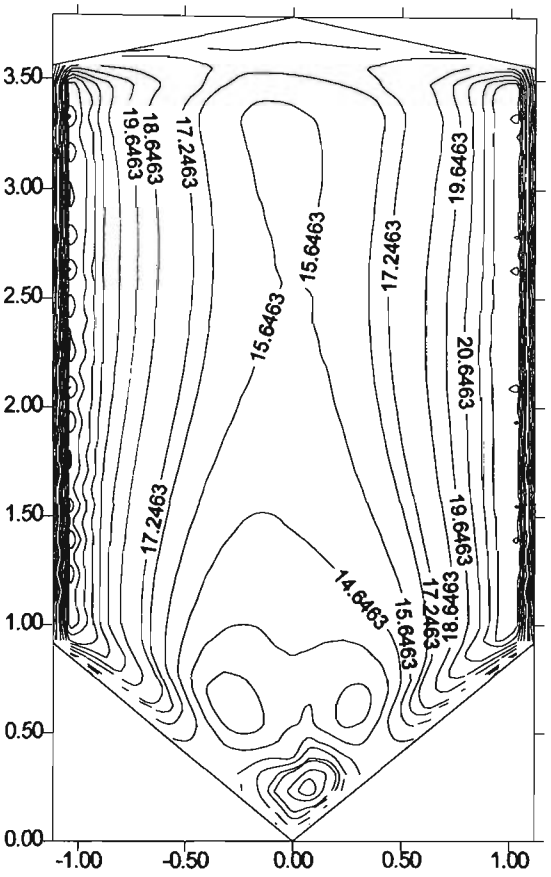


Temperature at day 60 (linear duct)

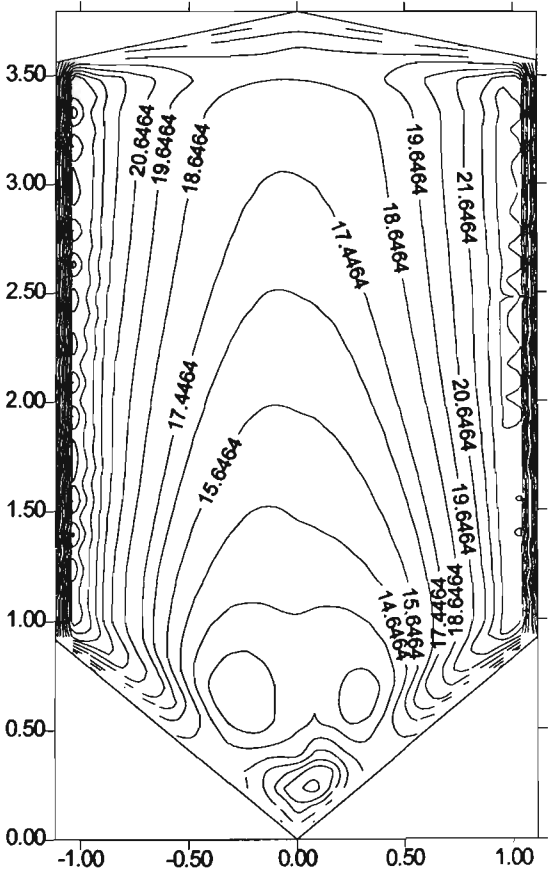
Figure 7.9 Temperature distributions in the silo fitted with a linear duct



Temperature at day 20 (annular duct)



Temperature at day 40 (annular duct)



Temperature at day 60 (annular duct)

Figure 7.10 Temperature distributions in the silo fitted with an annular duct

7.4 MOISTURE CONTENT DISTRIBUTIONS

Moisture content of grain denotes the quantity of water per unit mass of either wet or dry grain, and it is usually expressed on a percentage basis. Figures 7.14, 7.15 and 7.16 show the moisture content distributions in the non-aerated and the two aerated grain silos fitted with linear and annular ducts.

After 60 days simulation, compared with an initial condition of 13.64% (dry basis), we obtain: In the non-aerated silo, the centre region of grain moisture content is 13.63%, it is 0.07% (relative different, and as follows in this Chapter) lower than initial condition. In the silo fitted with the linear duct, the centre volume of the moisture content of grain has a 12.8% dry basis, it is 7% lower than the initial condition, and in the silo fitted with an annular duct, it is 12.36%, this is about 10% less than the initial moisture content.

Figure 7.14 that indicates the non-aerated silo during first 20 days storage, the moisture diffuse causes a high moisture content to develop at the bottom and the walls of the silo which have low temperatures, and the maximum moisture content is about 13.75%. However, molecular diffusion alone can not be the cause of the apparently rapid increase of grain moisture content near the boundaries of the silo. Such process would requires months, not days. It is suspected that respiration is the cause of the build up in moisture content, and whether or not this reflects reality is discussed below.

In figure 7.15, after 20 days aeration, the low temperature and the high relative humidity in the silo with linear aeration system is occurred around the duct, and the moisture content of the grain is therefore high. At the centre of the silo, the moisture content decreases to about average 12.8% dry basis. After 40 days aeration, the moisture content increases near the duct zone, and reduces in the centre of the silo. After 60 days aeration, the moisture content at upper surface of silo is about 4% lower

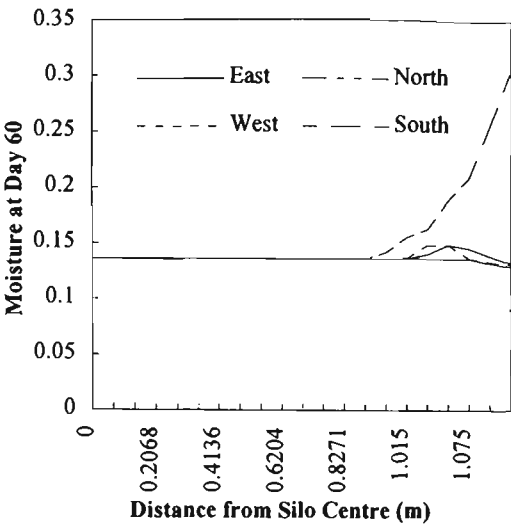


Figure 7.11 Radial profiles of the moisture content in the non-aerated case

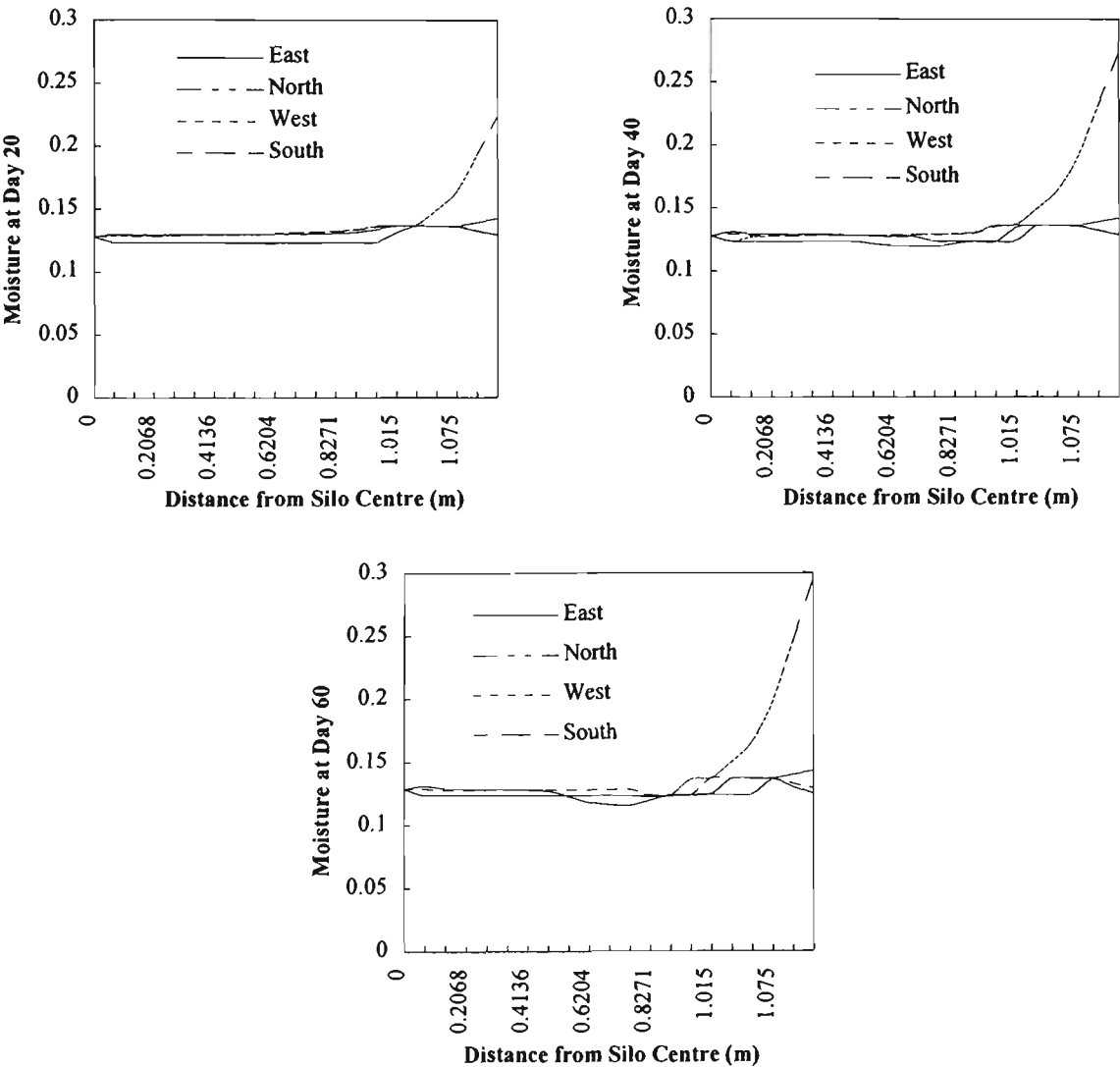


Figure 7.12 Radial profiles of the moisture content in the linear duct case

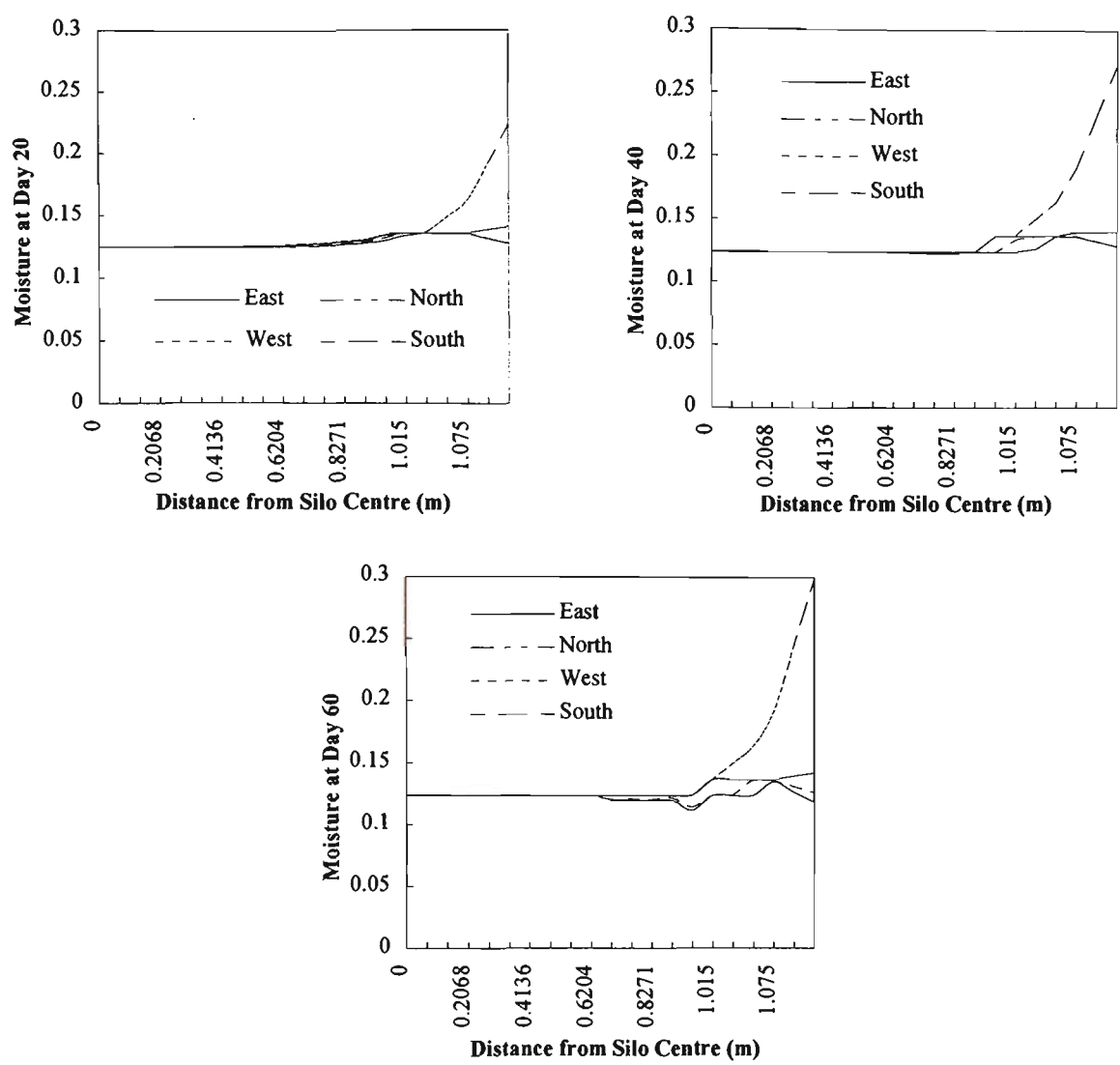


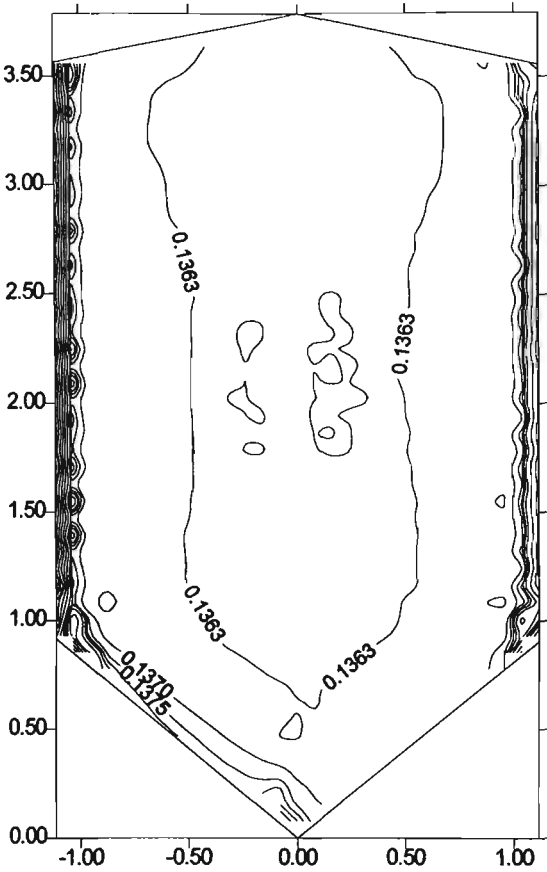
Figure 7.13 Radial profiles of the moisture content in the annular duct case

Figures 7.11, 7.12 and 7.13 show that the variation of moisture content from the centre of the silo to the facing of east, north, west and south sides of the silo in the cases of non-aerated and the two aeration systems considered. As would be expected, the moisture content of the grain in the centre of the non-aerated silo changes imperceptibly. However, the grain moisture content does decrease slightly in the centre of the silos fitted with linear and annular aeration ducts, this is expected from the work of Sutherland *et al.* (1971), who show that the passage of a cooling wave is associated with a fall in grain moisture content.

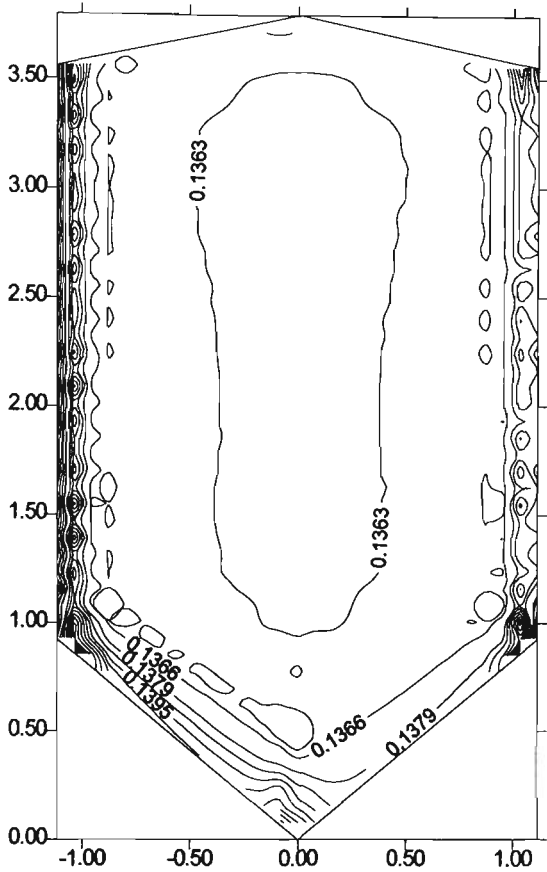
It has observed that the moisture content changes occur in the vicinity of the walls of both non-aerated and aerated silos. It is particularly noteworthy that on the coldest southern sides of all three causes are considered, the grain moisture content is observed to increase considerably. Figure 7.11 also indicates that the moisture migration is important up to about 10 cm away from the silo wall.

However, the apparent moisture migration to the southern of the wall occurs both non-aerated and aerated silos, as suggested above, the increase in moisture content may have resulted from respiration.

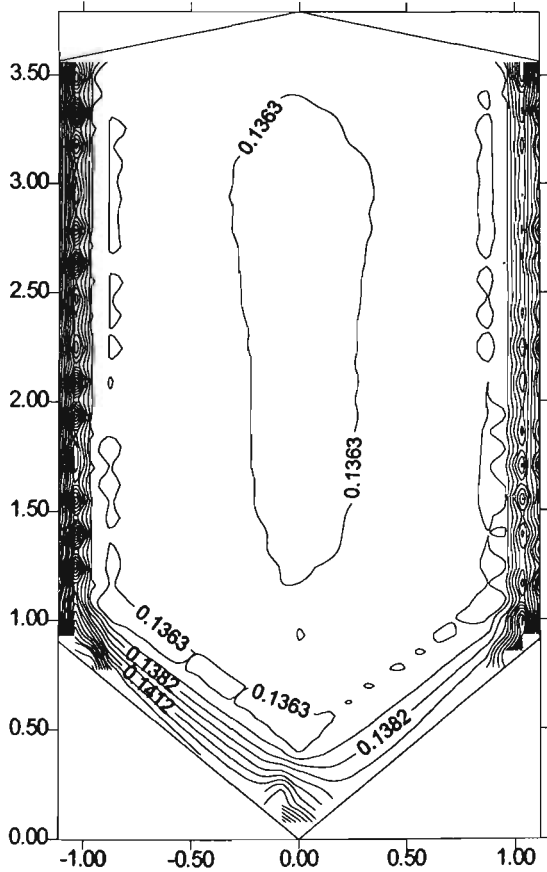
Furthermore, the grain moisture content is generally lower throughout the aerated silo than through the unaerated silo, this is consistent with the physics of one-dimensional heat and mass transfer processes that occur in grain (Thorpe, 1986).



Moisture content at day 20 (non-aerated)

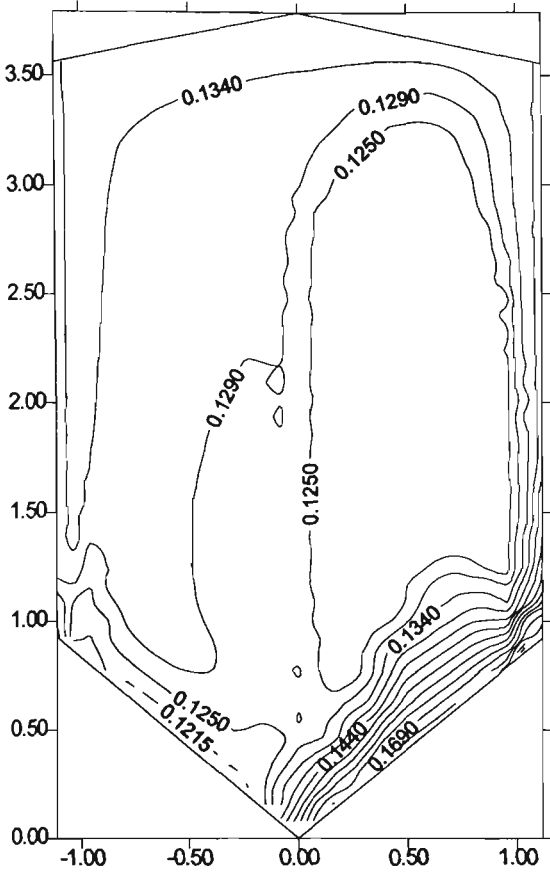


Moisture content at day 40 (non-aerated)

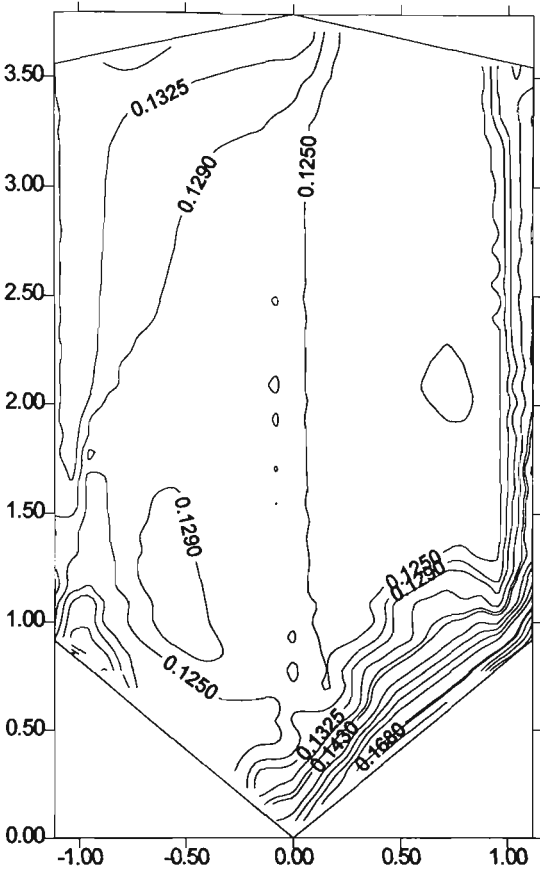


Moisture content at day 60 (non-aerated)

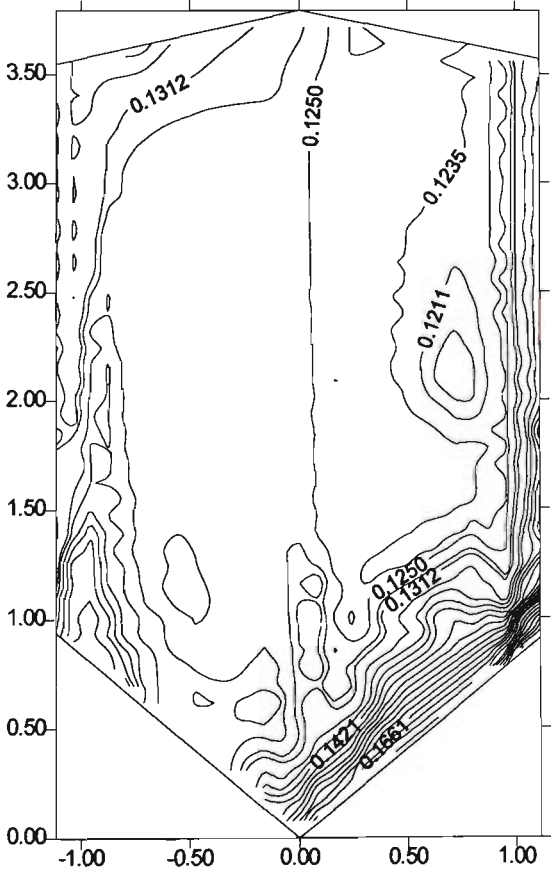
Figure 7.14 Moisture content distributions in the non-aerated silo



Moisture content at day 20 (linear duct)

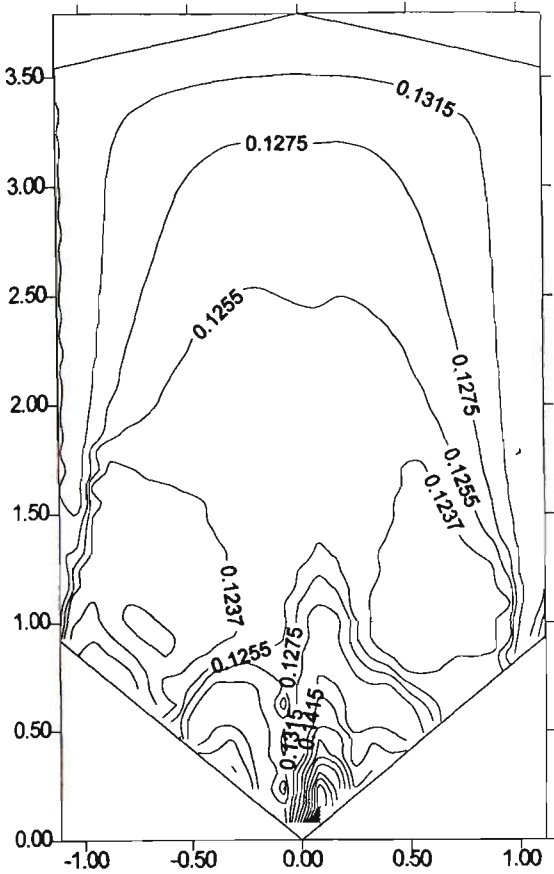


Moisture content at day 40 (linear duct)

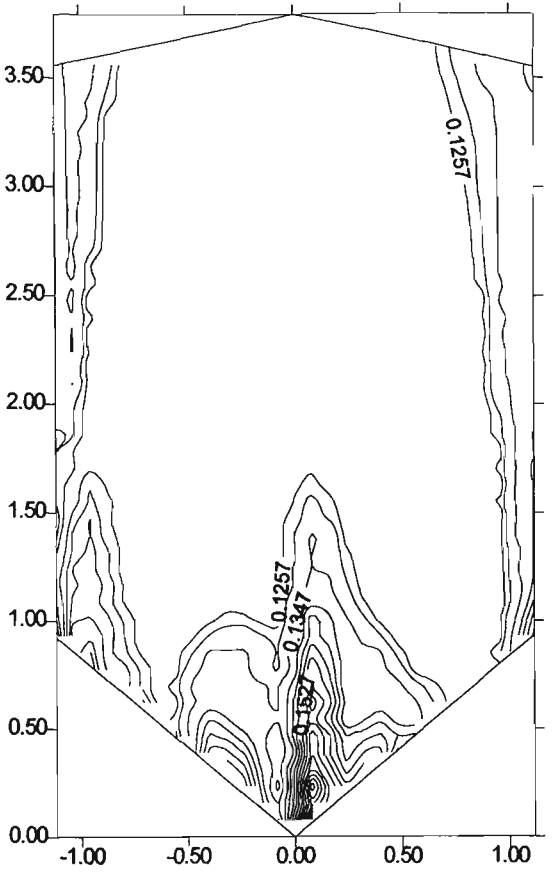


Moisture content at day 60 (linear duct)

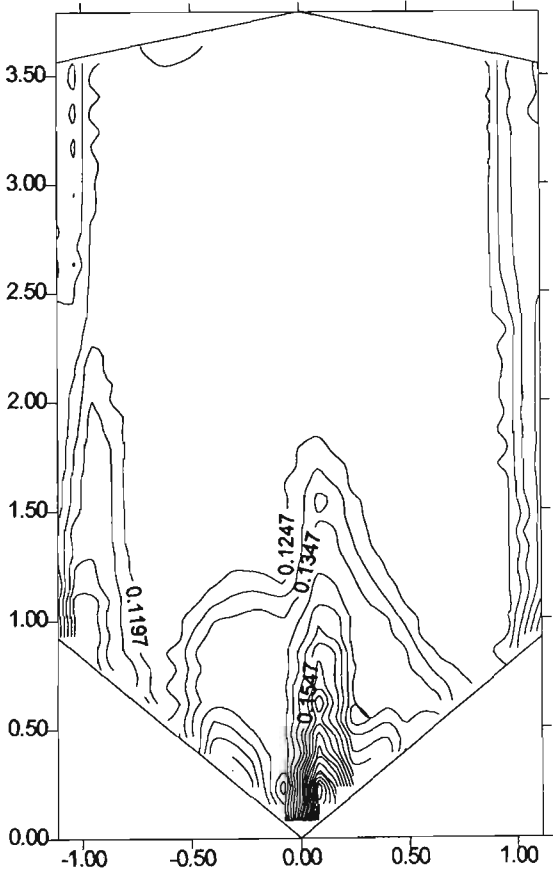
Figure 7.15 Moisture content distributions in the silo fitted with a linear duct



Moisture content at day 20 (annular duct)



Moisture content at day 40 (annular duct)



Moisture content at day 60 (annular duct)

Figure 7.16 Moisture content distributions in the silo fitted with an annular duct

7.5 ABSOLUTE HUMIDITY DISTRIBUTIONS

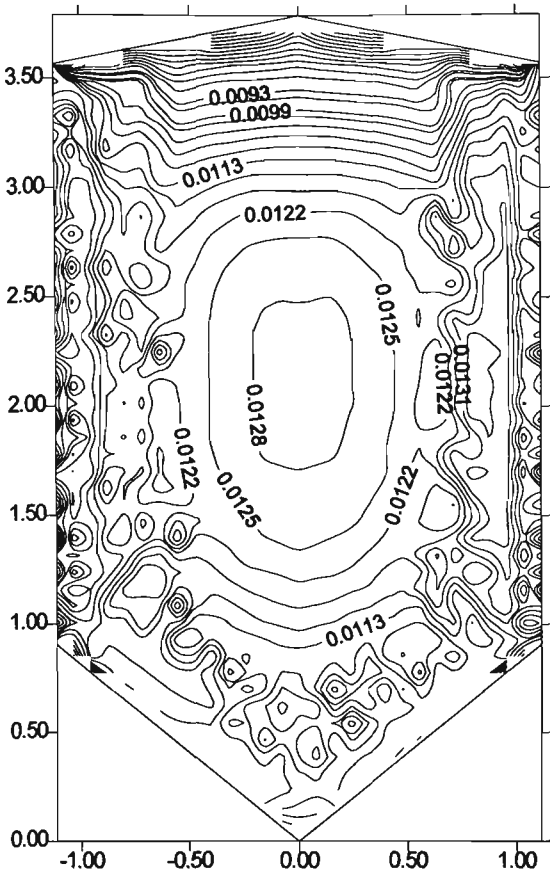
Absolute humidity of air is the mass of water vapour present in one kilogram grain of dry air. The absolute humidity of air is dependant on the temperature and grain moisture content, and these three variables are related by the sorption isotherm. The contour maps of absolute humidity of air in the non-aerated silo, and the silos fitted with linear and annular ducts are shown in figures 7.17, 7.18 and 7.19.

It is clear that after 60 days storage, with an initial humidity of 0.0136kg/kg, the absolute humidity of air in the non-aerated silo of the central region falls to 0.0106kg/kg, which is 28% less than initial condition. In the aerated silo fitted with a linear duct, the humidity is 0.0069kg/kg, this is 97% lower than the initial humidity condition. In the annular duct case, the absolute humidity of air at centre region is 0.0048kg/kg, about 183% lower than the initial condition.

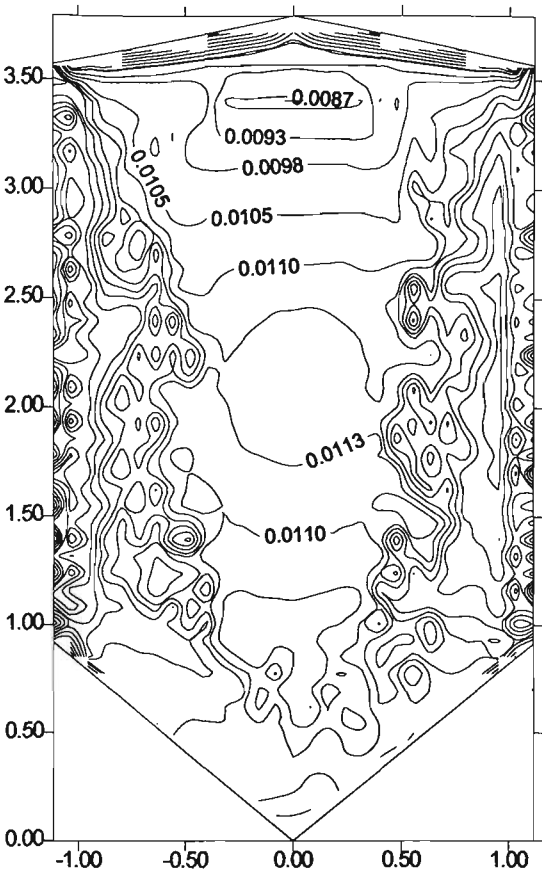
The main reason for the lowering of the humidities is the decrease in grain temperature, although drying of the grain contributes to the decrease in humidity.

The contour plots of the humidity of the intergranular air appear to be very noisy, and this is clearly shown in figure 7.17. One reason for this is that the model predicts very small humidity gradients in the grain bulk, but their presence is amplified by the plotting routine.

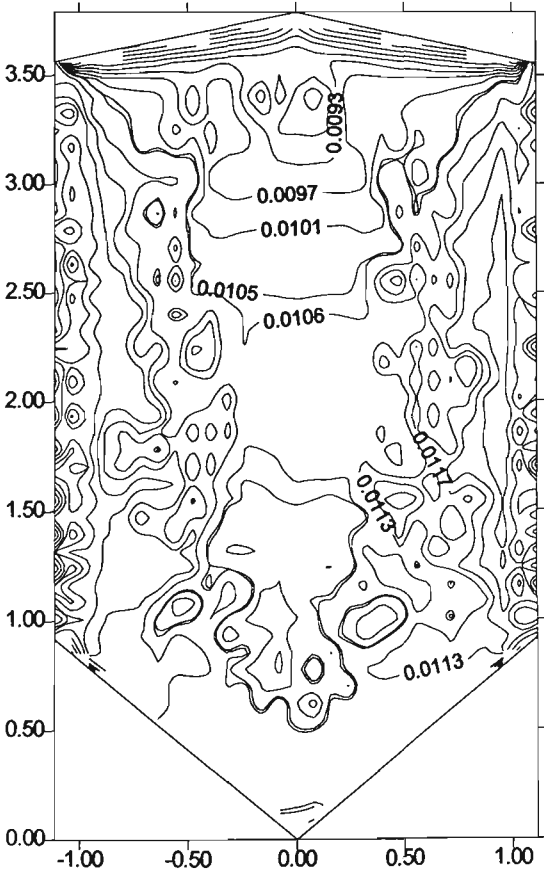
As might be expected, the higher absolute humidities appear near the linear aeration duct (as shown in figure 7.18). In the case of the silo fitted with an annular duct (it is indicated in figure 7.19), the high absolute humidity of air near the base of the cone reflects the respiration (actual or simply as a result of an artifice of the model) alluded to above.



Humidity at day 20 (non-aerated)

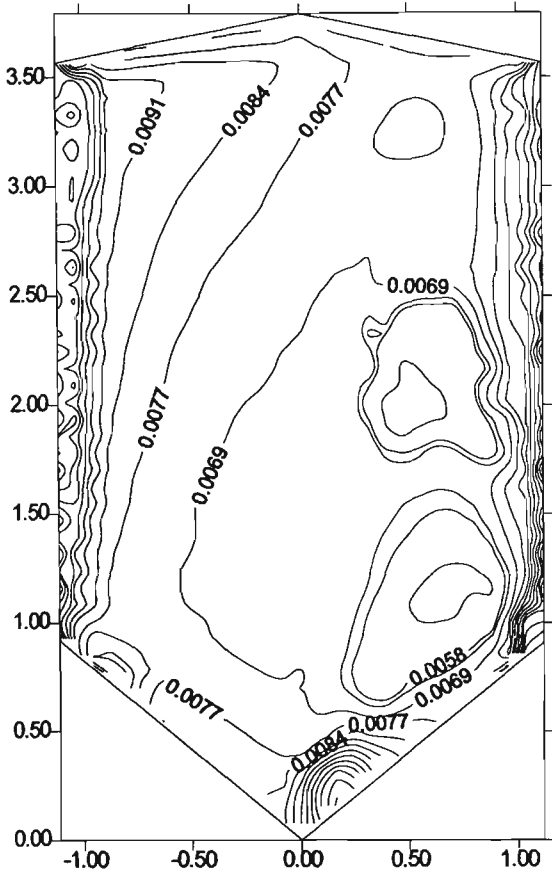


Humidity at day 40 (non-aerated)

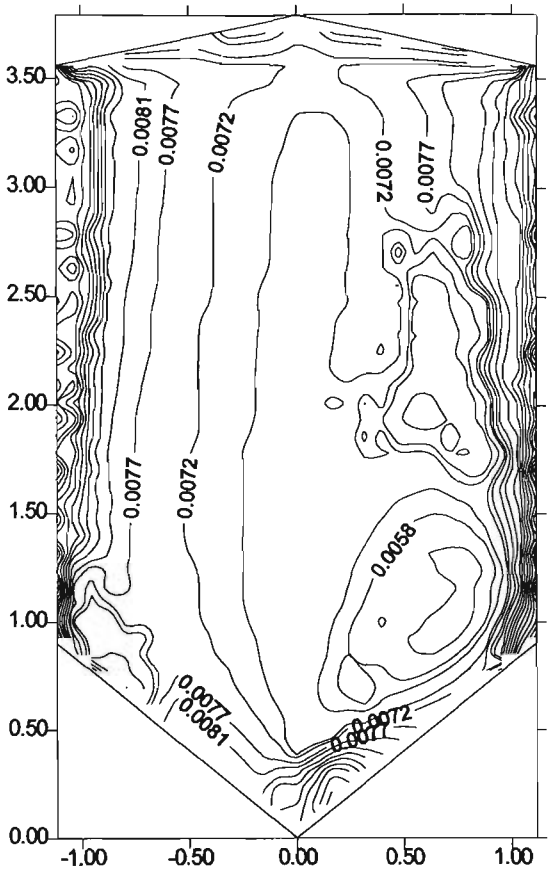


Humidity at day 60 (non-aerated)

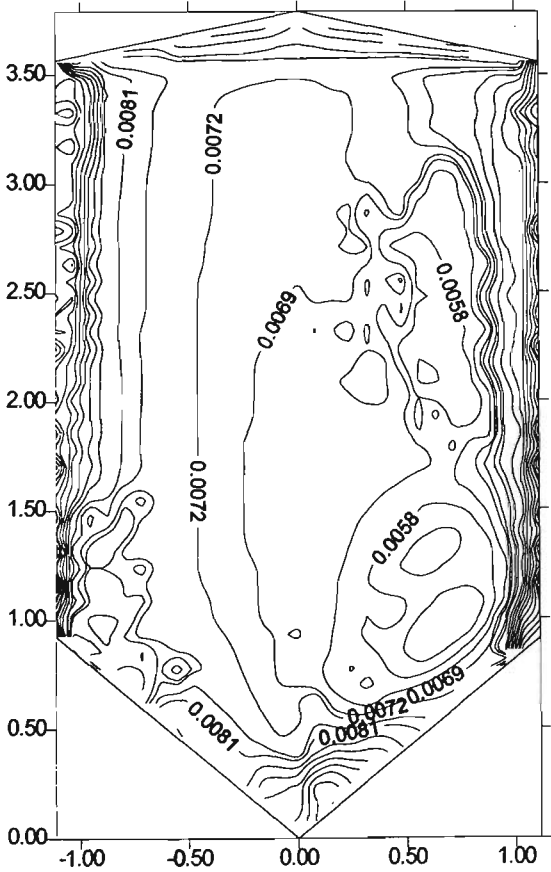
Figure 7.17 Humidity distributions in the non-aerated silo



Humidity at day 20 (linear duct)

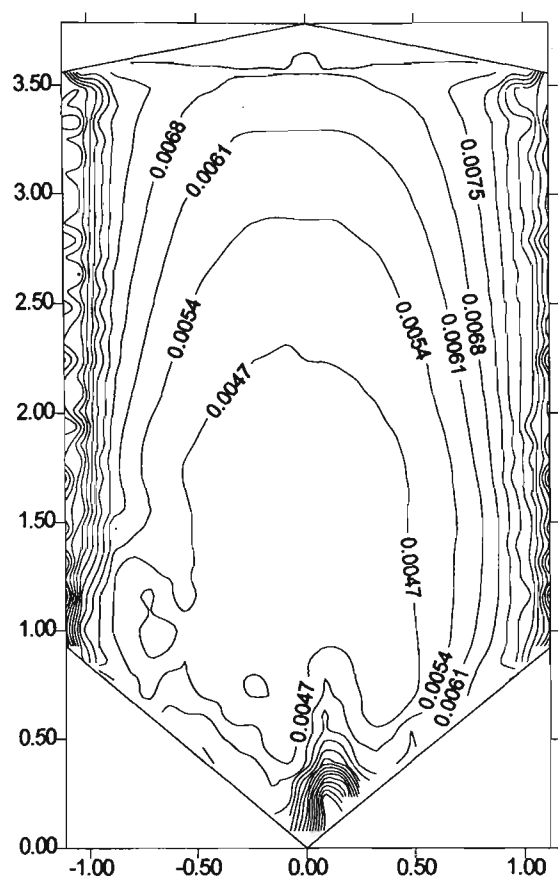


Humidity at day 40 (linear duct)

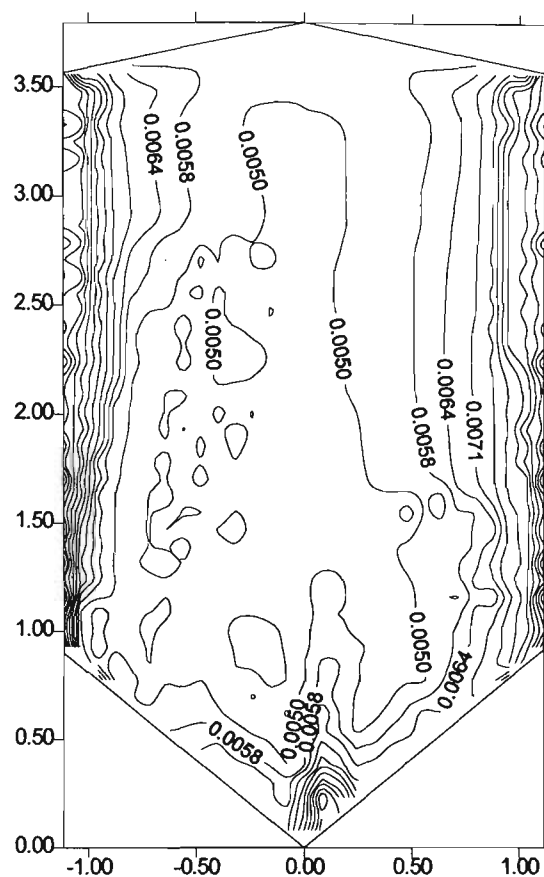


Humidity at day 60 (linear duct)

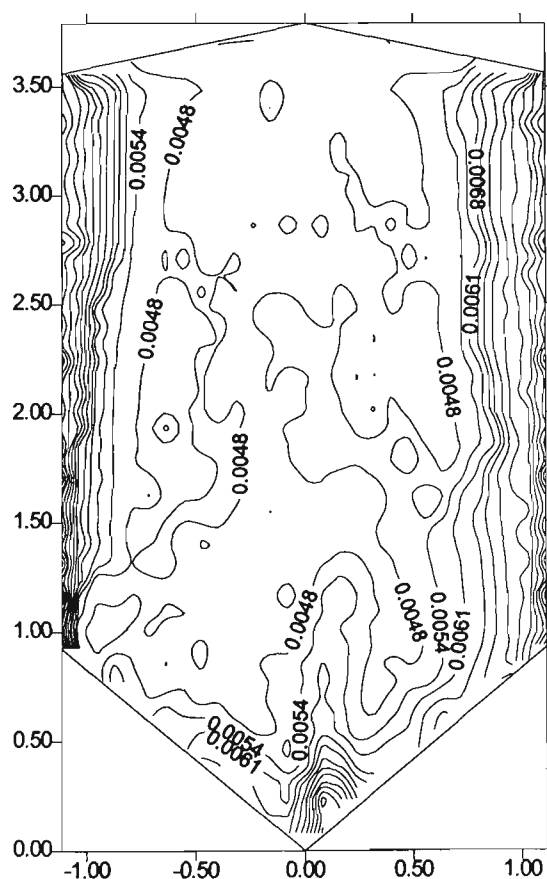
Figure 7.18 Humidity distributions in the silo fitted with a linear duct



Humidity at day 20 (annular duct)



Humidity at day 40 (annular duct)



Humidity at day 60 (annular duct)

Figure 7.19 Humidity distributions in the silo fitted with an annular duct

7.6 WET BULB TEMPERATURE DISTRIBUTIONS

Wet bulb temperature is the temperature reached by moist air and water, if the air is adiabatically saturated by evaporating the water. Wet bulb temperature in many way dictates the performance of aeration system, and it may be described as the joint effect of temperature and moisture content on the rate of increase of insect population. The contour maps of wet bulb temperature are presented in figures 7.20, 7.21 and 7.22.

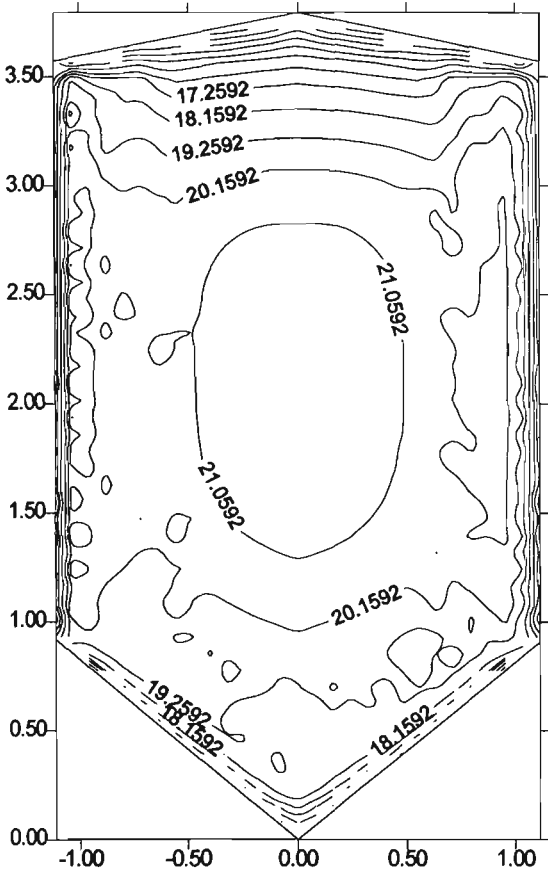
After 60 days storage with an initial wet bulb temperature of 22.3°C , in the non-aerated silo, the average of wet bulb temperature at centre region is 19.1°C , and in the linear duct aeration system is 14.1°C . In the silo fitted with annular aeration duct, the wet bulb temperature at centre area is 10.5°C .

In figure 7.20, it can be seen that in the non-aerated silo, after 20 days storage, the highest wet bulb temperature in the central region of the silo is about 21°C . After 40 days storage, the wet bulb temperature is continues to reduce due principally to conduction cooling. After 60 days storage, the wet bulb temperature at upper surface of grain has fallen to 17.3°C .

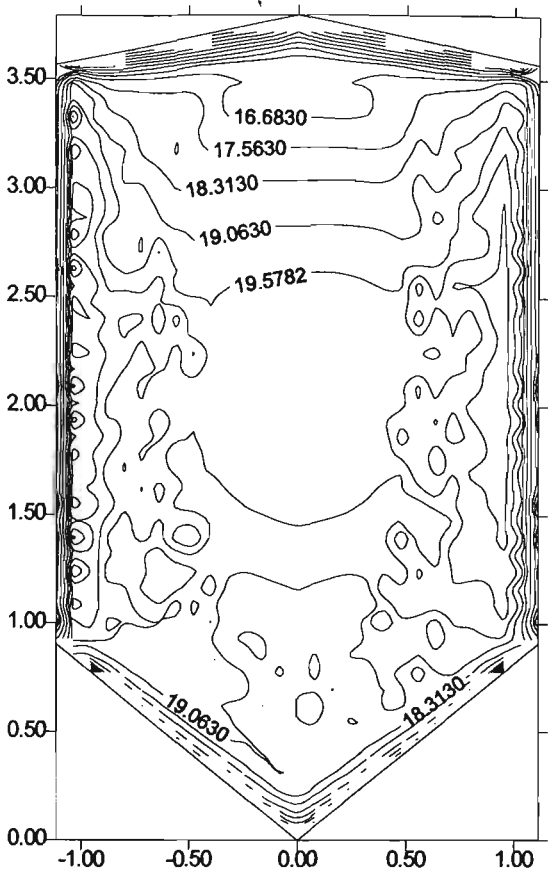
In the silo fitted with a linear aeration duct (as shown in figure 7.21), the wet bulb temperature falls most quickly in the region near the duct. It can be observed that a cooling front passes from the duct, and that the region of grain furthest from the duct is the slowest to cool. It is seen that little cooling occurs after day 40, when there appears to be a dynamic equilibrium set up by continued cooling being offset by conduction heating.

Figure 7.22 again shows, the passage of a cooling front from the annular duct and some dynamic equilibrium also appear to be approached. Most of the grains have attained wet bulb temperature around 10°C , which is inimical to insect population

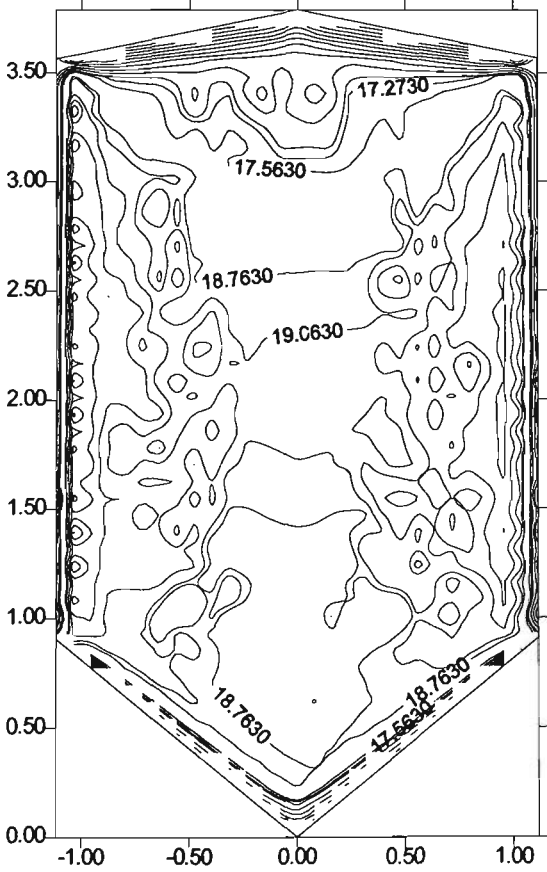
growth. It is noted that the distribution of the intergranular wet bulb temperature is asymmetrical as a result of uneven heating of the silo wall caused by the combined effects of solar radiation and ambient temperature.



Wet bulb temperature at day 20 (non-aerated)

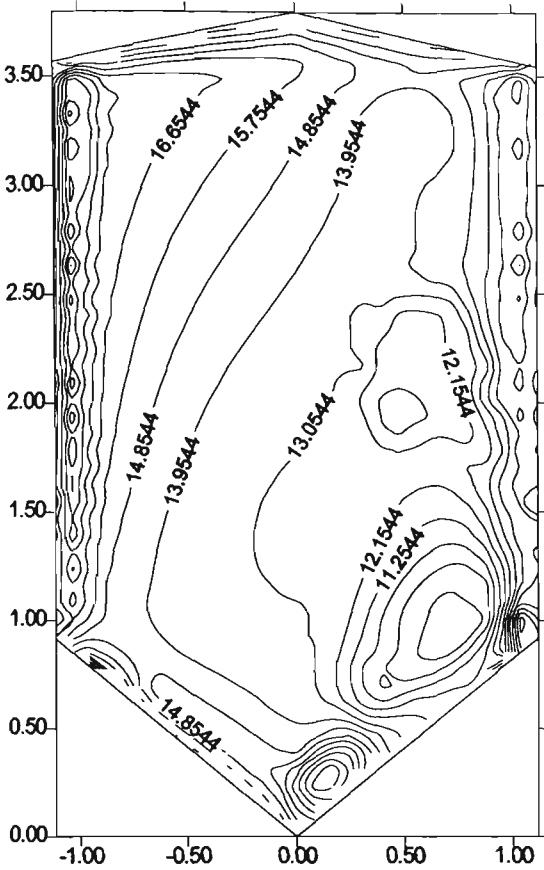


Wet bulb temperature at day 40 (non-aerated)

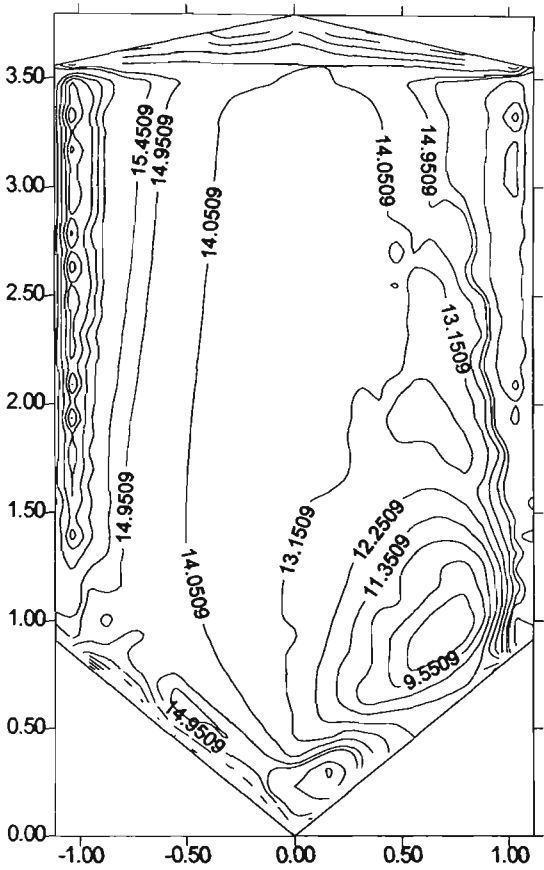


Wet bulb temperature at day 60 (non-aerated)

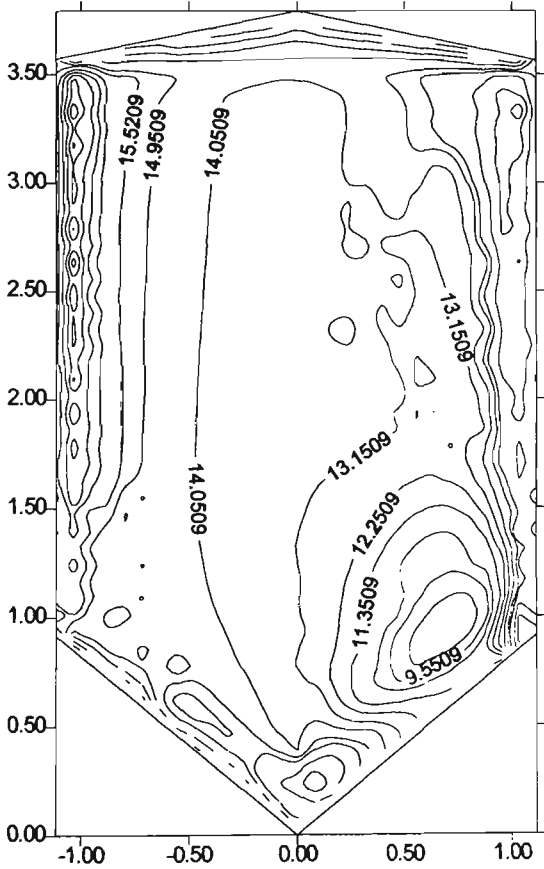
Figure 7.20 Wet bulb temperature distributions in the non-aerated silo



Wet bulb temperature at day 20 (linear duct)



Wet bulb temperature at day 40 (linear duct)



Wet bulb temperature at day 60 (linear duct)

Figure 7.21 Wet bulb temperature distributions in the silo fitted with a linear duct

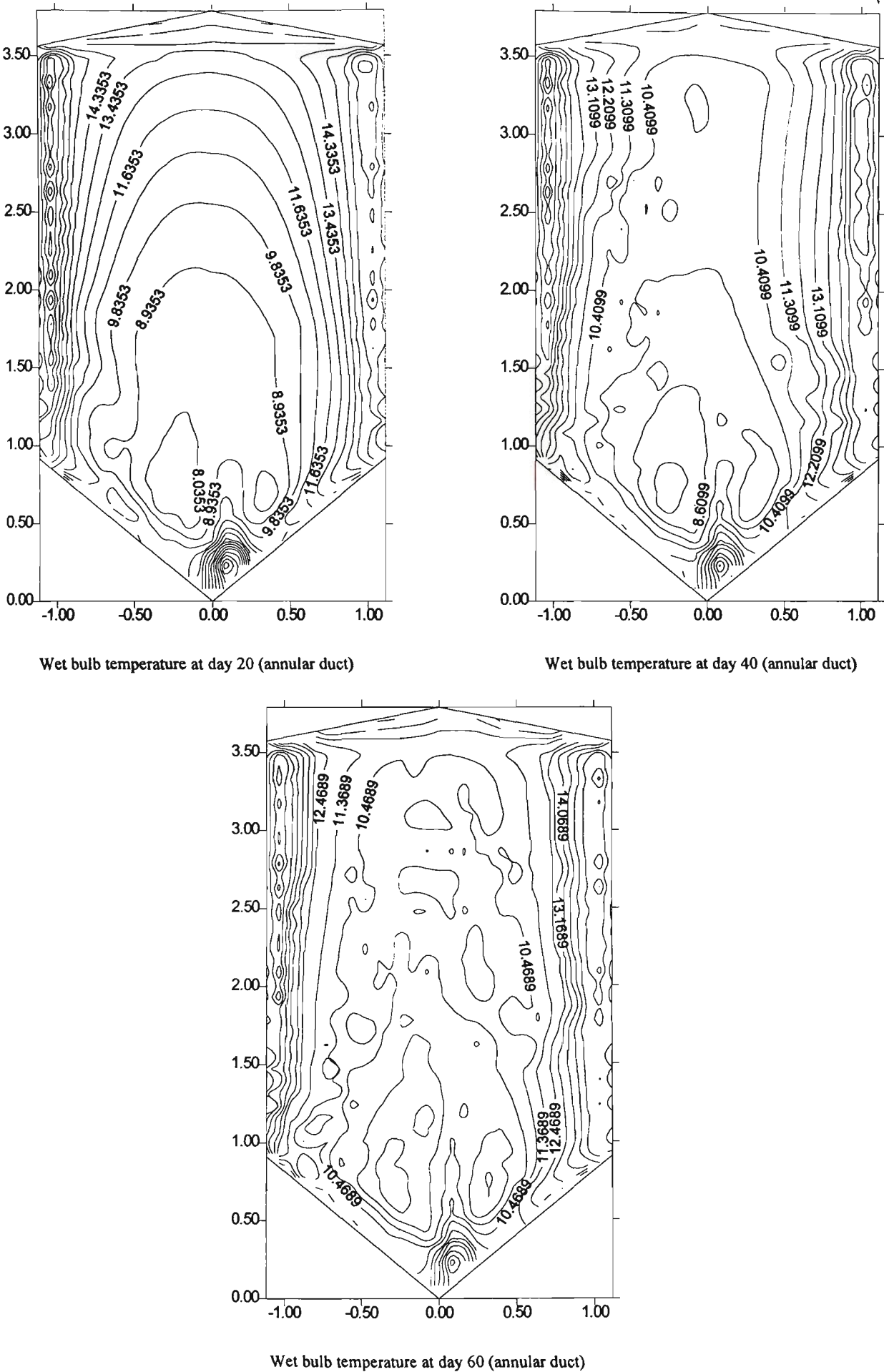


Figure 7.22 Wet bulb temperature distributions in the silo fitted with an annular duct

7.7 DRY MATTER LOSS DISTRIBUTIONS

Dry matter loss of grain results from an oxidative process accompanied by the release of carbon dioxide, water and heat. In the system considered in this thesis, the amount of dry matter loss occurs as a result of respiration, which occurs in the vicinity of the aeration duct, and the south facing wall. The rate of dry matter loss is a function of grain temperature, grain moisture content and time.

In the non-aerated simulation, no dry matter loss is evident on the east-west section of the grain store, because the grain stays very dry.

Dry matter loss in the silo fitted with the linear duct is observed near the aeration duct, as can be seen from figure 7.26. When the air enters the grain with a high relative humidity, the mass flow rate of air per unit volume of grain is very high in this region, and the grain becomes moist. From the initial dry matter loss of zero, after 20 days aeration, the maximum value of dry matter loss is 0.0136. After 40 days aeration, the maximum value is become to 0.0555, which is 308% higher than after 20 days aeration. After 60 days aeration, the maximum dry matter loss has reached 0.0701, this is 415% higher than after 20 days aeration.

Compared with whole the system, the total loss of dry matter is very small. In addition, the grain moisture content may increase as a results of respiration of moulds.

Moisture content is not observed in the cases of the silo aerated with an annular duct, as shown in figure 7.27, perhaps because the flow rate of air per unit volume of grain is somewhat lower. Hence the moisture in the air is adsorbed by a large volume of grain, so the dry matter loss near the annular duct does not appear to be a problem. Only at the base cone of the silo, the dry matter loss is seen to increase slightly. This is

because after the storage period, the respiration of grain appears to occur, thus giving rise to the production of moisture and dry matter loss.

Figures 7.23, 7.24 and 7.25 reflect moisture and temperature changes in the grain adjacent to the south facing portion of the wall. It is clear that aeration appear to have negligible effect on the rate of dry matter loss in these south facing regions.

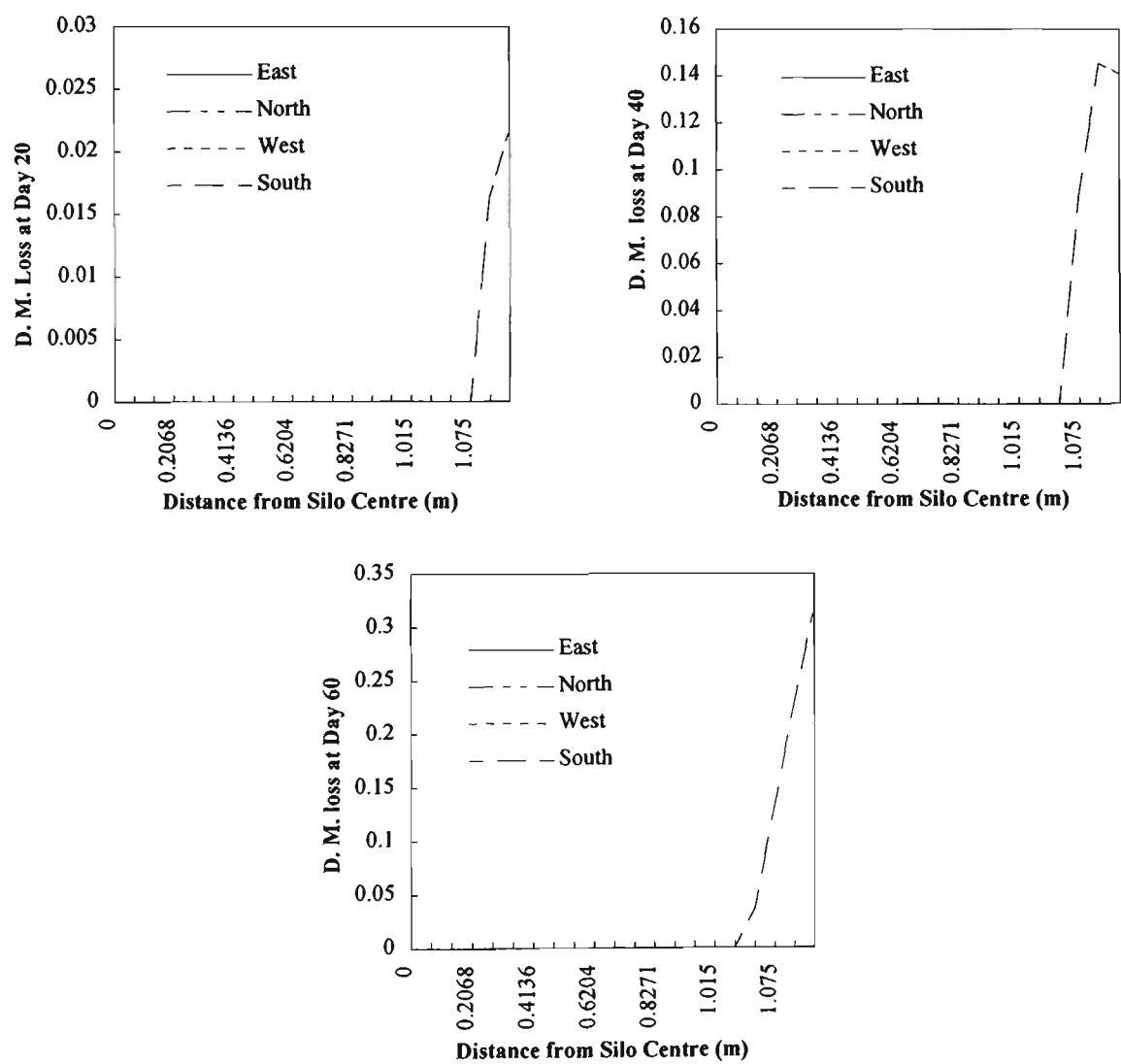


Figure 7.23 Radial profiles of the dry matter loss in the non-aerated case

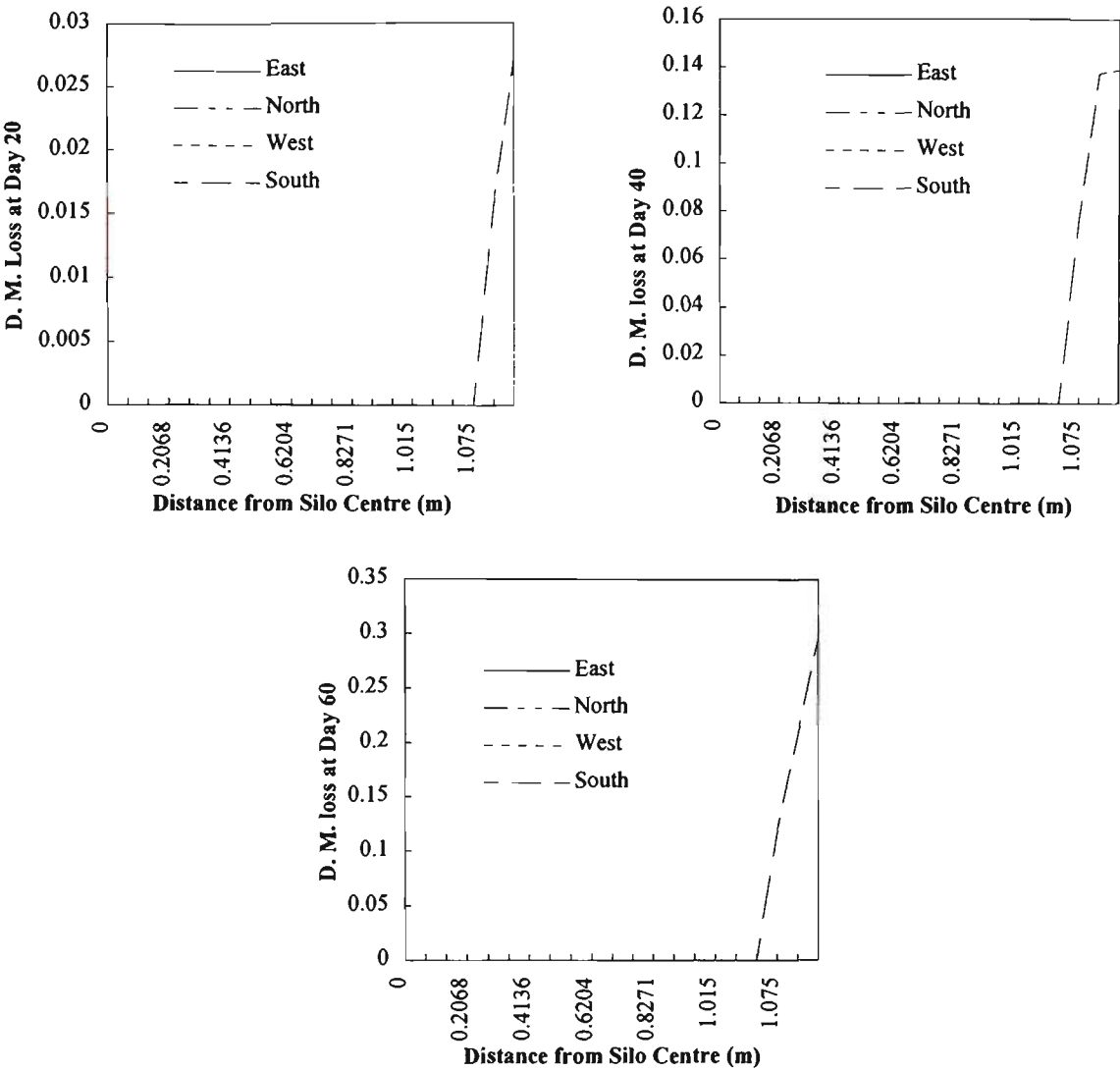
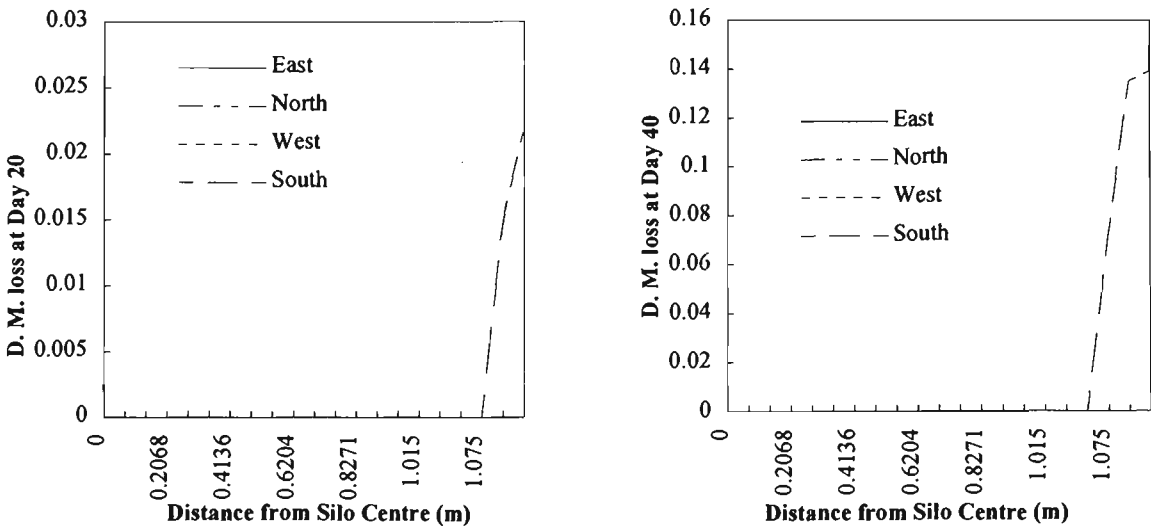


Figure 7.24 Radial profiles of the dry matter loss in the linear duct case



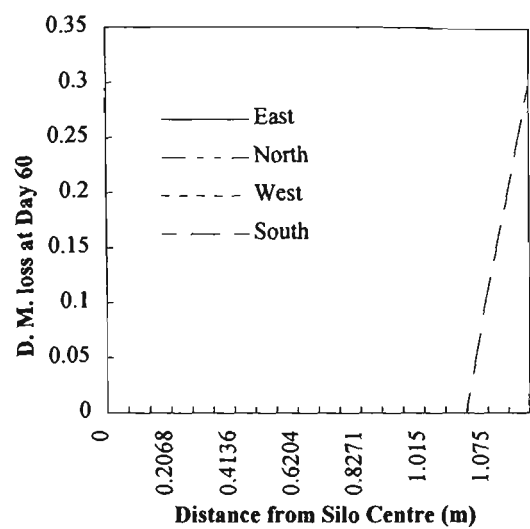


Figure 7.25 Radial profiles of the dry matter loss in the annular duct case

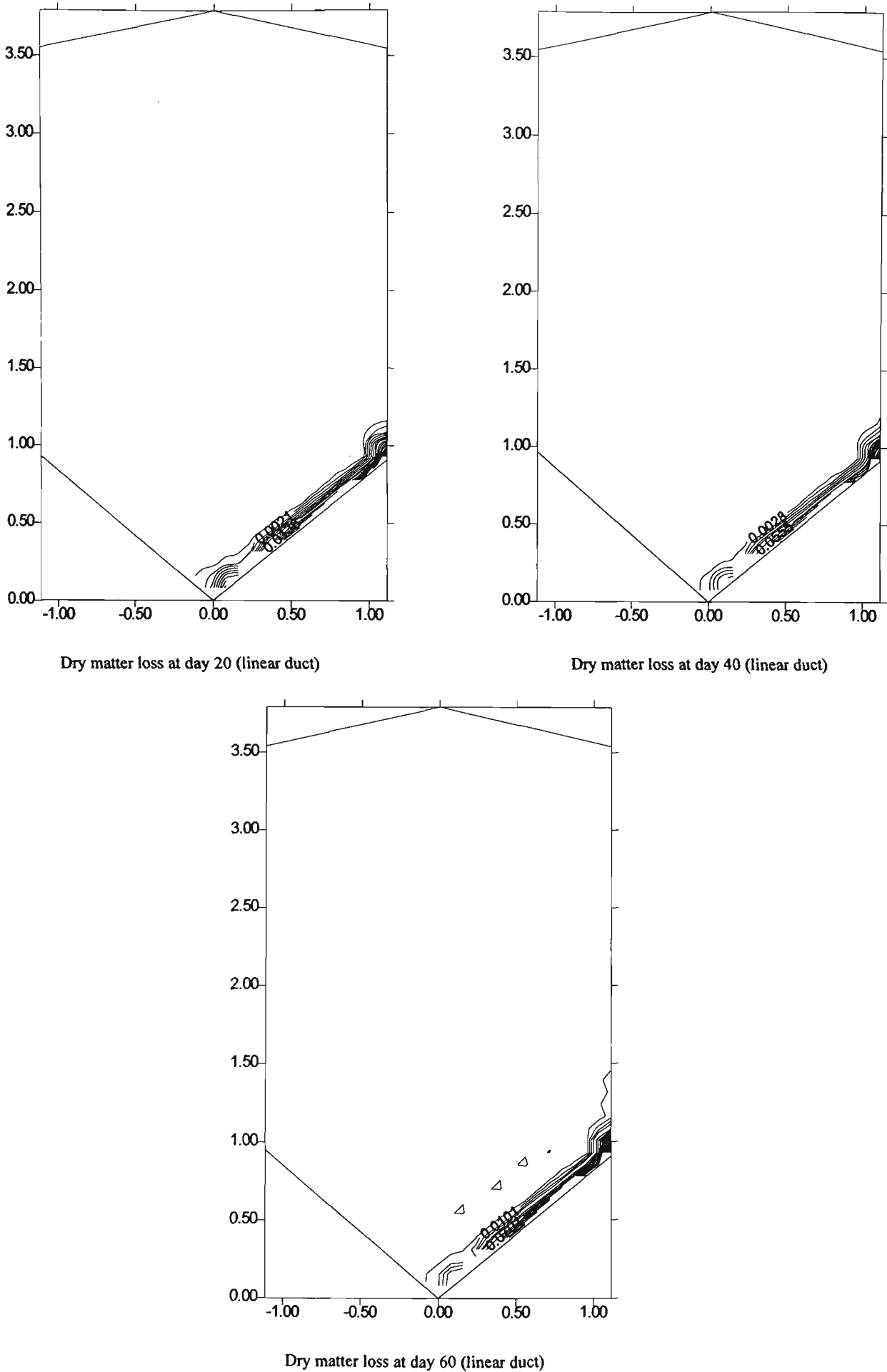


Figure 7.26 Dry matter loss distributions in the silo fitted with a linear duct

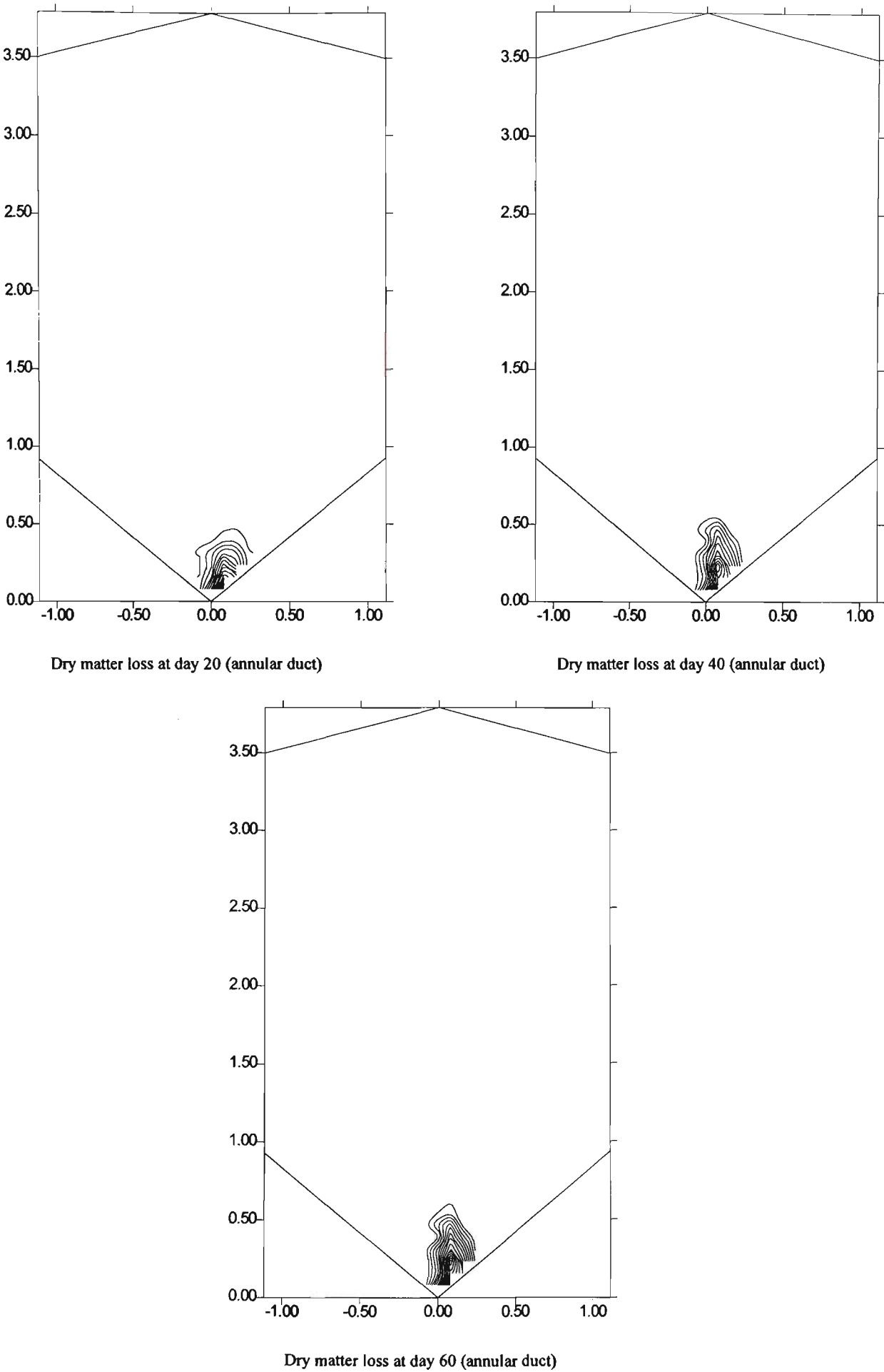


Figure 7.27 Dry matter loss distributions in the silo fitted with an annular duct

7.8 INSECT POPULATION DISTRIBUTIONS

Insects such as *Sitophilus oryzae*, *Rhizopotha dominica* and *Sitophilas zeamais* are likely to infest stored grain, and spoil its quality. Insect population growth has been linearly related to the wet bulb temperature of the intergranular air. As a result, insect population often grow rapidly in unaerated bulk of grain.

The potential for insect population growth is shown in figures 7.31 to 7.42. After two months storage in a non-aerated silo, the population of the strain *S. oryzae 1* has increased 180 fold. Compared with the initial concentration in the central region, it can be seen that aeration system is quite effective in controlling insect population growth, in a silo fitted with a linear aeration duct, the population of insects is 15 fold, and in the silo fitted with an annular duct, the population growth is only 3 fold.

Figure 7.31 shows in the non-aerated silo, the distribution of the more vigorous strain of *S. oryzae 1*, the population increases by about 6 fold in the centre, and typically 4 fold in the upper surface of the grain and bottom region of the bulk, this is because in the central region of the silo, the wet bulb temperature of the air is higher than at the boundaries. After 40 days storage, the insect population increase 36 fold in the central region. After 60 days storage, the upper surface of the grain has 40 insects, and at the bottom of the silo has around 80 fold increase.

Figure 7.32 indicates the effect on insect population growth in a silo fitted with a linear aeration duct. After 20 days aeration, the population of *S. oryzae 1* at the centre of the silo has increases by 3.5 fold, and at the warm region of the upper surface of grain, the maximum numbers of insects are about 5.15 fold. After 40 days aeration, the centre area of silo is maintained cool and the population growth is 7.5 fold, and 13.5 fold near the upper surface of the silo. After 60 days aeration, the rate of insects grown is lower

at the region is close to the duct, and higher distant from the duct. At the upper surface of grain, the maximum potential for insect growth is 28 times the initial population.

Figure 7.33 shows that after 20 days aeration of the silo fitted with an annular duct, the centre region of the silo has around 2.5 insects more than initially, at the upper surface of the grain, there is about 4.28 fold increase on *S. oryzae 1*. After 40 days of cooling, the rate of insect growth at centre area of the silo is small, this is because cold air provides insects a difficult environment for living, and the population increase is only 3.5 fold. After 60 days aeration, the insect growth at upper surface of the grain has become 12.67 fold.

In a similar way to *S. oryzae 1*, which is we discussed above, figure 7.34 shows insect population in a non-aerated silo after 60 days storage. In the centre area of the silo, insect *S. oryzae 2* grown to 87 times its initial population. From this point of view, we can see: Storage insect grown rapidly without aeration control, and causing the stored grain completely lost in the short period of time under storage environment. With a linear aeration duct, after 60 days aeration, *S. oryzae 2* only has increase 9 fold around the centre of the silo. Similarly, after two months aeration with the annular aeration duct, the population of the loss vigorous strain of *S. oryzae 2* has increased 2.77 times its initial value.

Figure 7.37 shows, the distributions of *R. dominica* in the non-aeration silo. After 60 days storage, the number of *R. dominica* at the centre region of the silo increases 16.5 fold. In the silo fitted with a linear duct (as shown in figure 7.38), after two months aeration cooling control, in the centre area of the silo the population of *R. dominica* has increased by 2.1 fold. In the silo fitted with an annular duct (as shown in figure 7.39), after 60 days period storage, the centre area of insect *R. dominica* is only 1.5 fold. It is clear that this species is not particularly cold tolerant.

The final insect species which are discussed in this thesis is *S. zeamais*. Figure 7.40 shows that the simulation results of *S. zeamais* distributions after two months storage without aeration. It is clear that at the centre area of the silo, the *S. zeamais* growth is 2.7 fold. In a silo fitted with a linear duct (see figure 7.41), the storage management keep the insect population under good control, only about 1.3 fold of insects *S. zeamais* in the centre region of the silo. When a silo is fitted with an annular duct (see figure 7.42), the population of *S. zeamais* appear to be very tightly controlled, and after 60 days storage, the population of *S. zeamais* has increased by about only 1.2 fold.

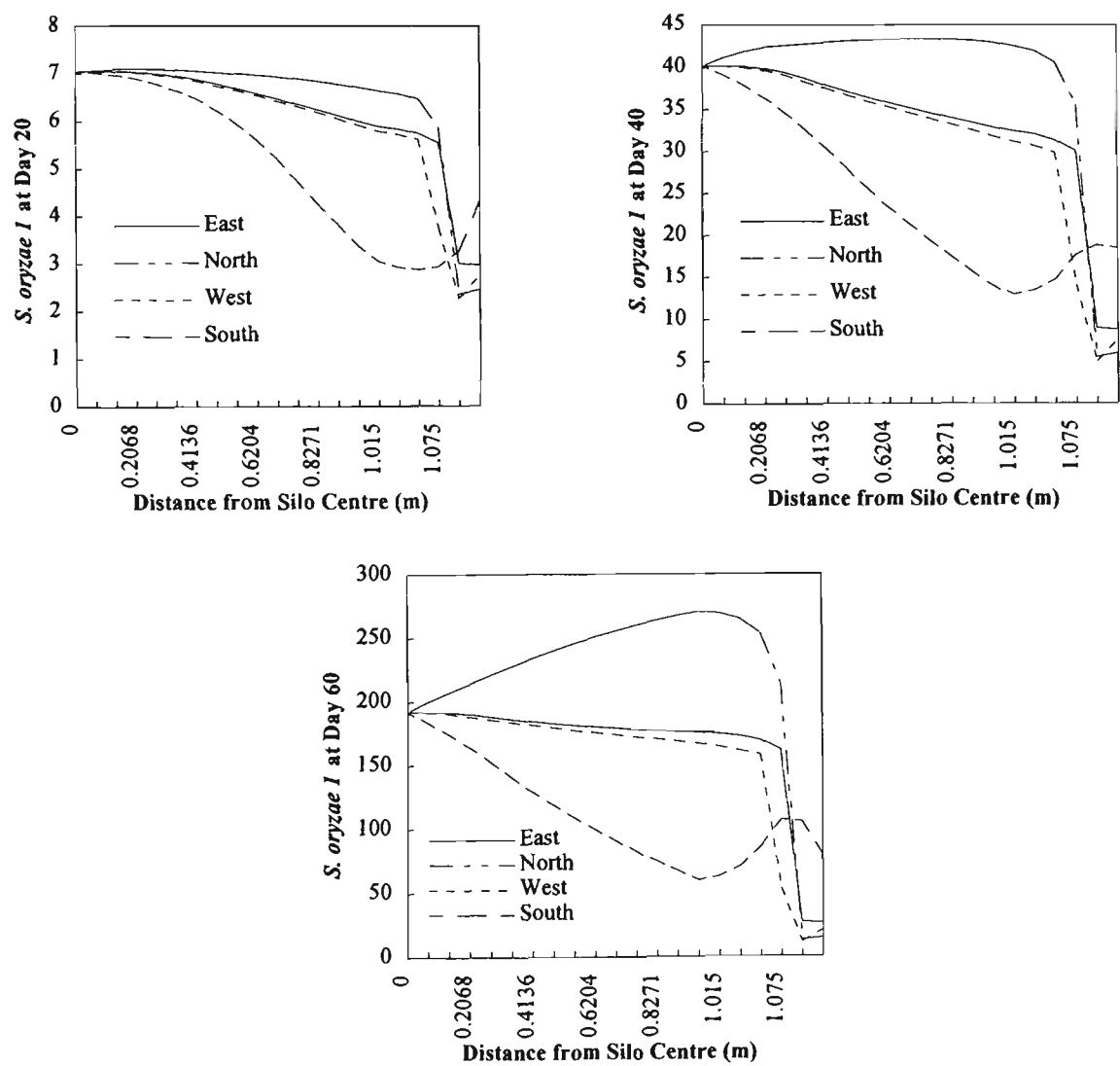


Figure 7.28 Radial profiles of the population of *S. oryzae I* in the non-aerated case

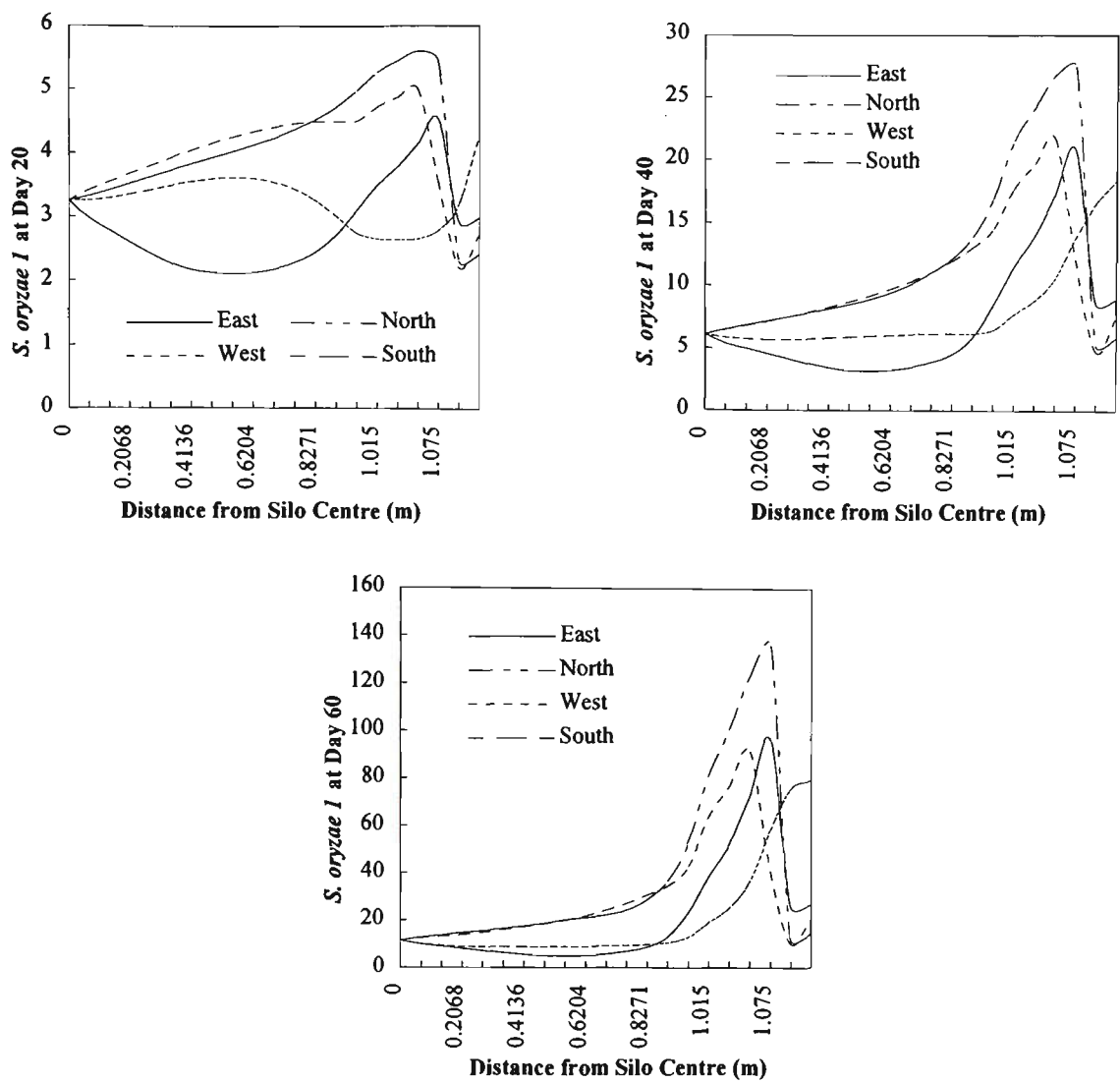
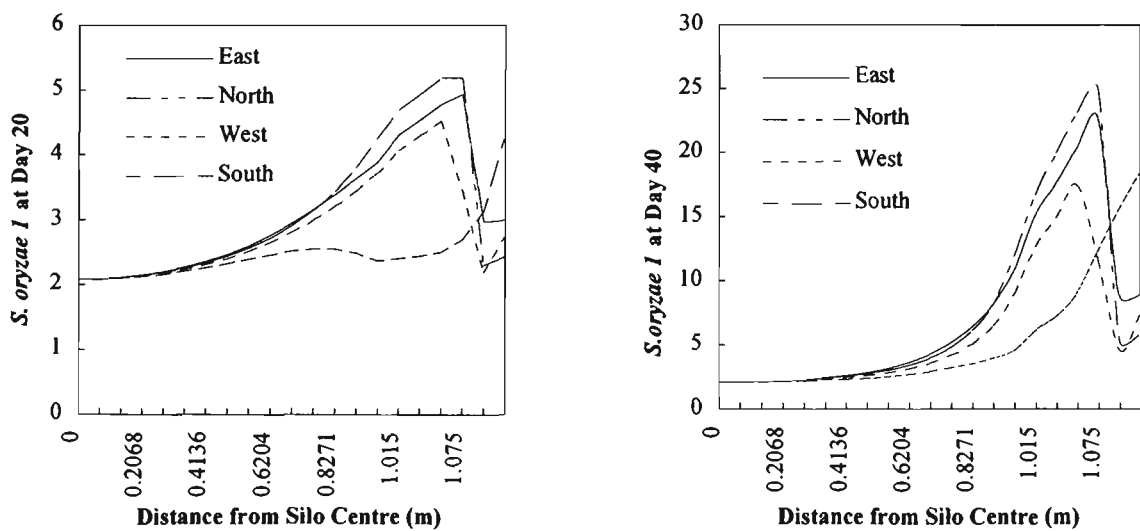


Figure 7.29 Radial profiles of the population of *S. oryzae I* in the linear duct case



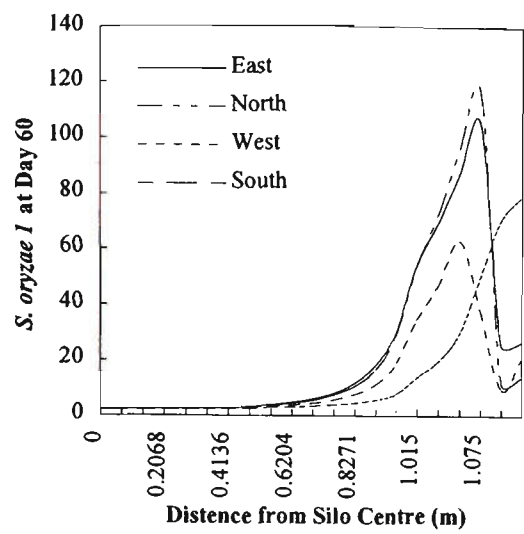
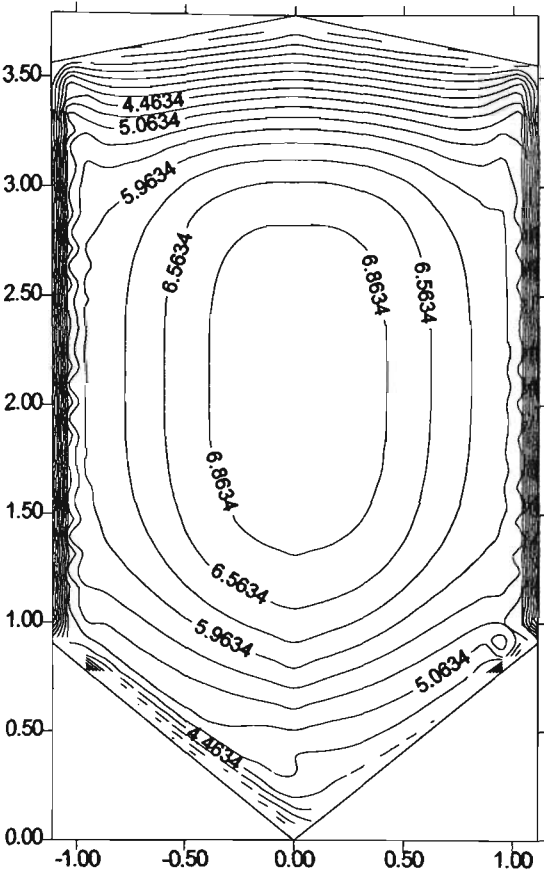


Figure 7.30 Radial profiles of the population of *S. oryzae1* in the annular duct case

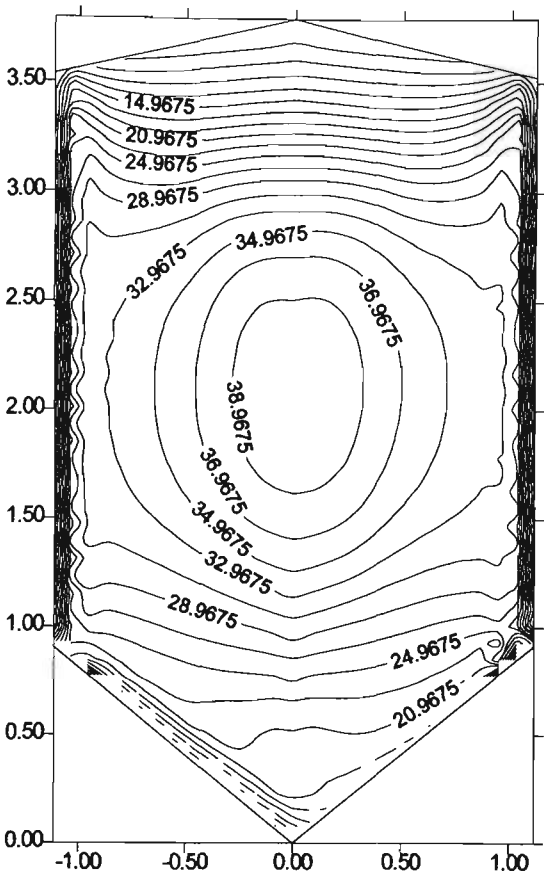
Figure 7.28 shows the insects of *S. oryzae1* along east, south, west and south radii of a non-aerated silo. It is clear to see that population of *S. oryzae1* continue to grow rapidly in the centre of the silo throughout the storage period. However, the population growth near the east, north and west facing regions of the silo is low, because of the high temperatures of the insolation during the noon. Population growth on the south side of the silo is generally lower, because of the lower grain temperatures that result from heat transfer process occurring the central region of the silo.

In the aerated silo fitted with a linear duct (as shown in figure 7.29), the population of *S. oryzae1* growth is lower near the centre of the silo, and higher within a 10 centimetre of the wall, this is because that the linear aeration system has controlled the central region of the silo, and the temperature along the wall of the silo is heated by solar radiation and ambient air during the day. The density of population *S. oryzae1* growth on the east, north and west facing of the silo is very low due to the high temperature occurring during the day.

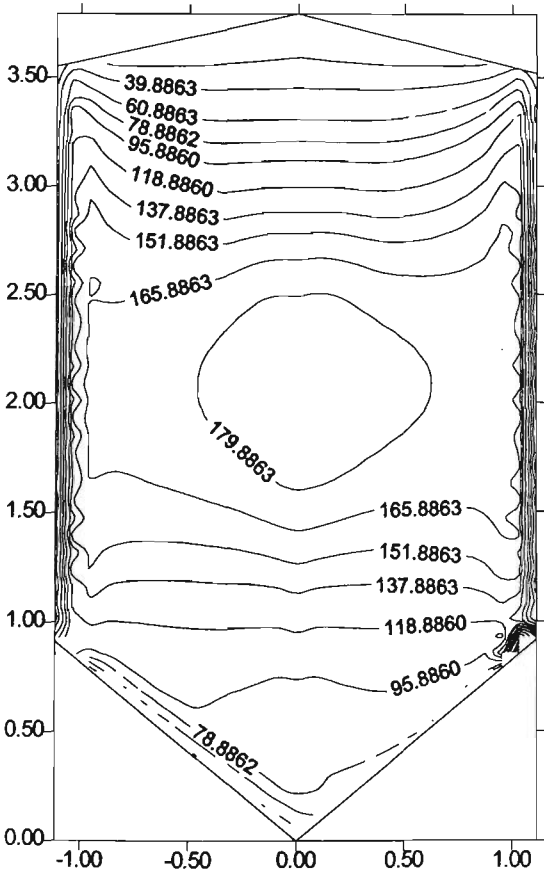
Similar with an annular duct (as shown in figure 7.30), it can be seen that the controlling of population growth of *S. oryzae1* is better than that linear aeration system in the centra region of the silo.



S. oryzae I at day 20 (non-aerated)

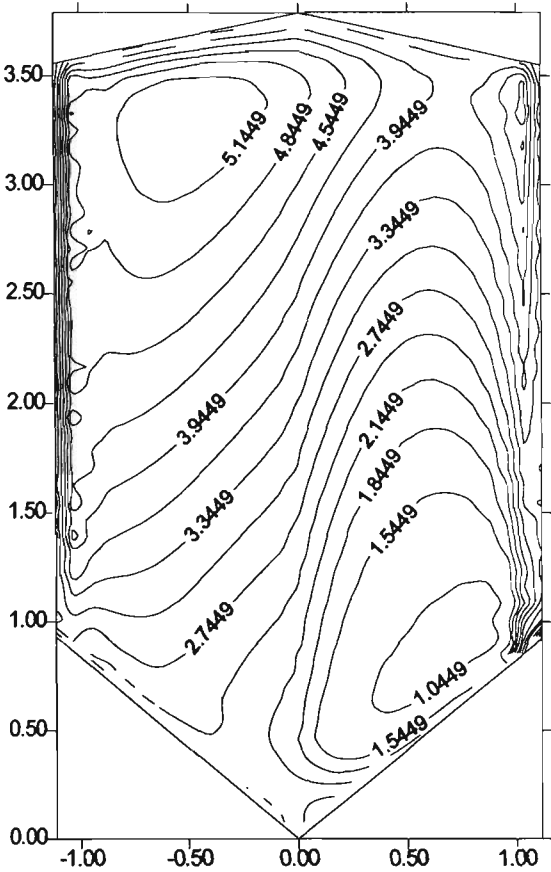


S. oryzae I at day 40 (non-aerated)

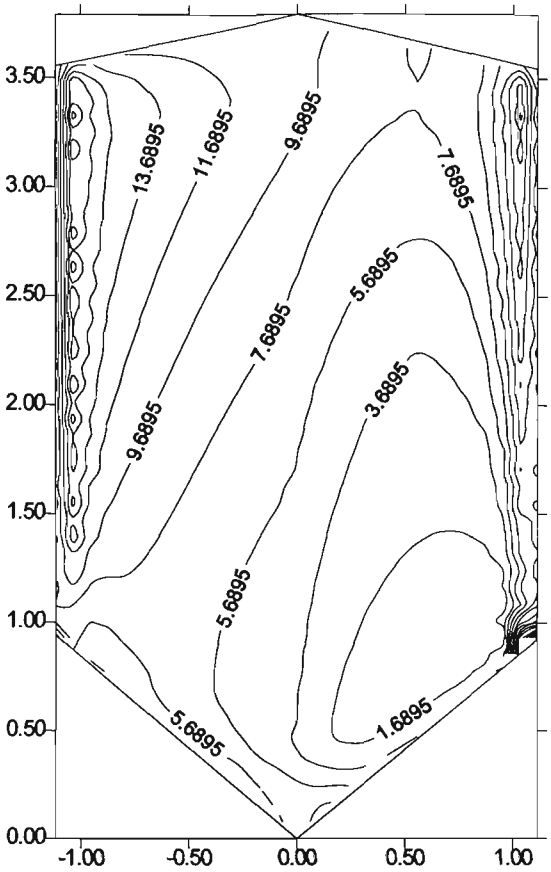


S. oryzae I at day 60 (non-aerated)

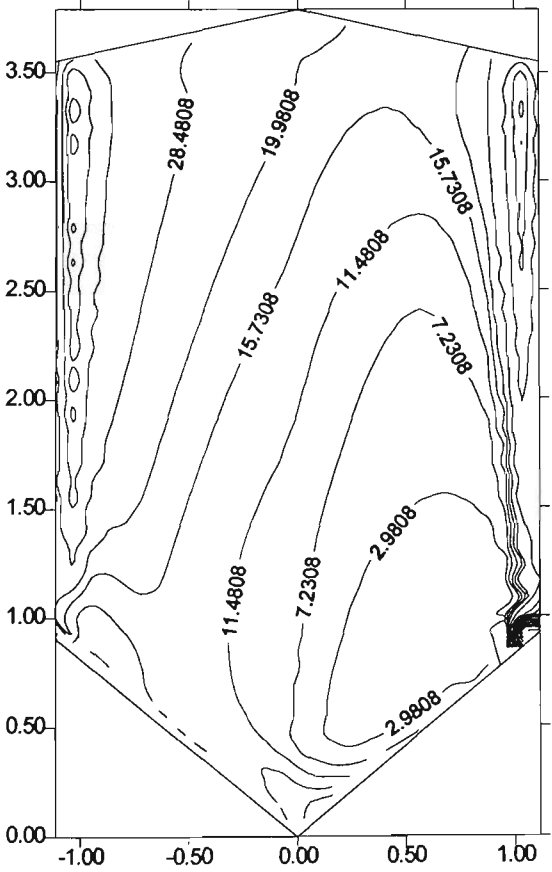
Figure 7.31 *S. oryzae* I distributions in the non-aerated silo



S. oryzae I at day 20 (linear duct)

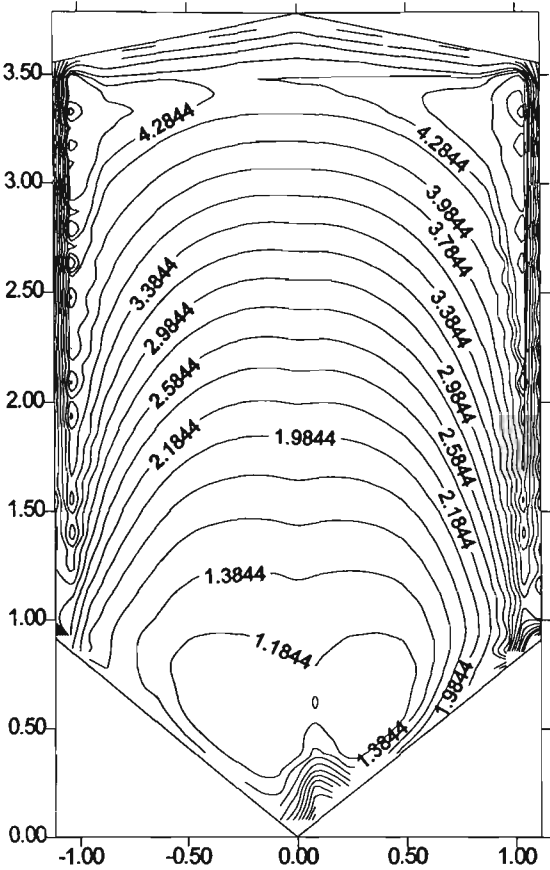


S. oryzae I at day 40 (linear duct)

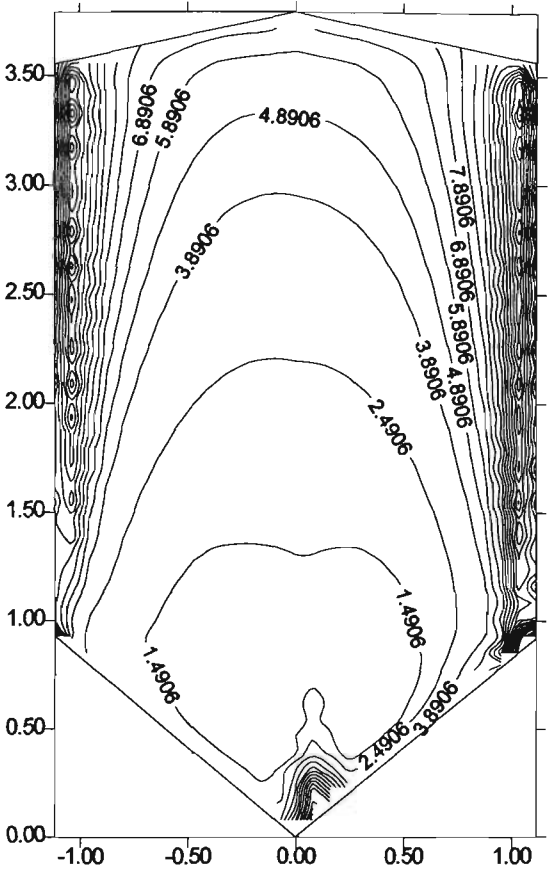


S. oryzae I at day 60 (linear duct)

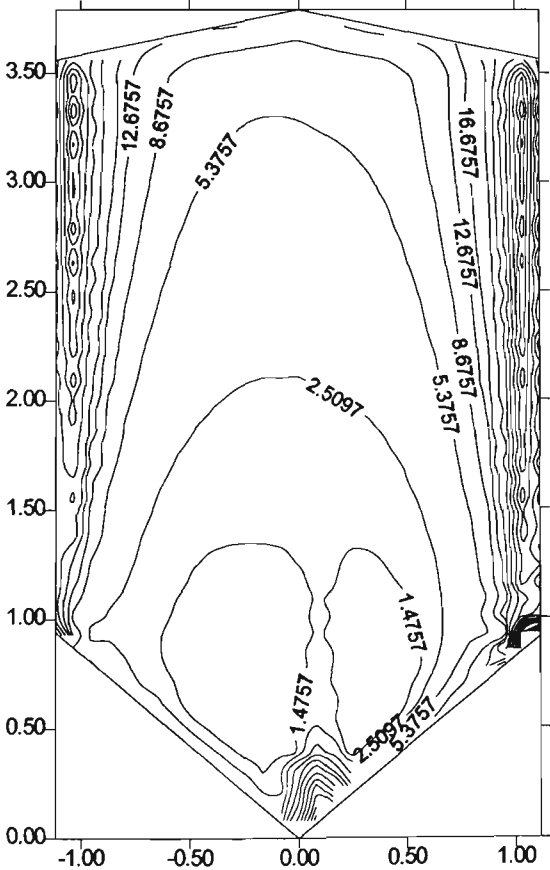
Figure 7.32 *S. oryzae* I distributions in the silo fitted with a linear duct



S. oryzae I at day 20 (annular duct)

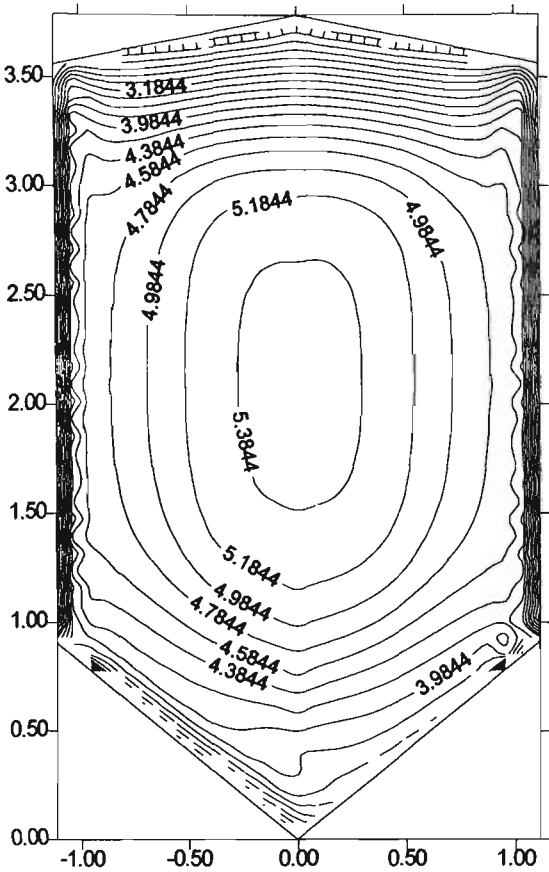


S. oryzae I at day 40 (annular duct)

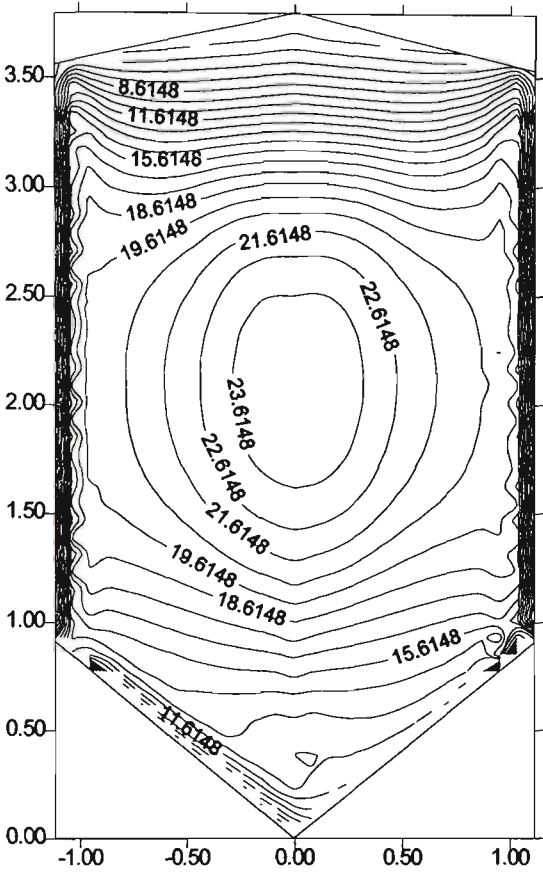


S. oryzae I at day 60 (annular duct)

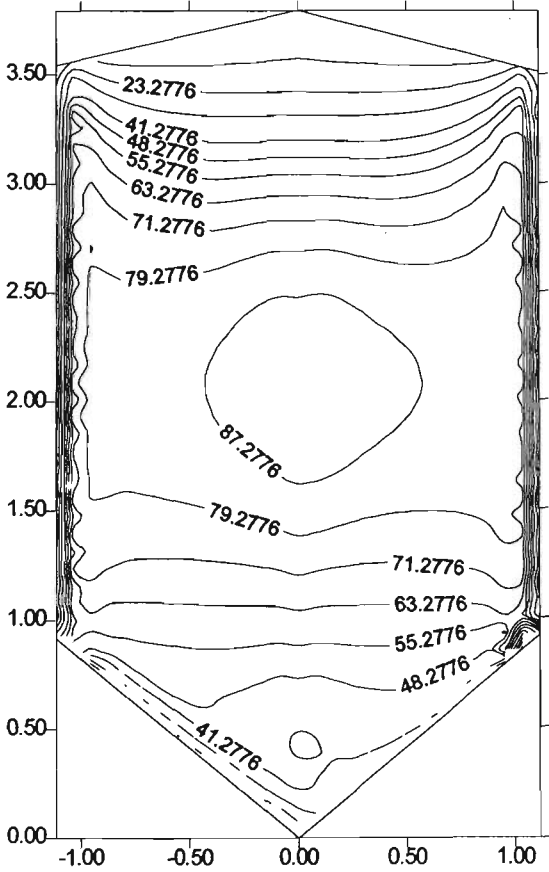
Figure 7.33 *S. oryzae* I distributions in the silo fitted with an annular duct



S. oryzae 2 at day 20 (non-aerated)

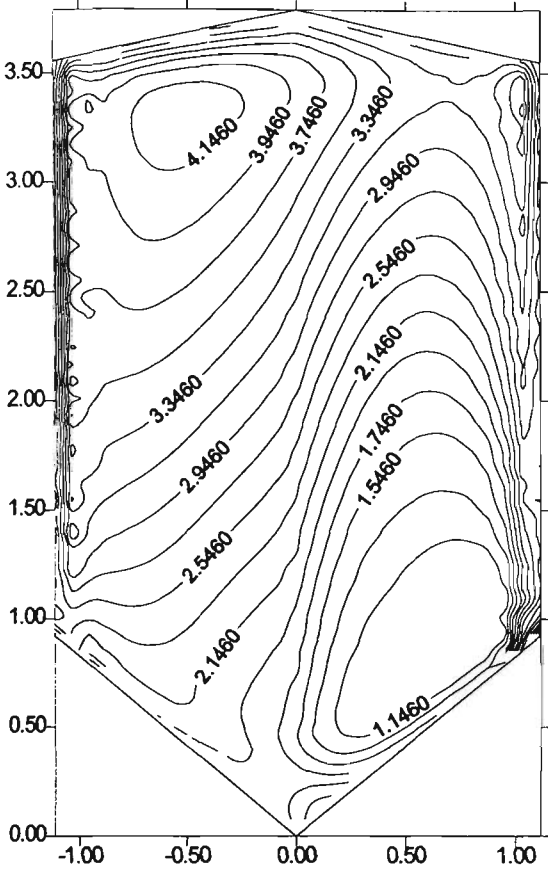


S. oryzae 2 at day 40 (non-aerated)

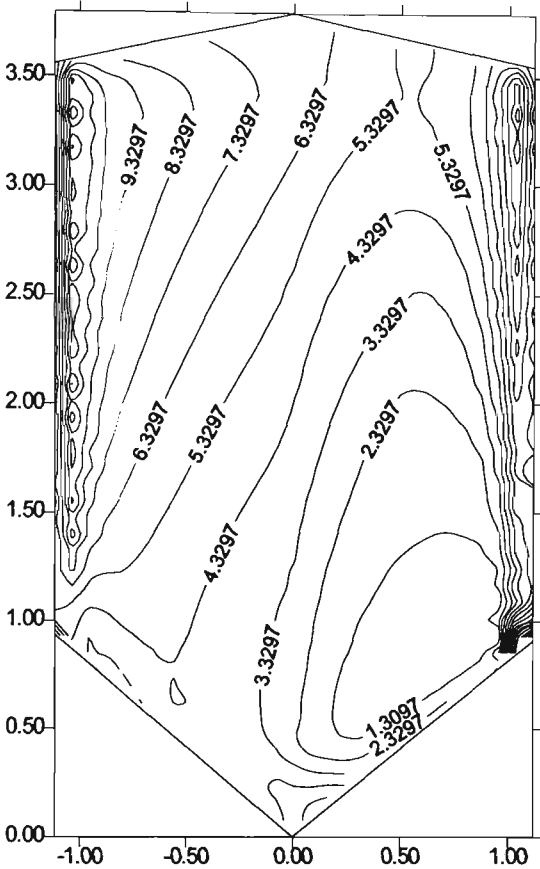


S. oryzae 2 at day 60 (non-aerated)

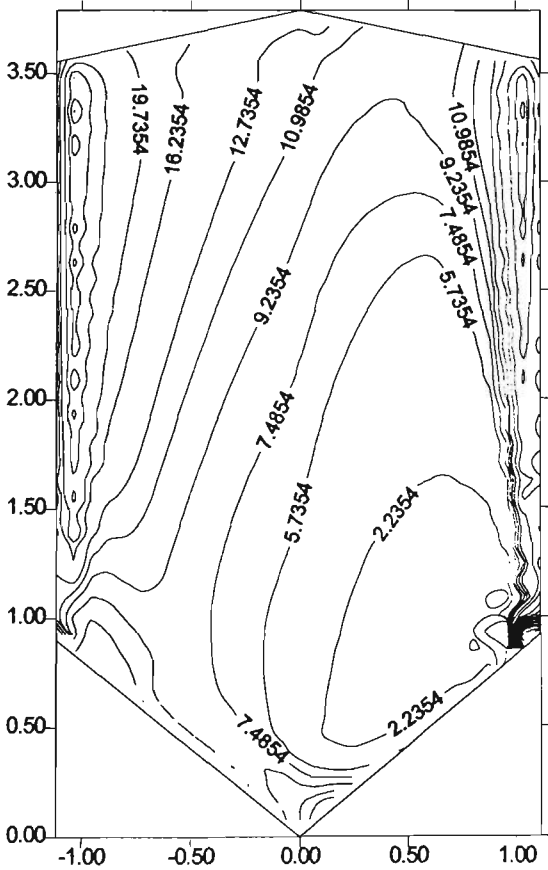
Figure 7.34 *S. oryzae* 2 distributions in the non-aerated silo



S. oryzae 2 at day 20 (linear duct)

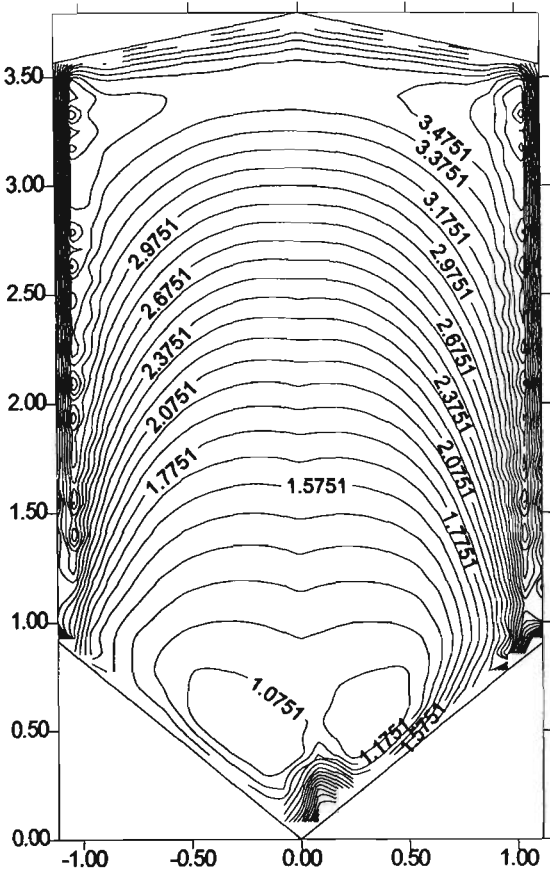


S. oryzae 2 at day 40 (linear duct)

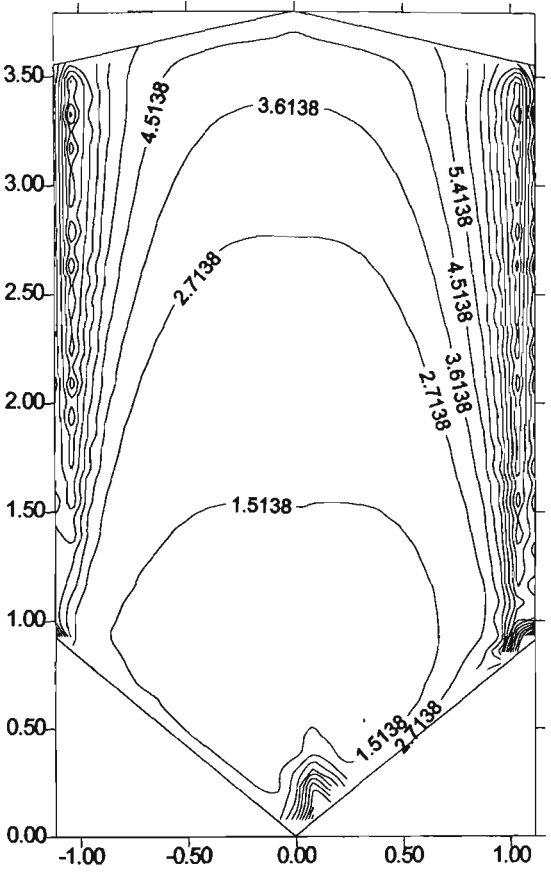


S. oryzae 2 at day 60 (linear duct)

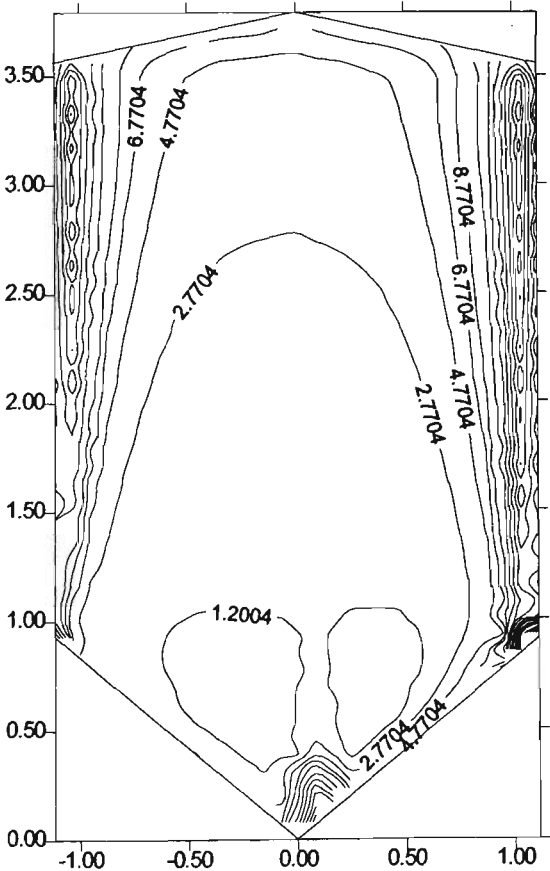
Figure 7.35 *S. oryzae*2 distributions in the silo fitted with a linear duct



S. oryzae 2 at day 20 (annular duct)

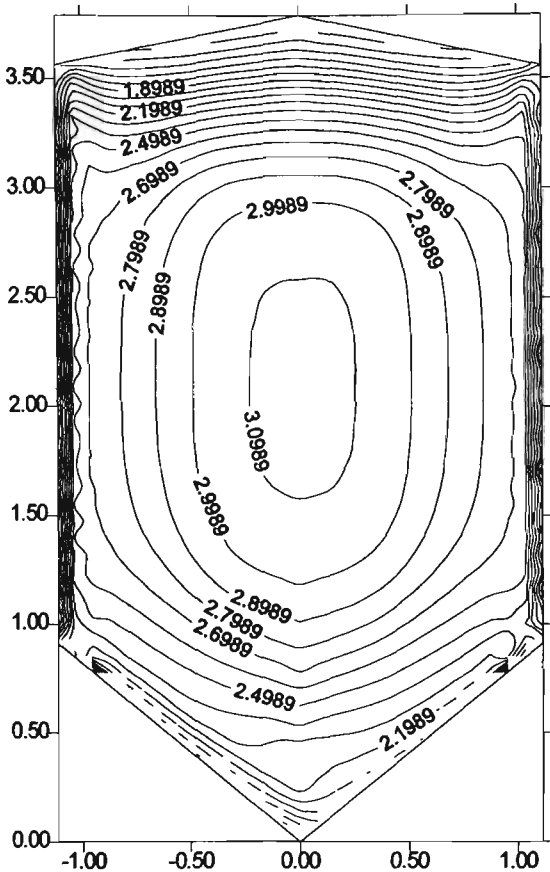


S. oryzae 2 at day 40 (annular duct)

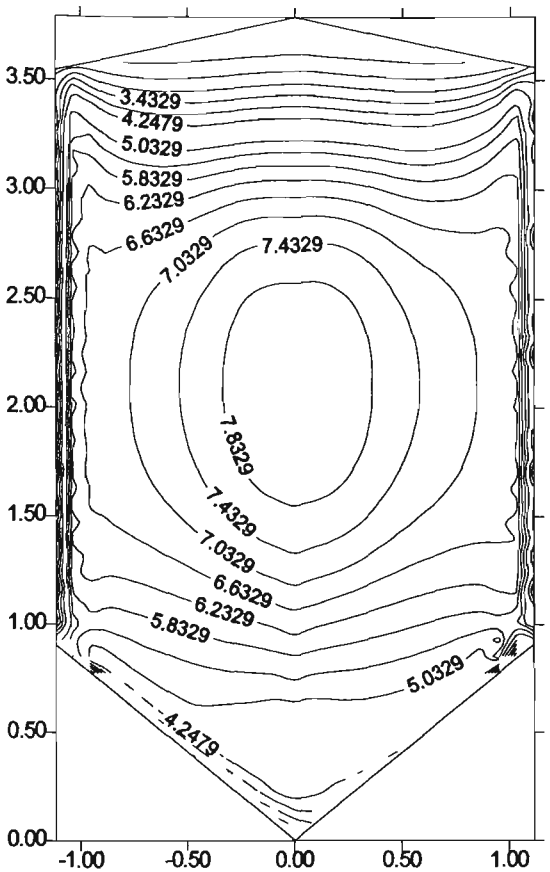


S. oryzae 2 at day 60 (annular duct)

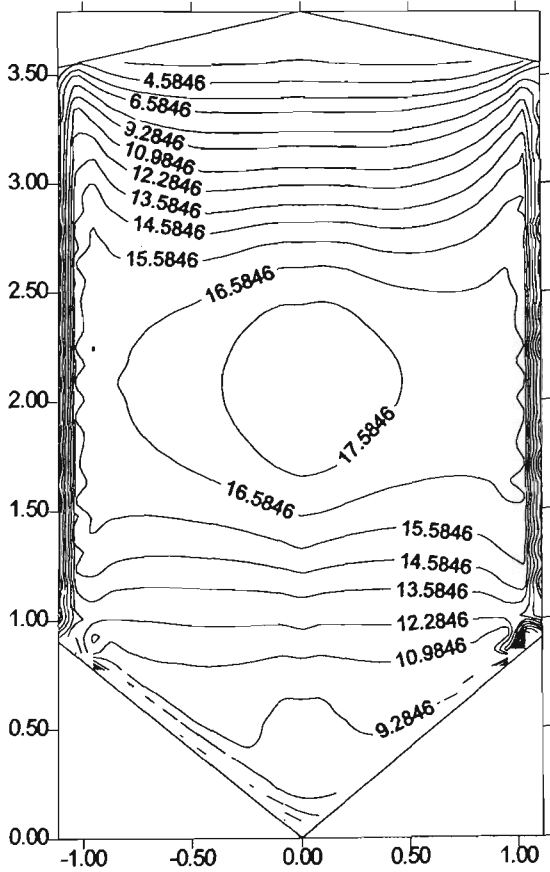
Figure 7.36 *S. oryzae* 2 distributions in the silo fitted with an annular duct



R. dominica at day 20 (non-aerated)

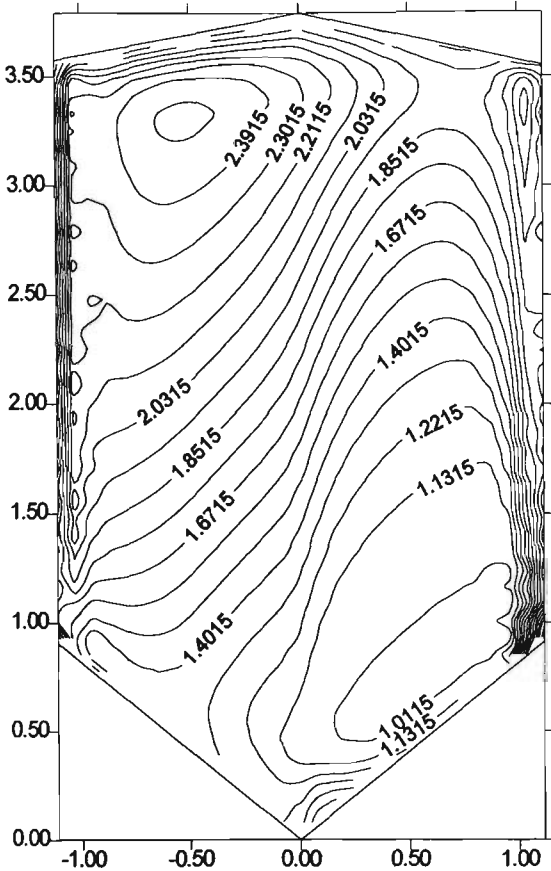


R. dominica at day 40 (non-aerated)

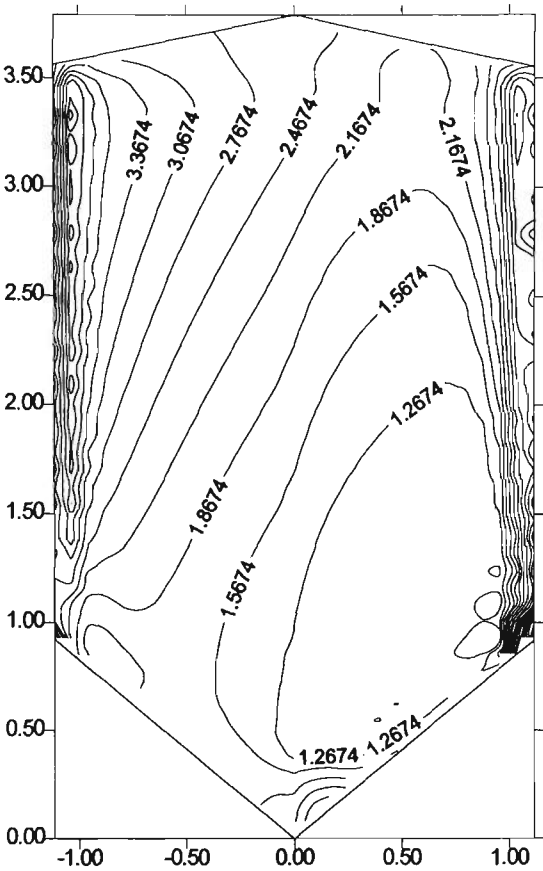


R. dominica at day 60 (non-aerated)

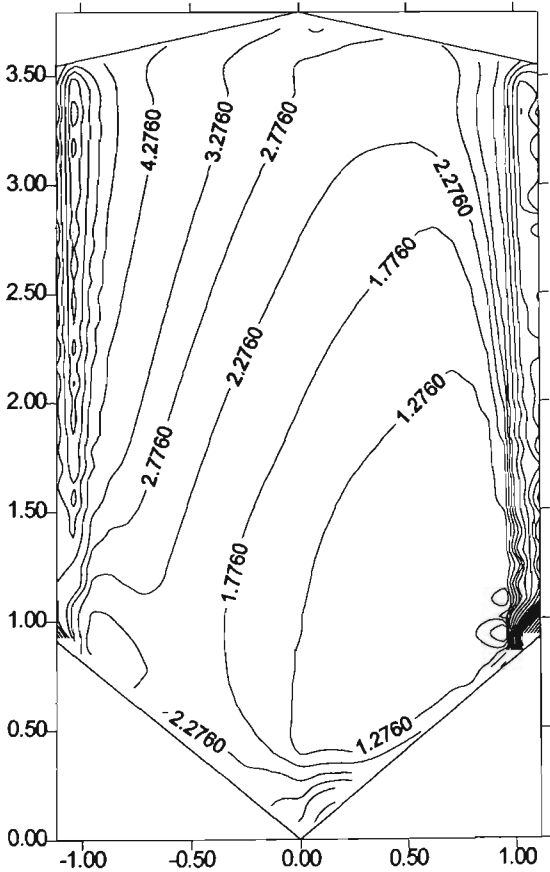
Figure 7.37 *R. dominica* distributions in the non-aerated silo



R. dominica at day 20 (linear duct)

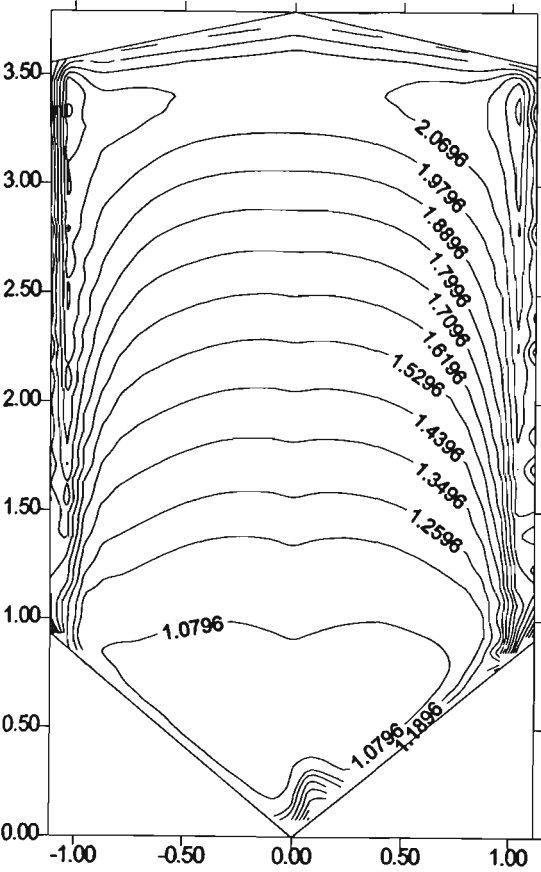


R. dominica at day 40 (linear duct)

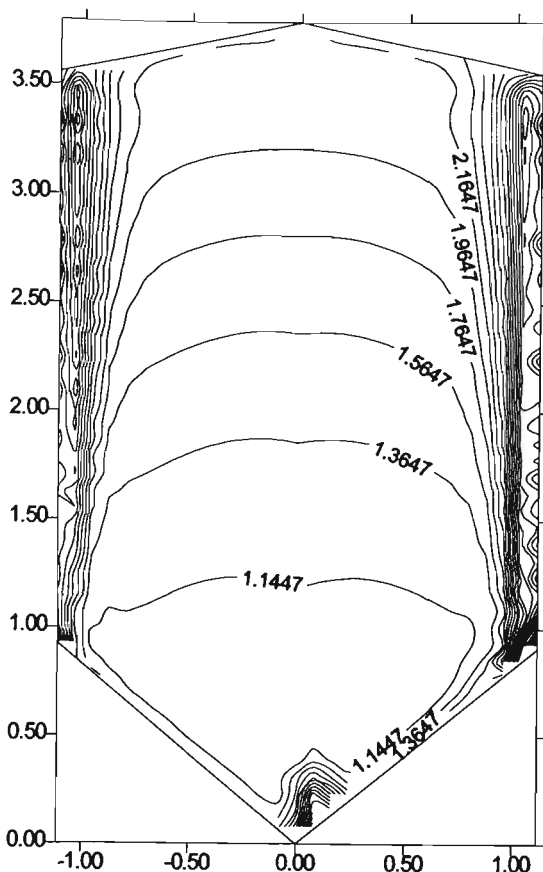


R. dominica at day 60 (linear duct)

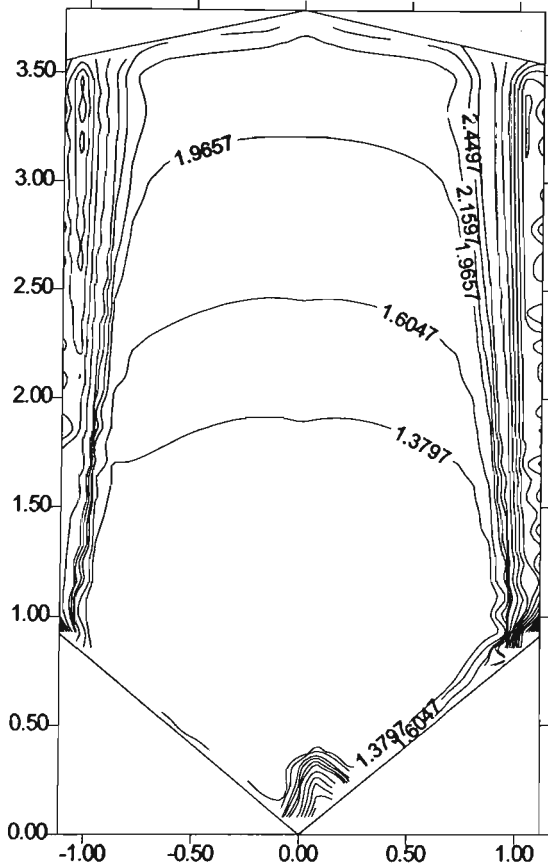
Figure 7.38 *R. dominica* distributions in the silo fitted with a linear duct



R. dominica at day 20 (annular duct)

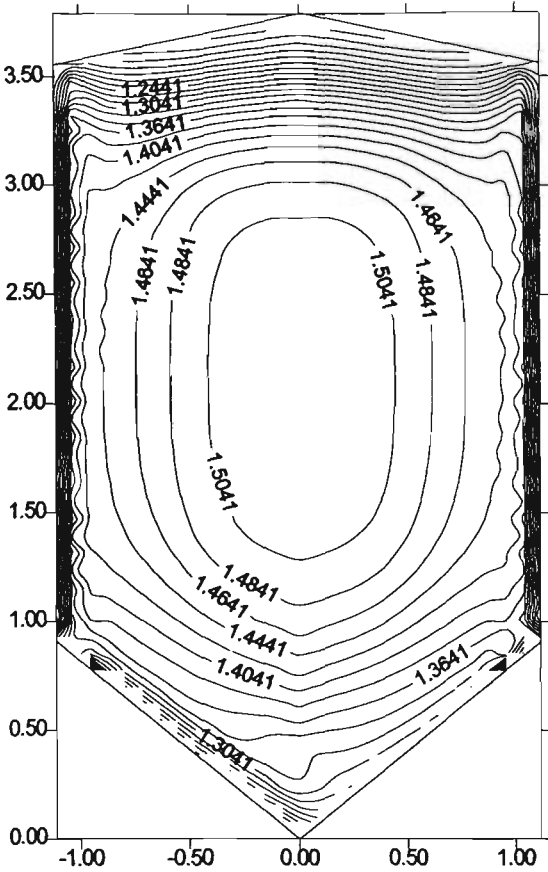


R. dominica at day 40 (annular duct)

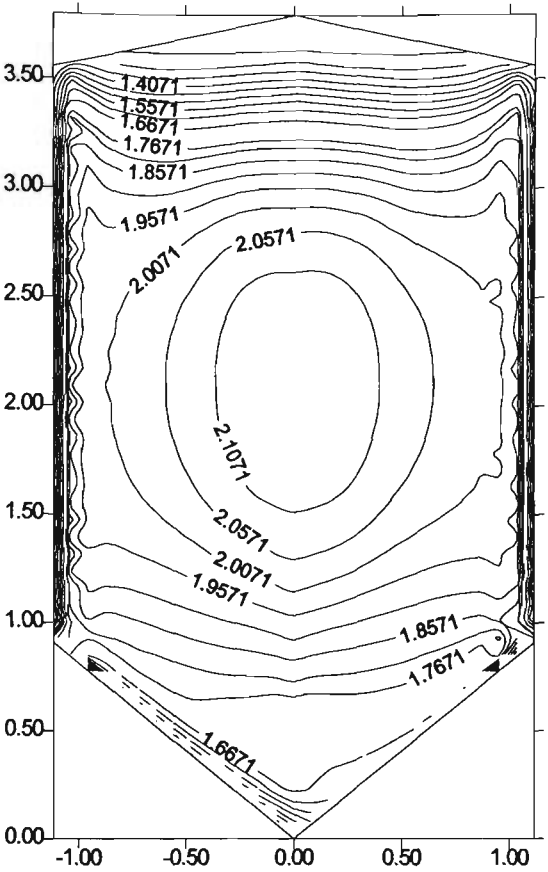


R. dominica at day 60 (annular duct)

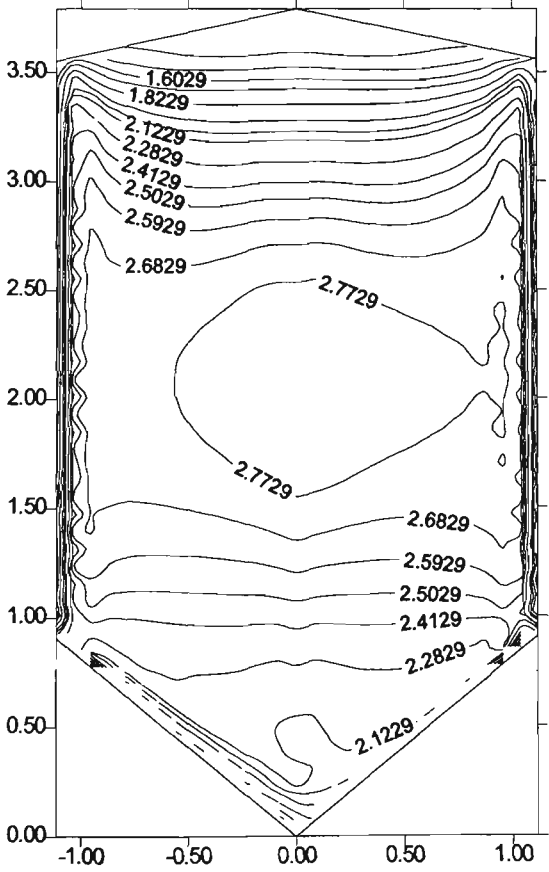
Figure 7.39 *R. dominica* distributions in the silo fitted with an annular duct



S. zeamais at day 20 (non-aerated)

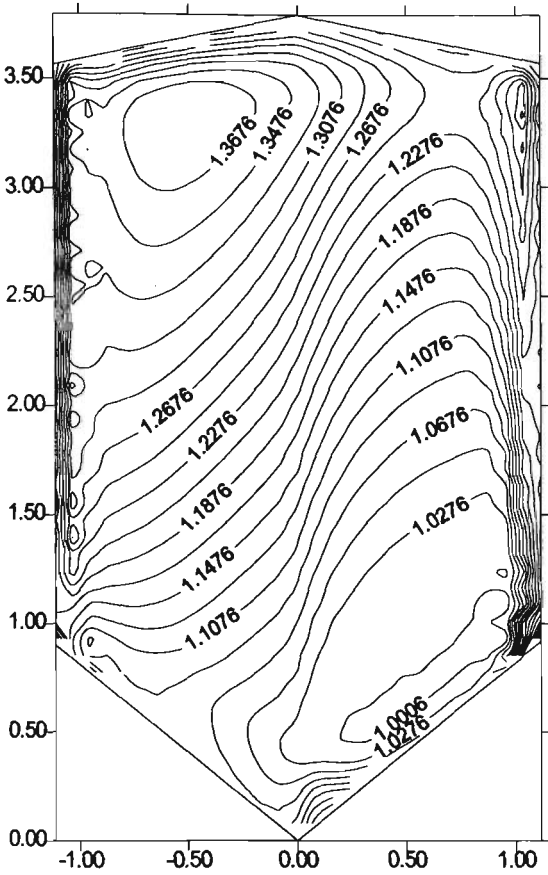


S. zeamais at day 40 (non-aerated)

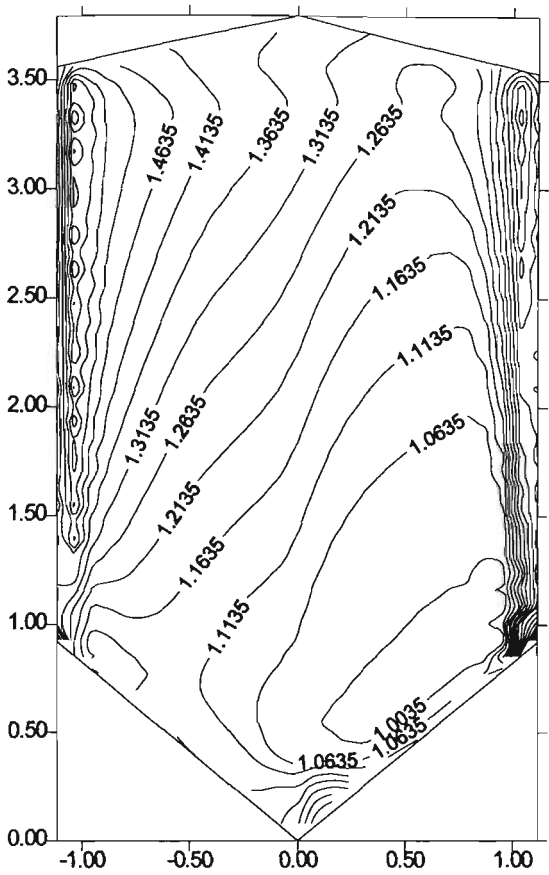


S. zeamais at day 60 (non-aerated)

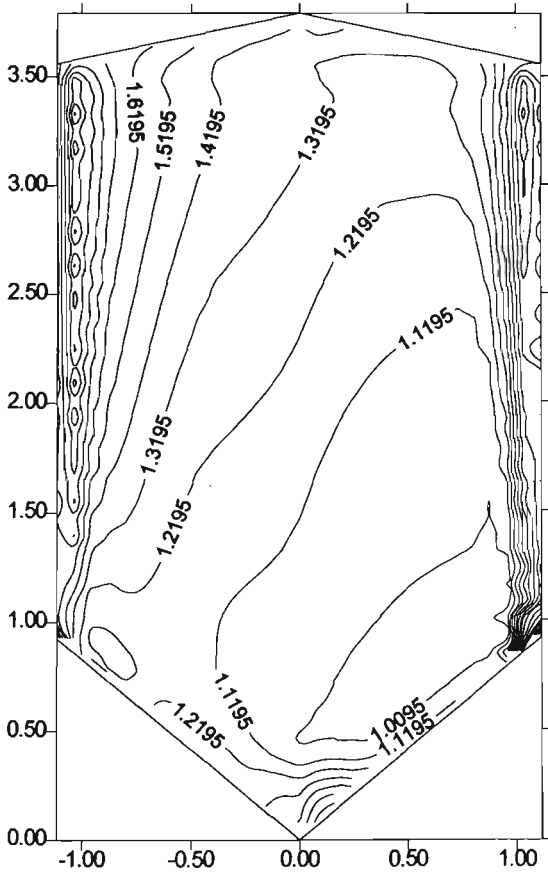
Figure 7.40 *S. zeamais* distributions in the non-aerated silo



S. zeamais at day 60 (linear duct)

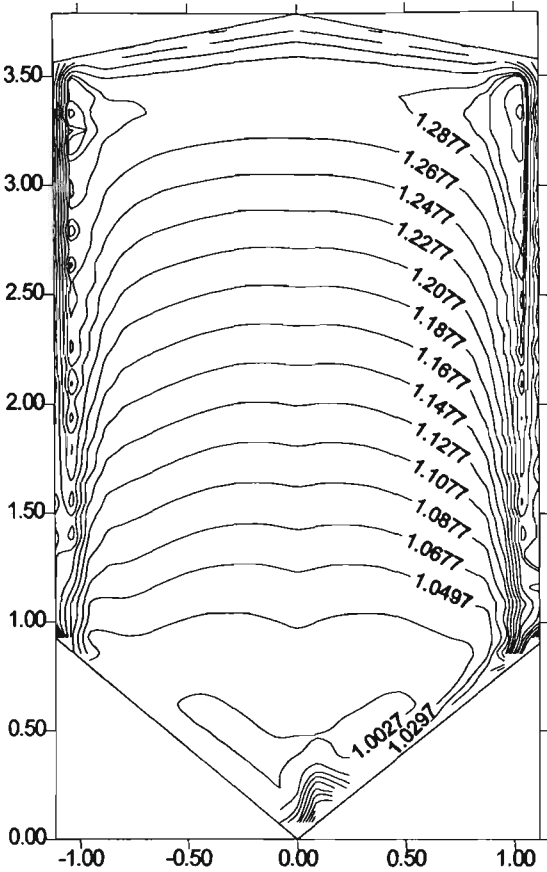


S. zeamais at day 40 (linear duct)

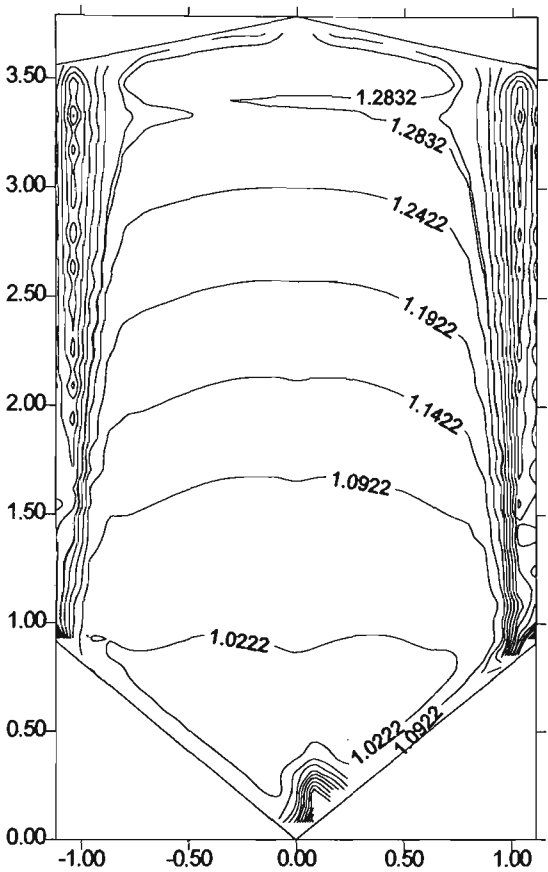


S. zeamais at day 60 (linear duct)

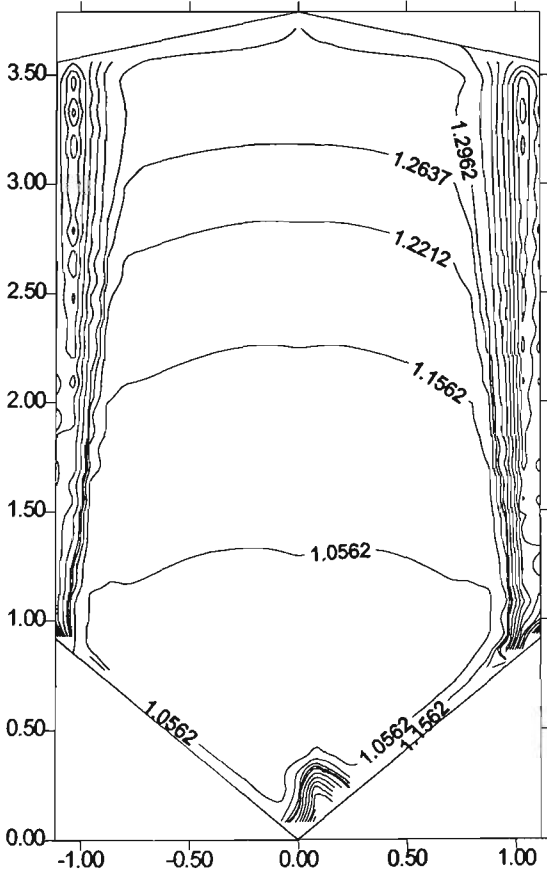
Figure 7.41 *S. zeamais* distributions in the silo fitted with a linear duct



S. zeamais at day 20 (annular duct)



S. zeamais at day 40 (annular duct)



S. zeamais at day 60 (annular duct)

Figure 7.42 *S. zeamais* distributions in the silo fitted with an annular duct

7.9 SEED VIABILITY DISTRIBUTIONS

The viability of seed grain is signified as the ability of the seed to develop into a young plant under favourable conditions in the absence of dormancy (*Brooker et al.*, 1992). The life of the viability of seed grain depends on temperature, moisture content and the length of time. Figures 7.46, 7.47, and 7.48 show, the variation of stored seed viability under three different storage conditions.

It is clearly to see, that after 60 days storage with an initial seed viability of initial 0.99, in the non-aerated silo, the centre area of seed viability is 0.95, which is 4.2% lower than initial condition. In the silo fitted with a linear aeration duct, the central zone of the seed viability is 0.97. In the silo fitted with an annular aeration duct, the centre region of seed viability is 0.98.

It is clear that aeration preserves seed viability of the rate of degradation the germ proteins and hydrolysis of the embryonic starch, and that the annular duct is slightly more effectively than the linear duct.

Figures 7.46, 7.46 and 7.47 reflect the seed viability responds to grain cooling. In the non-aerated silo as illustrated in figure 7.45, the viability of the grain is generally lower in the centre of the silo. This is because the grain remain warmest in this case.

Figure 7.46 clearly reflects the non-uniform passage of the cooling wave through the grain, and the viability of the seed is generally lower in the region furthest from the aeration duct,

The air flow distribution in the silo fitted with an annular duct is relatively uniform, and this is reflected in the seed viability patterns as shown in figure 7.47. Here we observe a large central region of the grain bulk that retains a large seed viability.

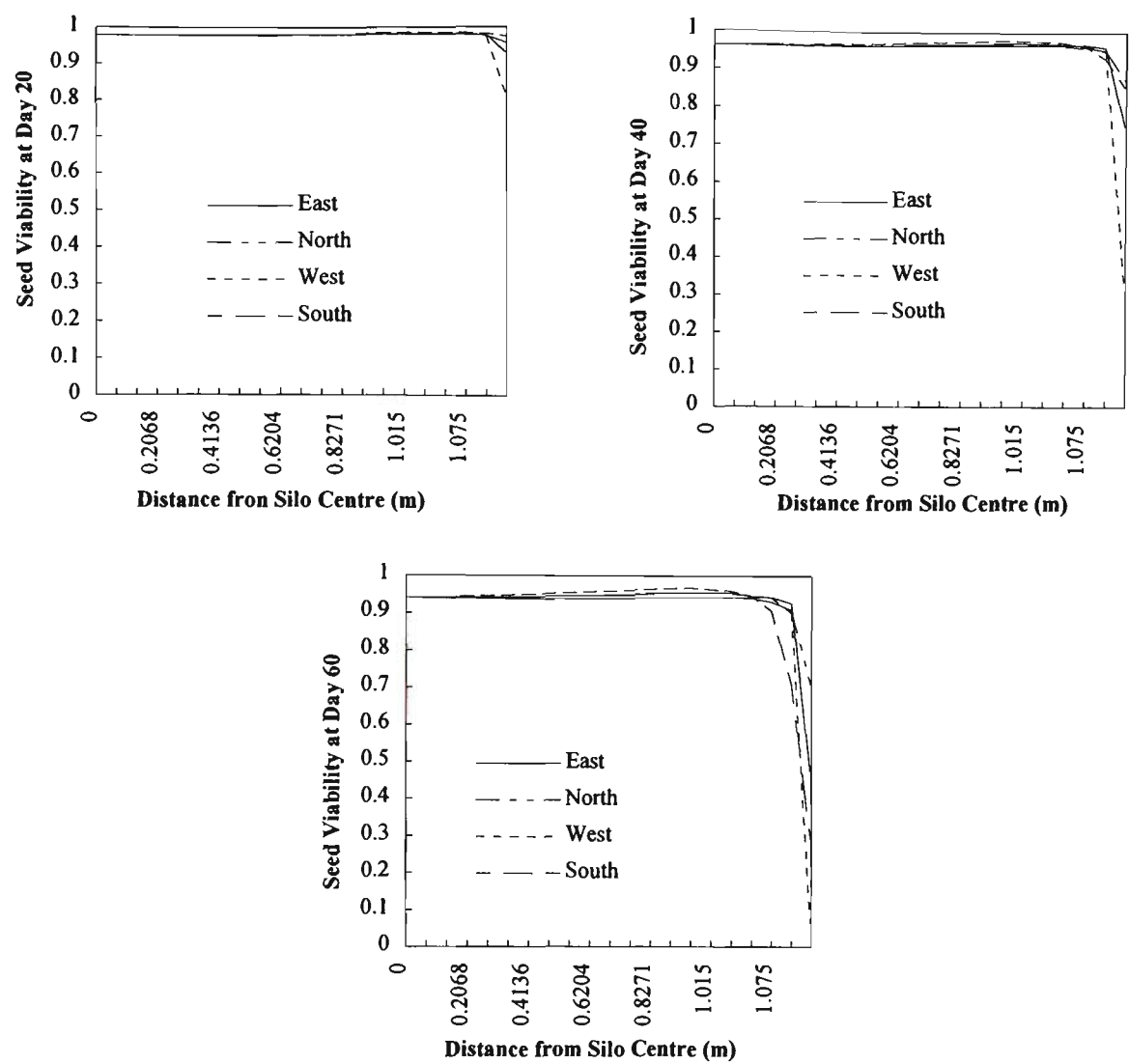
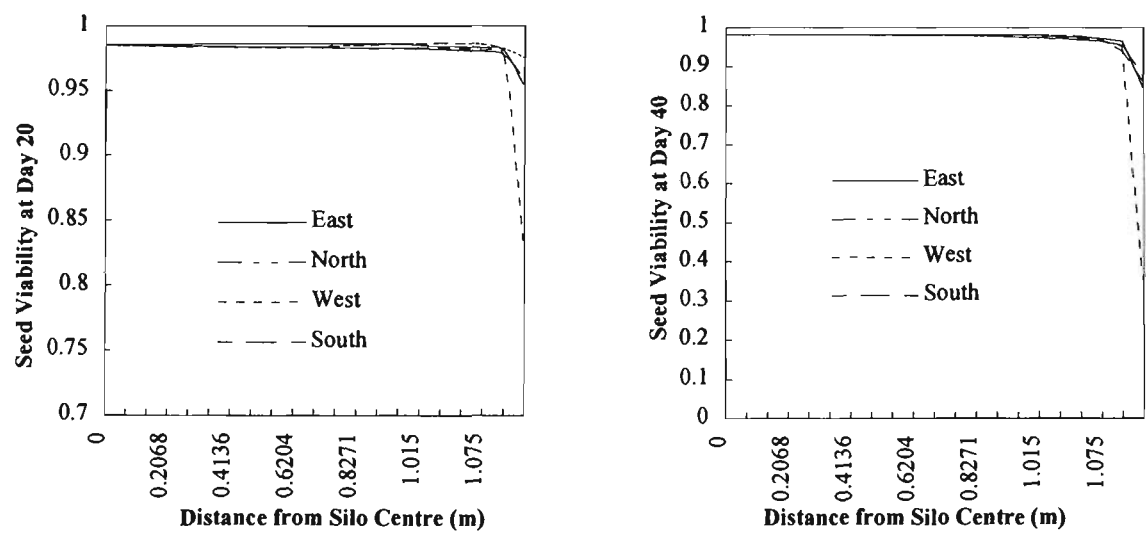


Figure 7.43 Radial profiles of the seed viability in the non-aerated case



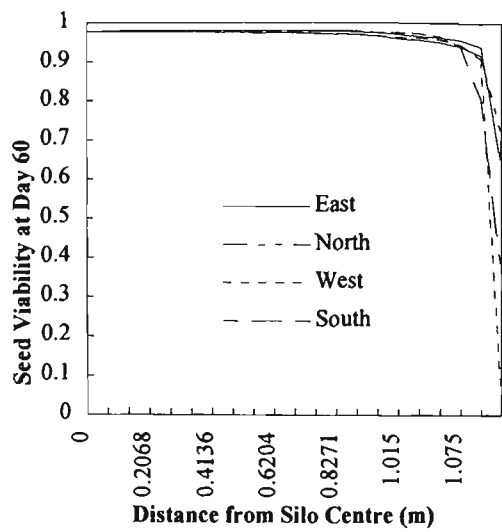


Figure 7.44 Radial profiles of the seed viability in the linear duct case

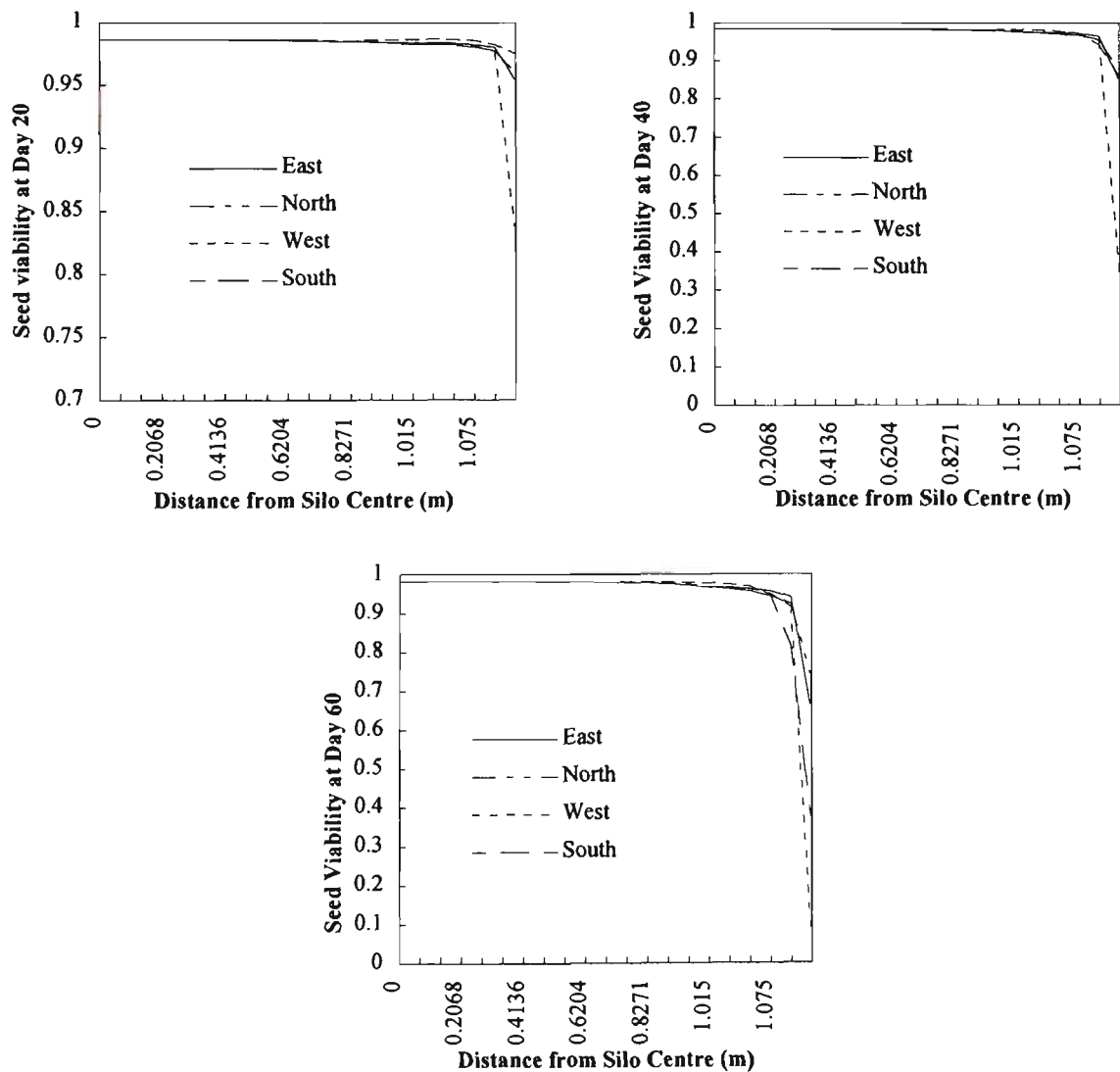


Figure 7.45 Radial profiles of the seed viability in the annular duct case

Figures 7.43, 7.44 and 7.45 show, the radial profiles of the seed viability along the north, south, east and west facing of the silo. Two observations have been made. Firstly, the seed viability in the central region of the grain bulk is higher in the aerated silos than in the non-aerated silo, and the silo fitted with the annular duct provide better result of seed preservation. Secondly, aeration appears to give litter protection to grain adjacent to those walls exposed to high temperatures. The stored seed near the west facing of the wall has a particularly low viability, because of the high temperature entering to which it has been exposed.

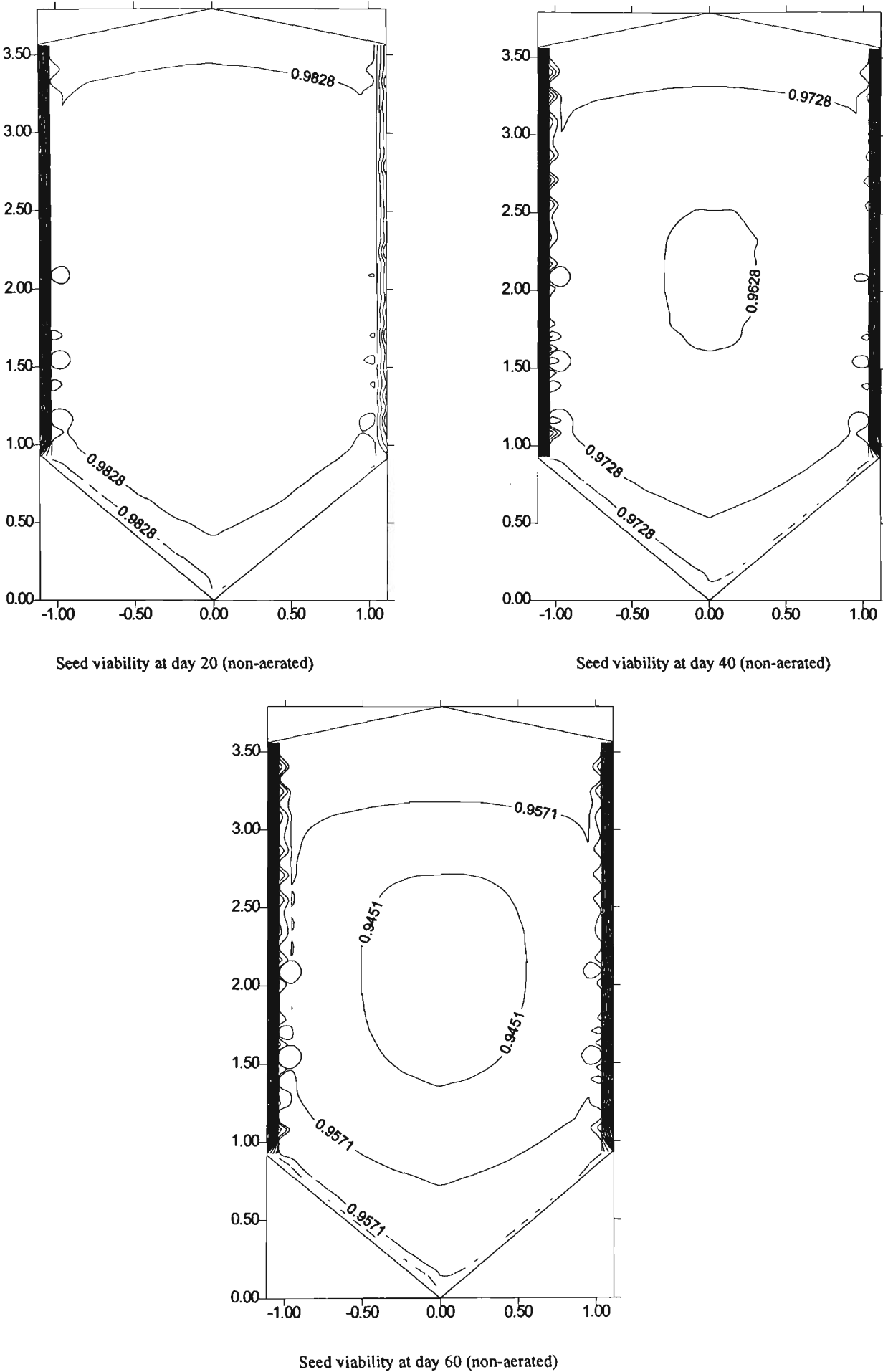
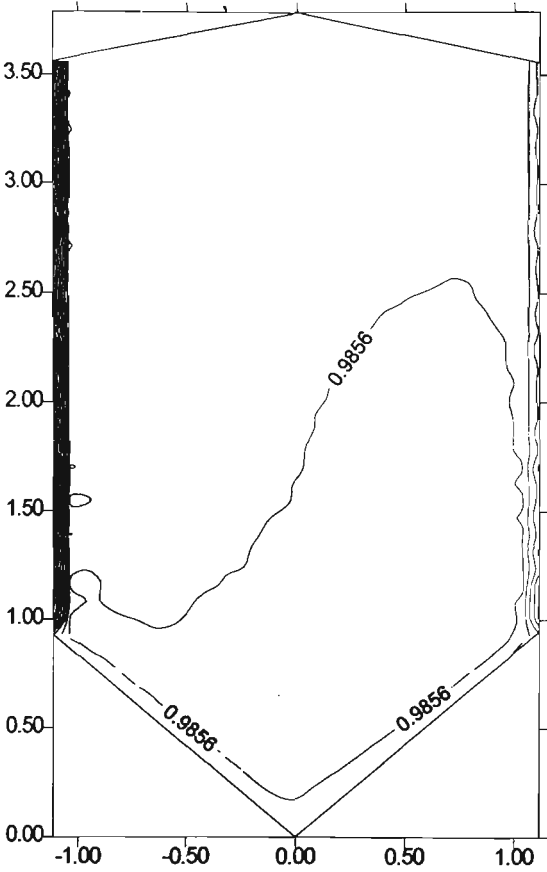
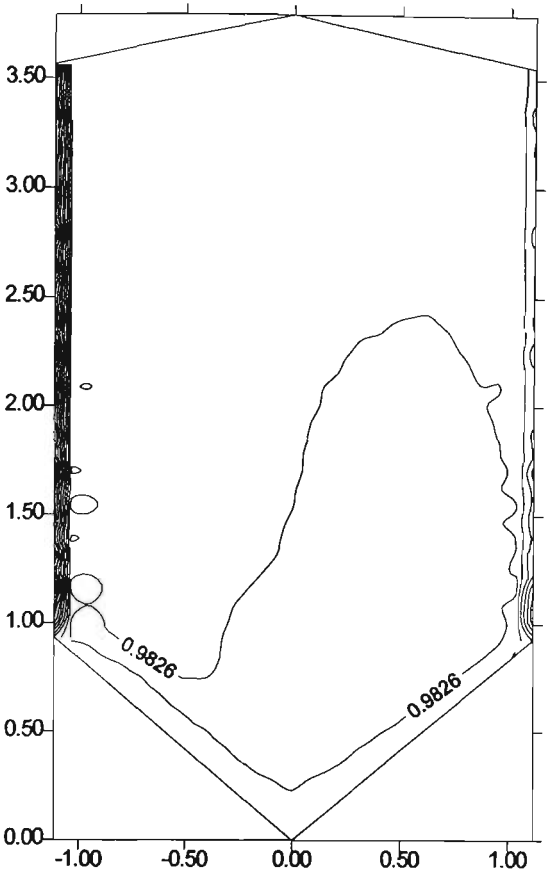


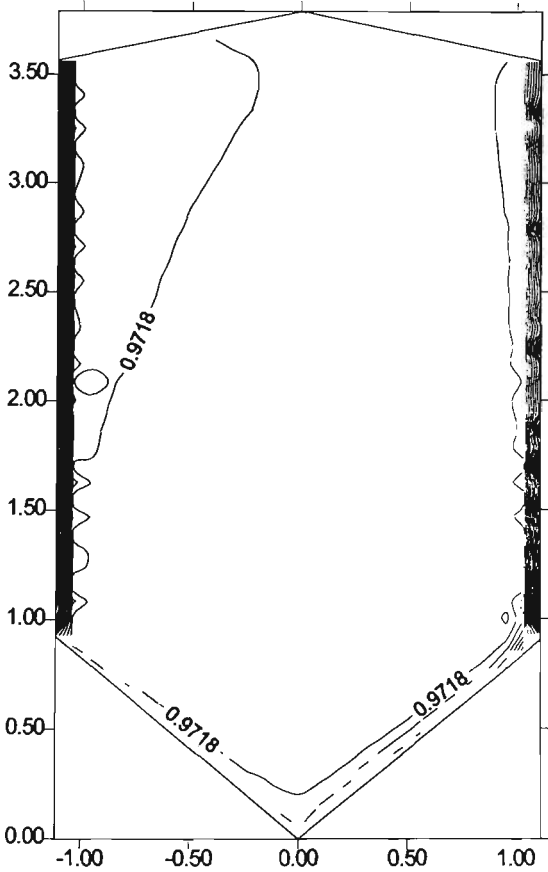
Figure 7.46 Seed viability distributions in the non-aerated silo



Seed viability at day 20 (linear duct)



Seed viability at day 40 (linear duct)



Seed viability at day 60 (linear duct)

Figure 7.47 Seed viability distributions in the silo fitted with a linear duct

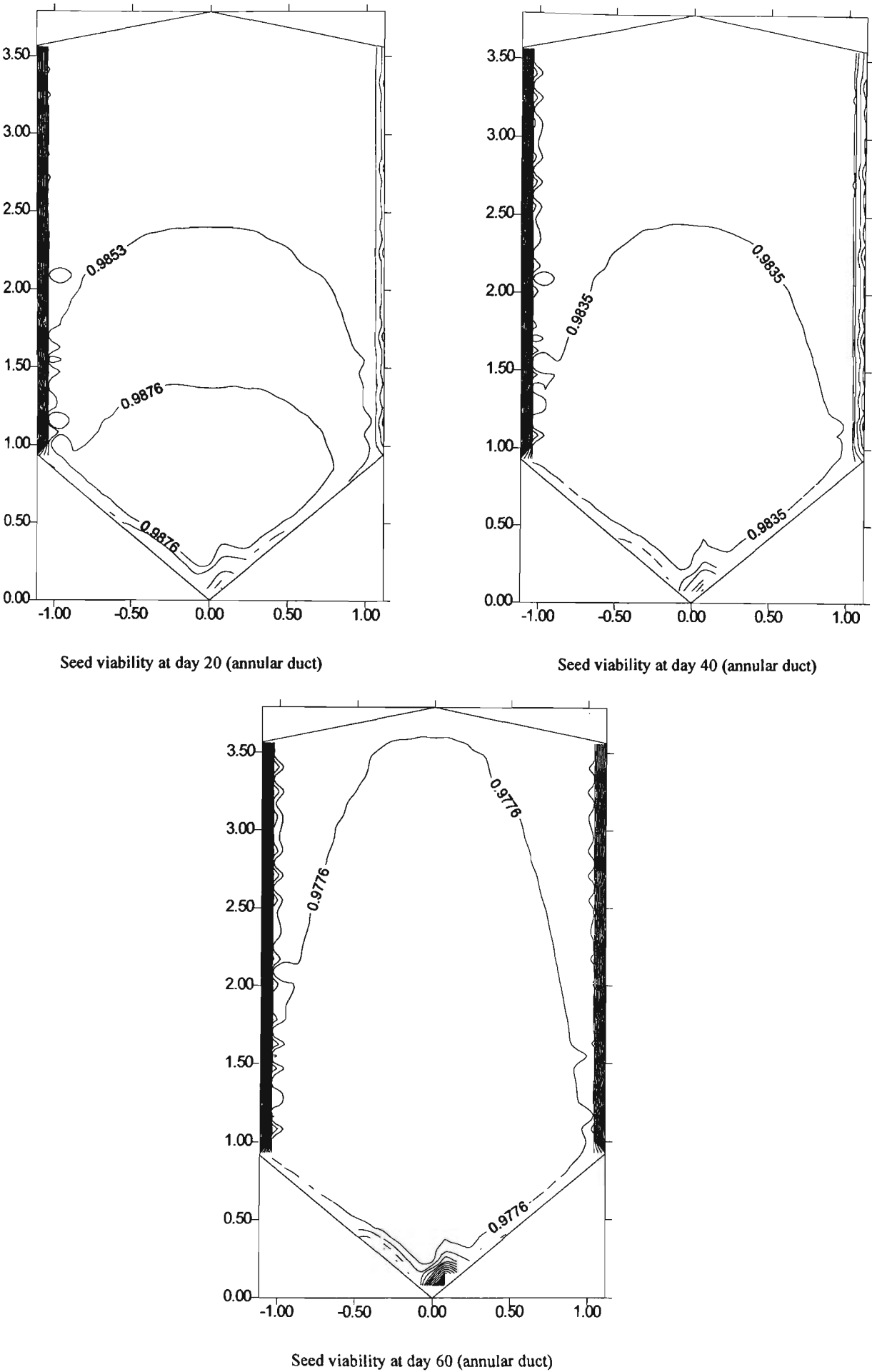


Figure 7.48 Seed viability distributions in the silo fitted with an annular duct

7.10 DECAY OF CHEMICAL PESTICIDE DISTRIBUTIONS

Temperature and moisture content are the major factors in the degradation of contact pesticides applied to grain. Pesticides can be effectively against the insects for many month, and can be applied to grain held in poorly constructed store without specialised equipment for their application.

Figures 7.52, 7.53 and 7.54 illustrate the distribution of the pesticide concentration in the stored grains. It is clear that the pesticide decays rapidly in the non-aerated silo. Indeed, the concentration of pesticide in the central region has falls to about 69% of its initial value of the 60 days storage (as shown in figure 7.52), this is because that the warm air flow is effected on this central region of the silo.

The rate of pesticide decays in the silo fitted with a linear duct clearly reflects the non-uniform cooling, it is shown in figure 7.53, and the pesticide concentration in the region furthest from the aeration duct is about 77% of its initial condition.

By contrast, it can be seen in figure 7.54 that the pesticide concentration in the silo fitted with the annular duct is generally about 80% of its initial pesticide decay in the central area of the silo, and reflects the uniform cooling wave to the pesticide decays in the silo.

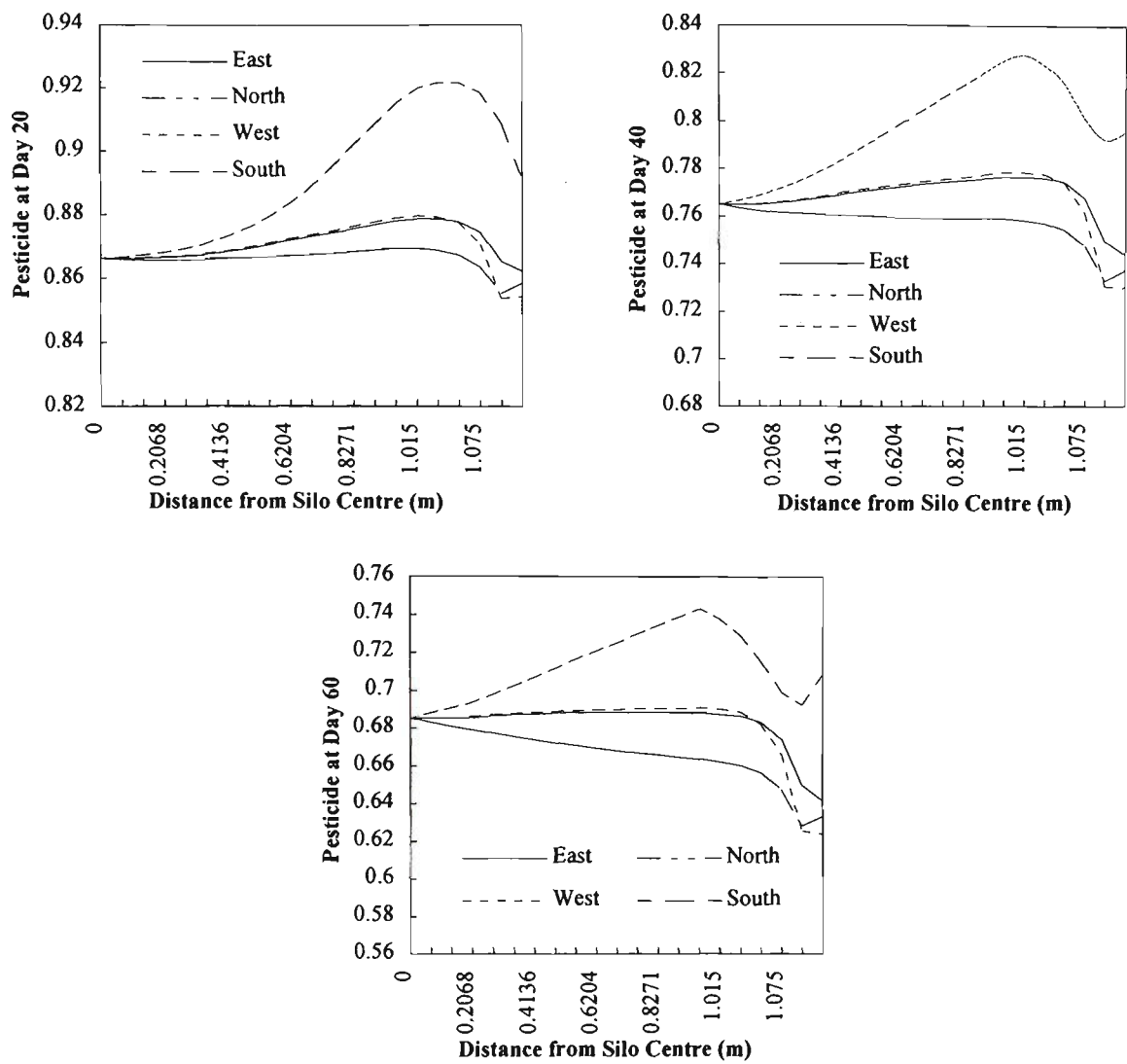
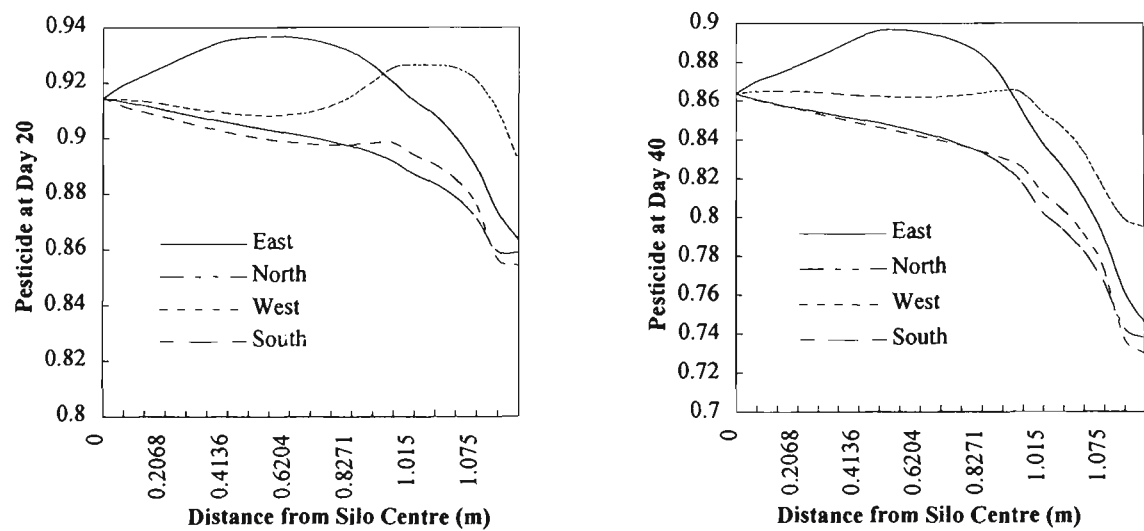


Figure 7.49 Radial profiles of the pesticide in the non-aerated case



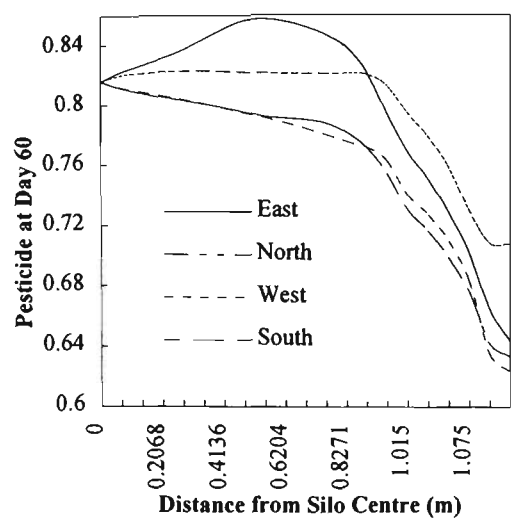


Figure 7.50 Radial profiles of the pesticide in the linear duct case

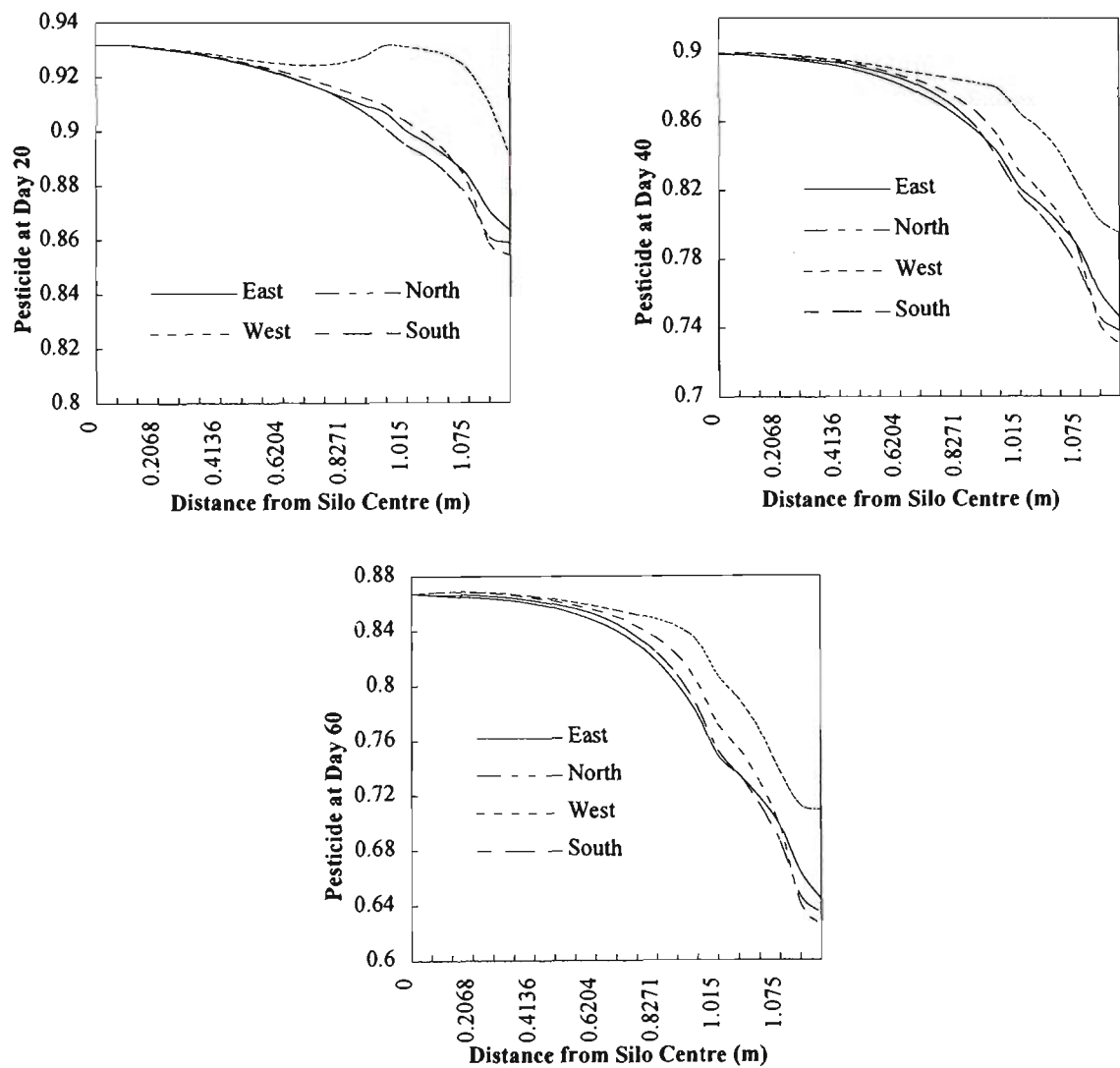
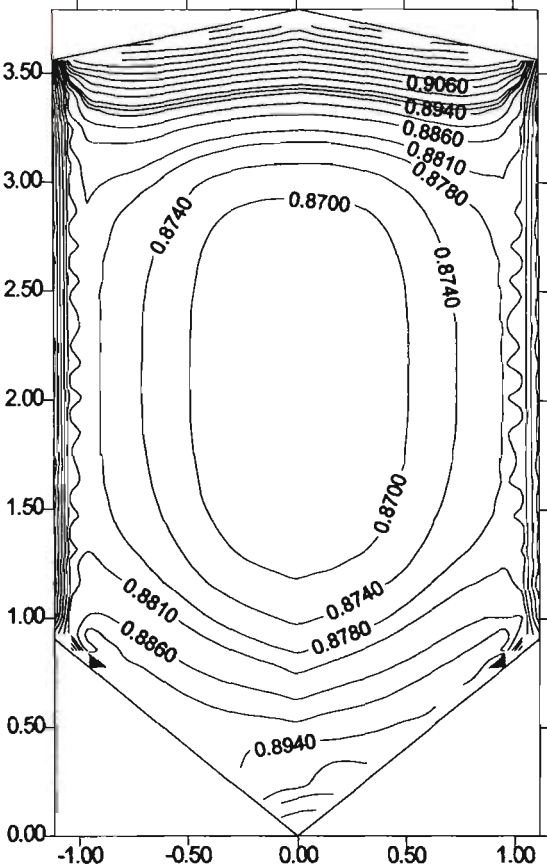


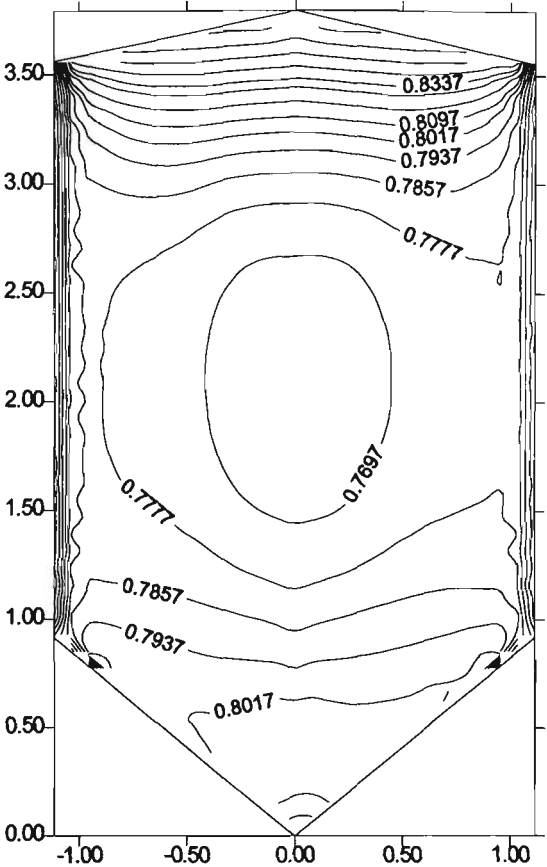
Figure 7.51 Radial profiles of the pesticide in the annular duct case

Figures 7.49, 7.50 and 7.51 show that the variation of the decay of chemical pesticide from the east, north, west and south facing portions of the wall. As would be expected, the pesticide concentration in the central region of the silo is higher in the aerated silos than in the non-aerated silo, and the silo fitted with an annular duct render the better results for protection the decay of pesticide than the silo fitted with a linear duct.

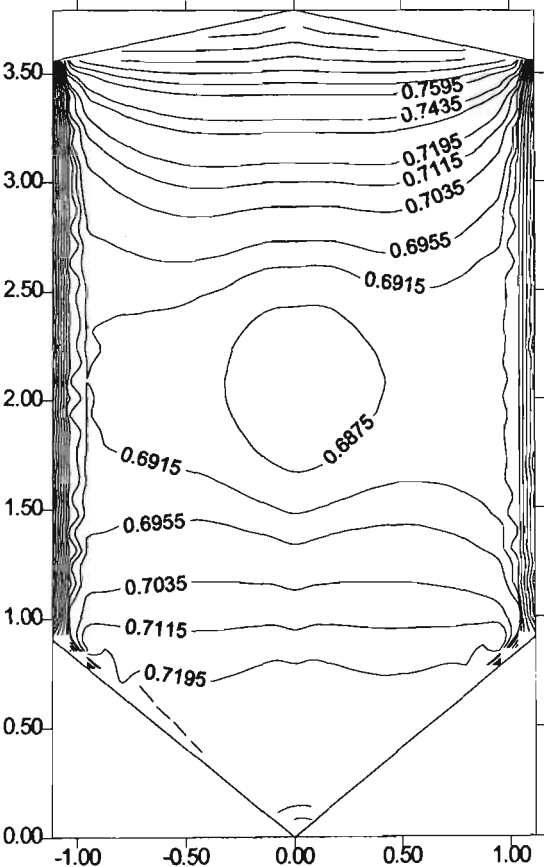
The rate of chemical pesticide is higher in the south side of the silo, this is because the sunlight is not strongly effected in this area, and the pesticide concentration is rapidly broken down at the east, west and north sides of the wall in the three cases by solar radiation heating during the day.



Pesticide at day 20 (non-aerated)



Pesticide at day 40 (non-aerated)



Pesticide at day 60 (non-aerated)

Figure 7.52 Pesticide distributions in the non-aerated silo

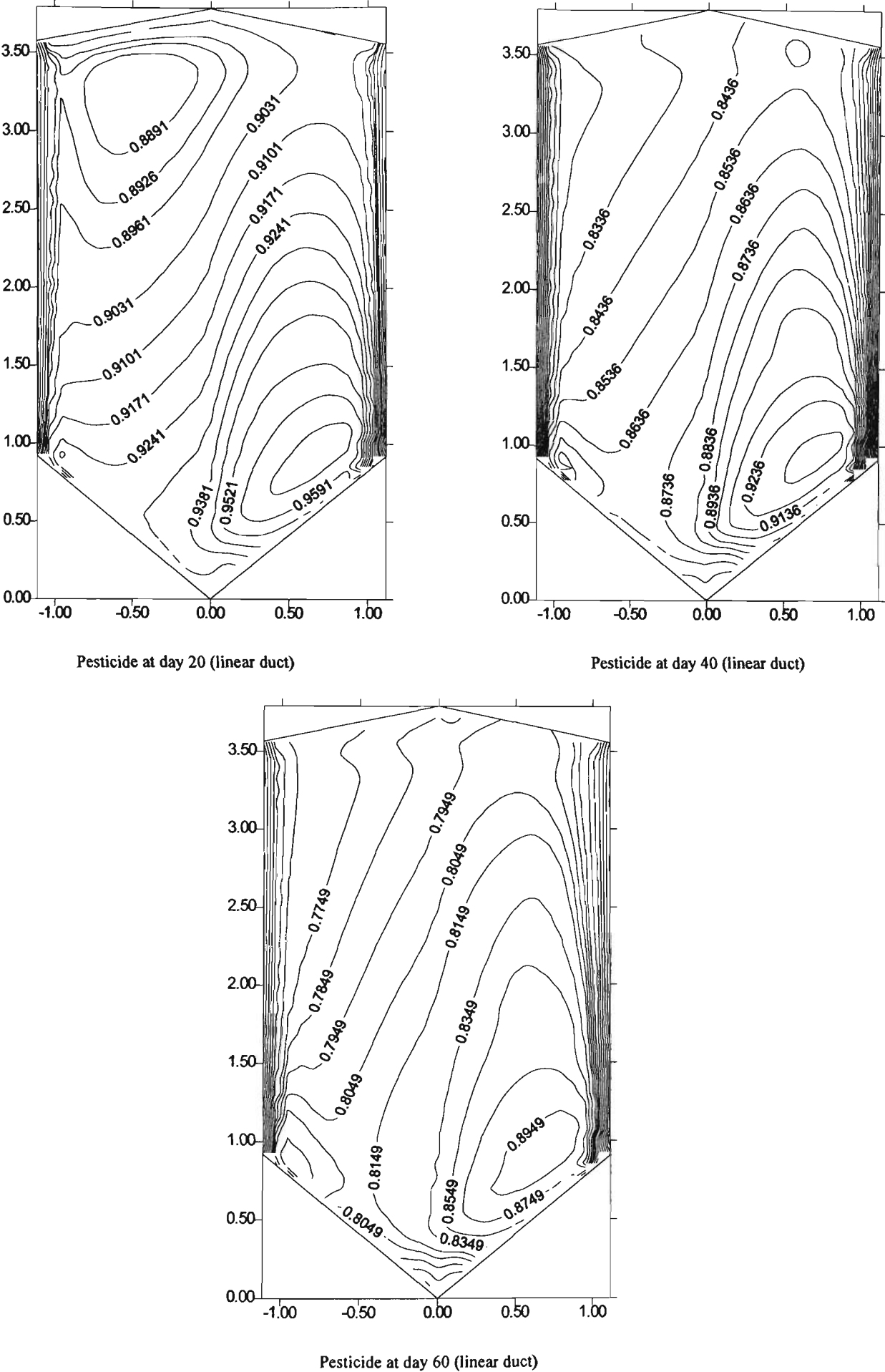


Figure 7.53 Pesticide distributions in the silo fitted with a linear duct

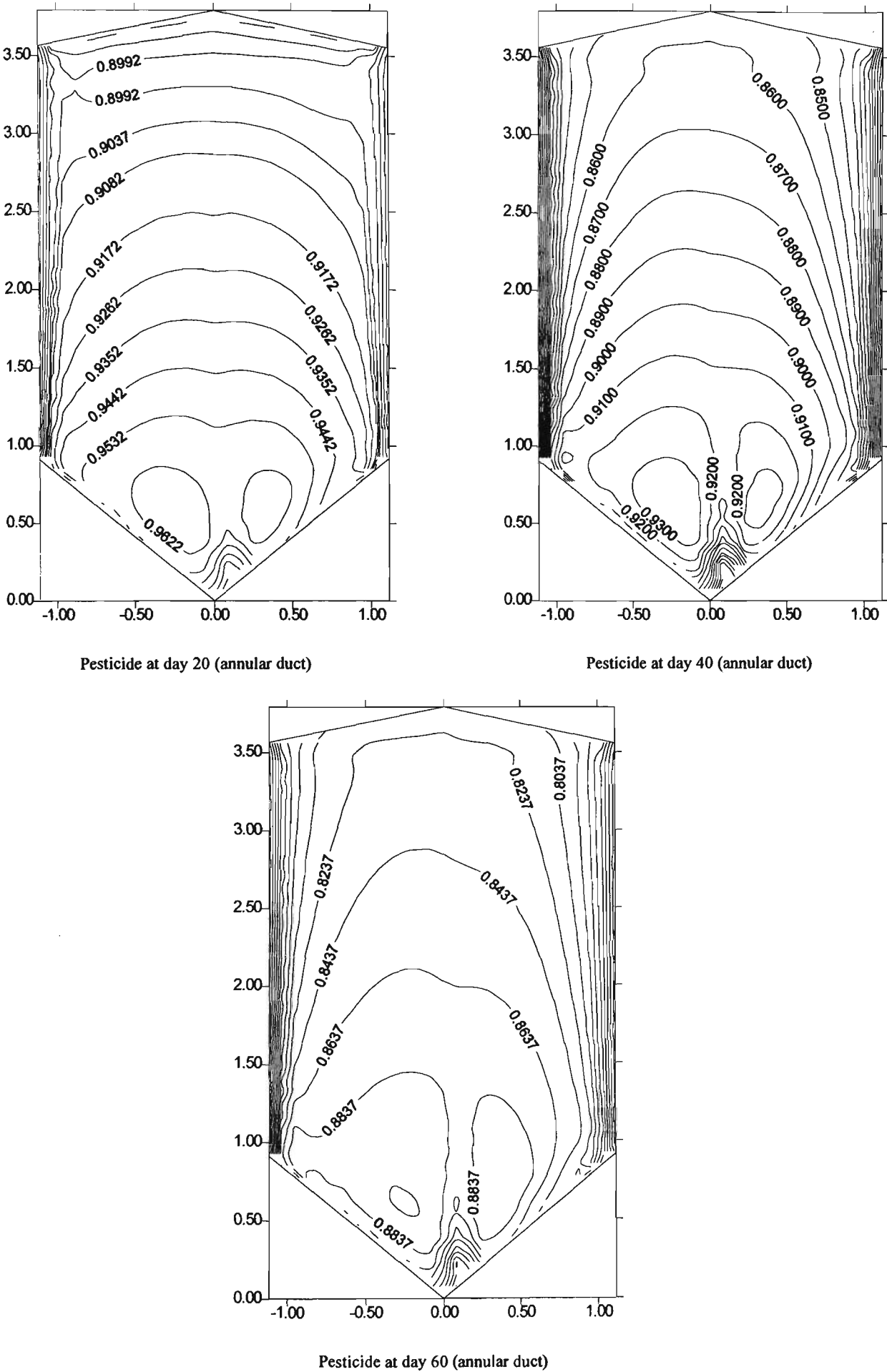


Figure 7.54 Pesticide distributions in the silo fitted with an annular duct

7.11 OVERVIEW

After 9 groups of profiles discussed, the performances between non-aerated, linear aeration and annular aeration systems are evident:

- Annular aeration system can provide strong and uniform flow of air to occurring in the silo symmetrically, and gives best results for protection of the environment of stored grain.
- Linear aeration system may provide a non-uniform airflow distribution, and offers a specific causes of special cooling results.
- The grains in the non-aerated system can be quickly damaged by insect pests attacking, and loss in the quantity and quality.
- In addition, the performances of simulation results which are used program SILO3DFTN to predict the ecosystems in a non-aerated silo, the silos fitted with linear and annular aeration ducts are summarised in table 7.1.

Table 7.1 The performance of non-aeration and aeration silos

	Non-aerated	Linear duct aeration	Annular duct aeration
Mean dry matter loss	0.0039	0.0038	0.0031
Mean concentration of fenitrothion	0.7092	0.7885	0.8238
Mean viability	0.9453	0.9647	0.9686
Mean concentration of <i>R. dominica</i>	12.7431	3.7367	2.6713
Mean concentration of <i>S. oryzae 1</i>	128.5328	24.2884	18.1394
Mean concentration of <i>S. oryzae 2</i>	63.0503	13.1513	10.0286
Mean concentration of <i>S. zeamais</i>	2.4118	1.3611	1.3197

7.12 LIMITATIONS OF THIS WORK

In this work that the insects are immobile, whereas in reality they are likely to translocate to more favourable microclimates. However, the results for insect growth indicate the potential for the growth of insect populations. Furthermore, the effects of aeration on the movement of insects has also been ignored. Essentially, the reason for this is that the biological data are simply not available, and this is an area worthy of study by stored products entomologist. In this work we have used rate of insect population data presented by Desmarchelier (1988). In this work it is explicitly acknowledged that there are differences in the behaviour of different strains of the same species of insects. The data presented by Desmarchelier (1988) are for age stable populations, which are highly unlikely to occur during the initial stages of grain storage.

Fungal activity appears to depend on a large number of variables, many of which relate to the postharvest conditions of the grain. Any deterministic model of mould activity must therefore be treated with extreme caution. In this work we have relied on the expression for the rate of respiration of grains presented by Lacey *et al.* (1994). This appears to give a rate of respiration much higher than that predicted by the work of Thompson (1972). Once more there is clearly a need for a much more detailed and deeper understanding of biological phenomena.

The data presented on the rate of decay of chemical pesticides are relatively deterministic, and since we are dealing with contact pesticides that are not labile. However, in practice, pesticides are unlikely to be applied with a uniform concentration as implied by this work, but variations can be easily accommodated.

CHAPTER 8

CONCLUSIONS

This chapter presents conclusions stemming from the work of the previous chapters. Also some suggestions and some further work directions within the framework introduced in this thesis.

8.1 SUMMARY OF CONTRIBUTIONS

- (1) A finite difference model for predicating the behaviour of the microclimate occurring within the conical bottomed circular silos was developed. The three-dimensional model was applied to estimate the actual variation of pressure, velocity, temperature, moisture content, absolute humidity, wet bulb temperature, dry matter loss, seed viability and pesticide decay in the grain storage.
- (2) A mapping technique provides a convenient methodology, and has strong ability to analysis the classical mathematical model for obtaining the numerical solution of partial differential equations in the arbitrary geometries.
- (3) Solar radiation is the major factor that influences the surface temperature on the silo wall. It can causes the temperature gradients raising to conduction, leading to

moisture transfer, and consequent grain damage. It is the important parameter for choice the colour of the silo, and the placement of the aeration duct.

- (4) The research has shown that grain temperatures remain high prolonged period of time in the non-aerated silo. Aeration is successful in cooling the grain bulk, but the grain at the peripheries is little affected by aeration.
- (5) Importantly, the results of the work demonstrated: The silo fitted with annular duct is more uniformly cooled than silo fitted with conventional linear duct. Grain in the annular aerated silo are stored in better condition with a higher viability and lower pesticide decay. Furthermore, insect population growth can also be better controlled in the silo fitted with an annular duct.
- (6) The mathematical analysis has been encoded in FORTRAN, and the program listing forms a part of this thesis (see Appendix III).

8.2 FUTURE WORK

The future research should be carried out in the following areas:

- (1) Research projects should validate the computer model by carrying out field experiment measurements, for investigating pressure, temperature and moisture content in a conical bottomed circular silo, with non-aerated, linear aeration and annular aeration systems. Moreover, the experiments should indicate the environmental variables which are relevant and pertain to practical situations.
- (2) Ecological study of computerization model should be used to investigate the likely success of aeration system in a range of climates, specially the methods of augmenting aeration with ambient air by mechanical refrigeration and solar

cooling are also worthy. Besides, the study should include the effect of the size of the silo and the duct placement on the performance of aeration system .

- (3) It is also important to study the interaction of the air in the headspace of a silo and the grain bulk.

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APPENDIX I

THOMAS ALGORITHM

Thomas algorithm is a particularly efficient method for solving the system of tri-diagonal matrix, and it is relatively simple. The product procedure is expressed as following.

The discretized triangular factorisation of the linear system is taken the form as:

$$b_1\omega_2 + c_1\omega_3 = d_1 - a_1\omega_1 \quad (\text{I-1})$$

$$a_2\omega_2 + b_2\omega_3 + c_2\omega_4 = d_2 \quad (\text{I-2})$$

$$a_3\omega_3 + b_3\omega_4 + c_3\omega_5 = d_3 \quad (\text{I-3})$$

.....

$$a_{ii}\omega_{i-1} + b_{ii}\omega_i + c_{ii}\omega_{i+1} = d_{ii} \quad (\text{I-4})$$

.....

$$a_{n-3}\omega_{n-3} + b_{n-3}\omega_{n-2} + c_{n-3}\omega_{n-1} = d_{n-3} \quad (\text{I-5})$$

$$a_{n-2}\omega_{n-2} + b_{n-2}\omega_{n-1} = d_{n-2} - c_{n-2}\omega_n \quad (\text{I-6})$$

in which $ii = i - 1$ ($ii = 1, \dots, n$; and $i = 1, \dots, n - 1$)

$$\text{if } ii = 1, \quad d_1 = d_1 - a_1\omega_1$$

$$\text{if } ii = n - 2 \quad d_{n-2} = d_{n-2} - c_{n-2}\omega_n$$

The matrix of coefficients is:

$$\begin{bmatrix}
 b_1 & c_1 & & & & \\
 & a_2 & b_2 & c_2 & & \\
 & & a_3 & b_3 & c_3 & \\
 & & & \dots & & \\
 & & & & a_{ii} & b_{ii} & c_{ii} \\
 & & & & & \dots & \\
 & & & & & & a_{n-3} & b_{n-3} & c_{n-3} \\
 & & & & & & & a_{n-2} & b_{n-2}
 \end{bmatrix} \times \begin{bmatrix} \omega_2 \\ \omega_3 \\ \omega_4 \\ \dots \\ \omega_i \\ \dots \\ \omega_{n-2} \\ \omega_{n-1} \end{bmatrix} = \begin{bmatrix} d_1 \\ d_2 \\ d_3 \\ \dots \\ d_i \\ \dots \\ d_{n-3} \\ d_{n-2} \end{bmatrix}$$

(I-7)

The basic idea for solving this matrix is to reduce one column at an equivalent triangular system by means of substitution and manipulation of the matrix coefficients into the form as below:

$$\begin{bmatrix}
 \beta_1 & c_1 & & & & \\
 & \beta_2 & c_2 & & & \\
 & & \beta_3 & c_3 & & \\
 & & & \dots & & \\
 & & & & \beta_{ii} & c_{ii} \\
 & & & & & \dots & \\
 & & & & & & \beta_{nn-1} & c_{nn-1} \\
 & & & & & & & \beta_{nn}
 \end{bmatrix} \times \begin{bmatrix} X_1 \\ X_2 \\ X_3 \\ \dots \\ X_{ii} \\ \dots \\ X_{nn-1} \\ X_{nn} \end{bmatrix} = \begin{bmatrix} \delta_1 \\ \delta_2 \\ \delta_3 \\ \dots \\ \delta_{ii} \\ \dots \\ \delta_{nn-1} \\ \delta_{nn} \end{bmatrix}$$

(I-8)

Firstly, we define:

$$b_1 = \beta_1 \quad (I-9)$$

$$d_1 = \delta_1 \quad (I-10)$$

$$\omega_2 = X_1; \omega_3 = X_2; \dots \omega_{n-1} = X_{nn} \quad (I-11)$$

So equation (I-1) and (I-2) can be written as:

$$\beta_1 X_1 + c_1 X_2 = \delta_1 \quad (\text{I-12})$$

$$a_2 X_1 + b_2 X_2 + c_2 X_3 = d_2 \quad (\text{I-13})$$

Multiplying equation (I-12) by $\frac{a_2}{\beta_1}$, we will get:

$$a_2 X_1 + \frac{a_2}{\beta_1} c_1 X_2 = \frac{a_2}{\beta_1} \delta_1 \quad (\text{I-14})$$

Then subtracting equation (I-13) from equation (I-14) yields:

$$(b_2 - \frac{a_2}{\beta_1} c_1) X_2 + c_2 X_3 = d_2 - \frac{a_2}{\beta_1} \delta_1 \quad (\text{I-15})$$

We define again:

$$\beta_2 = b_2 - \frac{a_2}{\beta_1} c_1 \quad (\text{I-16})$$

$$\delta_2 = d_2 - \frac{a_2}{\beta_1} \delta_1 \quad (\text{I-17})$$

Equation (I-15) becomes:

$$\beta_2 X_2 + c_2 X_3 = \delta_2 \quad (\text{I-18})$$

However, the summarisation calculation of the coefficient matrix is subject to the following recursion relations:

$$\beta_{ii} = b_{ii} - \frac{c_{ii} a_{ii}}{\beta_{ii-1}} \quad (\text{I-19})$$

$$\delta_{ii} = d_{ii} - \frac{\delta_{ii-1} a_{ii}}{\beta_{ii-1}} \quad (\text{I-20})$$

Continuing this procedure until an equation with only one unknown is obtained.

The solution of tri-diagonal system can be solved by using last equation to solve for X_m , such as:

$$X_m = \frac{\delta_m}{\beta_m} \quad (\text{I-21})$$

Then substituting the result of X_{nm} into the second last equation and solving for X_{nm-1} , and so forth. The general form for doing this procedure is written as:

$$X_{ii-1} = \frac{\delta_{ii-1} - c_{ii-1}X_{ii}}{\beta_{ii-1}} \quad (\text{I-22})$$

Remembering $\omega_{nm} = X_{nm}$. Update the value of X_{ii} to ω_i , then the tri-diagonal system is completely solved.

APPENDIX II

NEWTON-RAPHSON METHOD

Newton-Raphson method is applied to a non-linear equation as:

$$f(X) = 0 \quad (\text{II-1})$$

The algebraic rearrangements of equation (II-1) take the form is:

$$X = g(x) \quad (\text{II-2})$$

When equation (II-1) has an approximation to a root $X_n = \alpha$, the better approximation given by X_{n+1} , generally it is written as:

$$X_{n+1} = X_n - \frac{f(X_n)}{f'(X_n)} \quad (\text{II-3})$$

Equation (II-3) is the Newton-Raphson scheme. This scheme can be explained as the form as following:

$$\text{Nest Estimate} = \text{Current Estimate} + \text{Correction Term} \quad (\text{II-4})$$

in which the *Correction Term* of $\frac{-f(X_n)}{f'(X_n)}$ must be small, when X_n is close to the root if convergence is to be achieved.

When provide $f'(X_n) \neq 0$, the Newton- Raphson method is at least a second order process. The iterative equation (II-3) can be repeatedly used to find improved approximations to the real root α .

APPENDIX III

A LISTING OF PROGRAM - SILO3DFTN

```

c#####SILO3D#####
c  Calculate pressure,velocity,temperature and moisture      #
c  content and humidity distributions in ventilated grain    #
c  storage                                                    #
c#####
c
  Program silo3Dftn
  Include'dry.inc'
  Include'solar.inc'

c
  Open (unit=5,file='crop.in',status='unknown')
  Open (unit=6,file='crop.out',status='unknown')
  Open (unit=7,file='pv.out',status='unknown')
  Open (unit=8,file='pv.in',status='unknown')
  Open (unit=9,file='preplot.out',status='unknown')
  Open (unit=12,file='vciplot.out',status='unknown')
  Open (unit=13,file='verplot.out',status='unknown')
  Open (unit=15,file='surface.out',status='unknown')
  Open (unit=28,file='crop6.out',status='unknown')
  Open (unit=29,file='crop7.out',status='unknown')
  Open (unit=87,file='prewall.out',status='unknown')
  Open (unit=88,file='crop19.out',status='unknown')
  Open (unit=89,file='crop20.out',status='unknown')
  Open (unit=90,file='perr.out',status='unknown')
  Open (unit=91,file='pretime.out',status='unknown')
  Open (unit=92,file='vraplot.out',status='unknown')
  Open (unit=93,file='velwall.out',status='unknown')
  Open (unit=94,file='airflow.out',status='unknown')
  Open (unit=95,file='aerat.out',status='unknown')

c
  Call input
  Call display
  Call setcon
  Call props
  Call initial
  Call silosize
  Call surtemp
  Call ductbc(p,pduct)

c
  calculate pressure difference
  if(pnotfid)then

c
    Call pressure
    Call pvout
  else
    Call pvin
    Call pressure
    Call pvout
  end if

c
  write(*,9550)
  9550 format(1x,'pressure filed determined')

c
  Call flowrate

c
  Output pressure filed for plotting
  Call pvmod
  Call pressplot
  Call wallpress

c
  Output velocity filed for plotting
  Call velraplot
  Call velverplot
  Call velcirplot
  Call wallvel

c
  Call velsave

c
  ~~~~~
c  Begin heat and mass transfer calculations
  write(*,9600)
  9600 format(1x,'Begin heat and mass transfer calculations')

c
  Convert moisture content to dry basis
  if(mcb)then
    winitd=winit/(1.0-winit)
    write(28,3100)
    write(28,3200)titit
    write(28,3210)winit
    write(28,3220)winitd
    write(28,3230)qu

c
    3100 format(///1x,5x,'Mcbea cooler is invoked')

```

```

3200 format(1x,5x,'initial grain temperature',f7.1)
3210 format(1x,5x,'initial grain mc(wet bulb)',f7.4)
3220 format(1x,5x,'initial grain mc(dry bulb)',f7.4)
3230 format(1x,5x,'flow rate through cooler(m**3/s)',f7.4)
      else
c
c      write(28,3240)
3240 format(1x,5x,'Mcbea cooler is not invoked')
      end if
c
c      ~~~~~
c      Calculate the amplitude of the diurnal temperature variation
c      (amp) and the mean ambient temperature (tmean).
c
      amp=tmax(1)-tmin(1)
      tmean=0.5*(tmax(1)+tmin(1))
c
      aerationtime=0.0
      timer=0.0
      time=0.0
      hamb=humidity
      Call tprise
      dayhour=1.0
      kount=0
c
      tprint0=0.0
      tprint5=real(maxday)/12.0
      tprint10=real(maxday)/6.0
      tprint15=real(maxday)/4.0
      tprint20=real(maxday)/3.0
      tprint25=(real(maxday)*5.0)/12.0
      tprint30=real(maxday)/2.0
      tprint35=(real(maxday)*7.0)/12.0
      tprint40=(real(maxday)*2.0)/3.0
      tprint45=(real(maxday)*3.0)/4.0
      tprint50=(real(maxday)*5.0)/6.0
      tprint55=(real(maxday)*11.0)/12.0
      tprint60=real(maxday)
c
      kprint0=0
      kprint5=0
      kprint10=0
      kprint15=0
      kprint20=0
      kprint25=0
      kprint30=0
      kprint35=0
      kprint40=0
      kprint45=0
      kprint50=0
      kprint55=0
      kprint60=0
      kkp2=0
      kkp4=0
c
      do 50 kkk=1, ku1
      do 52 kk=1, ku2
          taerate1=aerate1*3600.0
          taerate2=aerate2*3600.0
          if((timer.le.taerate1).or.(timer.gt.taerate2))then
              write(*,9575)
              format(1x,'Aeration system off')
          9575
              noflow=1
              Call velconduct
              dtg=dtgconduct
              else
                  write(*,9595)
                  format(1x,'Aeration system on')
          9595
              noflow=0
              Call velaerate
              dtg=dtgaerate
              aerationtime=aerationtime+dtg/3600.0
c
              write(95,5420)aerationtime
              format(1x,'Total aeration fan operation=',f14.8,
                  &
                  'hours')
              end if
          5420
      &
      end if

```

```

c      ifreq=2.0*3600.0/dtg
      kount=kount+1
      kkount=kount/ifreq
      kkkount=kkount*ifreq
      time=time+dtg
      timer=timer+dtg

c
c      if(timer.gt.86400.0)then
          timer=timer-86400.0
      end if

c      timeh=time/3600.0
      timeday=time/(3600.0*24.0)
      tstop=3600.0*24.0*real(maxday)

c      dayhour=dayhour+dtg/3600.0

c      if(dayhour.ge.25.0)then
          dayhour=dayhour-24.0
      end if

c      kh=dayhour

c      tamb=tmean+0.5*amp*sin((timeh-9.0)*3.14159/12.0)

c      if(mcb)then
          Call wetbulb(tamb,hamb,twamb)
          Call mcbear(twamb,tamb,twout)
          Call twout1(twout,tin,hin)
      else
          tin=tamb+trise
          hin=hamb
      end if

c      if(smith)then
          Call wesmith(hin,tin,win)
      else
          Call we(tin,hin,win)
      end if

c
c      Call tbc(tamb)
      if(noflow.eq.0)Call ductbc(t,tin)

c
      do k=1,nz
      do j=1,nphi
      do i=1,nrm1
          if(smith)then
              Call humsm(i,j,k)
          else
              Call hum(i,j,k)
          end if
      end do
      end do
      end do

c      if(noflow.eq.0)Call ductbc(h,hin)

c      do 54 k=2,nzm1
      do 56 j=1,nphi
      do 58 i=2,nrm1

          if(smith)then
              Call respl(i,j,k,time)
          else
              Call resp(i,j,k)
          end if

          dmlloss(i,j,k)=dmlloss(i,j,k)+ddmdt*dtg

c      Solve moisture conservation equation and thermal energy equation

          Call moistu(i,j,k)
          Call tempera(i,j,k)

          continue
          continue
          continue
c      c~~~~~
c      Establish boundary conditions

```



```

else
  continue
end if

c
52  continue
c
c~~~~~~
c
  write(28,3950)time,timeh,timeday
  write(28,3955)aerationtime
  write(28,3960)timer
  write(28,3965)dayhour
  write(28,3970)kount

c
3950 format(1x,5x,'time(SECOND)',f12.4,2x,'timeh(HOURS)',f12.4,2x,
&
'TIME(DAY)',f12.4)
3955 format(1x,5x,'aerationtime',f10.3,'HOURS')
3960 format(1x,5x,'timer',f12.4)
3965 format(1x,5x,'dayhour',f8.4)
3970 format(1x,5x,'kount',I5)
c
  Call fileopen
  Call totals
  Call outputcooler(tamb,hamb,twamb,twout,tin,hin)
  Call outputhum(time,timeh)

c
  Call results

c
50  continue
c
  end

c
c#####
c##### Read input file
c#####
c#####
c
  Subroutine input
  Include'dry.inc'
  Include'solar.inc'

c
  read(5,1000)

```

```

read(5,1000)
read(5,1000)
read(5,1010)nr,nphi,nz
read(5,1010)ku1,ku2,maxday
read(5,1010)kp1,kp2
read(5,1020)dtp,digaerate,dtgconduct
read(5,1030)wR,wz1,specflo,res
read(5,1040)gam1,gam2
read(5,1050)tinit,winit
read(5,1060)tmean,tamp,humidity
read(5,1070)nphiminc,nphimaxdc,nrmindc,nrmmaxdc
read(5,1040)aerate1,aerate2
read(5,1080)mcb
read(5,1080)pnotfld
read(5,1080)smith
c
1000 format( )
1010 format(45x,3I8)
1020 format(45x,3f6.1)
1030 format(45x,4f10.4)
1040 format(45x,2f6.2)
1050 format(45x,2f7.4)
1060 format(45x,2f5.1,E7.1)
1070 format(45x,4I6)
1080 format(45x,L8)
c
  read(5,1000)
  read(5,1090)phi
  read(5,1100)(suns(k),k=1,6)
  read(5,1110)(nuda(k),k=1,6)
  read(5,1100)(tmin(k),k=1,6)
  read(5,1100)(tmax(k),k=1,6)
  read(5,1120)alpha,epsilon
  read(5,1000)
c
1090 format(45x,f6.2)
1100 format(45x,6f5.1)
1110 format(45x,6I4)
1120 format(45x,2f4.1)
c
  return

```



```

end
c
c#####
c      Display input file
c#####
c#####
c      Subroutine display
c      Include'dry.inc'
c      Include'solar.inc'
c
c      write(28,*)nr,nphi,nz
c      write(28,*)ku1,ku2,maxday
c      write(28,*)kp1,kp2
c      write(28,*)dtp,dgaerate,dtgconduct
c      write(28,*)wR,wz1,specflo,res
c      write(28,*)gam1,gam2
c      write(28,*)tinit,winit
c      write(28,*)tmean,tamp,humidity
c      write(28,*)nphimindc,nphimaxdc,nrmindc,nrmaxdc
c      write(28,*)aerate1,aerate2
c      write(28,*)mcb
c      write(28,*)pnotfld
c      write(28,*)smith
c
c      write(28,*)phi
c      write(28,*)(suns(k),k=1,6)
c      write(28,*)(nuda(k),k=1,6)
c      write(28,*)(tmin(k),k=1,6)
c      write(28,*)(tmax(k),k=1,6)
c      write(28,*)alpha,epsilon
c
c      return
c      end
c
c#####
c      Set up grain silo constants
c#####
c#####
c      Subroutine setcon
c      Include'dry.inc'
c
c      Dimension of bulk ( The radius of silo is wR; Thetall of silo's
c      wall is wz1; The total high of silo is wz; The corn of silo's
c      angels are gamma1 and gamma2 ).
c      nrm1=nr-1
c      nrm2=nr-2
c      nzm1=nz-1
c      nzm2=nz-2
c      pi=3.14159
c      wphi=2.0*pi
c      gamma1=gam1*pi/180.0
c      gamma2=gam2*pi/180.0
c      wz=wz1+wR*(tan(gamma1)+tan(gamma2))
c
c      Spacing of nodes
c      dphi=wphi/real(nphi)
c
c      Set uniform mesh for initial trials
c      hr(nrm1)=0.02/wR
c      hr(nrm2)=0.02/wR
c      hr(nr-3)=0.02/wR
c      hr(nr-4)=0.02/wR
c      hr(nr-5)=0.02/wR
c      hr(nr-6)=0.05/wR
c      nrm7=nr-7
c
c      do i=1, nrm7
c          hr(i)=(1.0-0.15/wR)/(real(nrm7))
c      end do
c
c      do k=1, nzm1
c          hz(k)=1.0/real(nzm1)
c      end do
c
c      Calculate the distance of radius r(i)
c      do i=1, nr
c          if(i.eq.1)then
c              r(1)=0.0
c          else
c              r(i)=r(i-1)+hr(i-1)*wR
c          end if
c      end do

```

```

c
c      Calculate the distance of vertical z(i,k)
do k=1, nz
  do i=1, nr
    z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
      (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
  end do
end do
&

c
c      Set mesh transformation constants
do 7 k=1, nz
  do 7 i=1, nr
    urz=z(i,k)-r(i)*tan(gamma1)
    vrz=real(wz)-r(i)*(tan(gamma1)+tan(gamma2))
    durzdr=tan(gamma1)
    dvrzdr=-(tan(gamma1)+tan(gamma2))

    alpha1(i,k)=1.0/(real(wR))
    alpha2(i,k)=(durzdr*vrz-urz*dvrzdr)/(vrz**2)
    alpha3(i,k)=0.0
    alpha4(i,k)=1.0/vrz

    beta1(i,k)=alpha1(i,k)**2+alpha3(i,k)**2
    beta2(i,k)=alpha2(i,k)**2+alpha4(i,k)**2
    beta3(i,k)=2.0*(alpha1(i,k)*alpha2(i,k)+alpha3(i,k)
      *alpha4(i,k))
    beta4(i,k)=0.0
    beta5(i,k)=(4.0*(-vrz*durzdr+urz*dvrzdr)*dvrzdr)/(\vrz
      **3)
    if(i.eq.1)go to 7
    beta6(i,k)=beta4(i,k)+alpha1(i,k)/r(i)
    beta7(i,k)=beta5(i,k)+alpha2(i,k)/r(i)
    beta8(i)=1.0/(r(i)**2)
  end do
7 continue

c
c      Set finite difference operators at the internodals
do i=2, nrml
  cr1(i)=hr(i)/(hr(i-1)*(hr(i-1)+hr(i)))
  cr2(i)=(hr(i)-hr(i-1))/(hr(i-1)*hr(i))
  cr3(i)=hr(i-1)/(hr(i)*(hr(i-1)+hr(i)))

  cr4(i)=2.0/(hr(i-1)*(hr(i)+hr(i-1)))
  cr5(i)=2.0/(hr(i-1)*hr(i))
  cr6(i)=2.0/(hr(i)*(hr(i)+hr(i-1)))
end do

c
do k=2, nrml
  cz1(k)=hz(k)/(hz(k-1)*(hz(k-1)+hz(k)))
  cz2(k)=(hz(k)-hz(k-1))/(hz(k-1)*hz(k))
  cz3(k)=hz(k-1)/(hz(k)*(hz(k-1)+hz(k)))
  cz4(k)=2.0/(hz(k-1)*(hz(k)+hz(k-1)))
  cz5(k)=2.0/(hz(k-1)*hz(k))
  cz6(k)=2.0/(hz(k)*(hz(k)+hz(k-1)))
end do

c
do j=1, nphi
  cp1(j)=1.0/(2.0*dphi)
  cp2(j)=0.0
  cp3(j)=1.0/(2.0*dphi)
  cp4(j)=1.0/(dphi**2)
  cp5(j)=2.0/(dphi**2)
  cp6(j)=1.0/(dphi**2)
end do

c
c      Set finite difference operators at the boundaries
crb4=(2.0*hr(nrml)+hr(nrml))/(hr(nrml)*(hr(nrml)+hr(nrml)))
crb5=(hr(nrml)+hr(nrml))/(hr(nrml)*hr(nrml))
crb6=hr(nrml)/(hr(nrml)*(hr(nrml)+hr(nrml)))

c
czb1=(-2.0*hz(1)+hz(2))/(hz(1)*(hz(2)+hz(1)))
czb2=(hz(1)+hz(2))/(hz(1)*hz(2))
czb3=-hz(1)/(hz(2)*(hz(2)+hz(1)))
czb4=(2.0*hz(nrml)+hz(nrml))/(hz(nrml)*(hz(nrml)+hz(nrml)))
czb5=(hz(nrml)+hz(nrml))/(hz(nrml)*hz(nrml))
czb6=hz(nrml)/(hz(nrml)*(hz(nrml)+hz(nrml)))

c
return
end

c
c#####
c##### Set up the properties of the system -#
c#####
c#####

```

```
c
c Subroutine props
  Include'dry.inc'
  Real keff

c
c constants associated with sorption isotherm
  cw1=-0.5016001
  cw2=5.6323
  cw3=-0.09832
  cw4=3.104
  cw5=11.4758
  p0=115840.0
  w0=(cw2**cw1/cw4**cw3)**(1.0/(cw3-cw1))
  revm=3.788
  wsat=0.32235
  h0=cw1*cw3/(cw3-cw1)*log(cw2/cw4)

c
c constants in integral heat of wetting equation
  hw1=0.0003476
  hw2=2.119
  hw3=-32.10
  hw4=303.24
  hw5=-1156.8
  hw6=0.01867
  hw7=0.1049
  hw8=-5.810
  hw9=14.975
  hw10=-14.868

c
c Thermophysical and other properties of the grain/air/water system
  eps=0.4
  rhos=1300.0
  rhob=(1.0-eps)*rhos
  rhoa=1.2
  cg=1300.0
  cw=4186.0
  ca=1000.0
  keff=0.15
  deff=0.000005
  dhvdr=-2377.0
  hv=2502390.0

c
c Subroutine props
  patm=101325.0

c
c Relative humidity of air leaving McBea cooler
  rhout=0.75

c
c Properties of the material
  deta=0.5

c
c Constants in the Lacey, Hamer and Magan equation
  a1lhm=0.00034583*20.0/21.0
  a2lhm=0.0001252*20.0/(21.0*3600.0)
  a3lhm=0.1737
  a4lhm=20.33
  a5lhm=0.9143
  a6lhm=-0.001036/3600.0
  a7lhm=-0.013634
  a8lhm=24.38

c
c Insect population growth parameters
  crdom=0.0435
  csoryz1=0.052
  csoryz2=0.048
  csz=0.018
  trdom=13.0
  tsoryz1=9.0
  tsoryz2=9.8
  tsz=14.0

c
c Kinetic constants determine the rate of pesticide decay
  bfe=0.036
  thalfe=8.467E6
  pduct=1000.0

c
  return
end

c
c#####
c Set up initial conditions of grain silo. Such as: pressure, #
c temperature, moisture content and dry matter loss, etc. #
c#####
```

```

c      Subroutine initial
      Include'dry.inc'

c      winitd=winit/(1.0-winit)
      do i=1,nr
        do j=1,nphi
          do k=1,nz
            p(i,j,k)=0.0
            t(i,j,k)=tinit
            w(i,j,k)=winitd
            dmlloss(i,j,k)=0.0
          end do
        end do
      end do

c      cfe(i,j,k)=1.0
      viability(i,j,k)=0.99
      savep(i,j,k)=0.0

c      if(smith)then
        Call humsmith(i,j,k)
      else
        Call hum(i,j,k)
      end if

c      rdomconc(i,j,k)=1.0
      soryz1c(i,j,k)=1.0
      soryz2c(i,j,k)=1.0
      szconc(i,j,k)=1.0
    end do
  end do
end do

c      return
      end

c#####
c      Calculate the volume of silo
c#####
c      Subroutine silosize
      Include'dry.inc'

c      write(15,1000)

c#####
c      Subroutine surtemp
      Include'dry.inc'
      Include'solar.inc'

c      write(15,1000)

c#####
c      Calculate the temperature of surface subjected to
      heating and cooling by radiation and convection
c#####
c      write(28,3677)volume,totvol
      format(/1x,5x,'volume=',f10.4,'sum of volume elements=',f10.4)

c      return
      end

c#####
c      Calculate the temperature of surface subjected to
      heating and cooling by radiation and convection
c#####
c      Subroutine surtemp
      Include'dry.inc'
      Include'solar.inc'

c      write(15,1000)

c#####
c      Calculate the temperature of surface subjected to
      heating and cooling by radiation and convection
c#####

```

```

write(15,1010)phi
write(15,1020)(suns(k),k=1,6)
write(15,1030)(nuda(k),k=1,6)
write(15,1040)(tmin(k),k=1,6)
write(15,1050)(tmax(k),k=1,6)
write(15,1060)alpha,epsilon

c
1000 format(1x,'Calculate the temperature of inclined surface:')
1010 format(1x,'Latitude=',f6.2)
1020 format(1x,'Sunshine hours per day=',6f5.1)
1030 format(1x,'Number of day of year=',6f5.1)
1040 format(1x,'Minimum daily temperature=',6f5.1)
1050 format(1x,'Maximum daily temperature=',6f5.1)
1060 format(1x,'Absorbtivity=',f4.1,1x,'Emissivity=',f4.1)

c
do ll=1, 2
  chi=pi/2.0
  if(ll.eq.2)then
    chi=(180.0-gam1)*pi/180.0
  end if

c
do mm=1, nphi
  gamma=pi/2.0+2.0*pi*real(mm-1)/real(nphi)
  rtime=0.0

c
do kh=1, 24
  rtime=(kh-0.5)*3600.0
  Call surface
end do
end do
end do

c
return
end

c
c#####
c      Calculate the solar radiation loads in grain silo
c#####
c#####
c
c      Subroutine surface
c      Include'dry.inc'

```

```

Include'solar.inc'
Real nu

c
month=1.0+rltime/(3600.0*24.0*30.0)
khour=1.0+rltime/3600.0
hc=7.0
rho=0.2
eta=5.67E-08
arc=pi/180.0

c
c Calculate sun's declination
dell=23.45*sin(2.0*pi*(284.0+nuda(month))/365.0)

c
c Convert angles to radians
nu=dell*arc
phi=phi*arc
cbp1=0.5*(1.0+cos(chi))
cbm1=0.5*(1.0-cos(chi))
rsurf=0.0
rb=0.0
rd=0.0
rt=0.0

c
c Calculate the length of the day and sunset hour angle ws
x=-tan(phi)*tan(nu)
ws=acos(x)

c
c Calculate ws in degree
wsdeg=acos(x)/arc
day=(2.0/15.0)*wsdeg
nightday=int(day/2.0)
light=12.0-nightday
dark=12.0+nightday

c
if((khour.lt.light).or.(khour.gt.dark))goto 650
kday=abs(12-khour)

c
c Calculate the total,ht, and diffuse,hdradiation on a horizontal
c surface
gsc=1353.0
a1=(24.0*3600.0*gsc/pi)*(1.0+0.033*cos(2.0*pi*nuda(month))

```

```

&      /365.0))
a2=cos(phi)*cos(nu)*sin(ws)*sin(phi)*sin(nu)
ho=a1*a2
ht=ho*(0.18+0.62*suns(month)/day)
hd=ht*(1.0-1.13*ht/ho)

c
c
c      Cross-check with Iqbal's expression
a3=ho*(0.163+0.478*suns(month)/day)
a4=ho*(0.655*(suns(month)/day)**2)
hiqbal=a3-a4

c
wd=kday*15.0*arc
a5=0.409+0.5016001*sin(ws-60.0*arc)
a6=0.6609-0.4767*sin(ws-60.0*arc)
rt=(pi/24.0)*(a5+a6*cos(wd))*(cos(wd)-cos(ws))/(sin(ws)-ws*
&      cos(ws))
rt=rt*ht/3600.0
rd=(pi/24.0)*(cos(wd)-cos(ws))/(24.0*(sin(ws)-ws*cos(ws)))
rd=rd*hd/3600.0
rp=rt-rd

c
c      Calculate the beam radiation on a sloping surface
ww=15.0*arc*(khour-12.0)
a7=sin(nu)*sin(phi)*cos(chi)
a8=-sin(nu)*cos(phi)*sin(chi)*cos(gamma)
a9=cos(nu)*cos(phi)*cos(chi)*cos(ww)
a10=cos(nu)*sin(phi)*sin(chi)*cos(gamma)*cos(ww)
a11=cos(nu)*sin(chi)*sin(gamma)*sin(ww)
cost=a7+a8+a9+a10+a11

c
costz=cos(nu)*cos(phi)*cos(ww)+sin(nu)*sin(phi)
rb=cost/costz

c
if(rb.lt.0.0)then
  rb=0.0
end if

c
rsurf=rp*rb
tbar=0.5*(tmax(month)+tmin(month))
amp=tmax(month)-tmin(month)
ta=tbar+0.5*amp*sin(pi*(khour-9.0)/12.0)

tsky=0.05522*(ta+273.15)**1.5
tsl=ta-5.0

c
c      Perform energy balance on surface
do 200 kk=1, 20
  an1=alpha*(rsurf+rd*cbp1+rt*rho*cbm1)
  an=an1-hc*(tsl-ta)-cbp1*eta*epsilon*((tsl+273.15)**4
&      -tsky**4)-eta*cbm1*epsilon*((tsl+273.15)**4-
&      (ta+273.15)**4)
c
  dan=-hc-4.0*cbp1*eta*epsilon*(tsl+273.15)**3-
&      4.0*cbm1*eta*epsilon*(tsl+273.15)**3
  tsnew=tsl-an/dan
c
  if(abs(tsnew-tsl).lt.1.0E-4)goto 500
  tsl=tsnew
  ts(l,mm,kh)=tsl

c
  write(15,5010)delt,wsdeg,day
  write(15,5020)ht,hd,hiqbal
  write(15,5030)rt,rd,rp
  write(15,5040)rsurf,rb
  write(15,5050)ta,tsky
  write(15,5060)khour
  write(15,5070)an1,an,dan
  write(15,5080)wd
  write(15,5090)ww
  write(15,5100)a7,a8,a9,a10,a11
  write(15,5110)ts(l,mm,kh)

c
  format(1x,'Declination=',f6.2,'/',sunset hour anglea=',f6.2,
&      ',',Daylength=',f6.2)
  format(1x,'Horizontal surface-Total radiation=',E10.4,'/',
&      'Diffuse radiation=',E10.4,'/','Iqbal=',E10.4)
  format(1x,'Instantaneous radiation-Total=',E12.4,'/',
&      'Diffuse=',E12.4,'/','Beam=',E10.4)
  format(1x,'Beam radiation on sloping surface',E12.7,'/',
&      'Ratio=',E12.7)
c
5010
&
5020
&
5030
&
5040
&
c

```

```

5050 format(1x,'Ambient temp=',f5.2,'/','Sky temp=',f6.2)
5060 format(1x,'Hour of day=',i3)
5070 format(1x,'An1=',E12.4,'/','An=',E10.4,'/','Dan=',E11.4)
5080 format(1x,'Wd=',f8.5)
5090 format(1x,'First w=',f8.5)
5100 format(1x,'A7,A8,A9,A10,A11',5E12.4)
5110 format(1x,'Surface temperature',f8.5)
c
      return
      end
c
c#####
c      Calculate the boundary conditions at the duct
c#####
c
c      Subroutine ductbc(g,ductin)
c      Include'dry.inc'
c      Dimension g(imax,jmax,kmax)
c
c      do j=nphiminc,nphimaxdc
c      do i=nrmindc,nrmaxdc
c      g(i,j,1)=ductin
c      end do
c      end do
c
c      return
c      end
c
c#####
c      Calculate pressure distributions
c#####
c
c      Subroutine pressure
c      Include'dry.inc'
c      Include'solar.inc'
c
c      atd=detal* dtp
c      time=0.0
c
c      do 150 loop=1,kp1
c      do 100 lop=1, kp2

```

Start of iterations implicit solution in r(xi) direction.

Explicit in phi and z(eta) direction.

do k=2,nzml

do j=1, nphi

do i=2, nrm1

if(j.eq.1) then

pijm1k= p(i,nphi,k)

else

pijm1k= p(i,j-1,k)

end if

if(j.eq.nphi) then

pijp1k= p(i,1,k)

else

pijp1k= p(i,j+1,k)

end if

ii=i-1

a(ii)=-atd*(beta6(i,k)*cr1(i)+beta1(i,k)*cr4(ii))

b(ii)=1.0-atd*(beta6(i,k)*cr2(ii)+beta1(i,k)*cr5(ii))

c(ii)=-atd*(beta6(i,k)*cr3(ii)+beta1(i,k)*cr6(ii))

d(ii)=beta1(i,k)*(cr4(i)*p(i-1,j,k)+cr5(i)*p(i,j,k)+

cr6(i)*p(i+1,j,k))+beta2(i,k)*(cz4(k)*p(i,j,k-1)

+cz5(k)*p(i,j,k)+cz6(k)*p(i,j,k+1))+beta3(i,k)*

(cz1(k)*(cr1(i)*p(i-1,j,k-1)+cr2(i)*p(i,j,k-1)+

cr3(i)*p(i+1,j,k-1))+cz2(k)*(cr1(i)*p(i-1,j,k)+

cr2(i)*p(i,j,k)+cr3(i)*p(i+1,j,k))+cz3(k)*(cr1(i)

*p(i-1,j,k+1)+cr2(i)*p(i,j,k+1)+cr3(i)*p(i+1,

j,k+1))+beta6(i,k)*(cr1(i)*p(i-1,j,k)+cr2(i)*p(i

j,k)+cr3(i)*p(i+1,j,k))+beta7(i,k)*(cz1(k)*p(i

j,k-1)+cz2(k)*p(i,j,k)+cz3(k)*p(i,j,k+1))+

beta8(i)*(pijm1k-2.0*p(i,j,k)+pijp1k)/(dphi**2)

end do

call thomas (qq,nrm2)


```

c~~~~~
Call ptime(time)
Call iterp(psierr)
psi(lop)=psierr
c
c      write(90,5888)lop,psi(lop)
5888      format(1x,I8,E16.7)
c
c      if(psierr.lt.5E-15)then
c          go to 780
c      else
c          continue
c      end if
c
c      100      continue
c
c~~~~~
780      write(6,2100)time
2100      format(1x,/'7x','TIME STEP=',f8.1)
c
c      write(6,2200)
c      write(6,2300)(i,i=1,nr)
c
c      2200      format(1x,75x,'THE PRESSURE DISTRIBUTION NODAL
&          POINTS')
2300      format(1x,'PHNR',21(4x,I2,4x))
c
c      do k=nz,1,-1
c          write(6,2400)k
2400      format(1x,'k=',I2)
c
c      do j=nphi,1,-1
c          write(6,2500)j,(p(i,j,k),i=1,nr)
2500      format(1x,I2,21(f10.4))
c
c      end do
c      end do
150      continue
c
c~~~~~
Call velocity
c

```

```

c~~~~~
write(6,2600)
format(1x,35x,'THE RADIAL COMPONENT OF VELOCITY')
2600      c
c      do k=1,nz
c          do j=1,nphi
c              write(6,2620)k,j,(Vra(i,j,k),i=1,nr)
2620      format(1x,'k=',I2,1x,'j=',I2,2x,21(E12.4,1x))
c          end do
c      end do
c~~~~~
write(6,2640)
format(1x,35x,'THE ANGULAR COMPONENT OF VELOCITY')
2640      c
c      do i=1,nr
c          do k=1,nz
c              write(6,2660)i,k,(Vci(i,j,k),j=1,nphi)
2660      format(1x,'i=',I2,1x,'k=',I2,2x,20(E12.4,1x))
c          end do
c      end do
c~~~~~
write(6,2680)
format(1x,35x,'THE VERTICAL COMPONENT OF VELOCITY')
2680      c
c      do j=1,nphi
c          do i=1,nr
c              write(6,2700)i,i,(Ver(i,j,k),k=1,nz)
2700      format(1x,'j=',I2,1x,'i=',I2,2x,21(E12.4,1x))
c          end do
c      end do
c
c      return
c      end
c
c#####
c      Calculate the sum of pressure near
c      the centre line of the silo
c#####
c#####
c

```



```

      d(il)=0.0
      go to 9
c
c   Calculate the pressure boundary conditions at the vertical wall
4   k=i-nr+1
      a(il)=alpha2(nr,k)*cz1(k)
      b(il)=alpha2(nr,k)*cz2(k)+alpha1(nr,k)*crb4
      c(il)=alpha2(nr,k)*cz3(k)
      d(il)=-alpha1(nr,k)*crb5*p(nrm1,j,k)-alpha1(nr,k)*crb6*
      &      p(nrm2,j,k)
c
      if(k.eq.nzm1) d(il)=d(il)-c(il)*p(nr,j,k+1)
9      continue
c
      maxm2=max-2
      Call thomas (qq,maxm2)
      do ib=1, maxm2
      il=ib+1
c
      if(ib.le.nrm1) then
        p(il,j,1)=qq(ib)
      end if
c
      k=ib-nrm1+1
      if(ib.gt.nrm1) then
        p(nr,j,k)=qq(ib)
      end if
c
      &
c
8      end do
      continue
c
c   Calculate the pressure boundary conditions at the top of the
c   bottom
      do j=1, nphi
        p(1,j,1)=-(czb2*p(1,j,2)+czb3*p(1,j,3))/czb1
      end do
c
c   Set conditions at duct
      Call ductbc(p,pduct)
c
      return

```

```

end
c#####
c      Calculate the three components
c      of velocity distributions
c#####
c
c   Subroutine velocity
c   Include'dry.inc'
c
c   nphihalf=nphi/2
c
c   do i=1,nr
c     do j=1,nphi
c       do k=1,nz
c
c         if(i.eq.1) then
c           if(j.lt.nphihalf) then
c             dpdxi=(p(2,j,k)-p(2,j+nphihalf,k))/(2.0*hr(i))
c           else
c             dpdxi=(p(2,j,k)-p(2,j-nphihalf,k))/(2.0*hr(i))
c           end if
c         end if
c
c         if(i.gt.1) then
c           if(i.lt.nr) then
c             dpdxi=cr1(i)*p(i-1,j,k)+cr2(i)*p(i,j,k)+
c             &      cr3(i)*p(i+1,j,k)
c           end if
c
c           if(i.eq.nr) then
c             dpdxi=crb4*p(nr,j,k)+crb5*p(nrm1,j,k)+
c             &      crb6*p(nrm2,j,k)
c           end if
c         end if
c
c         if(j.eq.1) then
c           pijm1k=p(i,nphi,k)
c         else
c           pijm1k=p(i,j-1,k)
c         end if

```

```

c      if(j.eq.nphi)then
c          pijp1k=p(i,1,k)
c      else
c          pijp1k=p(i,j+1,k)
c      end if

c      if(i.gt.1)then
c          dpdphi=cp1(j)*pijm1k+cp2(j)*p(i,j,k)+cp3(j)*pijp1k
c      end if

c      if(k.gt.1.and.k.lt.nz)then
c          dpdeta=cz1(k)*p(i,j,k-1)+cz2(k)*p(i,j,k)+cz3(k)*
c          &          p(i,j,k+1)
c      end if

c      if(k.eq.1)then
c          dpdeta=czb1*p(i,j,1)+czb2*p(i,j,2)+czb3*p(i,j,3)
c      end if

c      if(k.eq.nz)then
c          dpdeta=czb4*p(i,j,nz)+czb5*p(i,j,nzm1)+
c          &          czb6*p(i,j,nzm2)
c      end if

c      Calculate the velocity in radial,circular and vertical direction

c      Vra(i,j,k)=1.0/res*(alpha1(i,k)*dpdxi+alpha2(i,k)*
c      &          dpdeta)
c
c      if(i.gt.1)then
c          Vci(i,j,k)=1.0/(res*r(i))*dpdphi
c      end if

c      Ver(i,j,k)=1.0/res*(alpha4(i,k)*dpdeta)
c
c      end do
c      end do
c      end do
c      return
c      end

```

```

c      end
c      #####
c      Plot pressure and velocity fields
c      #####
c      Subroutine pvout
c      Include'dry.inc'
c
c      do k=1, nz
c      do j=1, nphi
c      do i=1, nr
c          write(7,1000)i,j,k,p(i,j,k),Vra(i,j,k),Vci(i,j,k),
c          &          Ver(i,j,k)
c          1000 format(1x,3I3,f9.4,2x,3(E12.4))
c      end do
c      end do
c      end do
c      return
c      end
c      #####
c      Input pressure and velocity fields
c      #####
c      Subroutine pvin
c      Include'dry.inc'
c
c      do k=1, nz
c      do j=1, nphi
c      do i=1, nr
c          read(8,1000)i,j,k,p(i,j,k),Vra(i,j,k),Vci(i,j,k),
c          &          Ver(i,j,k)
c          1000 format(1x,3I3,f9.4,2x,3(E12.4))
c      end do
c      end do
c      end do
c      return
c      end

```

```

c
c#####
c      Iteration control for convergenc of pressre
c#####
c
c      Subroutine interp(psierr)
c      Include'dry.inc'
c      Include'solar.inc'
c
c      sm=0.0
c      ep=0.0
c
c      do k=1, nz
c        do j=1, nphi
c          do i=1, nr
c            sm=sm+p(i,j,k)
c            ep=ep+abs(p(i,j,k)-savep(i,j,k))
c          end do
c        end do
c      end do
c
c      Calculate psi-error of pressure
c      psierr=ep/sm
c
c      Save old value of pressure distributions
c      do k=1, nz
c        do j=1, nphi
c          do i=1, nr
c            savep(i,j,k)=p(i,j,k)
c          end do
c        end do
c      end do
c
c      return
c      end
c
c#####
c      Calculate the air flow rate through
c      the upper surface of the silo
c#####
c
c#####
c      Subroutine flowrate
c      Include'dry.inc'
c
c      airflow=0.0
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c
c      Airflow in outer of grain regins
c      do j=1, nphi
c        do i=2, nrml
c          if(i.gt.1).and.(i.lt.nr))then
c            dpde(i,j)=czb4*p(i,j,nz)+czb5*p(i,j,nzm1)+czb6*
c              & p(i,j,nzm2)
c          end if
c
c      Airflow in the central region
c      if(i.eq.1)then
c        dpde(1,j)=czb4*p(1,1,nz)+czb5*p(1,1,nzm1)+czb6*
c          & p(1,1,nzm2)
c        end if
c
c      Airflow in region nearest the wall
c      if(i.eq.nr)then
c        dpde(nr,j)=czb4*p(nr,j,nz)+czb5*p(nr,j,nzm1)+czb6*
c          & p(nr,j,nzm2)
c        end if
c      end do
c      end do
c
c      Mean normal pressure
c      do j=1, nphi
c        do i=2, nr
c          dpdn(i,j)=0.5*(sin(gamma2)*(alpha2(i-1,nz)*dpde(i-1,j)+
c            & alpha2(i,nz)*dpde(i,j))+cos(gamma2)*(alpha4(i-1,nz)*
c            & dpde(i-1,nz)+alpha4(i,nz)*dpde(i,j)))
c
c      Calculate pressure gradients in vertical direction at the surface
c      airflow=airflow+3.14159*dpdn(i,j)*(r(i)**2-r(i-1)**2)/

```

```

&      (cos(gamma2)*real(nphi)*res)
c
      air(i,j)=airflow
      end do
      end do
c
      qup=-airflow
c
      do i=2, nr
        write(94,5777)dpdn(i,jphi),air(i,jphi),
&      dpdn(i,jphiby1),air(i,jphiby1),
&      dpdn(i,jphiby2),air(i,jphiby2),
&      dpdn(i,jphiby3),air(i,jphiby3)
c
5777      format(1x,'dpdn',f16.10,1x,'air',7(f16.10,1x))
      end do
c
      return
      end
c
c#####
c      Modify the pressure and velocity fields to
c      accomodate the revised duct pressure
c#####
c
      Subroutine pvmmod
      Include'dry.inc'
c
      pduct=qu/qup*educt
c
      do i=1, nr
        do j=1, nphi
          do k=1,nz
            p(i,j,k)=qu/qup*p(i,j,k)
            Vra(i,j,k)=qu/qup*Vra(i,j,k)
            Vci(i,j,k)=qu/qup*Vci(i,j,k)
            Ver(i,j,k)=qu/qup*Ver(i,j,k)
          end do
        end do
      end do
c
      if(abs(twb-twbn).lt.1.0E-06) go to 162
      twb=twbn

```

```

      return
      end
c
c#####
c      Calculate pressure drop across grain
c      and temperature rise in the fan
c#####
c
      Subroutine tprise
      Include'dry.inc'
c
      The efficiency of the fan is taken as being 60%.
      etafan=0.6
      trise=educt*qu/(rhoa*ca*etafan)
c
      return
      end
c
c#####
c      Using initial wet bulb temperature to
c      calculate the dry bulb temperature
c#####
c
      Subroutine wetbulb(tamb,hamb,twb)
      Include'dry.inc'
c
      twb=tamb
      do 160 kwb=1, 20
        ps=6.0E25/((twb+273.0)**5)*exp(-6800.0/(twb+273.0))
        ws=ps*gn/(patm-ps)
        dwsdps=gn/(patm-ps)*(1.0+ps/(patm-ps))
        dpsdt=ps*(6800.0/(twb+273.0)-5.0)/(twb+273.0)
        dwsdt=dwsdps*dpsdt
c
        flt=(tamb-twbn)+hamb*(2502.0+1.809*tamb-4.186*twb)-
          (2502.0-2.377*twb)*ws
        dffdt=-1.0-4.186*hamb-2502.0*dwsdt+2.377*(twb*dwsdt+ws)
        twbn=twb-flt/dffdt
c
        if(abs(twb-twbn).lt.1.0E-06) go to 162
        twb=twbn

```

```

160 continue
c
162 twb=twbn
c
    return
    end
c
c#####
c      Calculate the thermal performance
c      of the mcbea grain cooling unit
c#####
c
Subroutine mcbeasr(twin,tamb,twout)
Include'dry.inc'
c
    twout=167.0*qu**3-262.0*qu**2+149.0*qu-43+1.2*twin-
    &      0.045*(35.0-tamb)/qu
c
    if(twout.lt.5.0)then
        twout=5.0
    end if
c
    return
    end
c
c#####
c      Using wet bulb temperature to calculate the
c      dry bulb temperature and humidity of air
c#####
c
Subroutine twoutl(twb,tin,hin)
Include'dry.inc'
c
    Call Psat(pswbt,twb)
    ws=gn*pswbt/(patm-pswbt)
    tout=twb
c
do 164 jwb=1, 20
    Call Psat(pstout,tout)
    hout=rhout*pstout*gn/(patm-rhout*pstout)
    fh=(tout-twb)+hout*(2502.0+1.809*tout-4.186*twb)-

```

```

&      (2502.0-2.377*twb)*ws
c
    dhdp=rhout*gn/(patm-rhout*pstout)*(1.0+rhout/(patm-rhout*
    &      pstout))
    dpdt=pstout/(tout+273.0)*(6800.0/(tout+273.0)-5.0)
    dhdt=dhdp*dpdt
    dfhdt=1.0+dhdt*(2502.0+1.809*tout-4.186*twb)+1.809*hout
    toutn=tout-fh/dfhdt
c
    if(abs(toutn-tout).le.1.0E-5)go to 166
    tout=toutn
164 continue
c
166 tout=toutn
c
    Call Psat(pstout,tout)
    hout=rhout*pstout*0.622/(patm-rhout*pstout)
    tin=fout
    hin=hout
c
    return
    end
c
c#####
c      Calculate the saturation vapour pressure
c      of water as a function of temperature
c#####
c
Subroutine psat(ps,ts)
Include'dry.inc'
c
    ps=6.0E25/((ts+273.0)**5)*exp(-6800.0/(ts+273.0))
c
    return
    end
c
c#####
c      Calculate the equilibrium grain moisture content from
c      the temperature and the humidity by means of Smith's
c      sorption isostere equation
c#####

```

```

c
c Subroutine wesmith(hum,temp,weg)
c Include'dry.inc'

c
c pvap=patm*hum/(gn+hum)
c ps=6.0E25/((temp+273.0)**5)*exp(-6800.0/(temp+273.0))
c rh=pvap/ps
c aaa=9.304-0.052076*temp
c bbb=4.1483+0.0215*temp
c wew=aaa-bbb*log(1.0-rh)
c weg=wew/(100.0-wew)

c
c return
c end

c
c#####
c Calculate grain moisture content at the inlet of the bed as a function of air temperature and humidity
c#####
c#####

c Subroutine we(temp,hum,weg)
c Include'dry.inc'

c
c pvap=patm*hum/(gn+hum)
c ps=6.0E25/((temp+273.0)**5)*exp(-6800.0/(temp+273.0))

c
c rh=pvap/ps
c hrev=log(rh)/log(ps/p0)
c w1=((exp(hrev/cw3))/cw4)-((hrev/h0)**revm)/cw2*exp(hrev/cw1)/
c & (1.0-(hrev/h0)**revm)

c
c do jw=1, 10
c   ratw=(w1/w0)**cw5
c   den=1.0-ratw

c
c   dhdw1=cw1/(w1*den)+(ratw*cw1*cw5*log(cw2*w1))/(w1*den**2)-
c   &   ratw*cw3/(w1*den)-cw5*cw3*ratw*log(cw4*w1)/(w1*den)-
c   &   ratw**2*cw3*cw5*log(cw4*w1)/(w1*den**2)

c
c   hsdhvm1=(cw1*log(cw2*w1)-ratw*cw3*log(cw4*w1))/den
c   dfdhl=(ps/p0)**hsdhvm1*log(ps/p0)

```

```

c   dfdw=dfdhl*dhdw1

c
c   fhv=(ps/p0)**hsdhvm1-rh
c   wm=w1-fhw/dfdwl
c   if(abs(wm-w1).lt.1.0E-5)go to 168
c   w1=wm
c   end do

c
c 168 weg=wm
c   if(weg.gt.wsat)then
c     weg=wsat
c   end if

c
c   return
c end

c
c#####
c Calculate the humidity of the interstitial air from the temperature and moisture content of the grain
c#####
c Subroutine humsm(i,j,k)
c Include'dry.inc'

c
c Calculate saturation vapour pressure of water.
c ps=(6.0E25/((t(i,j,k)+273.0)**5))*exp(-6800.0/(t(i,j,k)+273.0))
c mw=100.0*w(i,j,k)/(1.0+w(i,j,k))
c aaa=9.104-0.052076*t(i,j,k)
c bbb=4.1483+0.0215*t(i,j,k)
c arg=(aaa-mw)/bbb
c rh=1.0-exp(arg)

c
c   pvap=ps*rh
c   h(i,j,k)=(pvap*gn)/(patm-pvap)

c
c Calculate the heat of sorption hs
c hvap=hv+dhdvt*t(i,j,k)
c hs=hvap*(1.0+23.0*exp(-40.0*w(i,j,k)))

c
c   return
c end

```



```

c #####
c Calculate the humidity of the intergranular air as a ##### #
c function of temperature and grains moisture content ##### #
c #####
c
c Subroutine hum(i,j,k)
c Include'dry.inc'
c #####
c Calculate saturation vapour pressure of water.
c  $ps=(6.0E25/((i,j,k)+273.0)**5)*exp(-6800.0/((i,j,k)+273.0))$ 
c
c Calculate relative humidity of interstitial air .
c  $hshvm1=(cw1*log(cw2*w(i,j,k))-(w(i,j,k)/w0))*cw5*cw3*log(cw4*$ 
c &  $w(i,j,k))/(1.0-(w(i,j,k)/w0))*cw5)$ 
c
c  $rh=(ps/p0)**hshvm1$ 
c  $hvap=hv+dhvdt*t(i,j,k)$ 
c  $hs=hvap*(1.0+hshvm1)$ 
c  $pvap=ps*rh$ 
c  $h(i,j,k)=(gn*pvap)/(patm-pvap)$ 
c
c return
c end
c #####
c Calculate the rate of respiration of wheat ##### #
c #####
c Subroutine resp(i,j,k,time)
c Include'dry.inc'
c
c  $dmw=100.0*w(i,j,k)/(1.0+w(i,j,k))$ 
c if(dmw.lt.14.5)then
c   dmdmt=0.0
c else
c   arg=(a5lhm+a6lhm*time+a7lhm*t(i,j,k))*(a8lhm-dmw)
c   z1=1.0+exp(arg)
c   z2=a2lhm
c   z3=a1lhm+a2lhm*time
c   z4=a6lhm*(a8lhm-w(i,j,k))*exp(arg)
c #####
c
c  $y=1.0+exp(a3lhm*(a4lhm-t(i,j,k)))$ 
c  $dmdmt=(z1*z2-z3*z4)/(z1**2*y)$ 
c end if
c
c return
c end
c #####
c Calculate the rate of dry matter loss of grain and the ##### #
c elapsed physiological time as a function of moisture ##### #
c content temperature and time increment ##### #
c #####
c Subroutine resp(i,j,k)
c Include'dry.inc'
c Real mddb,mcwb
c
c Using moisture contents on wet basis(mcwb) and dry basis(mddb).
c  $mcwb=w(i,j,k)*100.0/(1.0+w(i,j,k))$ 
c  $mddb=w(i,j,k)*100.0$ 
c  $ar=32.3*exp(-0.1044*t(i,j,k)-1.856)$ 
c
c if(t(i,j,k).le.15.and.mcwb.le.19)then
c   tmod=ar
c end if
c
c if(t(i,j,k).gt.15)then
c   if(mcwb.gt.19.and.mcwb.le.28)then
c     tmod=ar+((mcwb-19.0)/100.0)*exp(0.0183*t(i,j,k)-0.28437)
c   end if
c end if
c
c if(t(i,j,k).gt.15.and.mcwb.gt.28)then
c   tmod=ar+9.000001E-02*exp(0.0183*t(i,j,k)-0.2847)
c end if
c
c wmod=1.0
c if(mcwb.gt.13.and.mcwb.le.35)then
c   wmod=0.103*(exp(455.0/mddb**1.53)-8.4499999E-03*mddb+1.558)
c end if
c

```



```

&      h(i,j,k+1)
dhdpht=cphi1*hijm1k+cphi2*h(i,j,k)+cphi3*hijp1k
c
c  Dispersion terms
      gamaw=beta1(i,k)*(cr4(i)*h(i-1,j,k)+cr5(i)*
&      h(i,j,k)+cr6(i)*h(i+1,j,k))+beta2(i,k)*
&      (cz4(k)*h(i,j,k-1)+cz5(k)*h(i,j,k)+cz6(k)*
&      h(i,j,k+1))+beta3(i,k)*(cz1(k)*(cr1(i)*
&      h(i-1,j,k-1)+cr2(i)*h(i,j,k-1)+cr3(i)*
&      h(i+1,j,k-1))+cz2(k)*(cr1(i)*h(i-1,j,k)+
&      cr2(i)*h(i,j,k)+cr3(i)*h(i+1,j,k))+cz3(k)*
&      (cr1(i)*h(i-1,j,k+1)+cr2(i)*h(i,j,k+1)+
&      cr3(i)*h(i+1,j,k+1)))+beta8(i)*(cp4(j)*
&      hijm1k+cp5(j)*h(i,j,k)+cp6(j)*hijp1k)
c
      dwdt=-rhoa/rhob*(Vxi*dhdx+Veta*dhdelta+Vphi*
&      dhdpht)+(rhoa/rhob)*deff*gamaw+ddmdt*(0.6+
&      w(i,j,k))
      wnew(i,j,k)=w(i,j,k)+dwdt*dtg
c
      return
      end
c
c#####
c# Solve thermal energy equation
c#####
c#####
c
      Subroutine tempera(i,j,k)
      Include'dry.inc'
      Real keff,iw
c
      premu=rhoa*(ca+h(i,j,k)*(cw+dhvdt))
      Vxit=premu*(alpha1(i,k)*Vra(i,j,k)+alpha3(i,k)*
&      Ver(i,j,k))-keff*beta6(i,k)
      Vetat=premu*(alpha2(i,k)*Vra(i,j,k)+alpha4(i,k)*
&      Ver(i,j,k))-keff*beta7(i,k)
      Vphit=premu*Vci(i,j,k)/(wR*xi)
c
c  Set matching conditions for temperature when j=1 and j=nphi
      if(j.eq.1) then
          tijm1k= t(i,nphi,k)

```

```

c      Calculate first derivatives with respect to temperatures
      dTdx1=cx11*(t(i-1,j,k)+cx12*t(i,j,k)+cx13*
      &      t(i+1,j,k)
      dTdeta=ceta1*t(i,j,k-1)+ceta2*t(i,j,k)+ceta3*
      &      t(i,j,k+1)
      dTdphi=cphi1*tijm1k+cphi2*t(i,j,k)+cphi3*tijp1k
c
c      Dispersion terms
      gamat=beta1(i,k)*(cr4(i)*t(i-1,j,k)+cr5(i)*
      &      t(i,j,k)+cr6(i)*t(i+1,j,k))+beta2(i,k)*
      &      (cz4(k)*t(i,j,k-1)+cz5(k)*t(i,j,k)+cz6(k)*
      &      t(i,j,k+1))+beta3(i,k)*(cz1(k)*(cr1(i)*
      &      t(i-1,j,k-1)+cr2(i)*t(i,j,k-1)+cr3(i)*
      &      t(i+1,j,k-1))+cz2(k)*(cr1(i)*t(i-1,j,k)+
      &      cr2(i)*t(i,j,k)+cr3(i)*t(i+1,j,k))+cz3(k)*
      &      (cr1(i)*t(i-1,j,k+1)+cr2(i)*t(i,j,k+1)+
      &      cr3(i)*t(i+1,j,k+1)))+beta8(i)*(cp4(j)*
      &      tijm1k+cp5(j)*t(i,j,k)+cp6(j)*tijp1k)
c
      if(smith)then
        iw=0.575*(exp(-40.0*w(i,j,k))-1.0)
      else
        if(w(i,j,k).le.0.1)then
          iw=hw1+hw2*w(i,j,k)+hw3*w(i,j,k)**2+hw4*
          &      w(i,j,k)**3+hw5*w(i,j,k)**4
          end if
        if(w(i,j,k).gt.0.1)then
          iw=hw6+hw7*w(i,j,k)+hw8*w(i,j,k)**2+hw9*
          &      w(i,j,k)**3+hw10*w(i,j,k)**4
          end if
        end if
c
      dhwdt=dhvd*t*iw
      denom=(cg+cw*w(i,j,k)+dhwdt)*rhob+eps*rhoa*(ca+
      &      h(i,j,k)*(cw+dhvdt))
c
      aa=rhob*hs*dwdt
      bb=-(Vxit*dTdx1+Vetdt*dTdeta+Vphit*dTdphi)
      cc=keft*gamat
      dd=rhob*ddmdt*(1.5778E+07-0.6*hvap)

```

```

      ee=rhob*ddmdt*hvap*(iw-w(i,j,k))
      tnw(i,j,k)=(i,j,k)+dtg*(aa+bb+cc+dd+ee)/denom
c
      return
      end
c
c#####
c      Calculate the temperature boundary conditions
c#####
c#####
c
      Subroutine tbc(tamb)
      Include'dry.inc'
      Include'solar.inc'
c
c      Wall temperature
      do j=1, nphi
        do k=1, nz
          t(nr,j,k)=ts(1,j,kh)
          tnw(nr,j,k)=ts(1,j,kh)
        end do
      end do
c
c      Bottom of silo temperature
      do j=1, nphi
        do i=1, nr
          t(i,j,1)=ts(2,j,kh)
          tnw(i,j,1)=ts(2,j,kh)
        end do
      end do
c
c      Temperature at the upper surface
      do j=1, nphi
        do i=2, nrml
          tnw(i,j,nz)=tnw(i,j,nzml)
          if(noflow.eq.1)tnw(i,j,nz)=tamb
        end do
      end do
c
c      Temperature at centre of the bulk
      do j=1, nphi
c

```

```

c      At the upper surface
      t(1,j,nz)=-(czb5*t(1,j,nzm1)+czb6*t(1,j,nzm2))/czb4
      if(noflow.eq.1)t(1,j,nz)=tamb
      tnew(1,j,nz)=t(1,j,nz)

c
c      At bottom of the cone
      t(1,j,1)=ts(2,1,mm)
      tnew(1,j,1)=t(1,j,1)
      end do

c
c      At the centre
      do k=2, nzm1
      do j=1, nphi
      t(1,j,k)=sigmaT(k)/real(nphi)
      tnew(1,j,k)=t(1,j,k)
      end do
      end do

c      return
      end

c#####
c      Calculate the sum of temperature nera
c      the centre line of the silo
c#####
c#####

c      Function sigmaT(k)
      Include'dry.inc'
      Real sigmaT

c      sigmaT=0.0

c      do j=1,nphi
      sigmaT=sigmaT+t(2,j,k)
      end do
      return
      end

c#####
c      Calculate the humidity boundary conditions
c#####
c#####
c      Calculate the humidity boundary conditions at the vertical wall
      k=i-nr+1
      a(il)=alpha2(nr,k)*cz1(k)
      b(il)=alpha2(nr,k)*cz2(k)+alpha1(nr,k)*crb4

```

```

      c(il)=alpha2(nr,k)*cz3(k)
      d(il)=alpha1(nr,k)*crb5*h(nrm1,j,k)-alpha1(nr,k)*crb6*
      &      h(nrm2,j,k)
      if(k.eq.nzm1) d(il)=d(il)-c(il)*h(nr,j,k+1)
9      continue
c
      maxm2=21-2
      Call thomas (qq,maxm2)
      do ib=1, maxm2
      il=ib+1
c
      if(ib.le.nrm1) then
      h(il,j,1)=qq(ib)
      end if
c
      k=ib-nrm1+1
      if(ib.gt.nrm1) then
      h(nr,j,k)=qq(ib)
      end if
c
      end do
8      continue
c
      Calculate middle of centre conditions
      do k=2,nzm1
      do j=1,nphi
      h(1,j,k)=sigmaH(k)/real(nphi)
      end do
      end do
c
      Calculate humidity at the top of the grain
      do j=1, nphi
      h(nr,j,nz)=-(czb5*h(nr,j,nzm1)+czb6*h(nr,j,nzm2))/czb4
c
      Calculate humidity at the peak of the grain
      h(1,j,nz)=-(czb5*h(1,j,nzm1)+czb6*h(1,j,nzm2))/czb4
c
      Calculate humidity at the top of the bottom
      h(1,j,1)=-(czb2*h(1,j,2)+czb3*h(1,j,3))/czb1
c
      end do

```

```

c
c      Calculate humidity at duct
c      if(noflow.eq.0)Call ductbc(h,hin)
c
c      return
c      end
c
c#####
c      Calculate the sum of humidity near
c      the centre line of the silo
c#####
c
c      Function sigmaH(k)
c      Include'dry.inc'
c      Real sigmaH
c
c      sigmaH=0.0
c
c      do j=1,nphi
c      sigmaH=sigmaH+h(2,j,k)
c      end do
c      return
c      end
c
c#####
c      Calculate grain moisture content boundary conditions
c#####
c
c      Subroutine mcbc(win)
c      Include'dry.inc'
c
c      Moisture contents in the centre of the silo
c      do k=2, nzm1
c      do j=1, nphi
c      wnew(1,j,k)=sigmaW(k)/real(nphi)
c      end do
c      end do
c
c      Moisture content along the floor
c      do j=1, nphi
c      do i=1, nr

```

```

      wnew(i,j,1)=-((hz(1)+hz(2))*wnew(i,j,2)-hz(1)*wnew(i,j,3))
      &
c      Moisture content along the upper surface
      wnew(i,j,nz)=-((hz(nzm1)+hz(nzm2))*wnew(i,j,nzm1)-hz(nzm1)
      *wnew(i,j,nzm2))/hz(nzm2)
c
      end do
      end do
c
c      Moisture content along the wall
      do j=1, nphi
      do k=1, nz
      wnew(nr,j,k)=(hr(nrm1)+hr(nrm2))*wnew(nrm1,j,k)-hr(nrm1)
      *wnew(nrm2,j,k))/hr(nrm2)
      &
      end do
      end do
c
c      Moisture content at the duct
      if(noflow.eq.0)Call ductbc(wnew,win)
c
      return
      end
c
c#####
c      Calculate the sum of moisture content
      near the centre of the silo
c#####
c
      Function sigmaW (k)
      Include'dry.inc'
      Real sigmaW
c
      sigmaW=0.0
      do j=1,nphi
      sigmaW=sigmaW+wnew(2,j,k)
      end do
c
c      return
      end
c#####
c      Calculate dry matter loss along boundaries
      #
c#####
c
      Subroutine dmlssbc(time)

```

```

c#####
c      Calculate insect polpulation growth
      #
c#####
c
      Subroutine insect(twbb,tdrybulb,i,j,k)
      Include'dry.inc'
c
      dtweek=dtg/(3600.0*24.0*7.0)
c
      Increase rhyzopertha dominica
      rdom=crdom*(twbb-trdom)
      if(rdom.lt.0.0)rdom=0.0
      if(tdrybulb.ge.40.0)rdom=0.0
      rdomconc(i,j,k)=rdomconc(i,j,k)*exp(rdom*dtweek)
c
c      Increase sitophilus oryzael
      soryz1=esoryz1*(twbb-tsoryz1)
      if(soryz1.lt.0.0)soryz1=0.0
      if(tdrybulb.ge.35.0)soryz1=0.0
      soryz1c(i,j,k)=soryz1c(i,j,k)*exp(soryz1*dtweek)
c
c      Increase sitophilus oryzae2
      soryz2=esoryz2*(twbb-tsoryz2)
      if(soryz2.lt.0.0)soryz2=0.0
      if(tdrybulb.ge.35.0)soryz2=0.0
      soryz2c(i,j,k)=soryz2c(i,j,k)*exp(soryz2*dtweek)
c
c      Increase sitophilus zeamais
      sz=csz*(twbb-tszz)
      if(sz.lt.0.0)sz=0.0
      if(tdrybulb.ge.35.0)sz=0.0
      szconc(i,j,k)=szconc(i,j,k)*exp(sz*dtweek)
c
      return
      end
c
c#####
c      Calculate dry matter loss along boundaries
      #
c#####
c
      Subroutine dmlssbc(time)

```

```

c      Include'dry.inc'
c
c      Along the wall
do k=1, nz
do j=1, nphi
  if(smith)then
    Call resplhm(nr,j,k,time,ddmdt)
  else
    Call resp(nr,j,k,ddmdt)
  end if
end do
c      dmloss(nr,j,k)=dmloss(nr,j,k)+ddmdt*dtg
end do
c
c      Calculate upper surface of the grain
do j=1, nphi
do i=1, nr
  if(smith)then
    Call resplhm(i,j,nz,time,ddmdt)
  else
    Call resp(i,j,nz,ddmdt)
  end if
end do
c      dmloss(i,j,nz)=dmloss(i,j,nz)+ddmdt*dtg
end do
c
c      Calculate along the floor
do j=1, nphi
do i=1, nr
  if(smith)then
    Call resplhm(i,j,1,time,ddmdt)
  else
    Call resp(i,j,1,ddmdt)
  end if
end do
c      dmloss(i,j,1)=dmloss(i,j,1)+ddmdt*dtg
end do
c
c      return
end

c#####
c      Save the velocity fields during
c      aeration fan is turned on
c#####
c      Subroutine velsave
c      Include'dry.inc'
c
do i=1, nr
do j=1, nphi
do k=1, nz
  vrsave(i,j,k)=Vra(i,j,k)
  vpsave(i,j,k)=Vci(i,j,k)
  vzsave(i,j,k)=Ver(i,j,k)
end do
end do
end do
c      return
end

c#####
c      Reinstate the velocity fields after
c      aeration fan is turned off
c#####
c      Subroutine velaerate
c      Include'dry.inc'
c
do i=1, nr
do j=1, nphi
do k=1, nz
  Vra(i,j,k)=vrsave(i,j,k)
  Vci(i,j,k)=vpsave(i,j,k)
  Ver(i,j,k)=vzsave(i,j,k)
end do
end do
end do

```



```

c      return
c      end
c#####
c      Set the velocity fields to zero during          #
c      aeration fan is turned off                      #
c#####
c
c      Subroutine velconduct
c      Include'dry.inc'
c
c      do i=1, nr
c      do j=1, nphi
c      do k=1, nz
c      Vra(i,j,k)=0.0
c      Vci(i,j,k)=0.0
c      Ver(i,j,k)=0.0
c      end do
c      end do
c      end do
c
c      return
c      end
c#####
c      Calculate the concentration of pesticide on the grains          #
c#####
c
c      Subroutine pesti
c      Include'dry.inc'
c
c      do i=1, nr
c      do j=1, nphi
c      do k=1, nz
c      pvap=patm*h(i,j,k)/(0.622+h(i,j,k))
c      ts=t(i,j,k)
c      Call psat(ps,ts)
c      rh=pvap/ps
c      argfe=(1.3863*rh*dtg*10.0**(bfe*(t(i,j,k)-30.0)))/
c      &      thalfe
c#####
c      cfe(i,j,k)=cfe(i,j,k)*exp(argfe)
c      end do
c      end do
c      end do
c      return
c      end
c#####
c#####
c      Using the input values of temperature, grain moisture          #
c      content and the initial germination viability of the          #
c      seeds to calculate the updated viability after a time          #
c      dtg*dtfreq/(3600.0*24)
c#####
c#####
c      Subroutine viable(i,j,k)
c      Include'dry.inc'
c
c      heat=t(i,j,k)
c      wc=100.0*w(i,j,k)/(1.0+w(i,j,k))
c      dead=1.0-viability(i,j,k)
c
c      Call lifedata(sigma,halif,heat,wc)
c
c      timev=halif
c      Call timod(timev,dead,halif,sigma)
c      timev=timev+dtg*real(ifreq)/(3600.0*24.0)
c
c      Call survivors(surv,dead,timev,halif,sigma)
c      viability(i,j,k)=surv
c
c      return
c      end
c#####
c#####
c      Calculates the half life of seeds and the standard          #
c      deviation of the mortality of the grains                      #
c#####
c#####
c      Subroutine lifedata(sigma,halif,heat,wc)
c

```

```

      halif=10.0**(5.067-0.108*wc-0.05*heat)
      sigma=0.35*halif
c
      return
      end
c
c#####
c      Calculates the time and timev from
c      when half the seeds are dead
c#####
c
c      Subroutine timod(timev,dead,halif,sigma)
c
c      arg=abs(timev-halif)/(sigma*sqrt(2.0))
c      do j=1, 20
c
c          Call erf(arg,erfx,derfx)
c
c          if(dead.le.0.5)then
c              func=dead-0.5*(1.0-erfx)
c              x=arg-func/(0.5*derfx)
c
c              if(x.lt.0.0)x=0.0
c              else
c
c                  func=dead-0.5*(1.0+erfx)
c                  x=arg+func/(0.5*derfx)
c
c                  if(x.lt.0.0)x=0.0
c                  end if
c
c              if(abs(arg-x).lt.1.0e-5) go to 15
c                  arg=x
c              end do
c
c          15 arg=x
c
c          if(dead.ge.0.5)then
c              timev=halif+sigma*sqrt(2.0)*arg
c          else
c              timev=halif-sigma*sqrt(2.0)*arg
c
c          end if
c
c#####
c      Calculates values of erf(arg)and derf(arg)
c      designated as erfx and derf respectively.
c      If arg is less than or equal to unity is
c      evaluated from its series expansion which
c      converges rapidly. If arg is greater than
c      unity it is evaluated by integrating its
c      integral representation using Simpson's rule,
c      with the lower bound on arg taken as unity.
c#####
c
c      Subroutine erf(arg,erfx,derfx)
c
c      if(arg.le.1.0)then
c          Call erfl(arg,erfx)
c      else
c
c          In this integration of the error function by Simpson's rule.
c          we have:
c          n=the even number of integration intervals
c          h=length of the integration interval
c          x10=sum of the two extreme ordinates
c          x11=sum of the ordinates at even nodes
c          x12=sum of the ordinates at odd nodes
c
c          n=int(arg)*20
c          nml=n-1
c          hp=(arg-1.0)/real(n)
c          x10=exp(-1.0)+exp(-(arg**2))
c          x11=0.0
c          x12=0.0
c
c          do i=1, nml
c              x=1.0+real(i)*hp
c              ii=0.5*i
c              ii2=ii*2
c
c          end do
c
c#####

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```

c      if(i.eq.ii2)then
c        x12=x12+exp(-(x**2))
c      else
c        x11=x11+exp(-(x**2))
c      end if
c
c      end do
c
c      erfx=0.8427008+2.0*hp*(x10+2.0*x12+4.0*x11)/
c      & (3.0*sqrt(3.14159))
c
c      end if
c
c      derfx=2.0/sqrt(3.14159)*exp(-arg**2)
c
c      return
c      end
c
c#####
c      Calculates the error function as a direct integration
c      of a series expansion of the integrand
c#####
c
c      Subroutine erf1 (arg,erfx)
c
c      nfact=1
c      sum=arg
c
c      do n=2, 100
c        nfact=nfact*(n-1)
c        add=(-1.0)**(n-1)*arg**(2*n-1)/((2*n-1)*nfact)
c        sum=sum+add
c        if(abs(add).lt.1.0e-6)go to 11
c      end do
c
c      11      erfx=2.0*sum/sqrt(3.14159)
c
c      return
c      end
c
c#####
c      Calculate the number of dead and surviving insects
c#####
c
c      Subroutine survivors(surv,dead,timev,halif,sigma)
c
c      arg=abs((timev-halif)/(sigma*sqrt(2.0)))
c      Call erf(erfx,derfx)
c
c      if(timev.le.halif)then
c        dead=0.5*(1.0-erfx)
c      else
c        dead=0.5*(1.0+erfx)
c      end if
c
c      surv=1.0-dead
c
c      return
c      end
c#####
c      Output the variation of grain silo conditions
c      by time increase
c#####
c
c      Subroutine dayplot(timeday)
c      Include'dry.inc'
c
c      nrby2=nr/2+1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      nzby1=nz/4+1
c      nzby2=nz/2+1
c      nzby3=(nz*3)/4+1
c
c      if(timeday.ge.tprint0)then
c        if(kprint0.eq.0)then
c          write(29,7000)timeday,t(1,1,nzby2),
c          & w(1,1,nzby2), h(1,1,nzby2),
c          & viability(1,1,nzby2),soryz1c(1,1,nzby2),
c          & soryz2c(1,1,nzby2),szconc(1,1,nzby2),

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&      dmlloss(1,1,nzby2),cfe(1,1,nzby2),
&      rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
      write(88,7000)timeday,t(nrby2,jphiby1,nzby3),
&      w(nrby2,jphiby1,nzby3),
&      h(nrby2,jphiby1,nzby3),
&      viability(nrby2,jphiby1,nzby3),
&      soryz1c(nrby2,jphiby1,nzby3),
&      soryz2c(nrby2,jphiby1,nzby3),
&      szconc(nrby2,jphiby1,nzby3),
&      dmlloss(nrby2,jphiby1,nzby3),
&      cfe(nrby2,jphiby1,nzby3),
&      rdomconc(nrby2,jphiby1,nzby3),
&      twetbulb(nrby2,jphiby1,nzby3)
c
      write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
&      w(nrby2,jphiby2,nzby1),
&      h(nrby2,jphiby2,nzby1),
&      viability(nrby2,jphiby2,nzby1),
&      soryz1c(nrby2,jphiby2,nzby1),
&      soryz2c(nrby2,jphiby2,nzby1),
&      szconc(nrby2,jphiby2,nzby1),
&      dmlloss(nrby2,jphiby2,nzby1),
&      cfe(nrby2,jphiby2,nzby1),
&      rdomconc(nrby2,jphiby2,nzby1),
&      twetbulb(nrby2,jphiby2,nzby1)
c
      kprint0=1
      end if
      else
      continue
      end if

      if(timeday.ge.tprint5)then
      if(kprint5.eq.0)then
      write(29,7000)timeday,t(1,1,nzby2),
&      w(1,1,nzby2), h(1,1,nzby2),
&      viability(1,1,nzby2),soryz1c(1,1,nzby2),
&      soryz2c(1,1,nzby2),szconc(1,1,nzby2),
&      dmlloss(1,1,nzby2),cfe(1,1,nzby2),
&      rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
      write(88,7000)timeday,t(nrby2,jphiby1,nzby3),

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```
& w(nrby2,jphiby1,nzby3),
& h(nrby2,jphiby1,nzby3),
& viability(nrby2,jphiby1,nzby3),
& soryz1c(nrby2,jphiby1,nzby3),
& soryz2c(nrby2,jphiby1,nzby3),
& szconc(nrby2,jphiby1,nzby3),
& dmlloss(nrby2,jphiby1,nzby3),
& cfe(nrby2,jphiby1,nzby3),
& rdomconc(nrby2,jphiby1,nzby3),
& twetbulb(nrby2,jphiby1,nzby3)
c
& write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
& w(nrby2,jphiby2,nzby1),
& h(nrby2,jphiby2,nzby1),
& viability(nrby2,jphiby2,nzby1),
& soryz1c(nrby2,jphiby2,nzby1),
& soryz2c(nrby2,jphiby2,nzby1),
& szconc(nrby2,jphiby2,nzby1),
& dmlloss(nrby2,jphiby2,nzby1),
& cfe(nrby2,jphiby2,nzby1),
& rdomconc(nrby2,jphiby2,nzby1),
& twetbulb(nrby2,jphiby2,nzby1)
c
& kprint10=1
& end if
& else
& continue
& end if
c
& if(timeday.ge.tprint15)then
& if(kprint15.eq.0)then
& write(29,7000)timeday,t(1,1,nzby2),
& w(1,1,nzby2), h(1,1,nzby2),
& viability(1,1,nzby2),soryz1c(1,1,nzby2),
& soryz2c(1,1,nzby2),szconc(1,1,nzby2),
& dmlloss(1,1,nzby2),cfe(1,1,nzby2),
& rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
& write(88,7000)timeday,t(nrby2,jphiby1,nzby3),
& w(nrby2,jphiby1,nzby3),
& h(nrby2,jphiby1,nzby3),
& viability(nrby2,jphiby1,nzby3),
& soryz1c(nrby2,jphiby1,nzby3),
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```
& viability(nrby2,jphiby1,nzby3),
& soryz1c(nrby2,jphiby1,nzby3),
& soryz2c(nrby2,jphiby1,nzby3),
& szconc(nrby2,jphiby1,nzby3),
& dmlloss(nrby2,jphiby1,nzby3),
& cfe(nrby2,jphiby1,nzby3),
& rdomconc(nrby2,jphiby1,nzby3),
& twetbulb(nrby2,jphiby1,nzby3)
c
& write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
& w(nrby2,jphiby2,nzby1),
& h(nrby2,jphiby2,nzby1),
& viability(nrby2,jphiby2,nzby1),
& soryz1c(nrby2,jphiby2,nzby1),
& soryz2c(nrby2,jphiby2,nzby1),
& szconc(nrby2,jphiby2,nzby1),
& dmlloss(nrby2,jphiby2,nzby1),
& cfe(nrby2,jphiby2,nzby1),
& rdomconc(nrby2,jphiby2,nzby1),
& twetbulb(nrby2,jphiby2,nzby1)
c
& kprint15=1
& end if
& else
& continue
& end if
c
& if(timeday.ge.tprint20)then
& if(kprint20.eq.0)then
& write(29,7000)timeday,t(1,1,nzby2),
& w(1,1,nzby2), h(1,1,nzby2),
& viability(1,1,nzby2),soryz1c(1,1,nzby2),
& soryz2c(1,1,nzby2),szconc(1,1,nzby2),
& dmlloss(1,1,nzby2),cfe(1,1,nzby2),
& rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
& write(88,7000)timeday,t(nrby2,jphiby1,nzby3),
& w(nrby2,jphiby1,nzby3),
& h(nrby2,jphiby1,nzby3),
& viability(nrby2,jphiby1,nzby3),
& soryz1c(nrby2,jphiby1,nzby3),
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&      soryz2c(nrby2,jphiby1,nzby3),
&      szconc(nrby2,jphiby1,nzby3),
&      dmlloss(nrby2,jphiby1,nzby3),
&      cfe(nrby2,jphiby1,nzby3),
&      rdomconc(nrby2,jphiby1,nzby3),
&      twetbulb(nrby2,jphiby1,nzby3)
c
      write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
&      w(nrby2,jphiby2,nzby1),
&      h(nrby2,jphiby2,nzby1),
&      viability(nrby2,jphiby2,nzby1),
&      soryz1c(nrby2,jphiby2,nzby1),
&      soryz2c(nrby2,jphiby2,nzby1),
&      szconc(nrby2,jphiby2,nzby1),
&      dmlloss(nrby2,jphiby2,nzby1),
&      cfe(nrby2,jphiby2,nzby1),
&      rdomconc(nrby2,jphiby2,nzby1),
&      twetbulb(nrby2,jphiby2,nzby1)
c
      kprint25=1
&      end if
&      else
&      continue
&      end if
c
      if(timeday.ge.tprint30)then
&      if(kprint30.eq.0)then
&      write(29,7000)timeday,t(1,1,nzby2),
&      w(1,1,nzby2), h(1,1,nzby2),
&      viability(1,1,nzby2),soryz1c(1,1,nzby2),
&      soryz2c(1,1,nzby2),szconc(1,1,nzby2),
&      dmlloss(1,1,nzby2),cfe(1,1,nzby2),
&      rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
&      write(88,7000)timeday,t(nrby2,jphiby1,nzby3),
&      w(nrby2,jphiby1,nzby3),
&      h(nrby2,jphiby1,nzby3),
&      viability(nrby2,jphiby1,nzby3),
&      soryz1c(nrby2,jphiby1,nzby3),
&      soryz2c(nrby2,jphiby1,nzby3),
&      szconc(nrby2,jphiby1,nzby3),
&      dmlloss(nrby2,jphiby1,nzby3),
&      cfe(nrby2,jphiby1,nzby3),
&

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&      soryz2c(nrby2,jphiby1,nzby3),
&      szconc(nrby2,jphiby1,nzby3),
&      dmlloss(nrby2,jphiby1,nzby3),
&      cfe(nrby2,jphiby1,nzby3),
&      rdomconc(nrby2,jphiby1,nzby3),
&      twetbulb(nrby2,jphiby1,nzby3)
c
      write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
&      w(nrby2,jphiby2,nzby1),
&      h(nrby2,jphiby2,nzby1),
&      viability(nrby2,jphiby2,nzby1),
&      soryz1c(nrby2,jphiby2,nzby1),
&      soryz2c(nrby2,jphiby2,nzby1),
&      szconc(nrby2,jphiby2,nzby1),
&      dmlloss(nrby2,jphiby2,nzby1),
&      cfe(nrby2,jphiby2,nzby1),
&      rdomconc(nrby2,jphiby2,nzby1),
&      twetbulb(nrby2,jphiby2,nzby1)
c
      kprint20=1
&      end if
&      else
&      continue
&      end if
c
      if(timeday.ge.tprint25)then
&      if(kprint25.eq.0)then
&      write(29,7000)timeday,t(1,1,nzby2),
&      w(1,1,nzby2), h(1,1,nzby2),
&      viability(1,1,nzby2),soryz1c(1,1,nzby2),
&      soryz2c(1,1,nzby2),szconc(1,1,nzby2),
&      dmlloss(1,1,nzby2),cfe(1,1,nzby2),
&      rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
&      write(88,7000)timeday,t(nrby2,jphiby1,nzby3),
&      w(nrby2,jphiby1,nzby3),
&      h(nrby2,jphiby1,nzby3),
&      viability(nrby2,jphiby1,nzby3),
&      soryz1c(nrby2,jphiby1,nzby3),
&      soryz2c(nrby2,jphiby1,nzby3),
&      szconc(nrby2,jphiby1,nzby3),
&

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&      rdomconc(nrby2,jphiby1,nzby3),
&      twetbulb(nrby2,jphiby1,nzby3)
c
&      write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
&      w(nrby2,jphiby2,nzby1),
&      h(nrby2,jphiby2,nzby1),
&      viability(nrby2,jphiby2,nzby1),
&      soryz1c(nrby2,jphiby2,nzby1),
&      soryz2c(nrby2,jphiby2,nzby1),
&      szconc(nrby2,jphiby2,nzby1),
&      dmlloss(nrby2,jphiby2,nzby1),
&      cfe(nrby2,jphiby2,nzby1),
&      rdomconc(nrby2,jphiby2,nzby1),
&      twetbulb(nrby2,jphiby2,nzby1)
c
&      kprint35=1
&      end if
&      else
&      continue
&      end if
c
&      if(timeday.ge.tprint40)then
&      if(kprint40.eq.0)then
&      write(29,7000)timeday,t(1,1,nzby2),
&      w(1,1,nzby2), h(1,1,nzby2),
&      viability(1,1,nzby2),soryz1c(1,1,nzby2),
&      soryz2c(1,1,nzby2),szconc(1,1,nzby2),
&      dmlloss(1,1,nzby2),cfe(1,1,nzby2),
&      rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
&      write(88,7000)timeday,t(nrby2,jphiby1,nzby3),
&      w(nrby2,jphiby1,nzby3),
&      h(nrby2,jphiby1,nzby3),
&      viability(nrby2,jphiby1,nzby3),
&      soryz1c(nrby2,jphiby1,nzby3),
&      soryz2c(nrby2,jphiby1,nzby3),
&      szconc(nrby2,jphiby1,nzby3),
&      dmlloss(nrby2,jphiby1,nzby3),
&      cfe(nrby2,jphiby1,nzby3),
&      rdomconc(nrby2,jphiby1,nzby3),
&      twetbulb(nrby2,jphiby1,nzby3)
c
&      write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
&      twetbulb(nrby2,jphiby1,nzby3)

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&      w(nrby2,jphiby2,nzby1),
&      h(nrby2,jphiby2,nzby1),
&      viability(nrby2,jphiby2,nzby1),
&      soryz1c(nrby2,jphiby2,nzby1),
&      soryz2c(nrby2,jphiby2,nzby1),
&      szconc(nrby2,jphiby2,nzby1),
&      dmlloss(nrby2,jphiby2,nzby1),
&      cfe(nrby2,jphiby2,nzby1),
&      rdomconc(nrby2,jphiby2,nzby1),
&      twetbulb(nrby2,jphiby2,nzby1)
c
      kprint40=1
      end if
      else
      continue
      end if
c
      if(timeday.ge.tprint45)then
      if(kprint45.eq.0)then
      write(29,7000)timeday,t(1,1,nzby2),
&      w(1,1,nzby2), h(1,1,nzby2),
&      viability(1,1,nzby2),soryz1c(1,1,nzby2),
&      soryz2c(1,1,nzby2),szconc(1,1,nzby2),
&      dmlloss(1,1,nzby2),cfe(1,1,nzby2),
&      rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
      write(88,7000)timeday,t(nrby2,jphiby1,nzby3),
&      w(nrby2,jphiby1,nzby3),
&      h(nrby2,jphiby1,nzby3),
&      viability(nrby2,jphiby1,nzby3),
&      soryz1c(nrby2,jphiby1,nzby3),
&      soryz2c(nrby2,jphiby1,nzby3),
&      szconc(nrby2,jphiby1,nzby3),
&      dmlloss(nrby2,jphiby1,nzby3),
&      cfe(nrby2,jphiby1,nzby3),
&      rdomconc(nrby2,jphiby1,nzby3),
&      twetbulb(nrby2,jphiby1,nzby3)
c
      write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
&      w(nrby2,jphiby2,nzby1),
&      h(nrby2,jphiby2,nzby1),
&      viability(nrby2,jphiby2,nzby1),
&      soryz1c(nrby2,jphiby2,nzby1),

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&      soryz2c(nrby2,jphiby2,nzby1),
&      szconc(nrby2,jphiby2,nzby1),
&      dmlloss(nrby2,jphiby2,nzby1),
&      cfe(nrby2,jphiby2,nzby1),
&      rdomconc(nrby2,jphiby2,nzby1),
&      twetbulb(nrby2,jphiby2,nzby1)
c
      kprint50=1
      end if
      else
      continue
      end if
c
      if(timeday.ge.tprint55)then
      if(kprint55.eq.0)then
      write(29,7000)timeday,t(1,1,nzby2),
&      w(1,1,nzby2),h(1,1,nzby2),
&      viability(1,1,nzby2),soryz1c(1,1,nzby2),
&      soryz2c(1,1,nzby2),szconc(1,1,nzby2),
&      dmlloss(1,1,nzby2),cfe(1,1,nzby2),
&      rdomconc(1,1,nzby2),twetbulb(1,1,nzby2)
c
      write(88,7000)timeday,t(nrby2,jphiby1,nzby3),
&      w(nrby2,jphiby1,nzby3),
&      h(nrby2,jphiby1,nzby3),
&      viability(nrby2,jphiby1,nzby3),
&      soryz1c(nrby2,jphiby1,nzby3),
&      soryz2c(nrby2,jphiby1,nzby3),
&      szconc(nrby2,jphiby1,nzby3),
&      dmlloss(nrby2,jphiby1,nzby3),
&      cfe(nrby2,jphiby1,nzby3),
&      rdomconc(nrby2,jphiby1,nzby3),
&      twetbulb(nrby2,jphiby1,nzby3)
c
      write(89,7000)timeday,t(nrby2,jphiby2,nzby1),
&      w(nrby2,jphiby2,nzby1),
&      h(nrby2,jphiby2,nzby1),
&      viability(nrby2,jphiby2,nzby1),
&      soryz1c(nrby2,jphiby2,nzby1),
&      soryz2c(nrby2,jphiby2,nzby1),
&      szconc(nrby2,jphiby2,nzby1),
&      dmlloss(nrby2,jphiby2,nzby1),
&      cfe(nrby2,jphiby2,nzby1),

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&      rdomconc(nrby2,jphiby2,nzby1),
&      twetbulb(nrby2,jphiby2,nzby1)
c
      kprint60=1
      end if
      else
      continue
      end if

c
7000  format(1x,'day',f12.4,'t',f12.4,'m',f12.4,'h',f12.4,
&      'v',f12.4,'s1',f12.4,'s2',f12.4,'sz',f12.4,
&      'd',f12.8,'cf',f12.4,'td',f12.4,'wte',f12.4)
c
      return
      end

c
c#####
c      Output the results in 1/3 period of running time      #
c#####
c
c      Subroutine dayqut(time,timeh,timeday,aerationtime,timer,
&      dayhour,kount,tamb,hamb,twamb,twout,tin,
&      hin)
      Include'dry.inc'
c
      Open (unit=41,file=qin.out,status='unknown')
      Open (unit=42,file=qte.out,status='unknown')
      Open (unit=43,file=qmo.out,status='unknown')
      Open (unit=44,file=qhu.out,status='unknown')
      Open (unit=45,file=qvi.out,status='unknown')
      Open (unit=46,file=qso1.out,status='unknown')
      Open (unit=47,file=qso2.out,status='unknown')
      Open (unit=48,file=qs2.out,status='unknown')
      Open (unit=49,file=qdm.out,status='unknown')
      Open (unit=50,file=qfe.out,status='unknown')
      Open (unit=51,file=qrd.out,status='unknown')
      Open (unit=52,file=qwte.out,status='unknown')
      Open (unit=53,file=qwallt.out,status='unknown')
      Open (unit=54,file=qwallm.out,status='unknown')
      Open (unit=55,file=qwallh.out,status='unknown')
      Open (unit=56,file=qwallvi.out,status='unknown')

      Open (unit=57,file=qwalls1.out,status='unknown')
      Open (unit=58,file=qwalls2.out,status='unknown')
      Open (unit=59,file=qwallsz.out,status='unknown')
      Open (unit=60,file=qwalldm.out,status='unknown')
      Open (unit=61,file=qwallfe.out,status='unknown')
      Open (unit=62,file=qwallrd.out,status='unknown')
      Open (unit=63,file=qwallwte.out,status='unknown')

c
      Call infqut(time,timeh,timeday,aerationtime,timer,
&      dayhour,kount,tamb,hamb,twamb,twout,tin,
&      hin)
c
      Call tmqutplot
      Call moqutplot
      Call huqutplot
      Call viqutplot
      Call so1qutplot
      Call so2qutplot
      Call szqutplot
      Call dmqutplot
      Call fequtplot
      Call rdqutplot
      Call wtequtplot

c
      Call walltqutplot
      Call wallmqutplot
      Call wallhqutplot
      Call wallviqutplot
      Call wallsolqutplot
      Call walls2qutplot
      Call wallszqutplot
      Call walldmqutplot
      Call wallfequtplot
      Call wallrdqutplot
      Call wallwtequtplot

c
      close(41)
      close(42)
      close(43)
      close(44)
      close(45)

```



```
c
close(64)
close(65)
close(66)
close(67)
close(68)
close(69)
close(70)
close(71)
close(72)
close(73)
close(74)
close(75)
close(76)
close(77)
close(78)
close(79)
close(80)
close(81)
close(82)
close(83)
close(84)
close(85)
close(86)

c
return
end

c#####
Open files
#####
Subroutine fileopen
Include'dry.inc'

Open (unit=10,file='templot.out',status='unknown')
Open (unit=11,file='misplot.out',status='unknown')
Open (unit=14,file='humiplot.out',status='unknown')
Open (unit=16,file='crop2.out',status='unknown')
Open (unit=17,file='crop3.out',status='unknown')
Open (unit=18,file='crop4.out',status='unknown')

c#####
Open (unit=19,file='crop5.out',status='unknown')
Open (unit=20,file='viaplot.out',status='unknown')
Open (unit=21,file='so1plot.out',status='unknown')
Open (unit=22,file='so2plot.out',status='unknown')
Open (unit=23,file='szplot.out',status='unknown')
Open (unit=24,file='dmplot.out',status='unknown')
Open (unit=25,file='feplot.out',status='unknown')
Open (unit=26,file='rdmplot.out',status='unknown')
Open (unit=27,file='wreplot.out',status='unknown')
Open (unit=30,file='crop8.out',status='unknown')
Open (unit=31,file='crop9.out',status='unknown')
Open (unit=32,file='crop10.out',status='unknown')
Open (unit=33,file='crop11.out',status='unknown')
Open (unit=34,file='crop12.out',status='unknown')
Open (unit=35,file='crop13.out',status='unknown')
Open (unit=36,file='crop14.out',status='unknown')
Open (unit=37,file='crop15.out',status='unknown')
Open (unit=38,file='crop16.out',status='unknown')
Open (unit=39,file='crop17.out',status='unknown')
Open (unit=40,file='crop18.out',status='unknown')

c
return
end

c#####
Calculate the total amount of pesticide, the total
of dry matter loss, the total number of insects
and the total of seeds viability
c#####
Subroutine totals
Include'dry.inc'

totalrd=0.0
totalfe=0.0
totaldml=0.0
totalviab=0.0
totalso1=0.0
totalso2=0.0
totalsz=0.0

c#####
```

```

do k=1, nzm1
  do j=1, nphi
    do i=1, nrm1
      jp1=j+1
      if(j.eq.nphi)jp1=1
    c
      if(i.eq.1)then
        totalrd=totalrd+(rdomconc(1,j,k)+rdomconc(1,j,k+1)+
          & rdomconc(2,j,k)+rdomconc(2,j,k+1)+rdomconc(2,
          & jp1,k)+rdomconc(2,jp1,k+1))/6.0*vol(i,j,k)
      else
        totalrd=totalrd+(rdomconc(i,j,k)+rdomconc(i+1,j,k)+
          & rdomconc(i,j,k+1)+rdomconc(i+1,j,k+1)+
          & rdomconc(i,jp1,k)+rdomconc(i,jp1,k+1)+
          & rdomconc(i+1,jp1,k)+rdomconc(i+1,jp1,k+1))/
          & 8.0*vol(i,j,k)
        end if
      end do
    end do
  end do
c
do k=1, nzm1
  do j=1, nphi
    do i=1, nrm1
      jp1=j+1
      if(j.eq.nphi)jp1=1
    c
      if(i.eq.1)then
        totalfe=totalfe+(cfe(1,j,k)+cfe(1,j,k+1)+cfe(2,
          & j,k)+cfe(2,j,k+1)+cfe(2,jp1,k)+cfe(2,jp1,
          & k+1))/6.0*vol(i,j,k)
      else
        totalfe=totalfe+(cfe(i,j,k)+cfe(i+1,j,k)+cfe(i,j,
          & k+1)+cfe(i+1,j,k+1)+cfe(i,jp1,k)+cfe(i,jp1,
          & k+1)+cfe(i+1,jp1,k)+cfe(i+1,jp1,k+1))/8.0*
          & vol(i,j,k)
        end if
      end do
    end do
  end do
c
do k=1, nzm1
  do j=1, nphi
    do i=1, nrm1
      jp1=j+1
      if(j.eq.nphi)jp1=1
    c
      if(i.eq.1)then
        totalviab=totalviab+(viability(1,j,k)+viability(1,
          & j,k+1)+viability(2,j,k)+viability(2,j,
          & k+1)+viability(2,jp1,k)+viability(2,jp1,
          & k+1))/6.0*vol(i,j,k)
      else
        totalviab=totalviab+(viability(i,j,k)+viability(i+1,
          & j,k)+viability(i,j,k+1)+viability(i+1,j,
          & k+1)+viability(i,jp1,k)+viability(i,jp1,
          & k+1)+viability(i+1,jp1,k)+viability(i+1,
          & jp1,k+1))/8.0*vol(i,j,k)
        end if
      end do
    end do
  end do
c

```

[illegible]

```

Subroutine pressplot
Include'dry.inc'

c
  jphi=1
  jphib2=nphi/2+1
  do k=1, nz
    do i=1, nr
      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
&      (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
      write(9,3950)i,jphi,k,r(i),z(i,k),p(i,jphi,k)
      write(9,3950)i,jphib2,k,-r(i),z(i,k),p(i,jphib2,k)
    end do
  end do
c
  3950 format(1x,3f12.4)
c
  return
end

c
c#####
c      Output pressure fields by time increas  #
c#####
c
Subroutine ptime(time)
Include'dry.inc'

c
  nrby2=nr/2+1
  jphib1=nphi/4+1
  jphib2=nphi/2+1
  nzby1=nz/4+1
  nzby2=nz/2+1
  nzby3=(nz*3)/4+1

c
  if (time.eq.1.0)then
    write(91,5995)time,p(1,1,nzby2),p(nrby2,jphib1,nzby3),
&    p(nrby2,jphib2,nzby1)
  end if

c
  if (time.eq.1000.0)then
    write(91,5995)time,p(1,1,nzby2),p(nrby2,jphib1,nzby3),
&    p(nrby2,jphib2,nzby1)
  end if

c
  if (time.eq.16000.0)then
    write(91,5995)time,p(1,1,nzby2),p(nrby2,jphib1,nzby3),
&    p(nrby2,jphib2,nzby1)
  end if

```

```

c      if (time.eq.18000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.20000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.22000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.24000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.26000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.28000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.30000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.32000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.34000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.36000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.38000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.40000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.42000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.44000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.46000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.48000.0)then
        write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
        &      p(nrby2,jphiby2,nzby1)
        end if
c
c      if (time.eq.50000.0)then

```



```

      write(91,5995)time,p(1,1,nzby2),p(nrby2,jphiby1,nzby3),
      &
      p(nrby2,jphiby2,nzby1)
    end if
  end if
c
5995 format(1x,f8.1,3f12.4)
c
      return
    end
c
c#####
c Output pressure fields along East, West,
c South and North sides of the silo wall
c#####
c
c Subroutine wallpress
  Include'dry.inc'
c
  jphi=1
  jphiby1=nphi/4+1
  jphiby2=nphi/2+1
  jphiby3=(nphi*3)/4+1
c
  do k=1, nz
    do i=1,nr
      write(87,5550)i,k,z(i,k),p(nr,jphi,k),p(nr,jphiby1,k),
      &
      p(nr,jphiby2,k),p(nr,jphiby3,k)
    end do
  end do
c
5550 format(1x,2i3,5f12.4)
c
      return
    end
c
c#####
c Output the performance of grain cooler
c#####
c
c Subroutine outputcooler(tamb,hamb,twamb,twout,tin,hin)
c
      write(28,3760)tamb,hamb,twamb

```

```

      write(28,3770)tin,hin
      write(28,3780)twout
c
3760 format(1x,'ambient temperature:',f7.3,'ambient humidity:',
      &
      f7.3,'ambient wet-bulb temperature:',f7.3)
3770 format(1x,'temperature of air leaving cooler:',f7.3,
      &
      'humidity of air entering grain:',f7.3)
3780 format(1x,'wet-bulb temperature of the air leaving cooler:',
      &
      f10.4)
c
      return
    end
c
c#####
c Output fields arising from heat and mass transfer
c calculations,biological activity and decay of
c pesticides
c#####
c Subroutine outputhm(time,timeh)
  Include'dry.inc'
  Include'solar.inc'
c
      write(28,3400)time,timeh,kh
      write(28,3401)totalfe
      write(28,3402)totaldml
      write(28,3403)totalviab
      write(28,3404)totalrd
      write(28,3405)totalso1
      write(28,3406)totalso2
      write(28,3407)totalsz
c
3400 format(1x,5x,'ELAPSED TIME=',f12.4,2x,'ELAPSED TIME(HOURS)='
      &
      f12.4,2x,'HOUR OF DAY=',i3)
3401 format(1x,5x,'Mean concentration of fenitrothion=',f10.4)
3402 format(1x,5x,'Mean dry matter loss=',f10.4)
3403 format(1x,5x,'Mean viability=',f10.4)
3404 format(1x,5x,'Mean concentration of R.dominica=',f10.4)
3405 format(1x,5x,'Mean concentration of S.oryzael=',f10.4)
3406 format(1x,5x,'Mean concentration of S.oryzae2=',f10.4)
3407 format(1x,5x,'Mean concentration of S.zeamais=',f10.4)

```

```

c
c ~~~~~
      write(16,3420)
3420 format(1x,75x,'TEMPERATURE FIELD')
c
      write(16,3440)(i,j=1,nr)
3440 format(1x,'PHI',21(4x,12,4x))
c
      do k=nz,1,-1
        write(16,3460)k
3460 format(1x,'k=',12)
c
      do j=nphi,1,-1
        write(16,3480j),(t(i,j,k),i=1,nr)
3480 format(1x,12,21(19,4))
      end do
      end do
c
      write(16,3500)
3500 format(1x,75x,'GRAIN MOISTURE CONTENT FIELD')
c
      write(16,3440)
      do k=nz,1,-1
        write(16,3460)k
        do j=nphi,1,-1
          write(16,3480j),(w(i,j,k),i=1,nr)
        end do
      end do
c
      write(17,3520)
3520 format(1x,75x,'HUMIDITY FIELD')
c
      write(17,3440)
      do k=nz,1,-1
        write(17,3460)k
        do j=nphi,1,-1
          write(17,3480j),(h(i,j,k),i=1,nr)
        end do
      end do
c
      write(17,3540)
c ~~~~~

3540 format(1x,75x,'DRY MATTER LOSS FIELD')
c
      write(17,3440)
      do k=nz,1,-1
        write(17,3460)k
        do j=nphi,1,-1
          write(17,3481j),(dmloss(i,j,k),i=1,nr)
3481 format(1x,12,21(f12.8))
        end do
      end do
c
      write(17,3560)
3560 format(1x,75x,'INTERGRANULAR WET BULB TEMPERATURE')
c
      write(17,3440)
      do k=nz,1,-1
        write(17,3460)k
        do j=nphi,1,-1
          write(17,3480j),(twetbulb(i,j,k),i=1,nr)
        end do
      end do
c
      write(18,3580)
3580 format(1x,75x,'POPULATION INCREASE OF RHYPERTHA
& DOMINICA')
c
      write(18,3440)
      do k=nz,1,-1
        write(18,3460)k
        do j=nphi,1,-1
          write(18,3480j),(rdomeconc(i,j,k),i=1,nr)
        end do
      end do
c
      write(18,3600)
3600 format(1x,75x,'POLPULATION INCREASE OF SITOPHILUS
& ORYZAEI')
c
      write(18,3440)
      do k=nz,1,-1
        write(18,3460)k

```

```

do j=nphi,1,-1
  write(18,3480)j,(soryz1c(i,j,k),i=1,nr)
end do
end do
~~~~~
write(19,3620)
3620 format(1x,75x,'POLPULATION INCREASE OF SITOPHILUS
& ORYZAE2')
c
write(19,3440)
do k=nz,1,-1
  write(19,3460)k
  do j=nphi,1,-1
    write(19,3480)j,(soryz2c(i,j,k),i=1,nr)
  end do
end do
~~~~~
write(19,3640)
3640 format(1x, 75x,'POLPULATION INCREASE OF SITOPHILUS
& ZEAMAI5')
c
write(19,3440)
do k=nz,1,-1
  write(19,3460)k
  do j=nphi,1,-1
    write(19,3480)j,(szconc(i,j,k),i=1,nr)
  end do
end do
c
return
end
c#####
c# Output temperature fields for plotting
c#####
c#
c Subroutine templot
c Include'dry.inc'
c
c jphi=1
c jphiby2=nphi/2+1
c#####
c# Output radial velocity fields for plotting
c#####
c#
c Subroutine moistplot
c Include'dry.inc'
c
c jphi=1
c jphiby2=nphi/2+1
do k=1, nz
do i=1, nr
  z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
    (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
  write(11,3910)i,jphi,k,r(i),z(i,k),w(i,jphi,k)
  write(11,3910)i,jphiby2,k,-r(i),z(i,k),w(i,jphiby2,k)
end do
end do
c
3910 format(1x,313,3f12.4)
c
return
end
c#####
c# Output radial velocity fields for plotting
c#####
c#

```

```

c Subroutine velraplot
c Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c         do i=1, nr
c            z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c              (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
c            &
c            write(92,3850)i,jphi,k,r(i),z(i,k),Vra(i,jphi,k)
c            write(92,3850)i,jphiby2,k,-r(i),z(i,k),Vra(i,jphiby2,k)
c         end do
c      end do
c
c      3850 format(1x,3I3,2f12.4,f12.6)
c
c      return
c      end
c
c#####
c      Output vertical velocity fields for plotting
c#####
c#####
c Subroutine velvplot
c Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c         do i=1, nr
c            z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c              (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
c            &
c            write(12,5885)i,jphi,k,r(i),z(i,k),Vci(i,jphi,k)
c            write(12,5885)i,jphiby2,k,-r(i),z(i,k),Vci(i,jphiby2,k)
c         end do
c      end do
c
c      5885 format(1x,3I3,2f12.4,E16.4)
c
c      return
c      end
c
c#####
c      Output simulation results
c#####
c#####
c Subroutine results
c Include'dry.inc'
c
c      Call templot
c      Call moistplot
c      Call humidplot
c      Call viablplot
c      Call rdompplot
c      Call solplot
c      Call so2plot
c      Call szplot
c      Call feplot
c      Call dmplot

```



```

do i=1, nr
  z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
    (real(wz)-r(i)*tan(gamma1)+tan(gamma2)))
  &
  write(23,3550)i,jphi,k,r(i),z(i,k),szconc(i,jphi,k)
  write(23,3550)i,jphiby2,k,-r(i),z(i,k),szconc(i,jphiby2,k)
end do
end do
end do
c
3550 format(1x,3I3,3f12.4)
c
return
end
c
c#####
c      Output dry matter loss fields for plotting
c#####
c#####
c
Subroutine dmlplot
Include'dry.inc'
c
jphi=1
jphiby2=nphi/2+1
do k=1, nz
  do i=1, nr
    z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
      (real(wz)-r(i)*tan(gamma1)+tan(gamma2)))
    &
    write(24,3500)i,jphi,k,r(i),z(i,k),dmlloss(i,jphi,k)
    write(24,3500)i,jphiby2,k,-r(i),z(i,k),
      dmlloss(i,jphiby2,k)
    end do
  end do
end do
3500 format(1x,3I3,2f12.4,f12.8)
c
return
end
c
c#####
c      Output fenitrothion concentration fields for plotting
c#####
c#####
c
Subroutine feplot
c
3400 format(1x,3I3,3f12.4)

```

```

Include'dry.inc'
c
jphi=1
jphiby2=nphi/2+1
do k=1, nz
  do i=1, nr
    z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
      (real(wz)-r(i)*tan(gamma1)+tan(gamma2)))
    &
    write(25,3450)i,jphi,k,r(i),z(i,k),cfe(i,jphi,k)
    write(25,3450)i,jphiby2,k,-r(i),z(i,k),
      cfe(i,jphiby2,k)
    end do
  end do
end do
c
3450 format(1x,3I3,3f12.4)
c
return
end
c
c#####
c      Output R. dominica fields for plotting
c#####
c#####
c
Subroutine rdomplot
Include'dry.inc'
c
jphi=1
jphiby2=nphi/2+1
do k=1, nz
  do i=1, nr
    z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
      (real(wz)-r(i)*tan(gamma1)+tan(gamma2)))
    &
    write(26,3400)i,jphi,k,r(i),z(i,k),rdomconc(i,jphi,k)
    write(26,3400)i,jphiby2,k,-r(i),z(i,k),rdomconc(i,jphiby2,k)
    end do
  end do
end do
c
3400 format(1x,3I3,3f12.4)

```

```

c      return
c      end

c      #####
c      Outputs the intergranular wet bulb
c      temperature field for plotting
c      #####
c
c      Subroutine wteplot
c      Include'dry.inc'

c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c      do i=1, nr
c      z(i,k)=tau(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c      (real(wz)-tau(i)*(tan(gamma1)+tan(gamma2)))
c      write(27,3350)i,jphi,k,r(i),z(i,k),twetbulb(i,jphi,k)
c      write(27,3350)i,jphiby2,k,-r(i),z(i,k),twetbulb(i,jphiby2,k)
c      end do
c      end do
c      3350    format(1x,3f13,3f12.4)
c
c      return
c      end

c      #####
c      Output the temperature fields along East, West,
c      South and North sides of the silo wall
c      #####
c
c      Subroutine walltplot
c      Include'dry.inc'

c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1

c      do i=1,nr
c      write(30,8000)r(i),t(i,jphi,nzby2),t(i,jphiby1,nzby2),
c      &      t(i,jphiby2,nzby2),t(i,jphiby3,nzby2)
c      end do
c      8000    format(1x,5f12.4)
c
c      return
c      end

c      #####
c      Output the humidity fields along East, West,
c      South and North sides of the silo wall
c      #####
c
c      Subroutine wallhplot

```



```

c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr
c          write(32,8000)r(i),h(i,jphi,nzby2),h(i,jphiby1,nzby2),
c          &      h(i,jphiby2,nzby2),h(i,jphiby3,nzby2)
c      end do
c
c      8000  format(1x,5f12.4)
c
c      return
c      end
c
c#####
c      Output the seeds viability fields along East,      #
c      West, South and North sides of the silo wall      #
c#####
c
c      Subroutine wallviaplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr
c          write(33,8000)r(i),viability(i,jphi,nzby2),
c          &      viability(i,jphiby1,nzby2),
c          &      viability(i,jphiby2,nzby2),
c          &      viability(i,jphiby3,nzby2)
c      end do
c
c      8000  format(1x,5f12.4)
c
c#####
c      Output the S. oryzae1 fields along East, West,      #
c      South and North sides of the silo wall      #
c#####
c
c      Subroutine wallsolplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr
c          write(34,8000)r(i),soryz1c(i,jphi,nzby2),
c          &      soryz1c(i,jphiby1,nzby2),
c          &      soryz1c(i,jphiby2,nzby2),
c          &      soryz1c(i,jphiby3,nzby2)
c      end do
c
c      8000  format(1x,5f12.4)
c
c      return
c      end
c
c#####
c      Output the S. oryzae2 fields along East, West,      #
c      South and North sides of the silo wall      #
c#####
c
c      Subroutine wallsol2plot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1

```

```

c      nzby2=nz/2+1
c
c      do i=1,nr
c          write(35,8000)r(i),soryz2c(i,jphi,nzby2),
c          &      soryz2c(i,jphiby1,nzby2),
c          &      soryz2c(i,jphiby2,nzby2),
c          &      soryz2c(i,jphiby3,nzby2)
c
c      end do
c
c      8000  format(1x,5f12.4)
c
c      return
c      end
c
c#####
c      Output the S. zearnais fields along East, West,
c      South and North sides of the silo wall
c#####
c
c      Subroutine wallszplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr
c          write(36,8000)r(i),szconc(i,jphi,nzby2),
c          &      szconc(i,jphiby1,nzby2),
c          &      szconc(i,jphiby2,nzby2),
c          &      szconc(i,jphiby3,nzby2)
c      end do
c
c      8000  format(1x,5f12.4)
c
c      return
c      end
c
c#####
c      Output the dry matter loss fields along East,
c      West, South and North sides of the silo wall
c#####
c
c      Subroutine walldmplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr
c          write(37,8000)r(i),dmloss(i,jphi,nzby2),
c          &      dmloss(i,jphiby1,nzby2),
c          &      dmloss(i,jphiby2,nzby2),
c          &      dmloss(i,jphiby3,nzby2)
c      end do
c
c      8000  format(1x,f12.4,4f12.8)
c
c      return
c      end
c
c#####
c      Output the fenitrothion concentration fields along
c      East, West, South and North sides of the silo wall
c#####
c
c      Subroutine wallfeplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr

```

```

      write(38,8000)r(i),cfe(i,jphi,nzby2),
&      cfe(i,jphiby1,nzby2),
&      cfe(i,jphiby2,nzby2),
&      cfe(i,jphiby3,nzby2)
      end do
      8000 format(1x,5f12.4)
c
      return
      end
c
c#####
c      Output the R. dominica fields along East, West, #
c      South and North sides of the silo wall #
c#####
c
c      Subroutine wallrldmplot
      Include'dry.inc'
      jphi=1
      jphiby1=nphi/4+1
      jphiby2=nphi/2+1
      jphiby3=(nphi*3)/4+1
      nzby2=nz/2+1
c
      do i=1,nr
        write(39,8000)r(i),rdomconc(i,jphi,nzby2),
&      rdomconc(i,jphiby1,nzby2),
&      rdomconc(i,jphiby2,nzby2),
&      rdomconc(i,jphiby3,nzby2)
      end do
c
      8000 format(1x,5f12.4)
c
      return
      end
c
c#####
c      Output the intergranular wet bulb temperature #
c      fields along East, West, South and North #
c      sides of the silo wall #
c#####
c
c      Subroutine wallwteplot
      Include'dry.inc'
      jphi=1
      jphiby1=nphi/4+1
      jphiby2=nphi/2+1
      jphiby3=(nphi*3)/4+1
      nzby2=nz/2+1
c
      do i=1,nr
        write(40,8000)r(i),twetbulb(i,jphi,nzby2),
&      twetbulb(i,jphiby1,nzby2),
&      twetbulb(i,jphiby2,nzby2),
&      twetbulb(i,jphiby3,nzby2)
      end do
c
      8000 format(1x,5f12.4)
c
      return
      end
c
c#####
c      Output the performance of grain silo at 1/3 #
c      period of running time #
c#####
c
c      Subroutine infcut(time,timeh,timeday,aerationtime,timer,
&      dayhour,kount,tamb,hamb,twamb,twout,tin,
&      hin)
      Include'dry.inc'
      write(41,3900)
      write(41,3950)time,timeh,timeday
      write(41,3955)aerationtime
      write(41,3960)timer
      write(41,3965)dayhour
      write(41,3970)kount
c
      3900 format(1x,'In 20 days')
      3950 format(1x,5x,'time(SECOND)',f12.4,2x,'timeh(HOURS)',f12.4,2x,

```

```

&
3955 format(1x,5x,'aerationtime',f10.3,'HOURS')
3960 format(1x,5x,'timer',f12.4)
3965 format(1x,5x,'dayhour',f8.4)
3970 format(1x,5x,'kount',f5)
c
    write(41,3760)tamb,hamb,twamb
    write(41,3770)tin,hin
    write(41,3780)twout
c
3760 format(1x,'ambient temperature:',f7.3,'ambient humidity:',
&
3770 f7.3,'ambient wet-bulb temperature:',f7.3)
3770 format(1x,'temperature of air leaving cooler:',f7.3,
&
3780 'humidity of air entering grain:',f7.3)
3780 format(1x,'wet-bulb temperature of the air leaving cooler:',
&
    f10.4)
c
    return
    end
c
c#####
c      Output temperature fields at 1/3 period of running time      #
c#####
c
Subroutine tmqutplot
Include'dry.inc'

    jphi=1
    jphiby2=nphi/2+1
    do k=1, nz
        do i=1, nr
            z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
                (real(wz)-r(i)*tan(gamma1)+tan(gamma2)))
            write(43,3910)i,jphi,k,r(i),z(i,k),w(i,jphi,k)
            write(43,3910)i,jphiby2,k,-r(i),z(i,k),w(i,jphiby2,k)
        end do
    end do
c
3910 format(1x,3f13,3f12.4)
c
    return
    end
c
c#####
c      Output humidity fields at 1/3      #
c      period of running time      #
c#####
c
Subroutine huqutplot
Include'dry.inc'

    jphi=1
    jphiby2=nphi/2+1
    do k=1, nz
        do i=1, nr
            z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
                (real(wz)-r(i)*tan(gamma1)+tan(gamma2)))
            write(44,3750)i,jphi,k,r(i),z(i,k),h(i,jphi,k)
        end do
    end do
c
3900 format(1x,3f13,3f12.4)
c
    return

```

```

      write(44,3750)i,jphiby2,k,-r(i),z(i,k),h(i,jphiby2,k)
      end do
    end do
  c
  3750   format(1x,3I3,3f12.4)
  c
      return
    end
  c
c#####
c      Output seeds viability fields at
c      1/3 period of running time
c#####
c
  Subroutine viqutplot
  Include'dry.inc'
c
      jphi=1
      jphiby2=nphi/2+1
      do k=1, nz
        do i=1, nr
          z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
            (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
          write(45,3700)i,jphi,k,r(i),z(i,k),viability(i,jphi,k)
          write(45,3700)i,jphiby2,k,-r(i),z(i,k),
            viability(i,jphiby2,k)
        end do
      end do
  c
  3700   format(1x,3I3,2f12.4,f12.6)
  c
      return
    end
  c
c#####
c      Output S. oryzae1 fields at 1/3 period of running time
c#####
c
  Subroutine solqutplot
  Include'dry.inc'
c
      jphi=1
      jphiby2=nphi/2+1
      do k=1, nz
        do i=1, nr
          z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
            (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
          write(47,3600)i,jphi,k,r(i),z(i,k),soryz2c(i,jphi,k)
          write(47,3600)i,jphiby2,k,-r(i),z(i,k),
            soryz2c(i,jphiby2,k)
        end do
      end do
  c
  3600   format(1x,3I3,3f12.4)
  c
      return
    end
  c
c#####
c      Output S. oryzae2 fields at 1/3 period of running time
c#####
c
  Subroutine so2qutplot
  Include'dry.inc'
c
      jphi=1
      jphiby2=nphi/2+1
      do k=1, nz
        do i=1, nr
          z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
            (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
          write(47,3600)i,jphi,k,r(i),z(i,k),soryz2c(i,jphi,k)
          write(47,3600)i,jphiby2,k,-r(i),z(i,k),
            soryz2c(i,jphiby2,k)
        end do
      end do
  c
  3600   format(1x,3I3,3f12.4)
  c
      return
    end
  c
c#####

```

```

c#####
c      Output S. zeamais fields at 1/3 period of running time      #
c#####
c
c      Subroutine szqutplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c      do i=1, nr
c      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c      (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
c      &
c      write(48,3550)i,jphi,k,r(i),z(i,k),szconc(i,jphi,k)
c      write(48,3550)i,jphiby2,k,-r(i),z(i,k),szconc(i,jphiby2,k)
c      end do
c      end do
c
c      3550      format(1x,3I3,3f12.4)
c
c      return
c      end
c#####
c#####
c      Subroutine dmqutplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c      do i=1, nr
c      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c      (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
c      &
c      write(49,3500)i,jphi,k,r(i),z(i,k),dmloss(i,jphi,k)
c      write(49,3500)i,jphiby2,k,-r(i),z(i,k),
c      dmloss(i,jphiby2,k)
c      &
c#####
c#####
c      Subroutine fequtplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c      do i=1, nr
c      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c      (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
c      &
c      write(50,3450)i,jphi,k,r(i),z(i,k),cfe(i,jphi,k)
c      write(50,3450)i,jphiby2,k,-r(i),z(i,k),
c      cfe(i,jphiby2,k)
c      end do
c      end do
c
c      3450      format(1x,3I3,3f12.4)
c
c      return
c      end
c#####
c#####
c      Output R. dominica fields at 1/3 period of running time      #
c#####
c
c      Subroutine rdqutplot
c      Include'dry.inc'
c

```

```

jphi=1
jphiby2=nphi/2+1
do k=1, nz
  do i=1, nr
    z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
      (real(wz)-r(i))*tan(gamma1)+tan(gamma2)))
    &
c#####
c      write(51,3400)i,jphi,k,r(i),z(i,k),rdomconc(i,jphi,k)
c      write(51,3400)i,jphiby2,k,-r(i),z(i,k),rdomconc(i,jphiby2,k)
c      end do
c      end do
c
c3400    format(1x,3I3,3f12.4)
c
c      return
c      end
c#####
c      Output the intergranular wet bulb temperature      #
c      fields at 1/3 period of running time                #
c#####
c#####
c      Subroutine wtequtplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c      do i=1, nr
c        z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c          (real(wz)-r(i))*tan(gamma1)+tan(gamma2)))
c      &
c      write(52,3350)i,jphi,k,r(i),z(i,k),twetbulb(i,jphi,k)
c      write(52,3350)i,jphiby2,k,-r(i),z(i,k),twetbulb(i,jphiby2,k)
c      end do
c      end do
c
c3350    format(1x,3I3,3f12.4)
c
c      return
c      end
c
c      do i=1,nr
c        write(53,8000)r(i),t(i,jphi,nzby2),t(i,jphiby1,nzby2),
c          &
c          t(i,jphiby2,nzby2),t(i,jphiby3,nzby2)
c        end do
c      8000    format(1x,5f12.4)
c
c      return
c      end
c#####
c      Output the moisture content fields at 1/3 period      #
c      of running time in East, West, South and              #
c      North sides of the silo wall                            #
c#####
c      Subroutine wallmqtplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr

```

```

      write(54,8000)r(i),w(i,jphi,nzby2),w(i,jphiby1,nzby2),
      &
      end do
c
      8000   format(1x,5f12.4)
c
      return
      end

c#####
c      Output the humidity fields at 1/3 period of
c      running time in East, West, South and
c      North sides of the silo wall
c#####
c
      Subroutine wallhqutplot
      Include'dry.inc'
c
      jphi=1
      jphiby1=nphi/4+1
      jphiby2=nphi/2+1
      jphiby3=(nphi*3)/4+1
      nzby2=nz/2+1
c
      do i=1,nr
        write(55,8000)r(i),h(i,jphi,nzby2),h(i,jphiby1,nzby2),
        &
        h(i,jphiby2,nzby2),h(i,jphiby3,nzby2)
      end do
c
      8000   format(1x,5f12.4)
c
      return
      end

c#####
c      Output the seeds viability fields at 1/3 period
c      of running time in East, West, South and
c      North sides of the silo wall
c#####
c
      Subroutine wallviqutplot
      Include'dry.inc'
c
      jphi=1
      jphiby1=nphi/4+1
      jphiby2=nphi/2+1
      jphiby3=(nphi*3)/4+1
      nzby2=nz/2+1
c
      do i=1,nr
        write(56,8000)r(i),viability(i,jphi,nzby2),
        &
        viability(i,jphiby1,nzby2),
        &
        viability(i,jphiby2,nzby2),
        &
        viability(i,jphiby3,nzby2)
      end do
c
      8000   format(1x,5f12.4)
c
      return
      end

c#####
c      Output the S. oryzae1 fields at 1/3 period
c      of running time in East, West, South and
c      North sides of the silo wall
c#####
c
      Subroutine wallso1qutplot
      Include'dry.inc'
c
      jphi=1
      jphiby1=nphi/4+1
      jphiby2=nphi/2+1
      jphiby3=(nphi*3)/4+1
      nzby2=nz/2+1
c
      do i=1,nr
        write(57,8000)r(i),soryz1c(i,jphi,nzby2),
        &
        soryz1c(i,jphiby1,nzby2),
        &
        soryz1c(i,jphiby2,nzby2),
        &
        soryz1c(i,jphiby3,nzby2)
      end do
c

```



```

      end do
c
      8000  format(1x,5f12.4)
c
      return
      end
c
c#####
c      Output the performance of grain silo at 2/3      #
c      period of running time                        #
c#####
c
      Subroutine inhaf(time,timeh,timeday,aerationtime,timer,
&      dayhour,kount,tamb,hamb,twamb,twout,tin,
&      hin)
      Include'dry.inc'
c
      write(64,3900)
      write(64,3950)time,timeh,timeday
      write(64,3955)aerationtime
      write(64,3960)timer
      write(64,3965)dayhour
      write(64,3970)kount
c
      3900  format(1x,'In 40 days')
      3950  format(1x,5x,'time(SECOND)',f12.4,2x,'timeh(HOURS)',f12.4,2x,
&      'TIME(DAY)',f12.4)
      3955  format(1x,5x,'aerationtime',f10.3,'HOURS')
      3960  format(1x,5x,'timer',f12.4)
      3965  format(1x,5x,'dayhour',f8.4)
      3970  format(1x,5x,'kount',I5)
c
      write(64,3760)tamb,hamb,twamb
      write(64,3770)tin,hin
      write(64,3780)twout
c
      3760  format(1x,'ambient temperature:',f7.3,'ambient humidity',
&      f7.3,'ambient wet-bulb temperature:',f7.3)
      3770  format(1x,'temperature of air leaving cooler:',f7.3,
&      'humidity of air entering grain:',f7.3)
      3780  format(1x,'wet-bulb temperature of the air leaving cooler:',
&      f7.3)
c
      8000  format(1x,5f12.4)
c
      return
      end
c
c#####
c      Output temperature fields at 2/3 period of running time      #
c#####
c
      Subroutine tmhafplot
      Include'dry.inc'
c
      jphi=1
      jphiby2=nphi/2+1
      do k=1, nz
      do i=1, nr
      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
&      (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
      write(65,3900)i,jphi,k,r(i),z(i,k),t(i,jphi,k)
      write(65,3900)i,jphiby2,k,-r(i),z(i,k),t(i,jphiby2,k)
      end do
      end do
c
      3900  format(1x,3I3,3f12.4)
c
      return
      end
c
c#####
c      Output moisture content fields at 2/3      #
c      period of running time                        #
c#####
c
      Subroutine mohafplot
      Include'dry.inc'
c
      jphi=1
      jphiby2=nphi/2+1
      do k=1, nz
      do i=1, nr
      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*

```

```

&      (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
      write(66,3910)i,jphi,k,r(i),z(i,k),w(i,jphi,k)
      write(66,3910)i,jphiby2,k,-r(i),z(i,k),w(i,jphiby2,k)
      end do
    end do
  c
3910   format(1x,3I3,3f12.4)
  c
      return
    end
  c
c#####
c      Output humidity fields at 2/3
c      #
c      period of running time
c#####
c
c      Subroutine huhafplot
      Include'dry.inc'
  c
      jphi=1
      jphiby2=nphi/2+1
      do k=1, nz
        do i=1, nr
          z(i,k)=r(i)*(tan(gamma1)+real(k-1)/real(nz-1))*
            (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
          write(67,3750)i,jphi,k,r(i),z(i,k),h(i,jphi,k)
          write(67,3750)i,jphiby2,k,-r(i),z(i,k),h(i,jphiby2,k)
        end do
      end do
  c
3750   format(1x,3I3,3f12.4)
  c
      return
    end
  c
c#####
c      Output seeds viability fields at
c      2/3 period of running time
c      #
c#####
c
c      Subroutine vihafplot
      Include'dry.inc'
  c
      jphi=1
      jphiby2=nphi/2+1
      do k=1, nz
        do i=1, nr
          z(i,k)=r(i)*(tan(gamma1)+real(k-1)/real(nz-1))*
            (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
          write(69,3650)i,jphi,k,r(i),z(i,k),soryz1c(i,jphi,k)
          write(69,3650)i,jphiby2,k,-r(i),z(i,k),
            soryz1c(i,jphiby2,k)
        end do
      end do
  c
3650   format(1x,3I3,3f12.4)
  c
      return
    end
  c
c#####
c      Output S. oryzae1 fields at 2/3 period of running time
c      #
c#####
c
c      Subroutine so1hafplot
      Include'dry.inc'
  c
      jphi=1
      jphiby2=nphi/2+1
      do k=1, nz
        do i=1, nr
          z(i,k)=r(i)*(tan(gamma1)+real(k-1)/real(nz-1))*
            (real(wz)-r(i)*(tan(gamma1)+tan(gamma2)))
          write(69,3650)i,jphi,k,r(i),z(i,k),soryz1c(i,jphi,k)
          write(69,3650)i,jphiby2,k,-r(i),z(i,k),
            soryz1c(i,jphiby2,k)
        end do
      end do
  c
3650   format(1x,3I3,3f12.4)
  c
      return
    end
  c
c#####
c      Output S. oryzae1 fields at 2/3 period of running time
c      #
c#####

```

```

end
c#####
c      Output S. oryzae2 fields at 2/3 period of running time      #
c#####
c
c      Subroutine so2hafplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c      do i=1, nr
c      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c      &      (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
c      write(70,3600)i,jphi,k,r(i),z(i,k),soryz2c(i,jphi,k)
c      &      write(70,3600)i,jphiby2,k,-r(i),z(i,k),
c      &      soryz2c(i,jphiby2,k)
c      end do
c      end do
c
c      3600      format(1x,3I3,3f12.4)
c
c      return
c      end
c#####
c      Output S. zeamais fields at 2/3 period of running time      #
c#####
c
c      Subroutine szhafplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c      do i=1, nr
c      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c      &      (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
c      write(71,3550)i,jphi,k,r(i),z(i,k),szconc(i,jphi,k)
c      &      write(71,3550)i,jphiby2,k,-r(i),z(i,k),szconc(i,jphiby2,k)
c#####
c#####
c      Subroutine dmhafplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby2=nphi/2+1
c      do k=1, nz
c      do i=1, nr
c      z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
c      &      (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
c      write(72,3500)i,jphi,k,r(i),z(i,k),dmloss(i,jphi,k)
c      &      write(72,3500)i,jphiby2,k,-r(i),z(i,k),
c      &      dmloss(i,jphiby2,k)
c      end do
c      end do
c
c      3500      format(1x,3I3,2f12.4,f12.8)
c
c      return
c      end
c#####
c      Output fenitrothion concentration fields      #
c      at 2/3 period of running time      #
c#####
c
c      Subroutine fehafplot
c      Include'dry.inc'
c

```

```

jphi=1
jphiby2=nphi/2+1
do k=1, nz
  do i=1, nr
    z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
      (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
    &
    write(73,3450)i,jphi,k,r(i),z(i,k),cfe(i,jphi,k)
    write(73,3450)i,jphiby2,k,-r(i),z(i,k),
      cfe(i,jphiby2,k)
    &
    end do
  end do
  format(1x,3I3,3f12.4)
  return
end
c
c#####
c      Output R. dominica fields at 2/3 period of running time      #
c#####
c
Subroutine rdhafplot
Include'dry.inc'
c
jphi=1
jphiby2=nphi/2+1
do k=1, nz
  do i=1, nr
    z(i,k)=r(i)*tan(gamma1)+real(k-1)/real(nz-1)*
      (real(wz)-r(i))*(tan(gamma1)+tan(gamma2)))
    &
    write(74,3400)i,jphi,k,r(i),z(i,k),rdomconc(i,jphi,k)
    write(74,3400)i,jphiby2,k,-r(i),z(i,k),rdomconc(i,jphiby2,k)
    end do
  end do
  format(1x,3I3,3f12.4)
  return
end
c
c#####
c      Output the temperature fields at 2/3 period      #
c      of running time in East, West, South and      #
c      North sides of the silo wall      #
c#####
c
Subroutine wallhafplot
Include'dry.inc'
c
jphi=1
jphiby1=nphi/4+1
jphiby2=nphi/2+1
jphiby3=(nphi*3)/4+1
nzby2=nz/2+1
do i=1,nr
  write(76,8000)r(i),t(i,jphi,nzby2),t(i,jphiby1,nzby2),

```

```

&          t(i,jphiby2,nzby2),t(i,jphiby3,nzby2)
      end do
c
      8000  format(1x,5f12.4)
c
      return
      end
c
c#####
c      Output the moisture content fields at 2/3 period #####
c      of running time in East, West, South and #
c      North sides of the silo wall #
c#####
c
      Subroutine wallmhafplot
      Include'dry.inc'
c
      jphi=1
      jphiby1=nphi/4+1
      jphiby2=nphi/2+1
      jphiby3=(nphi*3)/4+1
      nzby2=nz/2+1
c
      do i=1,nr
          write(77,8000)r(i),w(i,jphi,nzby2),w(i,jphiby1,nzby2),
          &          w(i,jphiby2,nzby2),w(i,jphiby3,nzby2)
          end do
c
      8000  format(1x,5f12.4)
c
      return
      end
c
c#####
c      Output the seeds viability fields at 2/3 period #####
c      of running time in East, West, South and #
c      North sides of the silo wall #
c#####
c
      Subroutine wallvihafplot
      Include'dry.inc'
c
      jphi=1
      jphiby1=nphi/4+1
      jphiby2=nphi/2+1
      jphiby3=(nphi*3)/4+1
      nzby2=nz/2+1
c
      do i=1,nr
          write(79,8000)r(i),viability(i,jphi,nzby2),
          &          viability(i,jphiby1,nzby2),
          &          viability(i,jphiby2,nzby2),
          &          viability(i,jphiby3,nzby2)
          end do
c
      8000  format(1x,5f12.4)
c
c#####
c      Output the humidity fields at 2/3 period of #####
c      running time in East, West, South and #
c      North sides of the silo wall #
c#####
c
      Subroutine wallhahafplot
      Include'dry.inc'

```



```

c
c#####
c      Output the dry matter loss fields at 2/3 period      #
c      of running time in East, West, South and          #
c      North sides of the silo wall                      #
c#####
c
c      Subroutine walldmhafplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr
c         write(83,8000)r(i),dmloss(i,jphi,nzby2),
c         &      dmloss(i,jphiby1,nzby2),
c         &      dmloss(i,jphiby2,nzby2),
c         &      dmloss(i,jphiby3,nzby2)
c      end do
c
c      8000 format(1x,f12.4,f12.8)
c
c      return
c      end
c
c#####
c      Output the fenitrition concentration fields at      #
c      2/3 period of running time in East, West, South    #
c      and North sides of the silo wall                   #
c#####
c
c      Subroutine wallfehafplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c
c      nzby2=nz/2+1
c
c      do i=1,nr
c         write(84,8000)r(i),cfe(i,jphi,nzby2),
c         &      cfe(i,jphiby1,nzby2),
c         &      cfe(i,jphiby2,nzby2),
c         &      cfe(i,jphiby3,nzby2)
c      end do
c
c      8000 format(1x,5f12.4)
c
c      return
c      end
c
c#####
c      Output the R. dominica fields at 2/3 period      #
c      of running time in East, West, South and          #
c      North sides of the silo wall                      #
c#####
c
c      Subroutine wallrdhafplot
c      Include'dry.inc'
c
c      jphi=1
c      jphiby1=nphi/4+1
c      jphiby2=nphi/2+1
c      jphiby3=(nphi*3)/4+1
c      nzby2=nz/2+1
c
c      do i=1,nr
c         write(85,8000)r(i),rdomconc(i,jphi,nzby2),
c         &      rdomconc(i,jphiby1,nzby2),
c         &      rdomconc(i,jphiby2,nzby2),
c         &      rdomconc(i,jphiby3,nzby2)
c      end do
c
c      8000 format(1x,5f12.4)
c
c      return
c      end
c
c#####

```

```
c#####  
c      Output the intergranular wet bulb temperature      #  
c      fields at 2/3 period of running time in East,      #  
c      West, South and North sides of the silo wall      #  
c#####  
c#####  
c      Subroutine wallwtchafplot  
c      Include'dry.inc'  
c  
c      jphi=1  
c      jphiby1=nphi/4+1  
c      jphiby2=nphi/2+1  
c      jphiby3=(nphi*3)/4+1  
c      nzby2=nz/2+1  
c  
c      do i=1,nr  
c         write(86,8000)r(i),twetbulb(i,jphi,nzby2),  
c         & twetbulb(i,jphiby1,nzby2),  
c         & twetbulb(i,jphiby2,nzby2),  
c         & twetbulb(i,jphiby3,nzby2)  
c      end do  
c  
c      8000 format(1x,5f12.4)  
c  
c      return  
c      end  
c  
c#####END OF PROGRAM#####
```

```

c#####DRY.INC#####
c
parameter (imax=31, jmax=31, kmax=41, ikmax=imax+kmax)
c
common/heat/ nr,nphi,nz,wR,wz,wz1,nrm1,nrm2,nzm1,nzm2,dphi,pi,
& gamma1,gamma2,crb4,crb5,crb6,czb1,czb2,czb3,czb4,
& czb5,czb6,gam1,gam2,nphimindc,nphimaxdc,nrmindc,
& nrmadc,kprint5,kprint10,kprint15,kprint20,
& kprint25,kprint30,kprint35,kprint40,kprint45,
& kprint50,kprint55,kprint60,kprint0
c
common/prop/ cw1,cw2,cw3,cw4,cw5,hw1,hw2,hw3,hw4,hw5,hw6,hw7,
& hw8,hw9,hw10,p0,w0,h0,revm,wsat,eps,rhoa,rhos,rhob,
& eg,ca,cw,keff,deff,dhvd, hv,gn,patm,rhout,hs,hvap,
& a1lhm,a2lhm,a3lhm,a4lhm,a5lhm,a6lhm,a7lhm,a8lhm,
& crdom,csoryz1,csoryz2,csz, trdom,tsoryz1,tsoryz2,
& tsz,xi,dwdt,tprint5,tprint10,tprint15,tprint20,
& tprint25,tprint30,tprint35,tprint40,tprint45,
& tprint50,tprint55,tprint60,tprint0
c
common/soil/ dtg,dtg,dpduct,trise,qu,res,tinit,ku1,ku2,
& kp1,kp2,tmean,tamp, humidity,detal,qup,specflo,bfe,
& thalf,maxday,aerate1,aerate2,dtgaerate,ifreq,
& dtgconduct,noflow,volume,totallrd,totallfe,totalldml,
& totalviab,totalso1,totalso2,totalsz,ddmdt
c
common/room/ hr(imax),hz(kmax),r(imax),z(imax,kmax),cr1(imax),
& cr2(imax),cr3(imax),cr4(imax),cr5(imax),cr6(imax),
& cz1(kmax),cz2(kmax),cz3(kmax),cz4(kmax),cz5(kmax),
& cz6(kmax),cp1(jmax),cp2(jmax),cp3(jmax),cp4(jmax),
& cp5(jmax),cp6(jmax),heightc(kmax),heightr(kmax),
& slope(kmax)
c
common/seed/ alpha1(imax,kmax),alpha2(imax,kmax),dpdn(imax,jmax),
& alpha3(imax,kmax),alpha4(imax,kmax),air(imax,jmax),
& beta1(imax,kmax),beta2(imax,kmax),beta3(imax,kmax),
& beta4(imax,kmax),beta5(imax,kmax),beta6(imax,kmax),
& beta7(imax,kmax),beta8(imax),dpde(imax,jmax)
c
common/sign/ rdomconec(imax,jmax,kmax),soryz1c(imax,jmax,kmax),
& soryz2c(imax,jmax,kmax),szconec(imax,jmax,kmax),

```

```
c#####CROP IN#####  
c  STATEMENTS          INPUT DATA  
c#####  
c  
  nr,nphi,nz           21,20,21  
  kul,ku2,maxday       1,200000,60  
  kp1,kp2              1,2  
  dtp,dtagerate,dtgconduct  
  wR,wz1,specflo,res   1.115,2.7,1.5708,2000.0  
  gam1,gam2           38.67,10.17  
  tinit,winit          30.0,0.12  
  tneam,tamp,humidity  20.0,5.0,0.008  
  nphimindc,nphimaxdc,nrmindc,nrmaxdc  
  aerate1,aerate2      1,1,2,15  
  mcb                  0.0,6.0  
  pnotfld              .true.  
  smith                .false.  
  smith                .true.  
c  
  phi                  -37.67  
  daily sunshine hours 8.1,7.5,6.2,4.9,3.8,3.1  
  day of the year      17,47,75,105,135,162  
  daily minimum temperature  
  daily maximum temperature  
  alpha,epsilon        14.2,15.1,12.1,10.7,7.6,5.1  
                        26.3,26.4,23.2,20.7,16.5,13.4  
                        0.8,0.9  
c  
c#####END OF INPUT FILE#####
```